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2016 年 10 ~ 11 月期间北京市大气颗粒物污染特征与传输规律 张晗宇、程水潭、姚森、王晓琦、张俊峰(1999) 餐饮排放有机颗粒物的质量浓度、化学组成及排放因子特征 王红丽,景盛朝,乔利平(2010) 泰山顶(1 534 PM) 数9 冬季 PM。中元素浓度特征及其源分析 沈利娟、王红磊、银燕、陈髮、陈景华、施双双(2019) 郑州新乡冬季 PM。中元素浓度特征及其源分析 "月下,张朴真、黄海毒、高雅、张靖雯、宋鑫、张佳羽、李怀刚,曹治国、姜维韶、樊静、王跃思、金彩霞(2027) 我国 PM。浓度分阶段改善目标情景分析 贺晋瑜、燕丽、王彦超、雷宇、汪他颖(2036) 安阳市典型工业源 PM。排放特征及减排潜力估算 杜小申,燕丽、贺晋瑜、无地颖、王克、张瑞芹(2043) 郑州市典型工业炉窑细颗粒物排放特征及清单 起庆炎、韩土杰、张轶舜、杨留明、张瑞芹、燕启社(2052) 2015 年南京市城区挥发性有机物组成特征及大气反应活性 点天见、郭文讷、刘晓、陈凤、赵秋月,刘倩(2062) 兰州市化石燃料燃烧源排放 VOCs 的臭氧及二次有机气溶胶生成潜势 刘镇、朱玉凡、郭文讷、刘晓、陈瑗(2069) 12 种常见落叶果树 BVOCs 排放清单和排放特征 李双江、袁相洋、李琦、冯兆忠(2078) 我国典型陆地生态系统水位学离子特征及空间分布、黄丽、张心星、袁国富、朱治林、唐新斋、孙晓敏(2086) 我国典型区域地表水环境中抗生素污染现状及其生态风险评价 刘普、王曾、王字雷、李珍、杨超、厉思华、刘龙海(2016) 大连海域人海污染源中 PFASs 的赋存、输入通量和季节特征 陈虹、韩建波、张灿、程嘉增(2115) 干旱内陆河流域降水稳定同位素的时空特征及环境意义 袁瑞丰、李宗省、蔡玉琴、郑涛明(2122) 柳林泉域谷溶地像下水土至原面子特征及好境意义 袁瑞丰、李宗省、蔡玉琴、郑涛明(2122) 柳林泉域谷游地降水稳定同位素的时空特征及环境意义 袁瑞丰、李宗省、蔡玉琴、郑涛明(2123)三峡水库水体溶解磷与颗粒磷的输移转化特征分析 境景、清明、郑南、景、墨、郑靖、汉进和、张靖、李潜、汉地民(2150) 王峡水库水体溶解磷与颗粒磷的输移转化特征分析
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# 新型材料磁性氧化锆的除氟效能

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摘要:采用一步共沉淀法制备了磁铁矿纳米颗粒为核和水合氧化锆为壳的磁性氧化锆材料,研究了其除氟性能.结果表明,磁性氧化锆对氟的 Langmuir 最大吸附量为 35.46  $mg \cdot g^{-1}$ ,远高于磁铁矿、活性氧化铝和活性炭.磁性氧化锆对氟的吸附过程较快且吸附动力学数据符合准二级动力学模型,吸附过程为吸热反应.磁性氧化锆对氟的吸附量随 pH 升高而降低.  $Cl^{-1}$ 、 $NO_3^{-1}$  和  $SO_4^{-2}$  的共存对磁性氧化锆除氟没有明显影响,而  $HCO_3^{-1}$  和  $CO_3^{-2}$  明显抑制氟的吸附.磁性氧化锆吸附的氟可通过 1  $mol \cdot L^{-1}$  NaOH 成功脱附,脱附率  $99.5\% \sim 99.6\%$ . 脱附后的磁性氧化锆经过再生处理可继续使用.磁性氧化锆对实际井水中的氟的去除效果低于纯水,但适当增加投加量仍可以达到饮用水标准对氟浓度的要求.磁性氧化锆制备简单、使用后可从水中磁分离从而可反复使用,因此是一种有较好应用前景的除氟材料.

关键词:氟;吸附;磁性氧化锆;磁铁矿;水合氧化锆

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# Fluoride Removal Efficiency of Novel Material: Magnetite Core/Zirconia Shell Nanocomposite

