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同水分管理模式联合叶面喷施硅肥对水稻 Cd 累积的影响 ····································
魏宾坛,周航,刘佳炜,张竞颐,黄芳,霍洋,胡雨丹,辜娇峰,刘俊,廖柏寒(3855)
合剂 GLDA 对象草修复镉污染农田的影响 ······················· 覃建军, 唐盛爽, 蒋凯, 黄敬, 侯红波, 龙坚, 彭佩钦(3862) 植业面源污染防控技术发展历程分析及趋势预测 ································ 俞映倞, 杨林章, 李红娜, 朱昌雄, 杨根, 薛利红(3870)
F境科学》征订启事(3636) 《环境科学》征稿简则(3764) 信息(3538, 3628, 3724)



基于不同废污泥源的短程反硝化快速启动及稳定性

张星星1, 王超超1, 王垚1, 徐乐中1,2,3*, 吴鹏1,2,3

(1. 苏州科技大学环境科学与工程学院, 苏州 215009; 2. 城市生活污水资源化利用技术国家地方联合工程实验室, 苏州 215009; 3. 江苏省水处理技术与材料协同创新中心, 苏州 215009)

摘要:为探究不同废污泥源快速启动短程反硝化和实现稳定 NO_2^- -N积累的可行性,在 3 个完全相同的 SBR 反应器 (S1、S2 和S3)分别接种:实验室城市污水反硝化除磷系统排泥、城市污水厂剩余污泥及河涌底泥,比较其短程反硝化启动快慢和 NO_2^- -N积累特性,考察系统短程反硝化活性和 NO_3^- -N \to NO_2^- -N 转化性能,并从微生物学角度分析反应器功能菌群特征. 结果表明,在乙酸钠为唯一碳源、高碱度和适宜 COD/NO_3^- -N比进水条件下,3 个 SBR 短程反硝化反应器在短时间内均能够成功启动,系统平均 NO_3^- -N \to NO_2^- -N 转化率为 S1 > S2 > S3 (75. 92% > 73. 36% > 69. 90%). 同时发现持续低温条件下 S1 和 S2 呈现不同程度的短程反硝化性能恶化趋势,但 S3 能够稳定维持良好 NO_2^- -N积累性能. 微生物高通量测序表明,变形菌门和拟杆菌门居 PD 系统主导地位,3 个短程反硝化反应器 NO_2^- -N积累关键功能菌属 Thauera 属丰度差异明显: S3 > S1 > S2 (25. 09% > 4. 71% > 3. 60%),表明 S3 具备稳定高效的 NO_2^- -N积累性能,同时高丰度 Thauera 属可能是维持低温短程反硝化活性的重要原因.

关键词:短程反硝化(PD); 厌氧氨氧化(ANAMMOX); 废污泥源; 快速启动; 稳定性; 功能菌属中图分类号: X703 文献标识码: A 文章编号: 0250-3301(2020)08-3715-10 **DOI**: 10.13227/j. hjkx. 202001216

Rapid Start-up and Stability of Partial Denitrification Based on Different Waste Sludge Sources

ZHANG Xing-xing¹, WANG Chao-chao¹, WANG Yao¹, XU Le-zhong^{1,2,3*}, WU Peng^{1,2,3}

- (1, School of Environmental Science and Engineering, Suzhou University of Science and Technology, Suzhou 215009, China;
- 2. National and Local Joint Engineering Laboratory of Municipal Sewage Resource Utilization Technology, Suzhou 215009, China;
- 3. Jiangsu Collaborative Innovation Center of Technology and Material of Water Treatment, Suzhou 215009, China)

Abstract: To explore the feasibility of the rapid start-up of partial denitrification and the stable accumulation of NO_2^-N in different waste sludge sources, three-identical SBR reactors (S1, S2, and S3) were inoculated respectively with sludge discharged from a laboratory municipal wastewater denitrifying phosphorus removal system, surplus sludge from a municipal wastewater treatment plant, and river sediment sludge. The characteristics of the partial denitrification start-up and NO_2^--N accumulation were compared, and the partial denitrification activity of the system or $NO_3^--N \to NO_2^--N$ transformation performance were investigated by analyzing the characteristics of the functional bacteria genera of the reactor from the perspective of microbiology. The results showed that all three SBR partial denitrification reactors could be launched successfully in a short time with sodium acetate as the sole carbon source, under a high alkalinity, and by using a suitable COD/NO_3^--N ratio. The average $NO_3^--N \to NO_2^--N$ transformation ratio of the system was ranked as: S1 > S2 > S3 (75. 92% > 73. 36% > 69. 90%). It was found that S1 and S2 had different degrees of partial denitrification performance deterioration under a continuous low temperature, but that S3 could maintain a good NO_2^--N accumulation performance. High throughput sequencing showed that Proteobacteria and Bacteroidetes were dominant in the partial denitrification system, and that the abundance of *Thauera* was significantly different in the three PD reactors: S3 > S1 > S2 (25. O9% > 4.71% > 3.60%), thus indicating that S3 had stable and efficient NO_2^--N accumulation performance and that a high abundance of *Thauera* might play a significant role in maintaining low temperature partial denitrification activity.

