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目 次

多模式厌氧/缺氧/好氧污水处理工艺的稳态与动态模拟

周振1,吴志超2,王志伟2,杜兴治3,蒋玲燕3,邢灿1

(1. 上海电力学院环境与化学工程学院,上海 200090; 2. 同济大学环境科学与工程学院,污染控制与资源化研究国家重点实验室,上海 200092; 3. 上海城投污水处理有限公司,上海 201203)

摘要:数学模拟是污水处理系统教学科研、工艺评估、运行优化和自动控制的重要工具,在污水处理厂中得到了广泛应用. 利用过程数据对 ASM2d 模型进行校正,并分析评估了校正模型在多模式厌氧/缺氧/好氧(AAO)工艺3个模式15个工况下稳态模拟及 AO 模式下动态模拟的可靠性. 15个工况的稳态模拟表明,校正模型能准确模拟污泥浓度和出水水质;在 AO 模式的动态模拟中,模拟曲线与出水水质以及污泥浓度的变化趋势相一致,模拟结果具有较高的准确度.

关键词:污水处理:模拟:活性污泥:数学模型:厌氧/缺氧/好氧工艺

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Modeling and Dynamic Simulation of the Multimode Anaerobic/Anoxic/Aerobic Wastewater Treatment Process

ZHOU Zhen¹, WU Zhi-chao², WANG Zhi-wei², DU Xing-zhi³, JIANG Ling-yan³, XING Can¹

(1. College of Environmental and Chemical Engineering, Shanghai University of Electric Power, Shanghai 200090, China; 2. State Key Laboratory of Pollution Control and Resource Reuse, College of Environmental Science and Engineering, Tongji University, Shanghai 200092, China; 3. Shanghai Chentou Wastewater Treatment Limited Company, Shanghai 201203, China)

Abstract: Mathematical modeling is a useful tool for professional education, process development, design evaluation, operational optimization and automatic control of the wastewater treatment system, and has been extensively applied in numerous full-scale wastewater treatment plants. The ASM2d model was calibrated by the process data, and used to simulate 15 operational test runs of the multimode anaerobic/anoxic/aerobic (AAO) process. After calibration, the model was capable of simulating the sludge concentrations and effluent data in 15 test runs of the multimode AAO system. The dynamic simulation results showed an overall good agreement between the measured and simulated data, for both effluent data and sludge concentrations, with a good reproduction of dynamic processes in AO test runs.

Key words: wastewater treatment; simulation; activated sludge; mathematical model; anaerobic/anoxic/aerobic process

污水生物处理系统的数学模拟是利用数学模型类比复杂的生化反应以寻求过程规律的一种方法,是数学模型在污水处理厂应用的关键性步骤^[1,2].自从活性污泥数学模型(ASMs)^[3]推出以来,数学模拟在污水处理厂的应用得到了快速发展,并出现了许多专业模拟软件^[4].污水处理系统的数学模拟具有 4 方面的重要作用:①教学科研,通过模拟加深对流程的理解,并根据构思开发新工艺^[5,6];②工艺评估,通过模拟评估对比多个工艺方案^[7],在升级改造处理中应用较多^[5,8,9];③运行优化,通过工艺策略选择提高工艺稳定性,改善出水水质、降低系统能耗^[10,11];④自动控制,将工艺模型简化后纳入自动控制算法中,提高系统的控制品质^[12].

本研究将以多模式厌氧/缺氧/好氧(AAO)工艺为对象,以倒置 AAO 工艺的运行数据校正ASM2d模型,并分析校正模型在 AAO、倒置 AAO

和 AO 模式 15 个运行工况下稳态模拟及 AO 模式下 动态模拟中的准确性,以评估数学模拟在同一进水 条件、不同运行工艺下应用的可靠性.