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Abstract: Magnetite core/zirconia shell nanocomposite (abbreviated as  $Fe_3O_4@ZrO_2$  hereafter) was obtained using one-step coprecipitation method and its performance for removal of fluoride ion from water was studied. The results showed that the Langmuir maximum adsorption capacity of fluoride ion by  $Fe_3O_4@ZrO_2$  was 35. 46 mg·g<sup>-1</sup>, which was far higher than those of magnetite, activated alumina and activated carbon. Studies of adsorption kinetics indicated that the adsorption of fluoride ion by  $Fe_3O_4@ZrO_2$  was fast and could be well described by the pseudo-second-order model. The adsorption process of fluoride ion was an endothermic reaction. The adsorption of fluoride ion by  $Fe_3O_4@ZrO_2$  decreased with increasing pH. Chloride, nitrate and sulfate anions, which commonly coexist in drinking water, had little effect on  $F^-$  adsorption, although the coexistence of  $HCO_3^-$  and  $CO_3^2^-$  reduced the adsorption significantly by increasing the pH of the solution system. The fluoride adsorbed by  $Fe_3O_4@ZrO_2$  could be successfully desorbed with 1 mol·L<sup>-1</sup> NaOH solution as desorption agent. The desorption rate reached 99. 5% -99. 6%. The  $F^-$ -desorbed  $Fe_3O_4@ZrO_2$  could be reused for the removal of  $F^-$  after regeneration via restoring the protonation status of surface hydroxyl groups on hydrous zirconia. The removal efficiency of fluoride by  $Fe_3O_4@ZrO_2$  from actual well water was lower than that from pure water, but concentration limit for fluoride in drinking water could still be attained by increasing the dosage to a sufficiently high level.  $Fe_3O_4@ZrO_2$  is a promising material for fluoride removal due to its good performance, simple preparation method and easy separation from water by providing an external magnetic field.

Key words: fluoride; adsorption; magnetic zirconia; magnetite; hydrous zirconium oxide

氟是人体所必须的微量元素之一<sup>[1]</sup>. 但过量摄入氟会严重损害人体健康,引发骨质疏松症、关节炎、脑损伤等<sup>[2]</sup>. 我国生活饮用水卫生标准(GB 5749-2006)规定氟化物浓度不得超过1.0 mg·L<sup>-1</sup>. 有报道指出我国有近1亿人的饮用水中含氟量超过该标准<sup>[3]</sup>. 因此,含氟工业废水和氟超标饮用水的除氟处理已成为全球广泛关注的问题之一.

目前常用的除氟方法有沉淀法、膜分离法、离子交换法、吸附法、电凝聚法和电渗析法等<sup>[4~6]</sup>,但大部分技术在实际工程应用中仍很受限. 例如沉淀法、凝聚法等传统的处理方法很难将氟浓度削减到令人满意的水平,膜分离法和电化学法又成本较高<sup>[4~6]</sup>.

吸附法具有易于操作、成本较低、无二次副产

物产生等优点<sup>[1]</sup>. 但吸附法的技术优势取决于吸附剂的好坏. 因此, 氟吸附剂的研究是近年来的热点之一, 主要有金属氧化物<sup>[7-13]</sup>, 羟基磷灰石<sup>[3]</sup>、金属有机框架材料<sup>[14]</sup>等. 然而, 这些粉末态的吸附剂虽然除氟效果良好, 但使用后很难从水中分离回收. 为此, 人们近年来开始研究易于从水中分离回收和反复使用的氟吸附剂. 造粒是粉体吸附剂进行工程应用的传统方法, 这方面研究包括造粒羟基磷灰石<sup>[3]</sup>, 造粒水合氧化锆<sup>[15]</sup>和造粒无定形 Zr/Al 双

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氧化物等[16].另一个方法是将具有除氟能力的物质负载到传统树脂滤料表面,例如树脂基纳米钛锆氧化物[13]和水合氧化锆负载阴离子交换树脂[17]等.但总体来看,如何通过简单且低成本的方法制备易分离且除氟效果好的氟吸附剂仍面临着挑战.

磁性纳米颗粒吸附剂能以纳米粒子的形式使用,与水的接触面积达到最大化,且也具有使用后易于从水中磁分离从而可反复使用的优点.特别是无需固定床、不存在堵塞等问题,运行维护很方便,因而该技术用于水处理的研究近年来受到了较广泛的关注<sup>[18,19]</sup>.但用于除氟的磁性纳米颗粒吸附剂的研究却鲜见报道.

近年来,作者采用一步共沉淀的方法制备了以磁铁矿纳米颗粒为核和水合氧化锆为壳的磁性纳米颗粒吸附剂,已发现其可以用于水中含氧阴离子(磷)的吸附净化,效果良好<sup>[20~22]</sup>.该材料的制备方法简单、无需高温处理、无需除铁盐、锆盐和碱源(NaOH)之外的任何添加剂,只需控制合成条件即可一步得到,因而在生产成本上具备优势<sup>[20~22]</sup>.本研究的目的是分析该磁性吸附剂用于不含氧的阴离子(氟)的去除性能,以期为工业废水和饮用水的除氟处理提供一个新的技术选项.

