

# 脉冲电晕放电降解 $\text{CH}_2\text{Cl}_2$ 的初步研究\*

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**摘要** 对高压脉冲电晕放电降解  $\text{CH}_2\text{Cl}_2$  (实验气体为空气中含有  $42.8 \mu\text{mol} \cdot \text{L}^{-1}$  的  $\text{CH}_2\text{Cl}_2$ ) 进行初步研究, 比较了正负脉冲电晕降解的活性, 正脉冲电晕优于负脉冲电晕。探讨了脉冲形成电容  $C_P$  之值及反应器的电晕线材料对降解反应活性的影响。为进一步提高室温下  $\text{CH}_2\text{Cl}_2$  的降解, 在反应器中加入  $\text{BaTiO}_3$  为催化剂, 在高压脉冲电场下,  $\text{BaTiO}_3$  受激产生局部电晕, 增强了电晕放电流柱, 提高了反应活性,  $\text{CH}_2\text{Cl}_2$  的转化率达 90% 以上。

**关键词** 脉冲电晕放电, 脉冲形成电容,  $\text{CH}_2\text{Cl}_2$  降解,  $\text{BaTiO}_3$ , 催化作用。

空气中挥发性有机物的治理方法一般有活性炭吸附, 焚烧和催化氧化等<sup>[1-3]</sup>, 但这些治理方法能耗大。近几年来, 一种用高压脉冲电晕放电的技术正在探索中<sup>[4,5]</sup>。本文报道用高压脉冲电晕放电降解低浓度  $\text{CH}_2\text{Cl}_2$  的研究结果, 探索一条能耗低、设备简单且效率高的有机废气治理途径, 同时对脉冲电晕放电与催化相结合的探讨具有理论研究意义。

## 1 实验部分

(1) 材料 含  $\text{CH}_2\text{Cl}_2$  浓度为  $42.8 \mu\text{mol} \cdot \text{L}^{-1}$  的空气, 由无锡气体公司提供。

(2) 装置 实验装置如图1所示。电源部分为 0—100kV 直流基压, 通过旋转火花间隙开关 RSG 和脉冲形成电容  $C_P$  产生脉冲, 反应器为直径 22mm 长 300mm 的不锈钢圆筒, 电晕线为 4mm × 4mm 的星形黄铜线和不锈钢棒。用 KIKUSVI 5100型示波器测试脉冲波形: 上升前沿 3—4ms, 脉宽 0.4ms, 重复频率 20—200Hz。与系统相连的气相色谱仪(上分厂制 1102型, 氢火焰检测器)分析测定。

(3) 步骤 待通过电晕反应器含  $\text{CH}_2\text{Cl}_2$  的反应气流用色谱检测有恒定的读数后, 开启直流高压电源, 通过旋转火花隙 RSG 和脉冲成形电容  $C_P$  产生尖脉冲, 输送至电晕反应器 RE, 直流电源 DC 可同时提供直流基压, 用气相色谱测定在不同功率下  $\text{CH}_2\text{Cl}_2$  的转化率。实验在

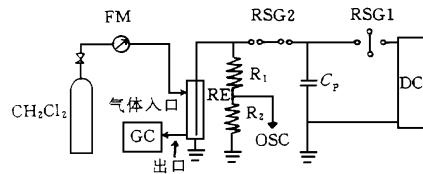


图1 实验装置简图

DC: 直流高压电源 RSG: 旋转火花隙  $C_P$ : 脉冲成形电容  
 $R_1$ : 限流电阻  $R_2$ : 分压电阻 OSC: 示波器 RE: 电晕反应器

常压与室温下进行。

## 2 实验结果和讨论

### 2.1 正负脉冲电晕对 $\text{CH}_2\text{Cl}_2$ 降解率的比较

分别用 2 台不同的直流电源产生正的和负的脉冲电晕放电, 实验气体流速相同, 电晕反应器采用黄铜棒作电晕线。图 2 给出了正、负脉冲电晕放电对  $\text{CH}_2\text{Cl}_2$  转化率的比较, 从图 2 中明显看出: 正脉冲电晕放电的降解率优于负脉冲。这可能因为正脉冲电晕流柱充满反应器的整个空间; 负脉冲的电晕流柱只局限于电晕线附近, 因而正脉冲电晕放电激活的空间大, 相应地  $\text{CH}_2\text{Cl}_2$  的降解率就较高, 以下的讨论均以正脉冲电晕为研究对象。

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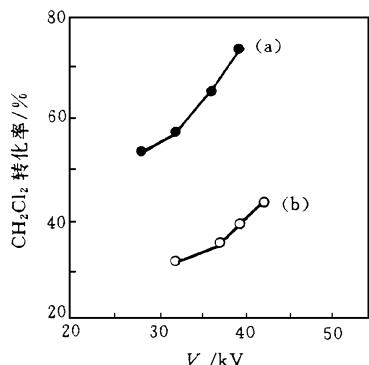


