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基于碳减排目标与排放标准约束情景的火电大气污染物减排潜力 李辉,孙雪丽,庞博,朱法华,王圣,晏培



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水平潜流人工湿地对畜禽养殖废水中特征污染物的去除

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摘要: 为了探究水平潜流人工湿地去除畜禽养殖废水污染物的性能,选择养殖废水中常见的特征污染物抗生素——四环素 (tetracycline, TC)和重金属 Cu²⁺,构建模拟水平潜流人工湿地,设置空白处理(CK)、进水中外加 1 mg·L⁻¹四环素(TC)、进水 中外加 5 mg·L⁻¹ Cu²⁺(Cu)、进水中外加 1 mg·L⁻¹四环素和 5 mg·L⁻¹ Cu²⁺(TC + Cu) 这 4 组潜流人工湿地,考察人工湿地对 畜禽养殖废水中污染物的去除效果. 结果表明, CK 组湿地对养殖废水中总有机碳(total organic carbon, TOC)、总氮(total nitrogen,TN)、NH₄+N和 PO₄-P 的去除率分别为(84.3±7.2)%、(78.6±7.0)%、(82.1±4.4)%和(88.0±6.0)%,与 CK 组 相比, TC、Cu 和 TC + Cu 组湿地对 TN 的去除率分别下降了 0.4%~21.7%、2.8%~25.5% 和 4.3%~27.0%,对NH;+N的去除 率分别下降了 1.6%~15.7%、2.5%~17.8% 和 8.4%~23.0%,进水中添加 TC 或 Cu²+对湿地 TN 和NH₄+-N的去除有明显抑制 作用. TOC、TN、NH4*-N和 PO4*-P 等污染物的去除主要发生在湿地前端. TC、Cu 和 TC + Cu 组人工湿地对 TC 和 Cu²+的去除 率均分别在99.9% 和91.4%以上.4 组湿地出水中 11 种四环素抗性基因(tetracycline resistance genes, TRGs) 绝对丰度均显著 低于进水(低约2~3个数量级). CK 组湿地出水 tetA、tetC、tetE、tetO、tetQ、tetT 和 tetBp 基因相对丰度均显著低于进水,这7 种 TRGs 的去除率为43.3% (tetC) ~96.3% (tetA). 与 CK 组相比,进水中添加 TC 或 Cu²+ 使湿地出水中 TRGs 相对丰度有所升 高,TC、Cu 和 TC + Cu 组湿地出水中 TRGs 相对丰度分别比 CK 组高 12%~52%、6.7%~51% 和 24%~82%. 人工湿地对抗生 素、重金属和抗生素抗性基因有好的去除率,是一种适宜净化畜禽养殖废水的深度处理技术.

关键词:人工湿地;水平潜流;畜禽养殖废水;四环素;铜离子;四环素抗性基因

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Removal of Characteristic Pollutants in Livestock Wastewater by Horizontal Subsurface Flow Constructed Wetlands

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Abstract: To explore the removal efficiency of characteristic pollutants in livestock wastewater by horizontal subsurface flow constructed wetlands (CWs), this study selected tetracycline (TC) and Cu^{2,*}, a familiar antibiotic and a typical heavy metal in livestock wastewater, respectively, to build the following four groups of CWs; control (CK group), 1 $\text{mg} \cdot \text{L}^{-1}$ TC in influent (TC group), 5 $\text{mg} \cdot \text{L}^{-1}$ Cu²⁺ in influent (Cu group), and both 1 $\text{mg} \cdot \text{L}^{-1}$ TC and 5 $\text{mg} \cdot \text{L}^{-1}$ Cu²⁺ in influent ("TC + Cu" group). The average removal rates for control CWs were (84.3 ± 7.2)% for total organic carbon (TOC), (78.6 ± 7.0)% for total nitrogen (TN), (82.1 ± 4.4)% for ammonia nitrogen (NH₄+N), and (88.0±6.0)% for PO₄³⁻-P in a long-term operation. Compared with that in the CK group, the removal rate of TN in the TC group, Cu group, and "TC + Cu" group decreased by 0.4% - 21.7%, 2.8% - 25.5%, and 4.3% - 27.0%, respectively, and the removal rate of NH₄ - N decreased by 1.6% - 15.7%, 2.5% -17.8%, and 8.4%-23.0%, respectively. TC or Cu²⁺ in the influent significantly inhibited the removal of TN and NH₄+-N in livestock wastewater by CWs. The removal of TOC, TN, NH₄⁺-N, and PO₃⁻-P by the CWs mainly occurred in the front section of the CWs. The removal rates for TC and Cu²⁺ were above 99.9% and 91.4% in the effluent of both CWs treated with TC, Cu2+ respectively and CWs treated with TC and Cu2+. The results showed that influent had a higher abundance of 11 tet genes than effluent by approximately two to three orders of magnitude through all CWs, suggesting that the CWs may play a dominant role in antibiotic resistance genes (ARGs) and the bacteria removal process. The relative abundances of seven tet genes (tetA, tetC, tetE, tetO, tetQ, tetQ, tetQ) in effluent were lower than those in influent, and seven tet genes were reduced by 43.3% (tetC)-96.3% (tetA) in the CK. Compared to that in the CK, the addition of TC or Cu²⁺ to the influent increased the relative abundance of TRGs in the effluent of CWs. The relative abundances of TRGs in the effluent of the TC group, Cu group, and "TC + Cu" group were 12%-52%, 6.7%-51%, and 24%-82% higher, respectively, than that in the CK. These results suggest that CW is suited for livestock wastewater advanced treatment, as it provides great application prospects in the removal of antibiotics and heavy metals and the alleviation of the future risk of antibiotic resistance genes.

Key words; constructed wetlands; horizontal subsurface flow; livestock wastewater; tetracycline; Cu²⁺; tetracycline resistance genes

规模化畜禽养殖能够降低运营成本、方便管 理,逐渐成为我国畜禽养殖业的主体,但畜禽养殖所 带来的环境污染问题却不容忽视. 2020 年第二次全 国污染源普查显示[1],畜禽养殖业是我国农业源污 染物的主要来源, 2017 年畜禽养殖业水污染物 COD、NH₄⁺-N、总氮和总磷的排放量分别占农业源 污染物总量的 93.8%、51.3%、42.1% 和 56.5%.