#### 1 材料与方法

### 1.1 试剂

氯氧化锆  $(ZrOCl_2 \cdot 8H_2O)$  购自阿拉丁试剂公司,纯度 98%. 其它化学试剂  $FeCl_3 \cdot 6H_2O$ 、 $FeSO_4 \cdot 7H_2O$ 、 NaOH、 HCl、  $H_2SO_4$ 、 CH<sub>3</sub>COOH、 CH<sub>3</sub>COONa、 NaF、 NaCl、 Na<sub>2</sub>SO<sub>4</sub>、 NaNO<sub>3</sub>、 NaHCO<sub>3</sub>、Na<sub>2</sub>CO<sub>3</sub>、CH<sub>3</sub>OCH<sub>3</sub>、La(NO<sub>3</sub>)<sub>3</sub>·6H<sub>2</sub>O 和 氟试剂均为分析纯,购自国药集团化学试剂公司. 氟储备液采用 NaF 配制.

#### 1.2 材料的制备

磁性氧化锆的制备:采用本研究室研发的一步共沉淀法 $^{[20^{-22}]}$ .将 0.125 mol FeSO $_4$ ·7H $_2$ O,0.25 mol FeCl $_3$ ·6H $_2$ O 以及0.0938 mol 的 ZrOCl $_2$ ·8H $_2$ O 溶于 500 mL 双蒸水中.在搅拌条件下(300 r·min $^{-1}$ )用蠕动泵以 3 mL·min $^{-1}$ 的速度滴加 6 mol·L $^{-1}$ 的 NaOH 溶液直至终点 pH 7.6.随后在60℃的烘箱中老化处理 18 h.用双蒸水和酒精分别清洗 2 次,最后将该固体置于 45℃烘箱中烘干 24 h,经过 80 目筛筛分后保存在密闭容器中供后续实验使用.磁性氧化锆为核(磁铁矿)/壳(无定形水合氧化锆)结构,饱和磁化强度 23.65 emu·g $^{-1}$ ;比表面积 150.58 m $^2$ ·g $^{-1}$ ,具体表征结果见文献[20].

本研究按文献[20]还合成了不含锆的磁铁矿

纳米颗粒和不含铁的水合氧化锆,并从江苏某活性 氧化铝生产厂家购入了用于除氟的活性氧化铝产 品,从福建某活性炭生产厂家购入了水处理中常用 的活性炭产品.

#### 1.3 吸附实验

称取一定质量的材料于50 mL 锥形瓶中,加入40 mL 氟溶液,在一定温度的摇床内反应一定时间后磁分离,用氟试剂分光光度法<sup>[23]</sup>测定上清液中的氟浓度. 原氟溶液的 pH 在7~8 之间(随氟浓度的增加而增加). 但除 pH 影响实验和离子竞争实验外,所有吸附实验的 pH 均调节为6.5±0.5. 材料对溶液中氟的吸附量按下式计算:

$$Q_{\rm e} \; = \; \frac{\left(\; c_0 \; - \; c_{\rm e}\;\right) \; \times \; V}{m}$$

式中,  $Q_e$  为平衡吸附量 $(mg \cdot g^{-1})$ ;  $c_0$  和  $c_e$  为吸附前后溶液中的氟浓度 $(mg \cdot L^{-1})$ ; V 为氟溶液的体积(L); m 为吸附剂质量(g).

吸附等温线实验条件:材料质量 0.1 g; 氟浓度  $1 \sim 250 \text{ mg} \cdot \text{L}^{-1}$ ; 温度  $25 \, ^{\circ} \text{C}$ ; 时间 24 h.

吸附动力学实验条件:材料质量 0.1~g; 氟浓度  $50~mg \cdot L^{-1}$ ; 温度  $25~40~\pi~55$ °C; 时间 0.5~2~5~10~15~20~40~60~120~240~480~960~1~440 和 2~880~min. 采用压滤 $(0.45~\mu m)$ 方法快速分离.

pH 影响实验条件:材料质量 0.1 g; 氟浓度  $50 \text{ mg} \cdot \text{L}^{-1}$ ; pH  $3 \sim 11 (\text{用 } 0.1 \text{ 或 } 0.01 \text{ mol} \cdot \text{L}^{-1}$ 的盐酸或氢氧化钠溶液调节,文中报道的是反应结束后的平衡 pH);温度  $25 \, \text{C}$ ;时间 24 h.

离子竞争实验条件:材料质量 0.1 g; 氟质量浓度  $50 \text{ mg·L}^{-1}$  (但氟溶液中含竞争离子. 竞争离子的浓度均为氟浓度的 10 倍, 即  $11.90 \text{ mol·L}^{-1}$ ); 温度  $25 \text{ $\mathbb{C}$}$ ; 时间 24 h.

投加量实验条件:投加不同质量材料至 40 mL的氟溶液(分别采用去离子水和湖南长沙郊区某饮用水井的井水配制,氟浓度 50 mg·L<sup>-1</sup>)中,形成 0.375 ~7.5 g·L<sup>-1</sup>的投加量.温度 25℃,时间 24 h.井水的金属离子浓度用 ICP-AES 仪(ICAP 6000 Radial, Thermo)测定;除  $CO_3^{2-}$ 和  $HCO_3^{-}$ 外的阴离子浓度用离子色谱仪(METROHM, MICI)测定; $CO_3^{2-}$ 和  $HCO_3^{-}$ 用酸碱滴定法测定.