图2 正、负脉冲电晕放电降解 CH<sub>2</sub>Cl<sub>2</sub>的比较  
 (a) 正脉冲电晕放电 (b) 负脉冲电晕放电  
 (反应气流速 37 ml·min<sup>-1</sup>, 黄铜棒电晕线)

## 2.2 脉冲成形电容对 CH<sub>2</sub>Cl<sub>2</sub>降解率的影响

直流高压电源通过 RSG<sub>1</sub>给脉冲成形电容 C<sub>P</sub>充电, C<sub>P</sub>击穿 RSG<sub>2</sub>对反应器放电, C<sub>P</sub>值对 CH<sub>2</sub>Cl<sub>2</sub>降解率有显著的影响。图3给出了在同一反应器(不锈钢电晕线)中,不同值 C<sub>P</sub>对 CH<sub>2</sub>Cl<sub>2</sub>转化率的影响, C<sub>P</sub>值从  $1.8 \times 10^{-4}$  μF(即 180 pF)增大到  $5.0 \times 10^{-4}$  M F(500 pF)时, CH<sub>2</sub>Cl<sub>2</sub>的降解率随之降低。因为随着 C<sub>P</sub>值的增大脉宽增加,火花电压下降,对降解不利。但 C<sub>P</sub>值过小会影响输入能量的减少,同样不利于降解率的提高。本实验结果表明选用 180 pF 作为脉冲成形电容较合适。

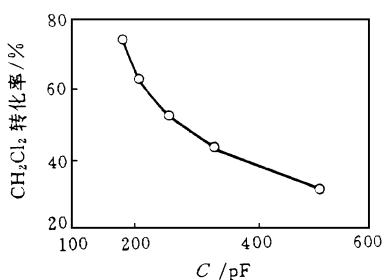


图3 CH<sub>2</sub>Cl<sub>2</sub>转化率随脉冲成形电容 C<sub>P</sub>值的变化  
 (功率 3.9 W; 实验气流速 25 ml·min<sup>-1</sup>)

## 2.3 电晕线材质不同对降解率的影响

发生脉冲电晕放电时,迁移率仅为电子 1% 的粒子(离子与原子等),在一个脉冲周期内来不及得到加速;而质量小迁移率大的电子却可

获得相当高的能量成为荷能电子(2–20 eV),这样,当脉冲宽度足够窄时,可以形成电子能量很高而其他粒子几乎不受影响的非平衡等离子体。这也是此种装置能耗低的理论依据。荷能电子与实验气体中的 CH<sub>2</sub>Cl<sub>2</sub>、O<sub>2</sub> 和 H<sub>2</sub>O 等碰撞,激活甚至电离这些气体分子,产生自由基(如 O<sup>·</sup>、OH<sup>·</sup> 等)活性物质,这些活性物质与激活了的 CH<sub>2</sub>Cl<sub>2</sub>发生反应,使降解反应能在室温下(常压)进行,总的反应可表示为:



实际发生的反应远不止此。

不同材质的2种电晕线(黄铜与不锈钢)对 CH<sub>2</sub>Cl<sub>2</sub>降解率的影响示于图4。从图4可看出:当实验条件相同下进行比较,黄铜棒为电晕反应器电晕线的降解活性明显高于不锈钢为电晕线的,如功率为 3.9 W,前者 CH<sub>2</sub>Cl<sub>2</sub>的转化率达 82%;而后者只达 66%。当高压脉冲电晕放电时,场能转化为化学能,产生荷能电子,而荷能电子的密度高低直接关系到其降解活性。黄铜电晕线与不锈钢电晕线,它们的材质不一样,结构不同,黄铜具有比不锈钢优良的导电性能,在黄铜中其自由电子密度高于不锈钢,因而用黄铜作电晕线时在高压脉冲电晕放电时产生的荷能电子密度要比不锈钢电晕线高得多,反应活性相应要强, CH<sub>2</sub>Cl<sub>2</sub>转化率就要高些。

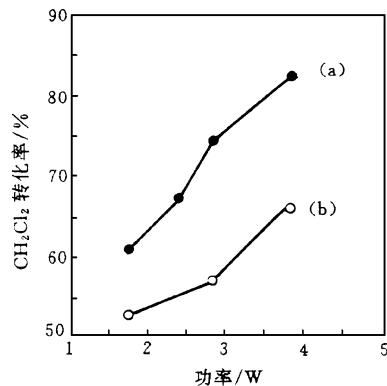


图4 反应器中不同电晕线对 CH<sub>2</sub>Cl<sub>2</sub>转化率的影响  
 (a) 方形(4mm × 4mm)黄铜电晕线  
 (b) 方形(4mm × 4mm)不锈钢电晕线  
 (实验气体流速为 28 ml·min<sup>-1</sup>)

此外,从图4还可以看到: CH<sub>2</sub>Cl<sub>2</sub>的转化率

随输入反应器的功率增加而提高, 这从另一个角度说明了使用导电性能优良的电晕线, 耗能少, 实际输入功率高, 降解反应活性就高.