Key words: partial denitrification (PD); anaerobic ammonium oxidation (ANAMMOX); waste sludge sources; rapid start-up; stability; functional bacteria genera

短程反硝化(partial denitrification, PD)是指异养反硝化菌以有机物为电子供体,还原 NO_3^- -N $\rightarrow NO_2^-$ -N的不完整生物反硝化过程[1]. 近年来, PD 由于可减少 60. 1% 外碳源, 50% 氧气需求, 84% 废污泥产量等优点[2~5],被认为是与厌氧氨氧化(anaerobic ammonium oxidation, ANAMMOX)耦合最具前景的 NO_2^- -N供给技术,成为新一轮污水生物脱氮研究的热点课题之一[6].

PD 功能的实现很大程度上依赖以NO, -N为产

物的反硝化菌属的富集^[3,7],而不同泥源富集NO₂-N积累菌属实现PD工艺启动及其活性表现仍有差异.鉴于工程应用所需大量的PD污泥实际较难获取,通过驯化常见废污泥为PD污泥,达到实现

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作者简介: 张星星(1995~),男,硕士研究生,主要研究方向为污水 处理与回用技术,E-mail:15862330853@163.com

* 通信作者,E-mail:kgre505@163.com

污泥资源化和避免对环境二次污染的目的. Cao 等 $^{[1]}$ 的研究发现 $C/NO_3^{-1}N=4$ 时缺/好氧污泥短暂 的NO;-N积累特征,NO;-N积累量仅为发酵液碳源 型反硝化污泥的 1/5,而后者在 108 d 培养中获得 NO_3^- -N $\rightarrow NO_2^-$ -N 转 化 率 (nitrate-to-nitrite transformation ratio, NTR) 达 80% 的高效稳定 PD 效 果. 毕春雪等^[8]在 21 d 培养中实现了污水厂二沉池 污泥和硝化反硝化除磷系统污泥向 PD 活性污泥的 转变,认为硝化反硝化除磷系统污泥反应器的 PD 性能最优. Shi 等[9]接种城市污水厂废活性污泥启 动 PD,运行 100 d 左右实现了 NTR 达 84% 的良好 NO; -N积累效果. 而这些研究普遍存在启动周期较 长缺陷,且基于常见废泥源实现 PD 工艺快速启动 的研究鲜见报道,另外,温度作为影响微生物功能酶 代谢活性的关键因素,尚未见研究人员开展温度变 化下对不同泥源驯化 PD 污泥的影响.

虽然乙酸营养型短程反硝化菌属已被广泛报道^[10,11],但研究人员并未提供 PD 污泥驯化成熟初期微生物分布信息^[1,8].此外,笔者对不同废泥源富集驯化的乙酸型 PD 污泥微生物种群差异仍缺乏认

知,而理解上述 PD 污泥菌群分布将对 PD 实际应用时的稳定高效运行有重要意义.

因此,本文探究了温度变化下短程反硝化工艺启动及稳定运行过程 PD 活性和 NTR 性能,并基于高通量测序技术分析了不同废污泥源驯化成熟的 PD 污泥微生物多样性,旨在为 PD 耦合 ANAMMOX 工艺的工程推广作铺垫.

1 材料与方法

1.1 实验装置与运行

本实验装置采用 3 个完全相同的序批式反应器 (SBR),上部敞口安装搅拌器,反应器材质为有机玻璃,内直径 12 cm,高 30 cm,有效容积 2 L.反应器壁自底部垂直平均布置 5 个取样口,通过电磁阀控制排水.反应器在缺氧和室温(15~22℃)条件下运行,无剩余污泥排放.

本实验共分为 2 个阶段, 阶段 I 为 PD 启动阶段(活性上升期), 阶段 II 为负荷提升阶段(活性稳定期), 3 个 SBR 每天周期运行参数一致, 如表 1 所示.

表 1 SBR 运行参数表

0 0	111	Table	1 Operation	onal parameters	of the SBR	. 1 /	- \	(. 6
时期	氮负荷	1 18		时间/min	/ 4		— 換水比/%	HRT/h	周期
門舟	$/\text{kg} \cdot (\text{m}^3 \cdot \text{d})^{-1}$	进水	搅拌	沉淀	排水	闲置	一 换水比/%	пк1/п	问别
1~15 d(阶段 I)	0.16	5	180	30	5	140	70	9	4
16~32 d(阶段Ⅱ)	0 48	5/ /	60	30	5	20	70	3	12

1.2 进水水质与接种污泥

反应器进水为人工配水,主要成分是以硝酸钠和无水乙酸钠配制的 60 mg·L⁻¹NO₃⁻-N及 180~210 mg·L⁻¹ COD, 配水其他组成如下: 0.10 mg·L⁻¹ MgSO₄·7H₂O, 0.40 mg·L⁻¹ CaCl₂, 0.05 mg·L⁻¹ KH₂PO₃, 1.25 mL·L⁻¹微量元素 A 及 B 溶液,微量元素配方如文献[12]的描述. 此外,采用 1 mol·L⁻¹ NaOH 溶液调节进水 pH 为 9.0 ± 0.1.

本研究 S1 反应器接种泥源来源于本实验室稳

定运行超过 180 d 的城市污水反硝化除磷系统排泥,该泥样在 - 20℃下存储 5 个月; S2 接种自苏州市某污水处理厂污泥浓缩池的混合剩余污泥; S3 接种自苏州某高校常年水质轻度富营养化的河涌底泥. 本研究所取泥样均经过 140 目筛网过滤去除体积较大杂质,再使用去离子水冲洗 3 遍后分别接种至 3 个 SBR 反应器,接种污泥初始参数如表 2 所示. 3 个 PD-SBR 反应器运行第 14、19 和 28 d 的污泥浓度变化见表 3.