1 材料与方法

1.1 试验装置与运行工况

多模式 AAO 试验装置位于白龙港污水处理厂, 共设3套,其选择池、缺氧池、厌氧池和好氧池的有效体积分别为2.7、18.9、10.8 和52.8 L; 二沉池体积为62.4 L,深度为1.05 m. 多模式 AAO 工艺可根据季节变化、排放要求和进水情况通过内回流的回流点调整或启闭在 AAO、倒置 AAO 和 AO 模式间灵活切换,如图1所示.

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作者简介:周振(1981~),男,博士,副教授,主要研究方向为污水处理原理与技术,E-mail;zhouzhen09@yahoo.com.cn

污水以恒定流量(Q_i) 200 L·d⁻¹以分段进水方 式分别进入装置选择池和厌氧池,以分段进水因子f 表征进入选择池的水量占总进水量的体积分数. 污 泥内外回流比(r和 R)范围分别为 25%~100%和

25%~200%. 好氧池溶解氧(DO)和 pH 分别控制 为 2.5 mg·L⁻¹ 和 7.0 ~ 7.5. 污泥龄(SRT) 通过剩余 污泥排放控制为10~20 d. 试验主要工况操作条件 如表1所示.

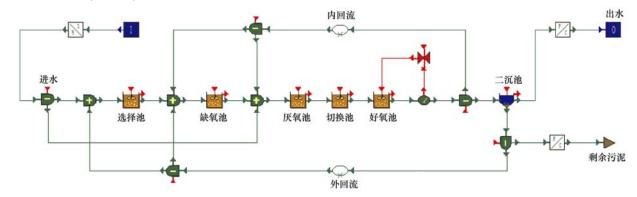


图 1 多模式 AAO 系统的工艺模型

Fig. 1 Runtime model of the multimode AAO process

表 1 多模式 AAO 现场试验工况参数与进水水质表 Table 1 Operational parameters and influent pollutants of pilot-scale multimode AAO test runs

	Tubic 1	operational	Parameter	5 and	minacin	Ponatanto	or prior sear	e manimoae	11110 100	, runs
行天数	水温	SRT	f	r	R	COD	$S_{ m NH}$	$S_{ m NO}$	TN	$S_{ m PO}$
/d	∕℃	/d	1%	1%	1%	/mg·L ⁻¹	$/\text{mg} \cdot \text{L}^{-1}$	/mg•L ⁻¹ /	′mg•L -1	/mg·I

运行	编号	运行天数	水温	SRT	f	r	R	COD	$S_{ m NH}$	$S_{ m NO}$	TN	$S_{ m PO}$	TP	X_{TSS}
模式	-710 3	/d	$^{\sim}$	/d	/%	/%	/%	/mg·L ⁻¹						
	P1	25	19. 5 ~ 23. 5	15	100	_	100	243. 2	23. 07	0. 92	32. 94	1.48	3. 39	123.3
	P2	35	15. 0 ~ 19. 5	15	100	_	50	287. 6	25. 52	0.65	35. 39	1.48	3. 55	108.4
AO	P3	25	11.9 ~ 14.2	15	100	_	25	292. 2	27. 52	0.74	35. 69	1.31	3.41	184. 0
	P4	60	16. 8 ~ 25. 0	10	100	_	50	273.3	27. 78	0.36	34. 75	1.88	3. 51	128.3
	P5	60	24. 2 ~ 30. 0	20	100	_	50	234. 1	26. 34	0.54	31. 35	1.67	2. 75	119.7
	R1	35	19. 5 ~ 23. 5	15	50	50	100	241.0	22. 70	0. 82	32. 31	1. 50	1. 60	112.0
	R2	35	15. 0 ~ 19. 5	15	30	50	50	287. 6	26. 28	0.65	35. 39	1.48	3. 55	131.4
倒置	R3	25	11. 9 ~ 14. 2	15	30	25	25	292. 2	28. 39	0.74	35. 69	1.31	3.41	140.0
AAO	R4	55	16. 8 ~ 24. 0	10	30	25	25	276. 1	28. 28	0.45	34. 78	1.83	3.48	163. 3
	R5	85	24. 0 ~ 30. 0	20	30	25	25	234. 7	24. 47	0.50	31.70	1.70	2. 90	131.2
	C1	35	19. 5 ~ 23. 5	10	100	100	60	253. 0	24. 99	0. 51	31. 65	2. 16	3. 71	130.6
	C2	45	15. 8 ~ 22. 0	15	100	200	30	289. 8	22. 25	0. 57	33.63	1.49	3. 57	183.7
AAO	C3	65	22. 0 ~ 30. 2	10	100	200	30	259.6	23. 9	0.73	30.68	1.82	3. 11	154. 9
	C4	75	18. 5 ~ 25. 2	20	100	100	30	256. 7	24. 42	0.69	31.70	1. 67	3. 26	192. 3
	C5	45	17. 6 ~ 25. 4	15	100	200	60	289. 8	26. 77	0.42	33. 63	1.49	3. 57	183.7