## 2.4 BaTiO<sub>3</sub>对脉冲放电降解 CH<sub>2</sub>Cl<sub>2</sub>的影响

将一定量的颗粒状 BaTiO<sub>3</sub>催化剂加入到电晕反应器中, 床层高约为200mm. 开启电源前, 使实验气体与 BaTiO<sub>3</sub>颗粒间达到吸附平衡(需4—5h), 然后开始脉冲电晕放电降解反应.

图5给出了在室温下, BaTiO<sub>3</sub>的加入与否CH<sub>2</sub>Cl<sub>2</sub>转化率的对比. 从图5中可见, 反应器中加入了高介电常数(约5000)的 BaTiO<sub>3</sub>铁电体后, CH<sub>2</sub>Cl<sub>2</sub>的降解率有了明显提高, 如功率为3.9W时, 加入 BaTiO<sub>3</sub>后, CH<sub>2</sub>Cl<sub>2</sub>的转化率从原来的82%提高到93%, 本实验采用黄铜棒作电晕线.

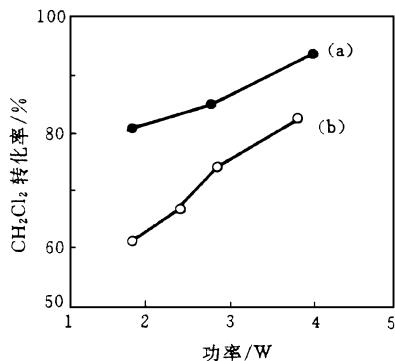


图5 BaTiO<sub>3</sub>对脉冲放电降解 CH<sub>2</sub>Cl<sub>2</sub>的影响  
(a) 加入了 BaTiO<sub>3</sub>颗粒 (b) 无 BaTiO<sub>3</sub>存在  
(黄铜棒为电晕线. 实验气体流速为 28ml•min<sup>-1</sup>)

文献[4]中, 把交流高压加在含铁电体 BaTiO<sub>3</sub>的反应器上, 借此产生电晕放电来降解有机废气, 此条件下电耗较大, 设备也比直流高压较为复杂. 本实验结果可能是由于 BaTiO<sub>3</sub>颗粒接触处发生了部分电晕放电, 增强了反应器内的电晕流柱, 使反应器内荷能电子与气体分

子碰撞机会增多, 产生的活性物质密度提高. 对于高介电常数的铁电体为催化剂, 在电晕条件下的催化行为正在作进一步的研究.

## 3 结论

(1) 正脉冲电晕放电降解 CH<sub>2</sub>Cl<sub>2</sub>的反应活性优于负脉冲电晕的反应活性.

(2) 选择脉冲成形电容适宜的值, 寻求与电晕反应器的良好匹配是提高反应活性的重要因素之一.

(3) 在高频电场作用下, 不同材料的电晕线对降解率有影响, 导电性能好的导体作电晕线对 CH<sub>2</sub>Cl<sub>2</sub>的降解有利.

(4) 电晕反应器中加入高介电常数的铁电体, 如 BaTiO<sub>3</sub>, 在高压脉冲电场下产生颗粒间接触处的部分电晕放电, 增强电晕流柱, 是提高降解反应活性的新途径.

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## 参 考 文 献

- Subbanan P, Green H L et al. Environ. Sci. Technol., 1988, **22**: 557
- Imamura S. Catalysis Today, 1992, **11**: 547
- Petrosius S, Drag o R et al. J. Am. Chem. Soc., 1993, **115**: 613
- Yamamoto T, Ramanathan K et al. IEEE Trans. Ind. Applicat., 1992, **28**(3): 528
- Masuda S, Hosokawa S et al. The International Conference on Applied Electrostatics. Beijing: 1993: 1-24
- Chakrabarti A, Mizuno A et al. IEEE Trans. Ind. Applicat., 1995, **31**(3): 500

## Groundwater Pollution near Waste Ash Ponds of Coal-fired Power Plant——A Case Study for F<sup>-</sup> Pollution in Paoche Ash Ponds of Xutang Power Plant, Jiangsu Province.