养殖废水主要由畜禽尿液、部分残余粪便和饲

料残渣、圈舍冲洗水等组成,含有较高浓度有机污 染物、氨氮、磷以及悬浮物,并且伴有恶臭.目前多 采用厌氧生物、好氧生物或"厌氧-好氧"联合生物 处理技术去除养殖废水中的污染物. 杜龑等[2]的研

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究利用上流式厌氧污泥床(up-flow anaerobic sludge bed, UASB)-序批式活性污泥反应器(sequencing batch reactor, SBR)组合工艺处理畜禽养殖废水,该 工艺对 COD、NH4+-N和 TN 去除率分别达 90.87%、 98.65%和71.59%.文献[3]提高了养殖废水排放 标准,地方养殖废水标准和水环境质量标准(广东、 浙江、四川等)的制订进一步提升了当地养殖废水 排放标准或受纳水体的环境质量标准. 从养殖废水 稳定达标排放的强制要求和保障受纳水体生态系统 功能两方面,需要对经生物处理工艺后的出水,进一 步选用生态处理技术进行深度处理. 人工湿地具有 运行成本低、易于维护和具有景观效应的优点,可 与生物处理工艺配合作为养殖废水的深度处理工艺 进一步净化出水水质[4]. 普遍认为人工湿地利用基 质-微生物-植物生态系统的物理、化学和生物协同 作用,通过过滤、吸附、沉淀、离子交换、植物吸收 和微生物分解等多种途径实现对污水[5]包括养殖 废水[6~8]的高效净化.

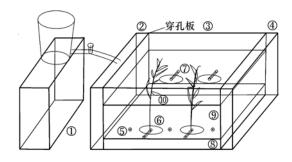
在畜禽养殖生产中,通常在动物饲料中添加抗 生素和重金属等具有杀菌、预防疾病和促生等作用 的药剂维持畜禽健康. 然而抗生素和重金属等物质 难以被畜禽吸收利用,有30%~70%的药剂以原药 或初级代谢物形式被排出动物体外[9],使得养殖废 水除了碳氮磷等常规污染物外,还含有多种抗生素 和重金属等污染物[10]. 养殖废水中抗生素种类繁 多,典型兽药如四环素类抗生素在废水中被频繁检 出,检出浓度可达 $\mu g \cdot L^{-1} \sim mg \cdot L^{-1[11\sim 13]}$,重金属如 Cu²⁺浓度则可达到mg·L⁻¹级别^[14]. 除这些污染物 外,因抗生素滥用所导致抗生素抗性基因(antibiotic resistance genes, ARGs)的潜在传播风险对生态环 境和人类健康有着更大的威胁,多种类型 ARGs 在 养殖废水中被检出,四环素抗性基因(tetracycline resistance genes, TRGs) 几乎有着最高的检出频 率[15]. 抗生素可通过抑制微生物功能基因表达,影 响污水生物处理设施的脱氮除磷功能[16], Chen 等[17]的研究表明在 2 mg·L-1和 5 mg·L-1TC 胁迫 下,SBR 系统的 TN 去除率由 80.2% 分别降至 69.2% 和 65.1%. 抗生素和重金属对 ARGs 在环境 中的行为特征有重要影响,Zhang等[18]的研究发现 在畜禽粪便厌氧消化过程中, Cu2+与抗生素存在共 选择作用,增加了 ARGs 丰度; Pal 等[19]的研究证 实,湿地进水中低浓度 Cu2+和 Zn2+对湿地土壤中 ARGs 种类和丰度有长期选择作用,而且 Cu2+的存 在增大了 ARGs 水平基因转移风险[20]. 人工湿地对 养殖废水中的抗生素和 ARGs 有较明显的去除效 果^[21], Li 等^[22]的研究发现人工湿地对养殖废水中

抗生素、ARGs 的平均去除率分别达 45.7% 和80.2%.然而有关畜禽养殖废水中抗生素和重金属复合污染对人工湿地去除碳氮磷和削减 ARGs 功能的综合影响却鲜见报道.因此本研究通过构造潜流人工湿地(人工湿地),针对实际养殖废水中的碳氮磷常规污染物以及抗生素、ARGs 和重金属等特征污染物,探究人工湿地对这些污染物的去除效果、去除特征以及可能的影响因素,评估人工湿地用于畜禽养殖废水深度处理和降低养殖废水排水中ARGs 传播风险的可行性.

1 材料与方法

1.1 水平潜流人工湿地的构建

本实验用水平潜流人工湿地为:长75.5 cm、宽 52.5 cm、高49 cm 的矩形结构,见图1.利用穿孔板 将湿地分为进水区、处理区和出水区这3个部分, 长度分别为8、59.5 和8 cm. 进水区前端设置高位 水池,通过阀门控制进水流速,出水区由底部向上间 隔 15 cm 设置 2 个 Ф15 mm 出水阀,用来调节人工 湿地水位和排出湿地出水. 湿地土壤取自福建省平 潭县稻田,碎石为本地建筑用碎石.湿地进、出水区 自上而下依次铺设30 cm 厚、粒径10~30 mm 的碎 石和 10 cm 厚、粒径 3~5 mm 的碎石. 处理区填料 层厚度为 40 cm; 上层(0~25 cm) 为土壤层, 中层 (25~30 cm) 为粒径 10~30 mm 碎石, 下层为粒径 (30~40 cm) 3~5 mm 碎石; 实验用芦苇采自附近 湿地,选取生长状况基本一致的芦苇移栽至湿地.在 湿地处理区一侧种植2株芦苇,芦苇种植密度为 10 株·m⁻², 芦苇栽种位置见图 2. 芦苇根系采用 300 目尼龙根袋包裹,湿地另一侧设置同样根袋,但根袋 内不种植芦苇,用根袋区分芦苇根际及非根际土壤. 分别在芦苇根际以及另一侧无植物的根袋内埋设电 极(ORP-33C, EA Instruments, UK), 监测芦苇根际 及非根际土壤氧化还原电位;在湿地处理区栽种植 物一侧, 距湿地底部 20 cm、沿池长布设 3 个土壤溶



① 高位水箱; ② 进水区; ③处理区; ④出水区; ⑤沿程采样点; ⑥根袋; ⑦电极; ⑧碎石层; ⑨土壤层; ⑩ 芦苇

图 1 人工湿地装置示意

Fig. 1 Schematic diagram of CWs

液采样器 (Rhizon CSS, Φ2.5 mm × 10 cm, Rhizosphere, Netherlands),采集沿程水样,采样点分别距进水穿孔板 8、30 和 52 cm,如图 2 所示.