吸附-脱附-再生实验条件:称取 0.3 g 的材料放入 250 mL 锥形瓶中,加入浓度为 50 mg·L<sup>-1</sup>的氟溶液 120 mL,在 25℃的摇床内反应 24 h 后磁分离并测定上清液中氟的浓度.用去离子水清洗 1 次,然后加入浓度为 1 mol·L<sup>-1</sup>的 NaOH 溶液 120 mL,脱附 1 h 并磁分离后,再次测定上清液中氟浓度,计算脱附量和脱附率.为恢复吸附剂表面羟基的质子

化状态从而实现吸附剂的再生,用 pH 3.0 的盐酸溶液对材料进行清洗,直至 pH 达到 4.0(吸附前的磁性氧化锆/水悬浊液的 pH 为 4.0). 再生完成后开始新一轮的吸附-脱附-再生实验,共循环 4 次.

#### 2 结果与讨论

#### 2.1 吸附等温线

磁性氧化锆以及作为对比的磁铁矿、水合氧化锆、活性氧化铝和活性炭对氟的吸附等温线如图 1 所示. 将吸附等温线的数据用 Langmuir 和Freundlich 模型进行了拟合, 其模型分别表示如下:

$$\begin{aligned} \frac{c_{\mathrm{e}}}{Q_{\mathrm{e}}} &= \frac{c_{\mathrm{e}}}{Q_{\mathrm{max}}} + \frac{1}{K_{\mathrm{L}} \times Q_{\mathrm{max}}} \\ \mathrm{lg}Q_{\mathrm{e}} &= \frac{1}{n} \mathrm{lg}c_{\mathrm{e}} + \mathrm{lg}K_{\mathrm{F}} \end{aligned}$$

式中, $c_e$  为吸附平衡后氟浓度( $\operatorname{mg} \cdot \operatorname{L}^{-1}$ ); $Q_e$  为反应平衡时材料对氟的吸附量( $\operatorname{mg} \cdot \operatorname{g}^{-1}$ ); $Q_{\operatorname{max}}$ 是根据 Langmuir 方程计算出的最大吸附量( $\operatorname{mg} \cdot \operatorname{g}^{-1}$ ); $K_L$  是 Langmuir 常数( $\operatorname{L} \cdot \operatorname{mg}^{-1}$ ); $K_F$  是 Freundlich 常数 [( $\operatorname{mg} \cdot \operatorname{g}^{-1}$ )·( $\operatorname{mg} \cdot \operatorname{L}^{-1}$ )<sup>-1/n</sup>];1/n 为与吸附密度相关的常数.

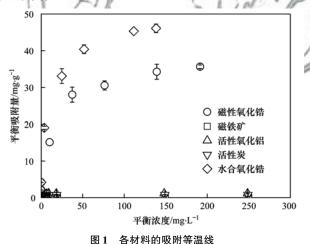


Fig. 1 Adsorption isotherms of several materials

磁性氧化锆和水合氧化锆的吸附等温线数据与两吸附模型的拟合结果见图 2 和表 1. 结果表明,磁性氧化锆和水合氧化锆的吸附等温线数据与Langmuir模型的拟合系数均高于 Freundlich 模型.但由于磁铁矿、活性氧化铝和活性炭对氟的吸附量

太小,难以用吸附模型进行拟合,故取实验中3种材料的实际最高吸附量作为氟最大吸附量,分别为:磁铁矿0.10 mg·g<sup>-1</sup>,活性氧化铝1.47 mg·g<sup>-1</sup>,活性炭0.91 mg·g<sup>-1</sup>.根据 Langmuir 模型计算的结果,磁性氧化锆对氟的最大吸附量为35.46 mg·g<sup>-1</sup>,远高于活性氧化铝和活性炭,也是磁铁矿(0.10 mg·g<sup>-1</sup>)的354.6倍.水合氧化锆对氟的最大吸附量为46.30 mg·g<sup>-1</sup>,高于磁性氧化锆,说明磁性氧化锆的吸附主体是位于外壳的无定形水合氧化锆、特别是在平衡浓度较低时磁性氧化锆的吸附等温线近乎呈现垂直形状,说明磁性氧化锆对浓度10 mg·L<sup>-1</sup>以下的氟的去除效果达到近100%.现国内大部分高氟地区的饮用水氟浓度在10 mg·L<sup>-1</sup>以下<sup>[24]</sup>,因此磁性氧化锆在饮用水深度达标处理中具有良好的应用前景.