1.2 样品采集与分析方法

每隔2~3d取进水、出水和好氧池混合液进行 常规分析,分析指标包括进水和出水 COD、氨氮 (S_{NH}) 、硝态氮 (S_{NO}) 、总氮(TN)、正磷酸盐 (S_{PO}) 、 总磷(TP)和总悬浮固体(X_{rss}),以及混合液悬浮固 体(MLSS)、挥发性悬浮固体(MLVSS)和污泥体积 指数(SVI),同时测定好氧段的 DO 和 pH 值. 工艺 过程数据(各反应段的 S_{NH} 、 S_{NO} 和 S_{PO})则每周测定 一次. 各工况的进水常规分析指标平均值如表 1 所示.

脱氮除磷系统的数学模拟还需进行进水 COD 和氮磷组分划分. COD 组分包括溶解性惰性组分 $S_{\rm I}$ 、颗粒性惰性组分 $X_{\rm I}$ 、易生物降解组分 $S_{\rm S}$ 、慢速 生物降解组分 $X_{\rm S}$ 、异养菌 $X_{\rm H}$ 、自养菌 $X_{\rm AUT}$ 和聚磷 菌 X_{PAO} ,组分划分可采用3组批式试验 $^{[13]}$ 完成.由 于组分划分工作量较大,将其作为模型输入值时将 不考虑季节等因素的影响,假定各组分在 COD 中所 占比例在所有水样中均为恒定值,具体划分比例参 见文献[14]. 氮磷组分转化因子则通过参数校正 确定.

2 结果与讨论

2.1 模型构建与参数校正

模型构建采用 WEST 3.7.5 完成. 多模式 AAO 工艺试验由于装置体积较小,基本可以充分混合,水 力模型可采用串联反应器模式近似[2]. 根据这一原 则构建的多模式 AAO 工艺模型如图 1 所示. 生化反应模型选择 ASM2d 模型的改进版本 ASM2dTemp,该模型可在不同温度下模拟碳氧化、硝化-反硝化以及包括反硝化除磷在内的生物除磷过程等. 二沉池模型则选用一维分层模型——双指数模型.

本研究的模型参数校正采用倒置 AAO 模式运

行数据,以过程数据为主、出水水质为辅的校正策略,具体校正方法与过程参见文献[14]. 除了氮磷组分因子 i_N 和 i_P 外, ASM2d 模型校正只需调整 $K_{NH,AUT}$ 、 $\eta_{NO,H}$ 、 q_{fe} 和 $\eta_{NO,PAO}$ 4 个动力学参数(表2). 二沉池模型参数根据 SVI 等操作参数计算调整 [15]. 在本研究的稳态和动态模拟中,除表 2 所列校正值和特别说明外,其它参数均取默认值.