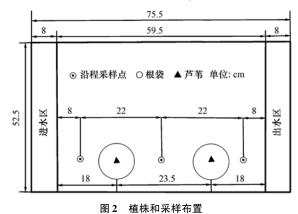


Fig. 2 Arrangement diagram of plants and sampling points

本实验用人工湿地有 4 组处理:空白处理即湿地进水为模拟养殖废水(CK);湿地进水中外源添加 1 $mg \cdot L^{-1}$ TC(TC 处理);湿地进水中外源添加 5 $mg \cdot L^{-1}$ Cu²⁺(Cu 处理);湿地进水中外源添加 1 $mg \cdot L^{-1}$ TC 和 5 $mg \cdot L^{-1}$ Cu²⁺(TC + Cu 处理),每组处理设置 2 个平行.湿地进水流量为 15 $L \cdot d^{-1}$,水力停留时间为 5 d.

1.2 进水水质

采用商品有机肥(主要原料为猪粪)浸出液配置模拟养殖废水,将有机肥和自来水按固液比1:40浸泡12 h 得浸出液,然后稀释浸出液,并添加葡萄糖、乙酸钠和氯化铵等碳、氮源,模拟养殖废水中碳、氮和磷污染物浓度. 本实验进水水质: $\rho(TOC)$ 为(133.3±62.2) mg·L⁻¹, $\rho(TN)$ 为(29.0±7.1) mg·L⁻¹, $\rho(NO_2^--N)$ 为(15.6±14.6) μg·L⁻¹, $\rho(NO_3^--N)$ 为(1.8±0.7) mg·L⁻¹, $\rho(PO_4^{3^-}-P)$ 为(26.6±11.9) mg·L⁻¹.

1.3 样品采集和测试分析

本实验期间,每周定期采集湿地进水、出水, TOC 采用总有机碳分析仪(multiN/C3100, Analytik Jena, Germany)测定; NH_4^+ -N采用纳氏试剂分光光度法(HJ 535-2009)测定, NO_2^- -N 采用 N-(1-萘基)-乙二胺分光光度法(GB 7493-87)测定, NO_3^- -N 采用紫外分光光度法(HJ/T 346-2007)测定,TN 采用碱性过硫酸钾紫外分光光度法(HJ 636-2012)测定; PO_4^{3-} -P采用钼酸铵分光光度法(HJ 670-2013)测定.参照 DeForest [23] 的分析方法,测定湿地土壤酶活性,包括磷酸酶、β-葡萄糖苷酶、β-纤维二糖甘酶、乙酰氨基葡萄糖苷酶、β-木糖苷酶、α-葡萄糖甘酶、亮氨酸氨肽酶、酚氧化酶和过氧化物酶;利用超高

效液相色谱串联质谱仪[Waters Acquity™ UPLC 串联 XevoTMTQ、WatersC₁₈色谱柱(100 mm×2.1 mm, 1.7 μm, Waters, USA)]测定水中 TC 浓度^[24];利用原子吸收分光光度计测定水中 Cu²⁺浓度.

1.4 TRGs 定量分析

分别采集各组湿地出水 0.5 L 于棕色玻璃瓶, 水样经 0.45 μm 玻璃纤维滤膜过滤后, 收集滤膜, 按照水样 DNA 提取试剂盒(Qiagen, Dneasy PowerWater Kit, USA) 说明提取 DNA. 采用微量分光 光度计(Thermo NanoDrop 2000c, USA)测定 DNA 浓 度(核酸纯度 A₂₆₀/A₂₈₀ > 1.8),将 DNA 样品保存于 -20℃冰箱.11 种 TRGs 分别为 tetA、tetC、tetE、 tetG, tetM, tetO, tetQ, tetW, tetT, tetBp π tetX, TRGs 及 16S rRNA 基因引物及退火温度见表 1. 使 用荧光定量 CFX96 仪 (CFX96Thermocycler Bio-Rad, USA) 对目标基因特异性扩增, 反应体系为 20 μL: SYBER 酶 10 μL, 上、下游引物各 0.4 μL, 模 板 DNA 2 μL, 无菌水 7.2 μL. 定量 PCR 反应程序 为:5℃预变性 5 min, 95℃ 30 s,退火温度 30 s, 72℃ 30 s, 35 个循环, 72℃ 5 min, 12℃ 1 min. 各 基因标准曲线相关系数 R2 均大于 0.99, 扩增效率 在90%~120%,符合定量 PCR 实验要求,可用于 各 TRGs 绝对丰度计算.

表 1 目标基因定量引物序列及退火温度

Table 1 Primer sequences and annealing temperature

for target genes of q-PCR 退火温度 目标基因 引物序列 文献 /°C. F: GCTACATCCTGCTTGCCTTC tetA60 [25] R: CATAGATCGCCGTGAAGAGG F: ACTACTGGGCTGCTTCCTAATG tetC58 [26] R:TCCTACGAGTTGCATGATAAA F: AAACCACATCCTCCATACGC [25] tetE55 R: AAATAGGCCACAACCGTCAG F:TTATCGCCGCCCCCTTC T tetG63 [26] R:TCATCCAGCCGTAACAGAAC F. ACAGAAAGCTTATTATATAAC tetM55 [27] R:TGGCGTGTCTATGATGTTCAC F: GATGGCATACAGGCACAGACC tetO58 [28] R:GCCCAACCTTTTGCTTCACTA F: AGAATCTGCTGTTTGCCAGTG 63 [27] tetO R: CGGAGTGTCAATGATATTGCA F: AAGGTTTATTATATAAAAGTG tetT46 [27] R: AGGTGTATCTATGATATTTAC F. GAGAGCCTGCTATATGCCAGC tetW60 [27] R: GGGCGTATCCACAATGTTAAC F: AAAACTTATTATATTATAGTG tetBp60 [27] R:TGGAGTATCAATAATATTCAC F: AGCCTTACCAATGGGTGTAAA [29] tetX60 R:TTCTTACCTTGGACATCCCG F:TGTGTAGCGGTGAAATGCG 16S rRNA 62 [30] $R_{\,:}\,CATCGTTTACGGCGTGGAC$

1.5 数据统计方法

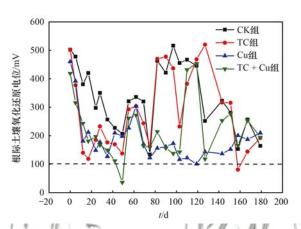
数据处理采用 Excel、Origin8.5 和 SPSS23 软件:污染物去除率计算公式:

 $\eta = (c_i - c_e)/c_i \times 100\%$ 式中, c_i 和 c_e 分别为进水和出水污染物浓度.