表 2 初始接种污泥特性

Table 2 Characteristics of the initial inoculation sludge

泥源	MLSS/g·L ⁻¹	MLVSS/g·L ⁻¹	VSS/SS/%	SV ₃₀ /%	SVI ₃₀ /mL·g ⁻¹
01	6. 60	2. 76	41. 82	30, 00	45. 45
S1 S2	2. 32	0. 80	34. 48	25. 20	108. 62
S3	14. 52	0. 36	2. 48	10.00	6. 89

表 3 PD-SBR 反应器运行期间污泥浓度变化

Table 3 Sludge concentration changes during the operation of the PD-SBR reactor

		第 14 d			第 19 d			第 28 d	
泥源	MLSS	MLVSS	VSS/SS	MLSS	MLVSS	VSS/SS	MLSS	MLVSS	VSS/SS
	/g•L ⁻¹	/g•L ⁻¹	/%	/g•L ⁻¹	/g•L ⁻¹	/%	/g•L ⁻¹	/g•L ⁻¹	/%
S1	6. 24	3.48	55.77	3.96	2. 08	52. 53	2. 96	1. 76	59. 46
S2	3.48	1.88	54. 02	2.48	1. 20	48. 39	1. 20	0.40	33. 33
S3	41. 32	3.60	8.71	31.8	3. 28	10. 31	24. 00	3.08	12. 83

1.3 分析方法

1.4 指标测定方法

1.4.1 SBR 长期运行 NTR

计算方法见式(1):

$$NTR = \frac{NO_{2}^{-} - N_{eff} - NO_{2}^{-} - N_{inf}}{NO_{3}^{-} - N_{inf} - NO_{3}^{-} - N_{eff}} \times 100\%$$
 (1)

式中, NO_2^- - N_{eff} 和 NO_2^- - N_{inf} 分别为 SBR 反应器出水和进水 NO_2^- -N浓度, $mg \cdot L^{-1}$; NO_3^- - N_{eff} 和 NO_3^- - N_{inf} 分别为 SBR 反应器出水和进水 NO_3^- -N浓度, $mg \cdot L^{-1}$.

1.4.2 SBR 长期运行出水NO₃ -N占 NO₇ -N 比 NP 计算方法见式(2):

$$NP = \frac{NO_3^- N_{\text{eff}}}{NO_2^- N_{\text{eff}} + NO_3^- - N_{\text{eff}}} \times 100\%$$
 (2)

式中,NO₂-N_{eff}和NO₃-N_{eff}分别为 SBR 反应器出水NO₃-N和出水NO₃-N浓度,mg·L⁻¹

1.4.3 SBR 典型周期 NTR

计算方法见式(3):

$$NTR = \frac{NO_{2}^{-}-N_{t} - NO_{2}^{-}-N_{initial}}{NO_{3}^{-}-N_{initial} - NO_{3}^{-}-N_{t}} \times 100\%$$
 (3)

式中, $NO_2^--N_t$ 和 $NO_2^--N_{initial}$ 分别为 SBR 反应器在 t 时刻和初始 NO_2^--N 浓度, $mg \cdot L^{-1}$; $NO_3^--N_t$ 和 $NO_3^--N_{initial}$ 分别为 SBR 反应器在 t 时刻和初始 NO_3^--N 浓度, $mg \cdot L^{-1}$.

1.4.4 SBR 原位批次活性实验比硝态氮还原速率 $\mu(NO_3^--N)$ 和比亚硝态氮积累速率 $\mu(NO_3^--N)$

 μ (NO₃⁻-N)和 μ (NO₂⁻-N)是通过拟合曲线计算得到,即每隔 0.083 ~ 0.167 h 取样测定NO₃⁻-N和NO₂⁻-N浓度(mg·L⁻¹)除以污泥 MLVSS(g·L⁻¹)获得, mg·(h·g)⁻¹;后依据 μ (NO₃⁻-N)和 μ (NO₂⁻-N)计算批次 NTR_B(%),计算方法见式(4)、(5)和(6):

$$\mu(\mathrm{NO_3^--N}) = [-\mathrm{d}\rho(\mathrm{NO_3^--N})/\mathrm{d}t]/\mathrm{VSS} \quad (4)$$

$$\mu(NO_2^--N) = [-d\rho(NO_2^--N)/dt]/VSS$$
 (5)

$$NTR_B = \mu(NO_2^--N)/\mu(NO_3^--N) \times 100\%$$
 (6)

式中, $\rho(NO_3^--N)$ 和 $\rho(NO_2^--N)$ 分别为 SBR 反应器在 t 时刻 NO_3^--N 和 NO_2^--N 浓度, $mg \cdot L^{-1}$.

1.5 微生物高通量测序分析

采集 S1、S2 和 S3 的 PD-SBR 反应器内运行第 30 d 的污泥样品,样品对应编号分别为 A1、B1 和 C1. 样品由上海美吉生物公司提供测序技术支持,测序方法见文献[12].