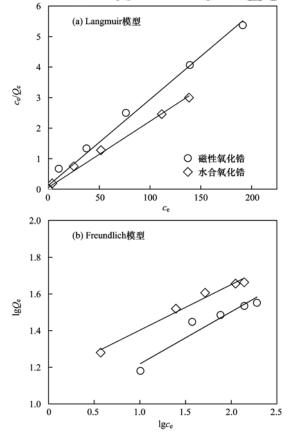


图 2 磁性氧化锆和水合氧化锆对氟的吸附 等温线数据与 2 种模型的拟合结果

Fig. 2 Fitting of the adsorption isotherms data to two kinds of equations for the adsorption of fluorine by  $Fe_3O_4 @ ZrO_2 \ and \ hydrous \ zirconium \ oxide$ 

#### 表 1 吸附等温线的拟合结果

Table 1 Fitting results of adsorption isotherms

材料	Langmuir 模型			Freundlich 模型			
171 AH	$Q_{ m max}/{ m mg}\cdot{ m g}^{-1}$	$K_{\rm L}/{ m L} \cdot { m mg}^{-1}$	$r^2$	$K_{\mathrm{F}}/(\mathrm{mg} \cdot \mathrm{g}^{-1}) \cdot (\mathrm{mg} \cdot \mathrm{L}^{-1})^{-1/n}$	n	$r^2$	
磁性氧化锆	35. 46	0. 222	0. 993 0	8. 59	3. 512	0. 915 6	
水合氧化锆	46. 30	0. 361	0. 995 0	14. 25	4. 018	0. 981 6	

表2列出了近年来国内外报道的一些粉体、造粒及以树脂为载体的吸附材料对氟的最大吸附量,可以看出磁性氧化锆是一种除氟性能良好的吸附材料.由于磁性氧化锆制备简单,且在实际应用过程中不存在固定床过滤处理中易出现的堵塞问题,因此具有较好的应用潜力.

#### 表 2 磁性氧化锆与其他吸附材料除氟能力的对比1)

Table 2 Comparison of fluorine adsorption capacities

of  $\mathrm{Fe_3O_4}$  @  $\mathrm{ZrO_2}$  with other adsorbents

of re <sub>3</sub> 0 <sub>4</sub> @ ZiO <sub>2</sub> with of	nor das	orbeine	
材料	pН	$Q_{\mathrm{max}}/\mathrm{mg}\cdot\mathrm{g}^{-1}$	文献
粒状羟基磷灰石	N. A.	7. 5	[3]
粉状羟基磷灰石	N. A.	15. 2	[3]
Ce-Fe 双氧化物	N. A.	60. 97	[7]
Mg-Al-Zr 三氧化物	7	22. 9	[8]
Ce-Zr 双氧化物	5.8	19. 5	[9]
Fe-Al-Ce 三氧化物	N. A.	2. 22	[10]
氧化铈(三种不同形状)	3.5	7.0 ~71.5	[12]
树脂基纳米钛锆氧化物	5.8	35. 1	[13]
MOF-801 金属有机框架材料	N. A.	38. 20 ~ 40. 26	[14]
粒状水合氧化锆	$3 \sim 4$	27. 72	[15]
粒状无定形 Zr/Al 双氧化物	7	65. 07	[16]
水合氧化锆负载阴离子交换树脂	6.5	20.9	[17]
无定形氧化铁	N. A.	60. 8	[19]
Mg-Al-Me 三氧化物(Me =La, Ce, Zr)	6	50. 89 ~ 54. 22	[25]
MgO/MgFe2O4 负载氧化石墨烯	6	34//	[26]
活性氧化铝	7	1.08	[27]
$\mathrm{Fe_3O_4} @~\mathrm{ZrO_2}$	6.5	35.46	本研究

1) N. A.: 文献中未提及

## 2.2 吸附动力学

磁性氧化锆对氟的吸附动力学实验结果如图 3 所示. 磁性氧化锆的氟吸附量随吸附时间增加先快速增加,后趋于平缓,24 h基本达到平衡. 吸附初

期磁性氧化锆表面和溶液之间的氟浓度差最大,吸附快速. 但随吸附时间增加,溶液氟浓度不断降低,磁性氧化锆表面的吸附位点逐渐达到饱和,吸附速率变慢且吸附量逐渐趋于稳定.

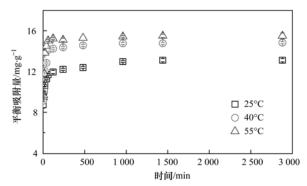


图 3 不同温度下磁性氧化锆的吸附动力学实验结果

Fig. 3 Adsorption kinetics of Fe<sub>3</sub>O<sub>4</sub>@ ZrO<sub>2</sub>

at different temperatures

将实验数据用准一级动力学和准二级动力学模型进行了拟合,结果见表 3. 两个模型的方程式分别如下:

$$\ln(Q_e - Q_t) = \ln Q_e - k_1 \times t$$

$$\frac{t}{Q_t} = \frac{1}{k_2 \times Q_e^2} + \frac{t}{Q_e}$$

式中, t 为反应时间(min);  $Q_e$  和  $Q_t$  为平衡时和时间为 t 时材料的氟吸附量(mg·g<sup>-1</sup>);  $k_1$  为准一级动力学常数(min<sup>-1</sup>);  $k_2$  为准二级动力学常数 [g·(mg·min)<sup>-1</sup>]. 拟合结果表明, 磁性氧化锆对氟的吸附动力学更加符合准二级动力学模型, 可以判断是一个化学吸附的过程<sup>[28]</sup>.