2 结果与讨论

2.1 人工湿地植物根际与非根际土壤的氧化还原 电位

土壤氧化还原电位(oxidation-reduction potential,ORP)用来反映土壤所处的氧化还原状态^[31].湿地运行期间芦苇根际及非根际土壤 ORP



值如图 3 所示. 在湿地未进水前各组湿地无论是根际土壤还是非根际土壤 ORP 值均在 400~600 mV 间,处于好氧状态^[32];人工湿地连续运行后,湿地内部处于淹水状态,非根际土壤 ORP 值逐渐降低,运行 17 d 后降低至 0 mV 以下,随后稳定在 - 100~0 mV 间,这种受淹水形成的还原状态利于微生物反硝化反应的进行;与非根际土壤不同,芦苇根系泌氧作用使根际土壤 ORP 值稳定在 100 mV 以上. 运行期间,各组人工湿地根际土壤 ORP 值始终高于非根际土壤. 湿地中厌氧、缺氧和好氧生境为硝化/反硝化细菌提供了良好生境,有利于微生物硝化和反硝化反应的进行,为湿地生物脱氮创造了条件.

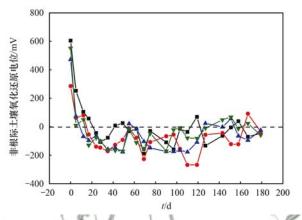


图 3 人工湿地植物根际和非根际土壤 ORP 值变化

Fig. 3 Variation in ORP in rhizosphere and non-rhizosphere soil in CWs

2.2 人工湿地对 TOC、NH₄⁺-N、TN 和PO₄³⁻-P的去除效果

自2020年5月起,人工湿地连续运行,各组湿 地对 TOC、NH₄⁺-N、TN 和PO₄³⁻-P的去除率如图 4. 模拟养殖废水经人工湿地处理后, CK、TC、Cu 和 TC + Cu 组湿地出水ρ(TOC)分别为 7.1~57、9.7~ 65、8.8~76 和 10.5~68 mg·L⁻¹,运行期间 4 组人 工湿地对 TOC 的去除率在 65%~93% 之间, CK 组 人工湿地对 TOC 的去除效率在70%以上,这表明人 工湿地对养殖废水中含碳有机物有良好的去除效 果. 人工湿地作为污水生态处理技术,对污染物的去 除性能受季节变化影响较大,从图 4 看出 TOC 去除 率在7月最高,可达85%~90%以上,进入11月后, TOC 去除率逐步下降至 70%.7 月是植物生长旺盛 期,南京11月的日均温度为8~16℃,芦苇开始枯 萎,12月的日均温度降至2~8℃,湿地中芦苇逐渐 衰败. 有研究表明,温度低于15℃,不利于微生物的 生长代谢[33],植物衰败和微生物活性降低,导致人 工湿地对 TOC 去除效率降低. CK、TC、Cu 和 TC + Cu 组出水 $\rho(PO_4^{3-}-P)$ 分别为 0.3~11、0.4~13、 0.5~12和0.2~16 mg·L⁻¹,运行初期4组人工湿 地对 PO_4^{3-} -P去除率可达 90% 以上,整个运行期间 PO_4^{3-} -P去除率稳定在 70% 以上. 通常认为湿地土壤、基质中含有大量 Ca^{2+} 、 Mg^{2+} 和 AI^{3+} 等离子,易与废水中的 PO_4^{3-} 结合生成磷酸钙和磷酸镁等吸附沉淀在土壤和基质中,这是人工湿地除磷的主要机制 $[^{134,35}]$.

CK、TC、Cu 和 TC + Cu 组 湿 地 出 水 $\rho(NH_4^+-N)$ 分别为 2.7~7.9、3.0~9.8、3.8~13.9 和 4.9~15.4 mg·L⁻¹, 出水 $\rho(TN)$ 分别为 2.6~9.8、4.4~20.3、5.3~17.7 和 7.3~21.5 mg·L⁻¹. CK 组湿地对 NH_4^+ -N的去除率可达到 74%~90%,对 TN 的去除率则在 77%~93%. 人工湿地主要通过微生物硝化-反硝化作用去除废水中的 $N^{[36,37]}$,Matheson 等 $[^{[38]}$ 的研究表明人工湿地通过微生物脱氮去除的 TN 占总去除率的 71%,湿地植物根系泌氧在潜流湿地内部形成的好氧-缺氧-厌氧交替微环境为硝化和反硝化细菌提供了适宜的氧生境. 湿地植物可吸收污水中的营养物质从而去除污染物,尉中伟等 $[^{[39]}$ 的研究表明湿地栽种芦苇可提高湿地脱氮率,芦苇地上部分氮吸收量占湿地脱氮量的 10.2%.

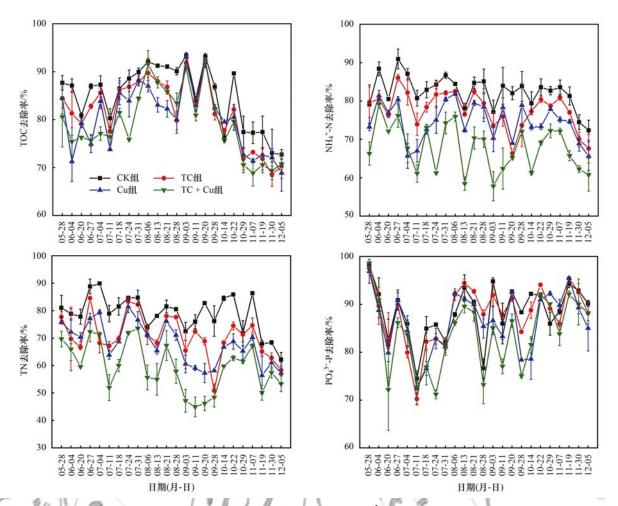


图 4 人工湿地对 TOC、NH₄⁺-N、TN 和PO₄³⁻-P的去除效果

Fig. 4 Removal efficiencies of TOC, NH₄⁺-N, TN, and PO₄³⁻-P of CWs

由图 4 可知,同一运行时间的湿地如 TC、Cu 和 TC + Cu 处理下的湿地对 TOC、 NH_4^+ -N和 TN 去除率均低于 CK 组.人工湿地运行初期,各组湿地对碳氮磷的去除率没有显著差异.运行 30 d 后,与 CK 组相比,进水中分别添加 TC 和 Cu^{2+} 使人工湿地对 NH_4^+ -N和 TN 的去除率显著降低,进水中添加 TC 处理使湿地对 NH_4^+ -N和 TN 去除率分别降低了 1.5%~16%和 0.4%~22%;进水中添加 Cu^{2+} 处理使湿地对 NH_4^+ -N和 TN 去除率降低了 2.8%~21%和 2.5%~25%; TC + Cu 组湿地对 NH_4^+ -N和 TN 的去除率分别下降了 8.3%~23%和 4.2%~37%.