2 结果与分析

2.1 不同废泥源短程反硝化系统快速启动及运行 特性

图 1(a)~1(c)分别为 32 d内 S1、S2 和 S3 反 应器短程反硝化启动运行特性. 从中可知,在阶段 I (1~15 d), 3 个反应器均在短时间内实现了 PD 反 应器的启动. S1 反应器运行第 6 d, 出水NO3-N和 NO₂-N浓度分别为 6.51 mg·L⁻¹和 37.57 mg·L⁻¹ NTR 值稳定维持 70% 左右, NP 值低至 14.77%, COD 去除率高达 100%, 表明 S1 已具备稳定高效的 PD 性能. S2 启动运行期(1~7 d),出水NO₂-N浓度 由 19.97 mg·L⁻¹缓慢增加至 38.63 mg·L⁻¹,而剩余 NO₃-N浓度则减少约 20 mg·L⁻¹, 平均出水 COD 为 20.24 mg·L⁻¹,PD 活性处于一个逐步上升阶段,第 7 d 系统 NTR 和 NP 值分别达到 69.23% 和12.22%, COD 去除率接近 100%, 表明此时 S2 具备良好的 PD 活性和脱硝除碳效果. S3 运行第9 d 系统 NTR 和 NP 分别达到 69.98% 和 13.68%, 此时出水 NO, -N 和 NO₃-N 浓度分别为 37.56 mg·L⁻¹ 和 5.95 mg·L-1,与 S1 反应器 PD 活性接近并能够稳定维 持,认为此时 S3 已基本实现 PD 反应器的启动. 在 各个反应器启动期(最长9d),均可观察到PD活性 的逐步提升,体现在NO₂-N积累量不断增加和剩余 NO3-N浓度持续减少,明显优于文献[8]的报道.这 主要是因为反应器运行过程部分反硝化菌属活性受 进水条件影响一直被抑制,系统全程反硝化性能始 终处于不良状态,而以NO;-N为产物的反硝化菌属 增殖未受干扰,因而高效的 PD 性能得以快速实现. 在阶段 II (16~32 d), 缺氧反应时间由 180 min 降 至 60 min, S1、S2 和 S3 反应器NO, -N积累和有机物 去除量并未因反应时间的减少发生明显变化,这意 味着PD反应所需时间较为短暂,而本研究阶段I 控制的 180 min 反应时间是为了前期促进反硝化种 群的增殖从而缩短反硝化属富集时间,阶段Ⅱ下调 反应器搅拌时间是为了阻断反硝化的连续进行,进 一步提升 PD 性能. 实际上,本研究中无论 180 min 还是 60 min 的反应时间都不会使系统生成的

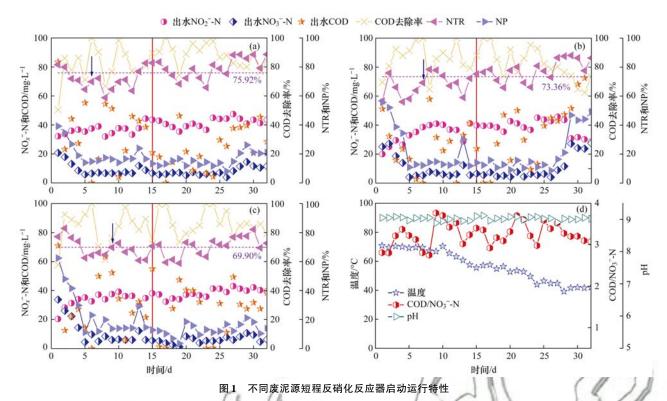


Fig. 1 Start-up and operational characteristics of partial denitrification reactors with different waste sludge sources

 NO_2^- -N被继续还原,这是因为反硝化菌可利用有机物几乎被全部消耗,而系统剩余 NO_3^- -N的存在又使得 NO_2^- -N不会被继续还原为其他氮类物质 $^{[14,15]}$,这也解释了 S1、S2 和 S3 高效的 NTR 性能、优越的 NO_3^- -N积累量和 COD 去除率.

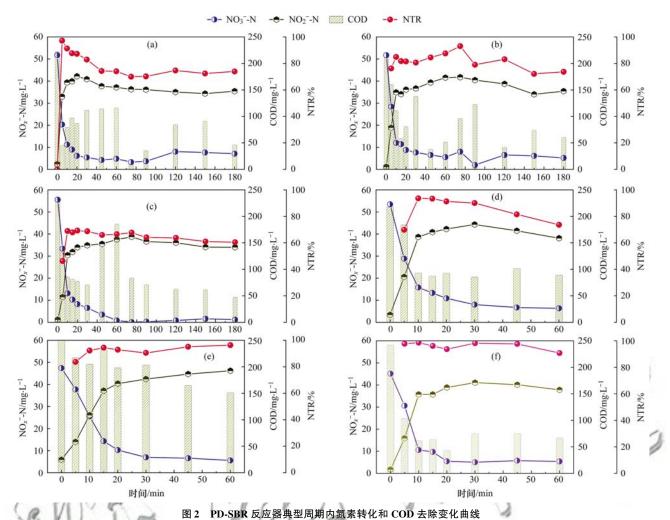
特别的是,S1 和 S2 反应器运行期间 PD 性能受 环境条件影响有较为明显的变化,而 S3 却能够维持 较为稳定的 PD 活性. 伴随室温变化(22.7~ 14.8℃),S1 和 S2 反应器NO, -N积累量、NP 值与 NTR 性能呈现波动趋势,S3 反应器运行则较为平 稳. 如在 20~23 d,实测 3个反应器运行水温由 18.2℃降至 16℃, S1、S2 和 S3 反应器NO, -N积累浓 度分别减少了 4.25、5.98 和 1.96 mg·L⁻¹,说明 S1 与 S2 反应器响应温度变化较为强烈, S3 则对温度 变化敏感程度较低. 推测这与反应器内接种泥源差 异导致的 PD 污泥不同的温度弹性相关. 反应器运 行后期(28~32 d),S1 和 S2 开始呈现不同程度的 PD活性恶化趋势,S1 反应器出水NO;-N浓度达到 14.46 mg·L⁻¹,平均出水 COD 升至 34.46 mg·L⁻¹, 出水NO₂-N却稳定维持43 mg·L⁻¹左右,PD 性能渐 趋下降. S2 出水急剧恶化:系统NO2-N浓度下降近 40%, 剩余NO3-N浓度由 8.98 mg·L⁻¹增至 27.53 mg·L-1,甚至超过接种第 1 d 出水 NO3-N浓度 25.06 mg·L⁻¹, S2 系统 PD 性能近乎崩溃. 有趣的 是,在第28~32 d, S3 反应器仍能够维持平均出水 NO_2^- -N和 NO_3^- -N浓度约为 40.61 $mg \cdot L^{-1}$ 和 7.86 $mg \cdot L^{-1}$, COD 去除率 80%以上效果,表明较 S1 和 S2 反应器内 PD 污泥,S3 内接种自河涌底泥的 PD 污泥抗低温能力较强,认为此类污泥可能是应用于低温环境下 PD 启动和运行的优选泥源. 当然,长期低温条件下 S3 反应器 PD 活性的变化仍有待进一步观察和研究.