表 2 模型校正中调整的参数默认值与校正值

Table 2	Calibrated	and	default	parameters	of	the	process	model
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参数	名称	单位	默认值	校正值
$i_{ m N,XI}$	X _I 的 N 含量[m(N)]/[m (COD)]	g•g ⁻¹	0. 03	0. 01
$i_{ m N,XS}$	X _S 的 N 含量[m(N)]/[m(COD)]	g•g-1	0.04	0. 02
$i_{ m P,SF}$	S _F 的 P 含量[m(P)]/[m(COD)]	g•g-1	0. 01	0.005
$i_{ m P,XI}$	X _I 的 P 含量[m(P)]/[m(COD)]	g•g ⁻¹	0.01	0.005
$i_{ m P,XS}$	X _S 的P含量[m(P)]/[m(COD)]	g•g ⁻¹	0. 01	0.005
$K_{ m NH,AUT}$	X_{AUT} 的氨氮半饱和系数(以N计)	$mg \cdot L^{-1}$	1.0	0. 5
$oldsymbol{\eta}_{ m NO,H}$	X_{H} 的反硝化降低因子	_	0.8	0. 6
$q_{ m fe}$	发酵速率常数	d ⁻¹	3.0	1.5
$oldsymbol{\eta}_{ ext{NO,PAO}}$	X_{PAO} 的缺氧降低因子	_	0.6	0.8

2.2 多模式 AAO 不同运行模式的稳态模拟

采用表 1 所列的多模式 AAO 系统 15 个工况的工艺参数,以进水污染物平均浓度为输入值,利用表 2 的校正参数对污泥浓度和出水水质进行稳态模拟. 稳态模拟值为多模式 AAO 系统长期稳定运行(至少 100 d)的模拟值;而实测值则为各个工况稳定运行阶段的平均值(\bar{x}). 对比时还考虑实测值95%(α = 0.05)的置信区间(CI),计算如式(1)所示.

$$CI = \bar{x} \pm 1.96 \left(\frac{\sigma}{\sqrt{n}}\right) \tag{1}$$

式中, σ 为总标准差,n 为样品数量.

多模式 AAO 工艺 15 个工况下好氧池污泥浓度实测值与稳态模拟值的对比如图 2 所示. 从中可见,除工况 C3 外,所有工况条件下 MLSS 的稳态模拟值均在实测值 95% 的置信区间内;而在 MLVSS模拟中, MLVSS/MLSS 取 15 组工况实测平均值 0.64,有4个工况(R5、P4、P5 和 C3)的模拟值明显偏离实测值. 经分析知,工况 C3 出现偏离是由于现场试验多次故障导致运行不稳定;而 R5 和 P5 的偏离则是由于 MLVSS/MLSS = 0.53 ± 0.02,明显低于 0.64 所致. 总体而言,校正后的工艺模型对多模式 AAO 系统污泥浓度的稳态模拟较为准确.

多模式 AAO 工艺试验各工况条件下出水 TSS、COD、 $S_{\rm NH}$ 、TN 和 TP 的实测值与稳态模拟值对比如图 3 所示. $X_{\rm TSS}$ 的准确模拟是出水 COD、TN 和 TP

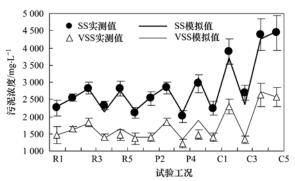


图 2 多模式 AAO 工艺试验 15 个工况污泥浓度的稳态模拟

Fig. 2 Simulation of sludge concentrations for 15 multimode AAO test runs

等指标准确模拟的前提^[16].除工况 C1 外,表 1 中的其它 14 个工况均测定了 X_{TSS} .在图 3(a)中,有 3个工况(P2、P4 和 C4)的模拟值明显偏离实测值.这主要是由于在小规模试验中,二沉池运行易于受各种因素干扰所致,同时系统运行故障导致的好氧池 MLSS 波动也会造成 X_{TSS} 的明显变化.显然,这些外界干扰所造成的二沉池运行波动很难在二沉池模型中体现.不过总体而言,校正后的工艺模型基本能够预测正常运行条件下各工况的 X_{TSS} .