各组湿地对碳氮磷去除率的差异可能与湿地土壤微生物受到 TC 和 Cu^{2+} 的持续胁迫有关. Cu^{2+} 通过影响土壤微生物的数量及酶活性影响土壤硝化作用和反硝化作用 $^{[40]}$. 不同处理下湿地的土壤酶活性见表 2,与 CK 相比, TC 和 Cu^{2+} 处理均使与碳代谢有关的土壤酶包括酚氧化酶、过氧化物酶、 α -葡萄糖甘酶、 β -葡萄糖苷酶、 β -纤维二糖甘酶和 β -木糖苷酶,与氮代谢有关的土壤酶包括乙酰氨基葡萄糖苷酶、亮氨酸氨肽酶以及与磷代谢有关的磷酸酶等

酶活性有所降低,其中酚氧化酶、β-纤维二糖甘酶、β-木糖苷酶、乙酰氨基葡萄糖苷酶、亮氨酸氨肽酶和磷酸酶等酶活性显著低于 CK(P < 0.05). 土壤酶活性与污染物去除率相关性见表 3,通过分析土壤酶活性与污染物去除率相关性,3组湿地 $PO_4^{3^-}$ -P去除率与磷酸酶活性均呈显著正相关(P < 0.05), TC组亮氨酸氨肽酶活性与 TN 去除率、Cu 组乙酰氨基葡萄糖苷酶活性与 NH_4^+ -N去除率相关系数分别为0.659 和 0.591. 乙酰氨基葡萄糖苷酶和亮氨酸氨肽酶均参与土壤氮代谢循环,湿地处理废水过程中,TC 和 Cu^{2^+} 由废水迁移并累积至湿地土壤和基质层,会影响湿地土壤微生物群落结构和土壤酶活性等,从而影响湿地对 NH_4^+ -N和 TN 的去除效果.

2.3 污染物浓度随湿地沿程的变化

人工湿地稳定运行后,分别在各组湿地进水区、处理区及出水区收集水样,分析碳氮磷等污染物的沿程变化,本实验数据取自 2020 年 10 月,如图 5. 各组人工湿地处理区前端时,TOC 和PO₄³⁻-P去除率分别可达 58%~94% 和 72%~90%. TOC 和PO₄³⁻-P随水流流经湿地浓度继续降低,但降低趋势趋于平缓.

表 2 不同处理对土壤酶活性的影响/nmol·(g·h)⁻¹

Table 2 Effect of different treatments on soil enzyme activities/nmol·(g·h) -1

土壤酶		处	理组	
工表問	CK	TC	Cu	TC + Cu
酚氧化酶	606. 3 ± 134. 6a	406.3 ± 169.1ab	443.8 ± 33.6ab	124. 3 ± 22. 2b
过氧化物酶	$2455.7\pm461.0a$	$1435.9 \pm 376.7a$	$2045.8 \pm 433.6a$	$1453.6 \pm 522.1a$
α-葡萄糖甘酶	$21.3 \pm 4.7a$	$16.1 \pm 2.4a$	11.9 ±4.6a	$15.0 \pm 3.6a$
3-葡萄糖苷酶	$94.5 \pm 4.8a$	$71.7 \pm 2.0a$	$80.0 \pm 10.4a$	$69.8 \pm 10.6a$
3-纤维二糖甘酶	$34.6 \pm 3.2a$	$26.0 \pm 0.4 ab$	$19.1 \pm 3.5 ab$	$23.6 \pm 5.8 \mathrm{b}$
3-木糖苷酶	$26.6 \pm 3.1a$	$14.3 \pm 5.4 ab$	$4.1 \pm 0.4 ab$	$14.6 \pm 7.6 $ b
乙酰氨基葡萄糖苷酶	$76.4 \pm 21.1a$	$16.3 \pm 2.2b$	$4.7 \pm 1.4 b$	$12.6 \pm 3.3b$
亮氨酸氨肽酶	$136.0 \pm 21.2a$	$80.6 \pm 14.4 \mathrm{b}$	$26.9 \pm 7.7b$	$33.5 \pm 14.8b$
磷酸酶	143.6 ± 11.1a	$89.6 \pm 19.1b$	$74.8 \pm 7.4 \mathrm{b}$	$87.9 \pm 12.2b$

¹⁾不同小写字母表示同种酶活性在不同处理下差异显著

表 3 土壤酶活性与污染物去除率相关性

Table 3 Correlation between soil enzyme activities and removal efficiencies of pollutants