2.2 SBR 典型周期不同废泥源短程反硝化系统 性能

为详细说明不同废泥源 PD 系统活性和 NTR 性能,对各反应器运行第 14 d 和第 28 d 典型周期内进行原位批次 PD 活性实验.

2.2.1 典型周期内氮素转化和 COD 去除特性

图 2 所示为 S1、S2 和 S3 反应器运行第 14 d[图 2 (a) ~2(c)]和 28 d[图 2 (d) ~2(f)]典型周期内 氮素转化和 COD 去除变化曲线,用以说明 PD-SBR 运行周期内NO $_3^-$ -N→NO $_2^-$ -N转化情况和有机物去除特性. 由图可得,各反应器运行初始阶段,NO $_2^-$ -N迅速积累,系统 NTR 值接近整个周期峰值,有机物和 NO $_3^-$ -N短时间内被迅速消耗和转化. Cao 等 [16] 研究原位批次 PD 活性的实验发现,搅拌时间为 1 ~2 min PD 系统 NTR 值已达到反应终止时(5~10 min)峰值. 与本实验在短时间内获得较优NO $_2^-$ -N积累量结果相似. 由图 2(a) ~2(c)可知,第 14 d 时典型周期内 S1、S2 和 S3 平均 NTR 分别为 79.66%、81.52%和 64.20%,最高积累 NO $_2^-$ -N浓度分别为



Variation of nitrogen conversion and COD removal in a typical cycle for PD-SBR reactors

42.19、41.79 和 38.73 mg·L⁻¹,反应终止时 COD 浓 度分别为 46. 24、60. 28 和 47. 38 mg·L⁻¹,可以看出 S1 和 S2 反应器 PD 性能优于 S3. 反应器运行至第 28 d 时, S1、S2 和 S3 平均 NTR 分别增加了 5.11%、 10.63%和31.95%,最高NO,-N浓度略微增加,表明 随着反应器运行,PD 活性和系统 NTR 性能也不断 提升,S3 反应器 PD 性能已达到较优运行状态.对图 2进行比较可知,第28d时S1和S2反应器运行终 点 COD 浓度明显高于第 14 d, 分别增加了 42.67 mg·L⁻¹和91.05 mg·L⁻¹,而S3 终点COD浓度仅增 加约13 mg·L⁻¹,COD浓度的增加与微生物裂解释 放胞内有机物相关,与 2.1 节叙述的 3 个 PD-SBR 反应器的性能变化相对应.

PD-SBR 反应器运行过程NO; -N达到峰值后基 本保持稳定,随后反应器剩余 COD 各自维持在一定 范围以内,且系统还会残留少量NO3-N.实际上,此 时剩余有机物很可能是微生物代谢释放的可溶性微 生物产物(SMP), Cao 等[17]的研究证明了这一点: 在原位 PD 活性批次实验中,以乙酸钠作为唯一进 水碳源,通过气相色谱未检测到出水乙酸盐的存在.

SMP 易在内源呼吸和饥饿状态下产生,而反应器内 培养的乙酸营养型 PD 微生物难以利用 SMP 物 质[9],故外碳源的匮乏使得系统NO; -N还原和 NO₂-N生成速率严重减缓.整个周期内,NO₂-N积累 量随NO3-N还原而持续增加,但当外碳源不足时,氮 素转化速率严重放缓.