在 COD 的稳态模拟中,工况 R5、P4 和 C3 的模拟值明显偏离实测值,但偏差均在 5 mg·L⁻¹以内. 工况 P4、C2 和 C5 中 S_{NH} 的稳态模拟值偏离实测值 95%的置信区间,但偏差均小于 0.2 mg·L⁻¹. 5 个工况(R4、P4、C1、C3 和 C4)的 TN 稳态模拟值在实测值置信区间外,但平均相对标准偏差仅为

9.7%. 15 个工况下 TP 的稳态模拟值与实测值最为接近,仅工况 R5 和 C1 略有偏差. 由图 3(d) 和 3(e) 可知,降低回流比(P1 ~ P3、R1 ~ R3)能有效降低出水 TP,但出水 TN 会显著上升^[14];延长污泥龄(P4 与 P5、R4 与 R5)能削减出水 $S_{NH}^{[1,17]}$,但会造成出水 TP 反弹^[18].模拟值能很好地反映上述变化趋势.由以上分析知,校正模型的稳态模拟值与实

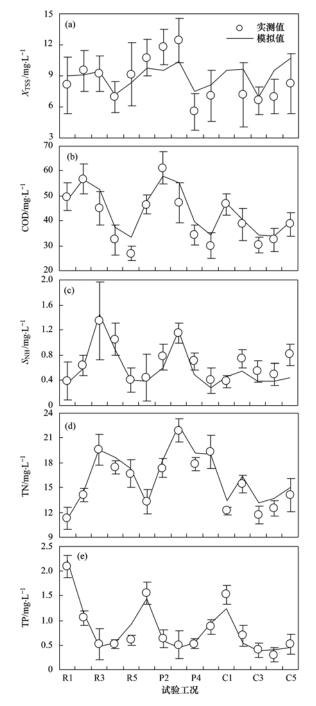


图 3 多模式 AAO 工艺试验 15 个工况出水污染物的稳态模拟 Fig. 3 Simulation of effluent pollutants

for 15 multimode AAO test runs

测值基本吻合.

2.3 多模式 AAO 系统的动态模拟

工况 R2 的动态模拟曾用于校正模型的验证, 其实测值与动态模拟曲线基本吻合^[14]. 本研究将以 AO 模式工况 P2 动态模拟分析同一进水条件、不同工艺下校正模型应用的可靠性. 动态模拟的初始值为前一工况(P1)的长期稳态模拟值. 模拟的准确程度采用式(2)所示的平均相对误差(ARD)评估:

ARD =
$$\frac{1}{n} \sum_{i=1}^{n} \left| 1 - \frac{c_{\text{sim}}(t_i)}{c_{\text{exp}}(t_i)} \right|$$
 (2)

式中, $c_{\text{sim}}(t_i)$ 和 $c_{\text{exp}}(t_i)$ 分别为 t_i 时刻模拟和实测值.

由图 4 可见,校正后的污水处理工艺模型能够很好地反映工况 P2 好氧段 MLSS 和 MLVSS 实测值的变化趋势. 在工况 P2 中, MLSS 和 MLVSS 模拟的ARD 值分别为 4.81% 和 5.02%. 由于受进水污染物浓度波动的影响,工况 P2 前 5 d 和最后 10 d 均出现了活性污泥浓度显著性增长的趋势,校正后工艺模型的动态模拟准确描述了这一规律.

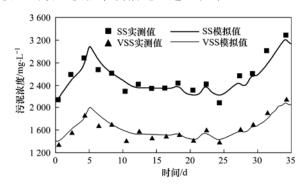


图 4 工况 P2 中好氧池污泥浓度的实测值与模拟值的对比

Fig. 4 Measured and simulated sludge concentrations of test run P2

图 5 (a) 描述了工况 P2 中 X_{TSS} 模拟值和实测值的变化. 工况 P2 前 16 d,SVI (49.8 mL·g⁻¹) 高于后期(41.3 mL·g⁻¹) 造成后期出水 X_{TSS} 较低. 由于出水 X_{TSS} 对低浓度区沉降特性参数 γ_p 的变化十分灵敏 [15,19],因此动态模拟时采取分阶段设定 γ_p 的方法,16 d 前后 γ_p 分别设为0.021 6和0.007 2. 采用该方法后 X_{TSS} 的 ARD 为 16.8%,误差集中于沉降性能波动较大的 14 d 和 16 d,但模拟曲线基本可反映 SS 的变化趋势.