处理组 项目 磷酸酶 β -葡萄糖 排售酶 β -纤维 二糖甘酶 乙酰氨基 葡萄糖苷酶 甘酶 α -葡萄糖 甘酶 完氨酸 氢肽酶 酚氧化酶 过氧化物酶 CK TOC 0.055 -0.013 0.436 -0.397 -0.413 0.016 0.435 -0.271 -0.021 MH $_4^+$ -N -0.643^* 0.360 0.630^* -0.028 -0.422 0.413 0.560 -0.321 -0.022 PO $_4^3$ -P 0.749^{***} -0.635^* -0.583^* -0.877^{***} -0.130 -0.678^* -0.468 0.005 -0.030 TOC 0.020 -0.045 -0.056 -0.638^* 0.067 -0.281 0.599^* -0.121 -0.044 TO 0.020 -0.045 -0.056 -0.638^* 0.067 -0.281 0.599^* -0.121 -0.044 TO 0.020 -0.045 -0.058 -0.067 -0.028 0.024 0.659^* -0.121 -0.044 TO 0.055 -0.490				-11-11-			1 1->-	-14-14-1-1-1			
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	处理组	项目	磷酸酶		•					酚氧化酶	过氧化物酶
$ \begin{array}{c} \text{CK} \\ \text{NH}_{4}^{+} - \text{N} \\ \text{O.} & -0.198 \\ \text{O.} & 360 \\ \text{O.} & 414 \\ \text{O.} & 460 \\ \text{O.} & 567 \\ \text{O.} & 0.18 \\ \text{O.} & 0.18 \\ \text{O.} & 0.413 \\ \text{O.} & 360 \\ \text{O.} & 386 \\ \text{O.} & 0.321 \\ \text{O.} & 0.077 \\ \text{O.} & 0.077 \\ \text{O.} & 0.077 \\ \text{O.} & 0.083^{\circ} - \text{O.} & 643^{\circ} \\ \text{O.} & 0.414 \\ \text{O.} & 0.460 \\ \text{O.} & 0.567 \\ \text{O.} & 0.583^{\circ} \\ \text{O.} & 0.877^{\circ\circ} \\ \text{O.} & 0.130 \\ \text{O.} & 0.678^{\circ} \\ \text{O.} & 0.468 \\ \text{O.} & 0.055 \\ \text{O.} & 0.030 \\ \text{O.} & 0.048 \\ \text{O.} & 0.055 \\ \text{O.} & 0.048 \\ \text{O.} & 0.056 \\ \text{O.} & 0.056 \\ \text{O.} & 0.068^{\circ} \\ \text{O.} & 0.067 \\ \text{O.} & 0.281 \\ \text{O.} & 0.599^{\circ} \\ \text{O.} & 0.121 \\ \text{O.} & 0.044 \\ \text{O.} & 0.044 \\ \text{O.} & 0.012 \\ \text{O.} & 0.044 \\ \text{O.} & 0.017 \\ \text{O.} & 0.042 \\ \text{O.} & 0.057^{\circ} \\ \text{O.} & 0.024 \\ \text{O.} & 0.024 \\ \text{O.} & 0.059^{\circ} \\ \text{O.} & 0.024 \\ \text{O.} & 0.029 \\ \text{O.} & 0.042 \\ \text{O.} & 0.041 \\ \text{O.} & 0.012 \\ \text{O.} & 0.053 \\ \text{O.} & 0.047 \\ \text{O.} & 0.042 \\ \text{O.} & 0.058 \\ \text{O.} & 0.012 \\ \text{O.} & 0.032 \\ \text{O.} & 0.072 \\ \text{O.} & 0.328 \\ \text{O.} & 0.078 \\ \text{O.} & 0.078 \\ \text{O.} & 0.048 \\ \text{O.} & 0.029 \\ \text{O.} & 0.042 \\ \text{O.} & 0.025 \\ \text{O.} & 0.042 \\ \text{O.} & 0.039 \\ \text{O.} & 0.041 \\ \text$				糖苷酶	裙T胟	匍匐裙甘鸭	甘胟	日胟	要	~	MP
$ \begin{array}{c} \text{CR} \\ \text{NH}_4^+ - \text{N} \\ \text{PO}_4^{3^-} - \text{P} \\ \text{O} \\ $		TOC	0.055	-0.013	0.436	-0.397	-0.413	0.016	0. 435	-0.271	-0.021
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	CK	TN	-0.198	0.360	0.630 *	-0.028	-0.422	0.413	0. 560	-0.321	-0.022
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	OK.	$\mathrm{NH_4^{+}}$ -N	-0.643 *	0.414	0.460	0. 567	0.018	0.460	0. 386	0.015	0.077
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$		PO ₄ P	0. 749 **	-0.635 *	-0.583*	-0. 877 **	-0.130	-0.678 *	-0.468	0.005	-0.030
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$		TOC	0. 020	-0.045	-0.056	-0.638*	0.067	-0.281	0. 599 *	-0.121	-0.044
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	TC	TN /	-0. 184	0. 314	0.017	-0.579 *	-0.108	0.024	0. 659 *	-0.420	-0.151
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$		NH ₄ -N	-0.340	0. 296	-0.047	-0. 422	-0.228	0. 220	0. 229	-0.024	-0.608*
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	61	PO ₄ P	0. 551	-0.492	-0.045	0. 175	0.112	-0.273	-0.319	0.601*	-0.041
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	7	TOC	0. 255	-0.087	0. 323	0. 476	0. 404			0. 183	0. 279
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	C.	TN	-0. 260	0.42	0. 265	-0.641 *	-0.058	-0.226	0. 483	-0.178	0. 137
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	C 3	NH ₄ -N	-0.627 *	0. 072	0.328	0. 591 *	-0.487	0. 186	0.452	0.341	0.301
TC + Cu	CRV	PO ₄ - P	0. 696 *	-0.490	-0.212	0. 078	0. 463	-0. 229	-0. 757 **	0.345	-0.316
TC + Cu NH ₄ ⁺ -N -0. 211 0. 267 -0. 224 0. 252 -0. 202 -0. 052 0. 229 0. 171 0. 185	100	TOC	0. 614 *	-0.344	0. 346	-0. 292	0. 382	-0.104	0.025	0.114	0. 370
NH_4^+ - N - 0. 211 0. 267 - 0. 224 0. 252 - 0. 202 - 0. 052 0. 229 0. 171 0. 185	TC 4 & 1	TN	0.012	0. 333	0. 105	- 0. 639 *	-0.016	-0.298	0. 427	-0.582*	-0.054
PO ₄ - P 0.653 * -0.684 * -0.064 0.386 0.296 -0.361 -0.786 ** 0.637 * -0.082	IG-F Gu	NH ₄ -N	-0.211	0. 267	-0.224	0. 252	-0.202	-0.052	0. 229	0.171	0. 185
	All	PO ₄ P	0. 653 *	-0.684 *	-0.064	0. 386	0. 296	-0.361	-0.786 **	0.637 *	-0.082