2.2.2 典型周期批次短程反硝化活性

对 PD-SBR 反应器运行第 2、14 和 28 d 活性进 行原位测定,以比反硝化速率计.如图3所示,运行 后期 S1 和 S2 较接种初期的比硝态氮还原速率和比 亚硝态氮积累速率有显著提高,在第28 d时的比反 硝化速率甚至达到第2d的6倍之多,S3则呈先上 升后下降趋势,说明 PD-SBR 反应器运行期间,S1 和 S2 的 PD 功能菌属活性得到了极大提升,S3 比硝 态氮还原速率和比亚硝态氮积累速率则维持在约 64.09 mg·(h·g) ⁻¹和 35.42 mg·(h·g) ⁻¹,这可能是 由于 S3 较大的污泥浓度(3.08~3.60 g·L-1,以 VSS 计,见表 3) 使得比反硝化速率很难有明显增加 而维持在一定范围内. 第28 d 时,S2 比硝态氮还原 速率达到了 301.48 mg·(h·g)⁻¹,比亚硝态氮积累

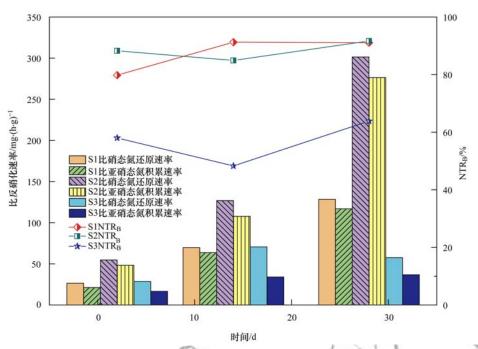


图 3 PD-SBR 反应器典型周期原位批次比反硝化活性和 NTR 性能

Fig. 3 Typical cycle in-situ batch denitrification activity and NTR performance of PD-SBR reactors

速率为 276. 40 mg·(h·g) ⁻¹, 远远超过 Cao 等^[18]报 道的 PD 原位最大比硝态氮还原速率 84. 9 mg·(h·g) ⁻¹的数值, 这是由于此时受持续低温影响污泥逐渐解体引起 MLVSS 值仅为第 14 d 时的 1/4 (见表 3), 导致了 PD 比反硝化活性的显著提升, 但 NO₃-N还原量却因生物量的降低而减少.

典型周期内 S1 的 NTR_B 维持在 79.81% ~ 91.25%, S2 平均 NTR_B 达到了 88.29%, S3 的 NTR_B 则整体维持 60% 左右. 表明 PD-SBR 反应器运行期间能够维持稳定的 PD 活性和 NTR 效率, S1 和 S2 批次 PD 活性与 Cao 等 [18] 获得的平均 88.3% 的 NTR 效率接近, 但高于之前报道的 PD 长期运行 80% 的 NTR 效果 [1]. NTR_B 是基于比亚硝态氮积累速率和比硝态氮还原速率的比值获得, 而 S3 长期运行过程中(见图 1) NO_2^- -N积累量明显低于 S1 和 S2,说明 S3 反应器内以 NO_2^- -N为最终产物的反硝化种群活性在 3 个 SBR 中最低, 故导致了批次实验中相对较小的比 NO_2^- -N积累速率和 NTR 性能.

2.3 不同废泥源短程反硝化系统微生物群落组成

2.3.1 门水平微生物群落结构

图 4 为不同泥源 PD-SBR 反应器运行 30 d 污泥样品门水平微生物丰度群落(微生物相对丰度 > 1.0%为主要菌门). 从中可知,不同泥源的污泥样品共检测出 7 个主要菌门,分别为变形菌门(Proteobacteria)、拟杆菌门(Bacteroidetes)、绿弯菌门(Chloroflexi)、厚壁菌门(Firmicutes)、Patescibacteria菌门、酸杆菌门(Acidobacteria)和放

线菌门(Actinobacteria). 按照门水平丰度高低排序, S1 反应器主要菌门分别为变形菌门(56.17%), 拟杆菌门(21.08%)、厚壁菌门(12.43%)和绿弯菌门(7.82%); S2 依次为拟杆菌门(48.77%)、变形菌门(38.40%)和绿弯菌门(6.08%); S3 反应器内变形菌门(78.50%)和拟杆菌门(13.45%)则构成了超过90%的门水平物种. 这说明 PD-SBR 反应器功能菌群落多样性低,富集程度高^[12],特别是 S3 反应器.

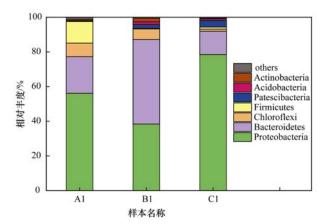


图 4 不同泥源 PD-SBR 反应器门水平微生物群落柱状图

Fig. 4 Bar chart showing the microbial community at the phylum level for PD-SBR reactors with different sludge sources

2.3.2 属水平微生物群落结构

图 5 为不同泥源 PD-SBR 反应器运行 30 d 污泥 样品属水平微生物丰度群落图(属水平相对丰度 > 1.0% 为主要分析对象). 明显地, Acinetobacter 属在 S1 中丰度高达 40.60%, 是该反应器绝对优势菌属,

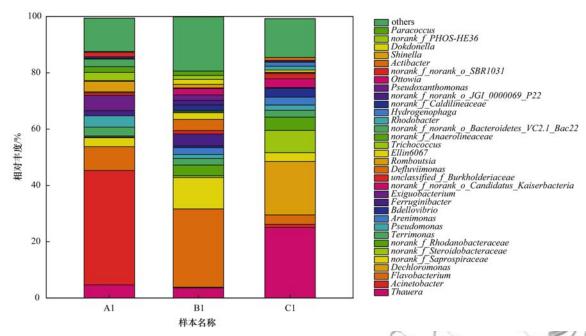


图 5 不同泥源 PD-SBR 反应器属水平微生物群落柱状图

Fig. 5 Bar chart showing the microbial community at the genus level for PD-SBR reactors with different sludge sources

其次分别是 Flavobacterium (8.46%)、Exiguobacterium(5.42%)和 Thauera(4.71%)等,以上4个属分别对应变形菌门、拟杆菌门、厚壁菌门和变形菌门、S2 中 Flavobacterium(27.79%)相对丰度占比最高,后面依次为 norank_f_Saprospiraceae (11.08%)、Ferruginibacter (4.25%)、Defluviimonas (3.99%)、norank_f_Rhodanobacteraceae (3.81%)和 Thauera(3.60%)等. S3 反应器内部优势菌属为 Thauera(25.09%)、Dechloromonas(18.98%)、norank_f_ Steroidobacteraceae (7.94%)及 norank_f_ Rhodanobacteraceae (4.68%)等. 显然, Thauera 属主导了S3 反应器菌属群落.