表 3 2 种动力学模型的拟合结果

Table 3 Fitting results of the two kinetic models

M E /00		准一级动力学模型	_	准	二级动力学模型	
温度/℃	$k_1/\min^{-1}$	$Q_{ m e}/{ m mg}\cdot{ m g}^{-1}$	$r^2$	$k_2/g \cdot (\text{mg} \cdot \text{min})^{-1}$	$Q_{ m e}/{ m mg}\cdot{ m g}^{-1}$	$r^2$
25	0.0022	13. 05	0. 928 4	0.011	13. 04	0. 999 8
40	0.0028	14. 84	0. 735 0	0.015	14. 84	1
55	0.0044	15. 49	0.6406	0.020	15. 50	1

为评价磁性氧化锆吸附氟的热力学性质, 计算了自由能变化  $(\Delta G^{\theta})$ 、焓变  $(\Delta H^{\theta})$  和熵变  $(\Delta S^{\theta})$ ,结果见表 4. 计算公式如下 $^{[29,30]}$ :

$$K_{\rm D} = \frac{Q_{\rm e}}{c_{\rm e}}$$
 
$$\Delta G^{\rm \theta} = -RT \ln K_{\rm D}$$

$$\Delta G^{\theta} = \Delta H^{\theta} - T \Delta S^{\theta}$$

式中,  $K_D$  为分配系数; R 为理想气体常数 8.314  $[J\cdot(\text{mol}\cdot K)^{-1}]$ ; T 为热力学温度(K);  $c_e$  为吸附平衡后的氟浓度 $(\text{mg}\cdot L^{-1})$ ;  $Q_e$  为吸附平衡后磁性氧化锆对氟的吸附量 $(\text{mg}\cdot g^{-1})$ .

计算结果表明, 焓变值  $\Delta H^{\theta}$  为 40.57 kJ·mol<sup>-1</sup>, 熵变值  $\Delta S^{\theta}$  为 179.67 J·(mol·K)<sup>-1</sup>.  $\Delta H^{\theta} > 0$  说明磁性氧化锆吸附氟的过程是吸热反应. 在 3 个温度下自由能变值  $\Delta G^{\theta}$  为 – 18.35 ~ – 12.97 kJ·mol<sup>-1</sup>,表明吸附过程属于自发过程.

表 4 磁性氧化锆吸附氟的热力学参数

Table 4 Thermodynamic parameters of fluoride adsorption by Fe<sub>3</sub>O<sub>4</sub>@ ZrO<sub>2</sub>

T/K	$\Delta G^{\theta}/\mathrm{kJ}\cdot\mathrm{mol}^{-1}$	$\Delta S^{\theta}/J \cdot (\bmod \cdot K)^{-1}$	$\Delta H^{\theta}/\mathrm{kJ}\cdot\mathrm{mol}^{-1}$
298	- 12. 97	179. 67	40. 57
313	- 15. 66	179. 67	40. 57
328	- 18. 35	179. 67	40. 57

#### 2.3 pH影响

如图 4 所示, 磁性氧化锆对氟的吸附量随着 pH 的上升而明显下降. 例如 pH 3 时吸附量为 20.61  $mg \cdot g^{-1}$ , 而当 pH 11 时吸附量仅为 0.88  $mg \cdot g^{-1}$ , 下降了约 23 倍. pH 在常规条件下一般为 6~7, 此时该材料的吸附量是 pH 3 时的 59.5% ~ 71.1%.

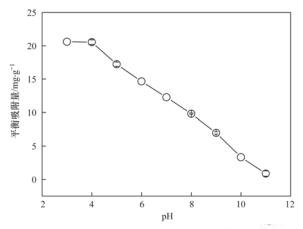


图 4 pH 对磁性氧化锆吸附除磷性能的影响

Fig. 4 Effect of pH on fluorine adsorption by Fe<sub>3</sub>O<sub>4</sub>@ ZrO<sub>2</sub>

pH 对磁性氧化锆吸附效果的影响可以用水合氧化锆吸附氟的机制来解释. 如 2.4 节所述, Cl<sup>-</sup>和 NO<sub>3</sub>·2 种阴离子不会影响水合氧化锆对氟的吸附. 前人的研究成果也证实了这点<sup>[31]</sup>. 因此, 属于物理吸附的静电引力作用不是水合氧化锆吸附氟的主要原因<sup>[32]</sup>. 推测水合氧化锆吸附氟更主要是一个化学吸附过程,表达如下<sup>[32]</sup>:

$$-Zr-OH_{(ads)} + F_{(aq)}^{-} \longrightarrow -Zr-F_{(ads)} + OH_{(aq)}^{-}$$

以上反应式可以解释酸性条件有利于磁性氧化 错吸附氟,而高 pH 会导致氟吸附能力的下降. 磁性氧化错吸附氟随 pH 上升而下降可解释为:①磁性氧化锆表面 Zeta 电位随 pH 上升而下降,甚至为负值<sup>[21,31]</sup>,不利于带负电的氟离子的吸附;②OH<sup>-</sup>对氟离子的竞争作用.