^{1)*}表示P<0.05, **表示P<0.01

与 TOC 和PO³⁻-P沿程变化情况类似,进水 $\rho(NH_4^+-N)$ 和 $\rho(TN)$ 经过处理区前端后均迅速降 低,各组湿地前端对NH₄+N去除率达57%~92%,对 TN 的去除率达 80%,湿地前端NH4+N和 TN 去除率 占到湿地总去除率的60%以上,甚至可达90%.总 体来看,湿地对NH₄ -N和 TN 的去除具有同步性. 不 同处理下,湿地沿程及出水 $\rho(NO_2^--N)$ 都较低,各组 湿地进水 ρ (NO₂-N)在 6.9 μ g·L⁻¹, 出水 $\rho(NO_2^--N)$ 在 4.8 ~ 7.9 μg·L⁻¹. $\rho(NO_3^--N)$ 除 CK 组在湿地前端由 3.5 mg·L⁻¹升高到 4.8 mg·L⁻¹, Cu 组在湿地前端由 3.5 mg·L-1 升高到 4.8 $mg \cdot L^{-1}$,其余组湿地水样中 $\rho(NO_3^- \cdot N)$ 沿程呈下降 趋势,出水 $\rho(NO_3^--N)$ 在1.2~1.6 mg·L⁻¹. 湿地进 水中氮主要以NH₄+N形式存在,湿地沿程和出水水 样中 $\rho(NO_2^--N)$ 和 $\rho(NO_3^--N)$ 较低,说明微生物的 硝化和反硝化过程较协调. 进水中的溶解氧和芦苇 根部泌氧为湿地前端土壤微生物提供了氧来源,废水中以 NH_4^+ -N为主的含氮污染物可被前端土壤中的硝化细菌等转化成 NO_2^- -N 和 NO_3^- -N,而人工湿地前端有机负荷高,为反硝化细菌提供了充足碳源,造成了水中 $\rho(TN)$ 和 $\rho(NH_4^+$ -N) 在湿地前端迅速下降.

2.4 人工湿地对 TC、Cu²⁺和 TRGs 的去除效果

湿地运行期间分别对进、出水中 ρ (TC)和 ρ (Cu²⁺)进行了测定,Cu组和TC+Cu组湿地Cu²⁺ 去除率见表 4. 实测进水 ρ (TC)约800 μ g·L⁻¹, ρ (Cu²⁺)约5~6 μ g·L⁻¹. 经人工湿地处理后,出水 μ (TC)降至0.028~0.309 μ g·L⁻¹(数据未显示), μ (Cu²⁺)降至0.034~1.4 μ g·L⁻¹,人工湿地对TC的去除率可以达到99%,对Cu²⁺的去除率维持在90%以上.人工湿地对抗生素的去除方式有基质吸附、植物吸收、微生物降解和水解转化.有研究表

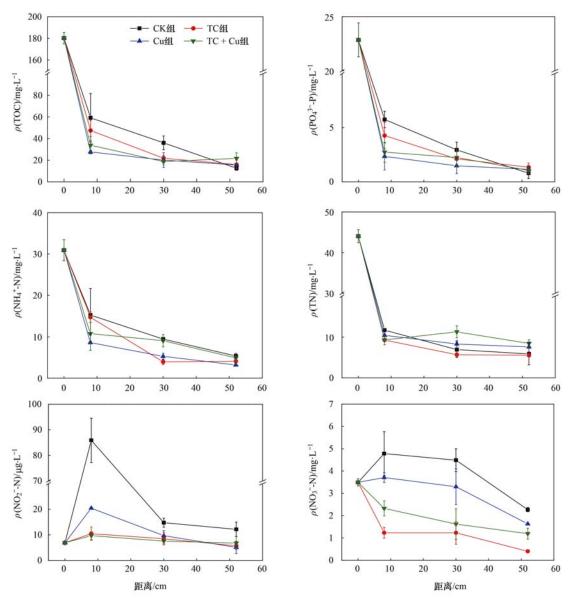


图 5 人工湿地污染物浓度沿程变化情况

Fig. 5 Contaminants concentration changes along the length of CWs

表 4 人工湿地对 Cu2+的去除率/%

Table 4 Removal efficiencies of Cu²⁺ by CWs/%

处理组	5 月	6月	7月	8月	9月	10 月	11 月
Cu	91.6 ± 0.8	91. 4 ± 2. 9	92. 8 ± 2. 2	97. 1 ± 0. 2	97. 0 ± 1. 6	94. 4 ± 0. 5	96. 7 ± 1. 9
TC + Cu	97.4 ± 3.7	98. 3 ± 2.4	94. 1 ± 2.5	96. 6 ± 0.4	98. 3 ± 0.2	96. 4 ± 0.5	97. 3 ± 1.4

明人工湿地对 TC 的去除率可达 85%~95%,这种高效去除主要通过湿地土壤、基质对 TC 的吸附截留来实现 $[^{41,42}]$. TC 可通过分子间作用力与土壤有机质表面吸附位点相结合,使 TC 被吸附在土壤中 $[^{43}]$,在 pH 近中性条件下,TC 可与多种金属阳离子生成不溶性螯合物. 人工湿地可通过化学沉淀、植物和微生物吸收等方式去除 Cu^{2+} ,湿地内部厌氧环境为硫酸盐还原成 S^{2-} 提供了有利条件, Cu^{2+} 与 S^{2-} 结合成低溶解性或不溶性沉淀可促使 Cu^{2+} 的去除 $[^{44}]$.

为评估人工湿地对废水中 TRGs 的去除效果, 分别对进水、出水 tetA、tetC、tetE、tetG、tetM、tetO、 tetQ、tetW、tetT、tetBp 和 tetX 等 11 种 TRGs 和 16S rRNA 基因做了定量检测,并计算各目标基因绝对 丰度.本实验数据取自 2020 年 10 月.

4 组人工湿地进、出水 TRGs 和 16S rRNA 基因绝对丰度 (lg) 变化如图 6. 进水 TRGs 绝对丰度在 $7.14 \times 10^6 \sim 4.55 \times 10^9$ copies·L⁻¹,不同抗性机制基因的绝对丰度有明显差异,编码四环素外排蛋白基因(tetA、tetC、tetE 和 tetG) 的绝对丰度 (7.48×10^8)

 \sim 4. 55×10^9 copies·L⁻¹) 高于编码核糖体保护蛋白基因(tetM、tetO、tetQ、tetBp、tetW 和 tetT) 的绝对丰度(7. $14 \times 10^6 \sim 2$. 15×10^8 copies·L⁻¹). 经湿地处理后,CK、TC、Cu 和 TC + Cu 组湿地出水 TRGs 绝对丰度分别为 9. $57 \times 10^3 \sim 8$. 35×10^6 、1. $13 \times 10^4 \sim 10^8$

 1.27×10^7 、 $8.57 \times 10^3 \sim 8.34 \times 10^6$ 和 $8.26 \times 10^3 \sim 1.83 \times 10^7$ copies·L⁻¹,出水 TRGs 和 16S rRNA 基因绝对丰度均显著低于进水(低约 2 ~ 3 个数量级),人工湿地对 TRGs 绝对丰度的去除率均在 99%以上.