3 讨论

3.1 不同废泥源短程反硝化系统快速启动及高效运行分析

3 个反应器在较短时间内均实现了 PD 的快速启动. 原因是本研究始终控制反应条件: 进水 pH 为 8. 90 ~ 9. 10、COD/NO $_3^-$ -N为 2. 75 ~ 3. 76. pH 被证明是选择富集NO $_2^-$ -N积累菌属的有效条件 $_2^{[9,13,19]}$,反硝化过程中NO $_3^-$ -N还原为 N $_2$ 是连续的 4 步酶促反应,反应的连续进行与电子接收、传递和消耗有关 $_3^{[3]}$,高 pH 则会降低反硝化过程碳氧化速率,进而加剧反硝化酶之间的电子竞争 $_2^{[20]}$, NO $_2^-$ -N还原酶活性明显受到高碱度抑制,而NO $_3^-$ -N还原酶活性基本不受影响,这导致了NO $_2^-$ -N暂时的积累 $_3^{[13,21]}$. Qian等 $_3^{[13]}$ 的研究表明,控制进水 pH = 9. 0 更利于富集NO $_3^-$ -N还原酶基因数高的反硝化物种; Shi 等 $_3^{[9]}$ 在

进水 pH = 9.0 条件下,提升废污泥 NTR 值达 84% 的良好 PD 活性. 因此, 本研究控制的进水 pH 为 9.0 ±0.1条件是实现3个反应器快速启动PD和有效 NO,-N积累的关键因素,能够快速筛选NO,-N积累 菌群和抑制NO, -N还原菌属增殖. 应当指出的是,虽 然本研究3个PD-SBR 反应器获得平均出水 NTR 最 高为75.92%,低于研究人员认为平均NTR=80%是 PD 反应启动成功的标志[1],但80%的 NTR 效率是 基于 PD 反应过程中取样点时刻NO; -N还原量和 NO; -N积累量而得,而本研究 S1、S2 和 S3 在运行期 间能够保持70%左右出水NTR效率,因而认为本实 验中反应器出水 NTR = 70% 是 PD 启动的一个标 志. 另外,限制低 COD/NO, -N比可以促进 PD 功能 菌的增殖,因为反硝化物种会优先储存易被利用碳 源而非直接利用^[21,22]. COD/NO₃-N比很大程度上 决定了反硝化进程,控制硝酸盐还原速率[23]. 相关 研究表明 COD/NO₃-N为 2.0~3.5 是 PD 高效运行 较优的控制条件[3,4,24],本研究实际运行中同样发现 在 COD/NO₃-N为 3.0~3.5 范围内 PD 活性较优, 两者还可能存在正相关性. 启动期间反硝化物种通 过种间选择,在乙酸盐有机物、高碱度和适宜 COD/ NO, -N比的反应条件下, NO, -N积累菌迅速占据优 势地位[24],NO,-N还原菌的增殖则被严重抑制,因 而 3 个 PD-SBR 反应器在短期内快速启动同时保持 运行的高效性.

值得注意的是,本研究 S1、S2 和 S3 在 32 d 的运行中分别获得平均 NTR 为 75.92%、73.36% 和 69.90% 效果,均明显优于 Qian 等[13] 接种反硝化污

泥在进水 pH = 9.0 条件下 PD 反应器平均出水 NTR = 57%, 这可能是因为后者控制 COD/NO $_3^-$ -N比为 3.0, 电子供体不足引起了NO $_3^-$ -N还原速率下降.

3.2 不同废泥源短程反硝化系统性能变化分析

碳源的选取对于 PD 反应速率有很大影响, Le 等[23] 比较了多种碳源对短程反硝化短期影响,发现 乙酸和甘油显示出高效的 PD 选择,并推测与电子 传递途径相关. Li 等[25] 同样发现相比乙酸物质, 葡萄糖反硝化反应会上调乙酸产出量和下调乙酸 利用率导致细胞内 NADH/NAD+比下降,进而降 低脱硝速率,因而认为乙酸盐是NO,-N积累的优 选碳源. 广泛的研究同样表明, 乙酸作为简单小分 子物质极易被微生物利用,因而 PD 反应选取乙酸 作为电子供体能够促进乙酸营养型 PD 种群快速 增殖,加快 PD 反应进程^[3,18,26]. 3 个 PD-SBR 反应 器均以乙酸钠作为唯一碳源,导致了剧烈的 PD 反 应速率. 批次实验表明,反应器在阶段 I 运行第14 d, 60 min 时系统NO₂-N积累量近乎峰值,随着运 行时间推移,阶段 II 运行第 28 d 时 S1、S2 和 S3 反 应器 30 min 时刻NO, -N浓度分别达 44. 31、42. 43 和 41.09 mg·L-1,高于或接近反应终点浓度,表明 本研究可进一步减少缺氧搅拌时间以获得更高的 NO, -N产量.