LiLi, Hai Huang (Dept. of Earth Sciences, Nanjing University, Nanjing 210093), Fahua Zhu (Nanjing Environmental Protection Research Institute for Electric Power, Nanjing 210031): *Chin. J. Environ. Sci.*, **18**(5), 1997, pp. 59—61  
A 2-dimensional pollutant transport model for groundwater pollution in the aquifer near ash ponds of Xutang Coal-fired Power Plant was established in this paper, and selecting F<sup>-</sup> as the simulating factor, the variations of groundwater hydraulic heads and F<sup>-</sup> concentration were simulated. At last, the polluted area and pollution degree of F<sup>-</sup> were predicted by the model. According to the simulating results, the model is reasonable, reliable and practicable. It provides a scientific method to predict the polluted area and pollution degree caused by the waste ash ponds.

**Key words:** groundwater pollution, pollutant transport model, numerical simulation, pollution prediction, coal-fired power plant.

## A Study of Pulsed Corona Discharges for Methlene Chloride Destruction.

Zheng Lei and Jiang Xuanzhen (Dept. of Chemistry, Zhejiang University, Hangzhou, 310027): *Chin. J. Environ. Sci.*, **18**(5), 1997, pp. 62—64

In this paper, High voltage pulsed corona Discharges has been used for destruction of methylene chloride with concentration of 42.8 μmol/L in air. Both positive and negative pulse generators were tested and found that the positive one can give much higher destruction efficiency than that on the negative one. The value of capacitors for pulse formation ( $C_p$ ) and the material of electrodes also influence the destruction efficiency. A packed bed corona reactor with 2—3 mm spherical BaTiO<sub>3</sub> pellets as a catalyst was used in this experiments. Enhancement of CH<sub>2</sub>Cl<sub>2</sub> destruction and the conversion of 90% were demonstrated. It may be attributed to the partial corona discharge induced by the contacted points between BaTiO<sub>3</sub> pellets, and then the density of corona was enhanced. The corona and catalyst combined technology gives a better destruction efficiency compared with that without BaTiO<sub>3</sub> catalyst.

**Key words:** pulse corona discharge, destruction, CH<sub>2</sub>Cl<sub>2</sub>, BaTiO<sub>3</sub>.

## Comparison of Effect for Removing Mutagens and Inorganic Ions in Tap Water by Reverse Osmosis and Nanofiltration.

Li Lingzhi (Dept. of Chem., Pingdingshan Teachers College, Henan, 467002), Zhou Rong and Wang Zhan-

sheng (Dept. of Environ. Eng., Tsinghua Uni., Beijing 100084): *Chin. J. Environ. Sci.*, **18**(5), 1997, pp. 65—67

In order to get superior drinking water, tap water was treated respectively by reverse osmosis (RO) and nanofiltration (NF) in the laboratory. The removal effects of mutagens and ions by RO and NF were compared. The Ames test results showed that both RO and NF could convert mutagenicity from positive to negative, while the ions removal effects of the RO and NF membranes are different, the removal rate of one-valence positive ions (Na<sup>+</sup>, K<sup>+</sup>) by NF is tenpercent lower than that by RO, the removal rate of two valence positive ions (Ca<sup>2+</sup>, Mg<sup>2+</sup>) is a little lower than that by RO. More ions which are beneficial to human health pass through nanofiltration membrane into drinking water.

**Key words:** reverse osmosis, nanofiltration, advanced water, mutagens, inorganic ions, Ames test.

## Study on Wet Desulphurization with Pyrolusite to Produce MnSO<sub>4</sub>·H<sub>2</sub>O in Smelting Plant.

Ning Ping, Sun Peishi et al. (Dept. of Environ. and Chem. Eng., Kunming University of Science and Technology, Kunming 650093): *Chin. J. Environ. Sci.*, **18**(5), 1997, pp. 68—70

An additional experiment, in which reduced pyrolusite(made in laboratory) is used as absorption agent in wet desulphurization to produce MnSO<sub>4</sub>·H<sub>2</sub>O, has been done in a foam tower at a smelting plant. Optimum conditions for both reduction of pyrolusite and absorption of SO<sub>2</sub> are obtained and pure of 95% MnSO<sub>4</sub>·H<sub>2</sub>O has been produced by primary crystallization of the absorption mother liquor.

**Key words:** sulfur dioxide, reduced pyrolusite, wet desulphurization, smelting gas, foam tower.

## Study on the Low Pressure Wet Catalytic Oxidation Treatment of High Concentration and Refractory Organic Wastewater.

Yang Run-chang, Zhou Shutian (Dept. of Environ. Eng., Dept. of chem. Eng. Xiangtan University, Xiangtan 411105): *Chin. J. Environ. Sci.*, **18**(5), 1997, pp. 71—74

Based on catalytic wet air oxidation and Fenton reagent, a new wet catalytic oxidation (LPWCO) method, which requires low pressure for the treatment of high concentration and refractory organic wastewater was studied. The method compared with general catalytic wet air oxidation, the pressure of the treatment is 0.1—0.6MPa, and the latter is 3.5—10M Pa. In addition, its temperature is