图 5(b)对比了工况 P2 出水 COD 实测值和动态模拟值的变化. 校正后的工艺模型模拟 COD 的 ARD 值为 11.3%, 其中第 27 d 实测值(80.2 mg·L⁻¹)偏离较大. 从出水组分来看,由于 $S_{\rm I}$ 在系

统中无法降解也无法沉降去除^[3,20,21],该组分在出水 COD 中所占比例很高,这与文献[16,22]报道结论类似.

出水综合性指标 TN 和 TP 可用于系统总体脱氮除磷效果的评价. 由图 5(c) 知, 出水 TN 浓度的模拟值与实测值基本吻合, 工况 P2 动态模拟的 ARD 为 6.12%. 而 TP 动态模拟的 ARD 为 14.8%, 沉降性能波动较大的 14 d 和 16 d 以及第 27 d 的误差较大. 但动态模拟曲线基本能够反映 TP 的波动趋势及出水 SS 波动对 TP 的显著性影响 [图 5 (d)]. 但在工况 P2 最后 15 d 中, TP 的模拟值略高于实测值,这可能是由于最后 15 d 实际温度降低至15.0%, 而模拟采用平均温度 17.3%. 由于 X_{PAO} 属于嗜冷性细菌 [23-25],因此实际试验的除磷效率会略高于模拟值.

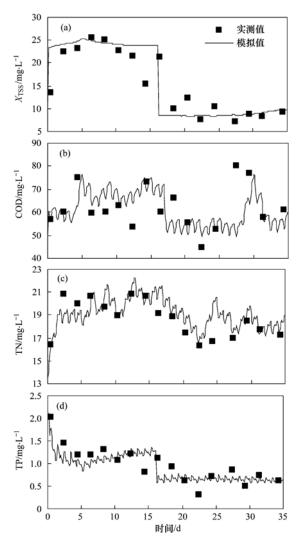


图 5 工况 P2 的出水综合性指标实测值与动态模拟值的对比 Fig. 5 Measured and simulated effluent composite variables of test run P2

3 结论

以倒置 AAO 模式过程数据对 ASM2d 模型进行校正,并将校正模型应用于多模式 AAO 系统 3 个模式 15 个工况的模拟. 15 个工况污泥浓度和出水水质的模拟结果表明,校正后模型的稳态模拟值基本都在实测值 95% 的置信区间内. 对 AO 模式的动态模拟结果表明,模型校正后的模拟曲线与出水 X_{TSS} 、COD、TN 和 TP 以及好氧段活性污泥的变化趋势相一致,模拟结果具有较高的准确度.