近期, Meng 等^[27]的研究发现硝化菌和反硝化菌能够承受较高范围的温度变化扰动,但持续低温下传统反硝化菌相对丰度仍会逐渐下降^[28]. S1 和S2 反应器种泥由于长期处于中温(~25℃)环境,耐冷菌丰度不足,因而温度降低反硝化活性也会随之发生明显减弱,长期低温抑制下S2污泥甚至失活死亡(观察到明显的污泥白化,出水透明度较低). S3取自河道底泥的表层反硝化菌可能适应了自然界中比生物反应器更低的温度^[29],因此低温影响下PD活性并未受明显影响.

3.3 不同废泥源短程反硝化系统微生物种群分析

接种泥源为城市污水处理系统反硝化除磷单元的 S1 反应器,变形菌门、拟杆菌门、厚壁菌门和绿弯菌门为主导菌门,而在城市污水培养的 PD 污泥也检测出类似菌门^[9].变形菌门在良好性能的活性污泥系统含量最高,包含了氮循环功能相关的氨氧化菌、亚硝酸盐氧化菌和反硝化菌等^[30],先前的 PD 系统中也发现变形菌门通常占比极高(44.1%~82.3%)^[31],与本研究类似.因此高丰度的变形菌门是 PD 系统高效 NTR 的保证,PD-SBR 变形菌门丰度高低依次为 S3 > S1 > S2(78.50% > 56.17% > 38.40%),对应反应器运行至 30 d 时 PD 性能 S3 最优,S1 渐趋恶化,S2 近乎崩溃. 拟杆菌门和绿弯菌门

通常具备降解易溶有机物(如短链脂肪酸)、胞外聚合物和衰亡菌体等功能^[32],拟杆菌门还与反硝化作用和颗粒形成紧密相关^[12],S2中两类菌门占比高达54.85%,远高于S1和S3[28.9%和13.45%(仅拟杆菌门)],进一步说明S2污泥严重衰亡引起了拟杆菌门和绿弯菌门的大量增殖.

Thauera 属为广泛报道的 PD 反应器中实现 NO, -N积累的功能菌属[9,12,13],其在微生物群落中 丰度分布对 PD 活性影响极大. 反应器运行至 30 d 时,S3 中 Thauera 属相对丰度高达 25.09%,而 S1 和 S2 中仅有 4.71% 和 3.60%, 这解释了 S3 反应器在 长期低温影响下仍能保持良好 PD 活性和NO, -N积 累效果的特性.有研究表明,随温度下降,提升功能 菌属生物量丰度能够维持微生物氮降解活性[33].长 期运行 S1 和 S2 反应器平均 NTR 分别为 75.92% 和 73.36%,均高于 S3 的 69.90%,这可能是因为在适 宜温度下,S1 和 S2 内 Thauera 属活性高于 S3,而长 期低温 S1 和 S2 内 Thauera 属活性和丰度下降, S3 内 Thauera 属则维持高丰度. S1 中属于变形菌门的 Acinetobacter 属是其优势菌属,在污水处理系统发挥 高效的自养反硝化作用,因而有利于维持 S1 系统的 反硝化性能^[34]. S2 菌属中 Flavobacterium 、norank_f _Saprospiraceae 和 Ferruginibacter 比例达 43. 12%,均 属于可利用死亡细菌残体物质的拟杆菌门,解释了 该系统污泥衰亡恶化、性能崩溃的现象.

4 结论

- (1) 在 22 ~ 23℃, pH = 9.0 ± 0.1 和 COD/NO $_3$ -N为 3.0 ~ 3.5 条件下,S1、S2 和 S3 分别在第 6、7 和 9 d 成功启动 PD,系统长期运行平均 NTR 为 S1 > S2 > S3(75.92% > 73.36% > 69.90%).
- (2)短程反硝化活性批次实验表明,乙酸钠为碳源和适宜 COD/NO_3^- -N比的进水水质,PD-SBR 反应器获得良好的比反硝化速率和 NTR 性能,第 28 d 典型周期内 S1、S2 和 S3 平均 NTR 分别为 84. 77%、92. 15% 和 96. 15%, 最大比 NO_2^- -N 积 累 速 率 为 116. 95、276. 40 和 36. 73 $mg\cdot(h\cdot g)^{-1}$.
- (3)运行期间,S1 和 S2 反应器 PD 活性响应温度变化较为明显,而 S3 反应器 PD 活性对温度敏感程度较低,推测河涌底泥可能是低温实现短程反硝化快速启动和稳定运行的优选种泥.
- (4)变形菌门和拟杆菌门是 PD 反应器主导微生物菌门, PD 活性和高 NO_2^- -N积累量取决于属于变形菌门的 *Thauera* 属丰度. S3 反应器 *Thauera* 属丰度高达 25.09%, 是其维持低温 PD 活性的重要原因.

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《环境科学》连续8次荣获 "中国最具国际影响力学术期刊"称号

2019年10月28日,中国学术期刊(光盘版)电子杂志社(CNKI)等机构发布"2019中国最具国际影响力学术期刊"评选结果.《环境科学》荣获"2019中国最具国际影响力学术期刊"称号,是唯一人选的环境科学与资源科学类中文期刊,也是自首次评选以来连续8次获此殊荣.评选以期刊国际影响力指数进行排序,遴选出排名前5%(Top5%)的期刊获评"中国最具国际影响力学术期刊".

HUANJING KEXUE

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