#### 2.4 离子竞争作用

实际饮用水中除了氟离子外,还存在大量的其他离子,它们可能会与氟离子发生竞争吸附.为了进一步探索磁性氧化锆在饮用水除氟中的应用前景,选择了饮用水中 5 种常见离子  $Cl^-$ 、 $NO_3^-$ 、 $SO_4^{2^-}$ 、 $CO_3^{2^-}$  和  $HCO_3^-$ ,研究了其对磁性氧化锆除氟的影响. 竞争离子的浓度为氟浓度的 10 倍,以便更好地了解竞争离子的影响. 由于 pH 也影响磁性氧化锆除氟,还测定了不同竞争离子共存下的最终 pH.

离子竞争的实验结果见图 5. 与纯水相比,  $Cl^-$ 、 $NO_3^-$  和  $SO_4^{2-}$  共存对 pH 影响很小, 因此这 3 种离子共存时产生的吸附差异可归因于离子本身的

影响, 而不是 pH 的作用. 由图 5 可以看出 Cl 和 NO; 对氟离子的吸附几乎无影响; SO<sub>4</sub> 的共存使 得磁性氧化锆对氟的吸附能力略有降低(幅度 4.2%); 而 HCO<sub>3</sub> 和 CO<sub>3</sub> 则会大幅降低磁性氧化 锆对氟的吸附性能(降低幅度分别为52.0%和 92.6%). Cl<sup>-</sup>、NO<sub>3</sub> 和 SO<sub>4</sub> - 共存对氟离子的吸附 影响结果体现了磁性氧化锆对氟离子的良好选择 性. SO<sub>4</sub> 对氟吸附的影响高于 Cl 和 NO<sub>3</sub> 可以解 释为 2 价的 SO<sub>4</sub><sup>2-</sup> 对氟的竞争强于 1 价的 Cl<sup>-</sup> 和 NO<sub>3</sub> - [33]. 由于加入 CO<sub>3</sub> - 和 HCO<sub>3</sub> 显著提高了反 应体系的 pH, 2 种离子共存对氟吸附的强烈影响既 来自2种离子本身, 也来自 pH 的作用. 由于相同 条件下  $CO_3^{2-}$  水解生成  $OH^-$  的能力强于  $HCO_3^-$ , 故 CO<sub>3</sub><sup>2</sup> 对 pH 的提高幅度大于 HCO<sub>3</sub>, 也更大程度上 降低了氟的吸附能力. 进一步的研究表明 pH 7.8 和 9. 9 时 (与 HCO; 和 CO; 共存时的 pH 相同但无  $HCO_3^-$ 和  $CO_3^{2-}$  共存, 因此反映 pH 的单独作用) 氟 吸附量下降 33.0% 和 77.3%, 说明 pH 确实是 HCO; 和 CO; 影响磁性氧化锆吸附氟的主要原 因. 但由于 pH 单独引起的下降幅度低于 pH 和  $HCO_3^-$ (或  $CO_3^{2-}$ )的总影响,说明  $HCO_3^-$ 和  $CO_3^2$ 身对氟吸附也有影响,而且其影响程度大于 Cl NO<sub>3</sub> 和 SO<sub>4</sub> -.

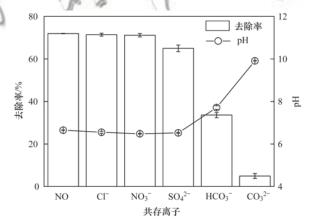


图 5 磁性氧化锆除氟的离子竞争实验结果

Fig. 5 Effect of competing anions on fluoride adsorption by Fe<sub>3</sub>O<sub>4</sub>@ ZrO<sub>2</sub>

#### 2.5 循环再生实验

为了验证磁性氧化锆是否可以反复使用,进行了循环再生实验,结果如图 6 所示. 从中可见随着循环次数的增加,磁性氧化锆的氟吸附量呈现缓慢降低的趋势,但变化幅度不大. 用永久钕铁硼磁铁可进行快速高效地磁分离,且使用 1 mol·L<sup>-1</sup> NaOH作为脱附剂时,脱附率达到了 99.5% ~ 99.6%,显示了磁性氧化锆的良好稳定性和在实际应用中可反复使用的潜力.