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HUANJING KEXUE

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Vol. 34 No. 4 Apr. 15, 2013

CONTENTS

Water-soluble Inorganic Salts in Ambient Aerosol Particles in Tangshan Characterization of Water-soluble ions in PM _{2.5} at Dinghu Mount Characteristics of Mass Size Distributions of Water-Soluble Inorganic Ions During Summer and Winter Haze Days of Beijing Characteristics of Particles o	ZHAO Ya-nan, WANG Yue-si, WEN Tian-xue, et al. (1232) HUANG Yi-min, LIU Zi-rui, CHEN Hong, et al. (1236) YUN Hui, HE Ling-yan, HUANG Xiao-feng, et al. (1245) YI Zhi-gang, HUANG Xing-ran, BI Jun-qi, et al. (1252)
Simulation of Air Pollution Characteristics and Estimates of Environmental Capacity in Zibo City Diurnal Changes in Greenhouse Gases at Water-Air Interface of Xiangxi River in Autumn and Their Influencing Factors Influence of Human Activities on Groundwater Environment Based on Coefficient Variation Method Nitrogen Non-Point Source Pollution Identification Based on ArcSWAT in Changle River Study on the Content and Carbon Isotopic Composition of Water Dissolved Inorganic Carbon from Rivers Around Xi'an City First Flush Effects of Storm Events of Baoxiang River in Lake Dianchi Watershed	XUE Wen-bo, WANG Jin-nan, YANG Jin-tian, et al. (1264) HUANG Wen-min, ZHU Kong-xian, ZHAO Wei, et al. (1270) ZHAO Wei, LIN Jian, WANG Shu-fang, et al. (1277) DENG Ou-ping, SUN Si-yang, LÜ Jun (1284) GUO Wei, LI Xiang-zhong, LIU Wei-guo (1291) GUO Huai-cheng, XIANG Nan, ZHOU Feng, et al. (1298)
Estimation of Releasing Fluxes of Sediment Phosphorous in the Three Gorges Reservoir During Late Autumn and Early Winter Distributions and Pollution Status of Heavy Metals in the Suspended Particles of the Estuaries and Coastal Area of Eastern Hainan Environmental Characteristics of Heavy Metals in Surface Sediments from the Huanghe Estuary Distribution and Potential Ecological Risk Assessment of Heavy Metals in Sediments of Zhalong Wetland Ecological Risk Evaluation of Heavy Metals of the Typical Dredged Mud in Shanghai Pollution Characteristics of Heavy Metals in Sludge from Wastewater Treatment Plants and Sludge Disposal in Chinese Coastal Areas	XIN Cheng-lin, REN Jing-ling, ZHANG Gui-ling, et al. (1315)
Comparison of the Estrogenic Activity of Organic Compounds in Source Water and Finished Water from the Yangtze River and Taihu Occurrence and Fate of Phthalates in Wastewater Treatment Plants in Beijing, China Research on Sludge Toxicity Caused by DMF Biodegradation and Toxicity Spatial Distribution in Sludge Flocs	
Study on the Ecological Risk of Wild Veined Rapa Whelk (<i>Rapana venosa</i>) Exposured to Organotin Compounds in Bohai Bay, Chir A	ıa ·····
Bioaccumulation of Mercury in Crassostrea sp. Exposed to Waste Seawater Discharged from a Coal-fired Power Plant Equipped with	a Seawater Flue-gas Desulfuriaztion System ·····
Effects of Imidazolium Chloride Ionic Liquids on the Acute Toxicity and Weight of Earthworm	····· HUANG Ruo-nan, FAN Jun-jie, TU Hong-zhi, et al. (1380)
Influencing Factors and Mechanism of Arsenic Removal During the Aluminum Coagulation Process Removal of DON in Micro-polluted Raw Water by Coagulation and Adsorption Using Activated Carbon	····· CHEN Gui-xia, HU Cheng-zhi, ZHU Ling-feng, et al. (1386)
Mechanism of Catalytic Ozonation for the Degradation of Paracetamol by Activated Carbon Mechanism of Catalytic Ozonation for the Degradation of Paracetamol by Activated Carbon	WANG Is an DALO: show VII is at al. (1402)
Reductive Degradation of Chlorophenols in Aqueous Solution by Gamma Irradiation	WANG Jia-yu, DAI QI-znou, 10 Jie, et al. (1402)
Effect of C/N Ratio on Nitrite Accumulation During Denitrification Process	VIIAN Vi. HIIANG Yong DENG Hui-ping et al. (1416)