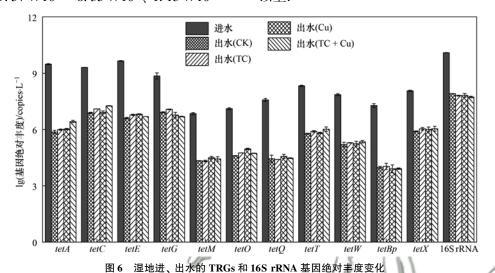
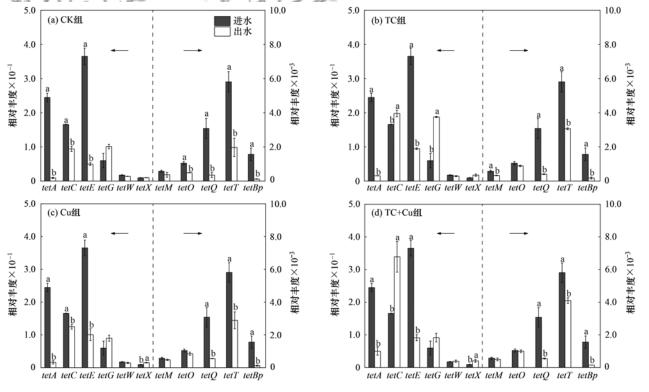


Fig. 6 Changes in absolute abundance of TRGs and 16S rRNA gene in influent or effluent of CWs

4 组人工湿地进、出水 TRGs 相对丰度变化如图 7. 进水 TRGs 相对丰度在 5.7×10^{-4} (tetM) ~ 3. 7 $\times 10^{-1}$ (tetE). CK 组湿地处理后出水 TRGs 相对丰度在 1.2×10^{-4} (tetBp) ~ 1.0×10^{-1} (tetG), 出水 tetA、tetC、tetE、tetO、tetQ、tetT 和 tetBp 基因相对丰

度显著低于进水 (P < 0.05), CK 组湿地对 7 种 TRGs 的去除率在 43.3% (tetC) ~ 96.3% (tetA) 之 间. 人工湿地对废水中 ARGs 有良好的去除效果, Liu 等 [45] 的研究利用人工湿地对养殖废水中 tetM、tetO 和 tetW 进行处理, 3 种基因的去除率均在 50%



不同小写字母表示进、出水基因相对丰度差异显著

图 7 湿地进、出水的 TRGs 相对丰度变化

Fig. 7 Changes in relative abundance of TRGs in influent or effluent of CWs

以上. 本实验结果表明人工湿地不仅可以有效降低废水中 TRGs 绝对丰度,对其相对丰度同样有良好的去除效果. 养殖废水在流经人工湿地时,湿地土壤可通过过滤截留等方式去除水体中的微生物达到去除 ARGs 的目的^[46], Chen 等^[47]的研究结果显示人工湿地可通过基质吸附截留有效去除废水中ARGs,去除率可达 50.0%~85.5%. Vacca 等^[48]的研究表明废水经人工湿地处理后出水总细菌数要比进水降低约 1.5~2 个数量级.

不同处理导致湿地出水 TRGs 相对丰度有所变 化. 可能受到 Cu^{2+} 和 TC 影响, TC 组湿地出水 tetC、 tetG 和 tetX 相对丰度要明显高于进水, 3 种 TRGs 相 对丰度分别比进水提高了 16.4%、90.4% 和 45.9%; TC + Cu 组湿地出水 tetC、tetG、tetW 和 tetX 基因丰度则比进水高出 51.2%、34.7%、11.1% 和 54.5%; TC、Cu 和 TC + Cu 组出水 TRGs 相对丰度 分别比 CK 组出水 TRGs 相对丰度高 12%~52%、 6.7%~51%和24%~82%.在污水处理系统中,出 水抗性基因丰度不仅与进水中抗性基因丰度有关, 同时也受进水抗生素浓度的影响^[49]. TRGs 丰度与 TC 浓度之间存在着明显正相关[50]. Huang 等[51]的 研究表明出水 TRGs 相对丰度会因进水 TC 浓度增 加而提高. 养殖废水中微量抗生素及铜、锌对 ARGs 赋存和进化存在共选择关系,会增加 ARGs 丰度和 种类^[52], Berg 等^[53]的研究表明由于 Cu²⁺对土壤中 微生物抗生素抗性的共选择作用,微生物群落对四 环素的抗性因土壤中 Cu2+含量的增加而提高. 废水 的持续流入,导致 TC 和 Cu2+累积在湿地土壤,长期 累积在土壤层中的 TC 和 Cu2+在共选择作用下会诱 导土壤中微生物抗性基因丰度增加,这可能导致处 理组出水部分 TRGs, 如 tetC、tetG 和 tetX 相对丰度 高于进水以及处理组出水 TRGs 相对丰度高于 CK.

3 结论

- (1)受植物根际泌氧影响,人工湿地植物根际 土壤 ORP 值在 100 mV 以上,而非根际土壤 ORP 值 在 0 mV 以下,植物根际与非根际土壤氧生境存在 明显差异.
- (2)与 CK 组相比,进水中添加 TC 或 Cu²⁺对湿地 TN 和NH₄⁺-N去除率有明显抑制; 4 组人工湿地对 TOC、TN、NH₄⁺-N和PO₄³⁻-P的去除主要发生在湿地前端; 湿地对 TC 和 Cu²⁺的去除率分别在 99.9%和 91.4%以上.
- (3)4组湿地对11种TRGs绝对丰度去除率均在99%以上;CK组湿地处理后出水tetA、tetC、tetE、tetO、tetQ、tetT和tetBp等基因相对丰度显著

低于进水;与 CK 组相比,进水中添加 TC 或 Cu^{2+} 使 TC 组出水 tetC 和 tetG, Cu 组出水 tetX 和 TC + Cu 组出水 tetC 和 tetX 相对丰度显著高于进水.

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