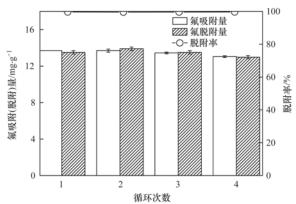


图 6 循环再生实验中氟在各循环中的吸附(脱附)量和脱附率

Fig. 6 Fluorine removal rate and desorption rate in each cycle of recycling study

#### 2.6 投加量实验

在实际应用中,吸附剂的投加量是一个重要的技术参数. 本研究考察了 0. 375 ~ 7.5 g·L<sup>-1</sup>投量下磁性氧化锆对 40 mL 浓度为 50 mg·L<sup>-1</sup> 的氟溶液 (纯水与井水配制)的吸附效果,结果见图 7. 为了解投加量的影响和纯水与井水的差异,所有实验的pH 均调至 6.5±0.28. 纯水配制的氟溶液中氟的去除率由 0.375 g·L<sup>-1</sup>投加量时的 28.0% 上升到了7.5 g·L<sup>-1</sup>投加量时的 100%,反应后的残余浓度由36.61 mg·L<sup>-1</sup>下降至 ~ 0 mg·L<sup>-1</sup>、即 7.5 g·L<sup>-1</sup>投加量时的残余氟浓度远低于我国生活饮用水卫生标准(GB 5749-2006)中规定的 1.0 mg·L<sup>-1</sup>. 这是由于投加量的增加可以提供更多的吸附位,从而改善净化效果. 在井水配制的氟溶液环境下,去除率由0.75 g·L<sup>-1</sup>投加量时的 22.1%上升到了 7.5 g·L<sup>-1</sup>投加量时的99.6%,反应后的残余浓度由38.43

mg·L-1下降至 0.20 mg·L-1, 依旧符合我国生活饮 用水卫生标准. 但与纯水配制的氟溶液相比, 相同 投加量下磁性氧化锆对井水配制的氟溶液中氟的去 除率和吸附量都有所下降. 以 0.75 g·L-1投加量为 例,去除率下降了26.9%,磁性氧化锆的吸附量下 降了29.0%. 常见离子浓度的测定结果见表5(但 还有其它未测成分,包括 Fe、Mn等). 可见井水中 含有各种溶解性物质, 这些已测和未测成分的共存 显然对氟的去除有一定影响. 但如图 7 所示, 适当 增加投加量可以提高磁性氧化锆去除实际饮用水中 的氟离子的效率,而且即使在初始浓度高达50 mg·L-1的情况下,采用适当高的投加量也可以达到 饮用水要求的氟浓度(1 mg·L<sup>-1</sup>以下). 因此磁性氧 化锆具备饮用水除氟的实际应用价值. 但需要指出 的是, 对于井水而言, 为获得对应于所需去除率的 投加量,实际工程应用时需要取得更多投加量条件 下的实验数据.

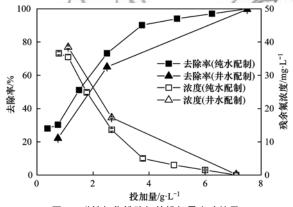


图 7 磁性氧化锆除氟的投加量实验结果

Fig. 7 Effect of Fe<sub>3</sub>O<sub>4</sub>@ ZrO<sub>2</sub> dosage on fluoride adsorption

表 5 井水中部分成分浓度测定结果

Table 5 Results of concentration of partial components in well water

			FF		
项目	浓度/mg·L-1	项目	浓度/mg·L-1	项目	浓度/mg·L-1
Li +	0. 373 8	$NO_2^-$	0. 291 9	As	< 0.03
Na +	6. 675 5	SO <sub>4</sub> -	4. 368 1	Cd	< 0.002
$\mathrm{NH_4}^+$	0. 111 5	$NO_3^-$	5. 979 0	Cr(VI)	< 0.004
K +	4. 344 3	$HCO_3^-$	0. 029	Hg	< 0.02
Mg <sup>2 +</sup>	0. 849 5	CO <sub>3</sub> <sup>2</sup> -	< 0.004	Pb	< 0.03
Mg <sup>2 +</sup> Ca <sup>2 +</sup>	2. 975 7	PO <sub>4</sub> -	0. 250 9	Se	< 0.06
Cl -	1. 482 0	·			

#### 3 结论

与磁铁矿相比,磁性氧化锆由于表面负载了水合氧化锆,对氟的吸附能力大幅度提高,饱和吸附量为 35. 46  $\text{mg}\cdot\text{g}^{-1}$ . 磁性氧化锆对低浓度氟具有很好的去除效果. 磁性氧化锆对水中氟的吸附速度较快,1 h 即可达到平衡吸附量的 82.0%. 其吸附机制为配位体交换,吸附过程属吸热反应. 磁性氧化锆对氟的吸附受 pH 影响明显,但  $\text{Cl}^-$ 、 $\text{NO}_3^-$  和  $\text{SO}_4^{2-}$  的共存未对氟形成明显的竞争作用. 吸附后

的磁性氧化锆经 1 mol·L<sup>-1</sup> NaOH 脱附并再生后可反复使用. 磁性氧化锆在实际井水中的去除效果良好,且可以通过适当提高投加量来达到饮用水标准对氟浓度的要求.

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