Nitrous Oxide Emission During Denitrification for Activated Sludge Acclimated with Methanol as the Organic Carbon	ZHAI Xiao-feng, IIANG Cheng-ai, WU Guang-xue, et al. (1421)
Comparison and Optimization of Cellulose Carbon Source for Denitrification Filter	
A Novel Municipal Wastewater Treating Process for Energy Production and Autotrophic Nitrogen Removal Based on ANAMMOX ····	
Modeling and Dynamic Simulation of the Multimode Anaerobic/Anoxic/Aerobic Wastewater Treatment Process	······ ZHOU Zhen, WU Zhi-chao, WANG Zhi-wei, et al. (1442)
Comparing Microbial Community of High Ammonia Wastewater and Municipal Sewage in a Partial Nitrification System	ZHAO Zhi-rui, MA Bin, ZHANG Shu-jun, et al. (1448)
Analysis of the Fractal Structure of Activated Sludge Flocs	RUAN Xiao-dong, LIU Jun-xin (1457)
Rapid Cultivation of Aerobic Nitrifying Granular Sludge with Alternate Loading Method	SHEN Na, YANG Chang-zhu, PU Wen-hong, et al. (1464)
Acceleration of the Formation of Aerobic Granules in SBR by Inoculating Different Proportions and Different Diameters of Mature Ae	robic Granules
Mechanisms of the Improvement in Dewaterability of Alkaline Fermented Sludge by Simultaneous Ammonium and Phosphate Recover	
Use of Flow Cytometric Sorting to Assess the Diversity of Eukaryotic Picophytoplankton of Lakes	
Allelopathy Effects of Ferulic Acid and Coumarin on Microcystis aeruginosa	GUO Ya-li FU Hai-van HUANG Guo-he et al. (1492)
Spatiotemporal Characteristics of Zooplankton Community Structure and Diversity in the Strong Temperature Increment Seawaters near	r Guohua Power Plant in Xiangshan Bay
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	ZHU Yi-feng, HUANG Jian-yi, LIN Xia, et al. (1498)
Screening of Epoxy-degrading Halophiles and Their Application in High-salt Wastewater Treatment	WANG Jin, XU Zhen, PENG Shu-chuan, et al. (1510)
Biodegradation of Decabromodiphenyl Ether by Intracellular Enzyme Obtained from Pseudomonas aeruginosa	
Influence of Yeast Extract on the Fermentation of Glucose by the Demulsifying Strain Alcaligenes sp. S-XJ-1	
Phylogenetic Analysis of Methanogenic Corn Stalk Degrading Microbial Communities	
Inhibition of Methanogenium by Erythromycin and Its Domestation	
Sand Box Study on Fingering Front Morphology for NAPLs Infiltrated in Homogeneous Porous Media Vertical Distribution and Possible Sources of Polycyclic Aromatic Hydrocarbon in Sewage Area Soil	
Characteristic and Evaluation of Soil Pollution by Heavy Metal in Different Functional Zones of Hohhot	
Distribution Characteristics of Rice Photosynthesized Carbon in Soil Aggregates of Different Size and Density	
Profile of Soil Microbial Biomass Carbon in Different Types of Subtropical Paddy Soils	
Effect of Composting Organic Fertilizer Supplies on Hexachlorobenzene Dechlorination in Paddy Soils	
Remediation of Cu-Pb-Contaminated Loess Soil by Leaching with Chelating Agent and Biosurfactant	
$ \hbox{ Effects of Different Temperatures Biochar on Adsorption of Pb(${\rm II}$) on Variable Charge Soils } \\$	
Preparation and Performance Investigation of Trichoderma viride-Modified Corn Stalk as Sorbent Materials for Oil Spills	
Removal of PO ₄ ³⁻ from Solution, Wastewater and Seawater by Modification and Granulation Magnesium and Aluminium Layered Do	•
Influence of Carboxylic Carbon Nanotube Supported Platinum Catalyst on Cathode Oxygen Reduction Performance of MFC	
Flue Gas Desulfurization by a Novel Biomass Activated Carbon	
Method for Grading Industrial Sectors in Energy Consumption and Its Application Dynamics and Environmental Load of Food Carbon Consumption During Urbanization; A Case Study of Xiamen City, China	
Dynamico and Entriormental Estat of Food Canson Consumption During Citianization; A Case Study of Mainen City, Chilla	1711, 231011, GOT SHEIR-HILL, LA GUI-HIL, et al. (1030)

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