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高爽、白霉、白岩、雷团团、土刚、李时海、陆朝阳、七娜、郝明亮、黄同峰(1575) 2015~2017年北京及近周边平房燃煤散烃及其污染排放遥感测算 起文意、李令军、鹿海峰、姜磊、张立坤、王新辉、邱昀(1594) 基于地基遥感的杭州地区气溶胶光学特性 齐冰、车慧正、徐婷婷、杜荣光、胡德云、梁卓然、马千里、姚杰(1604) 四川省人为源挥发性有机物组分清单及其臭氧生成潜势 周子航、邓也、谭钦文、吴柯颖、宋丹林、黄凤霞、周小玲(1613) 餐饮源挥发性有机物组成及排放特征 高雅琴、王红丽、许睿哲、景盛翱、刘跃辉、彭亚荣(1627) 广州番禺大气成分站一次典型光化学污染过程 PAN 和 O3 分析 邹宇、邓雪娇、李菲、殷长秦(1634) 北京市典型道路扬尘化学组分特征及年际变化 胡月琪、李萌、颜起、张超(1645) 南昌市扬尘 PM、中多环芳烃的来源解析及健康风险评价 于瑞莲、郑权、刘贤荣、王珊珊、敖旭、张超(1646) 现实工况下挖掘机尾气排放特征分析 马帅、张凯山、王帆、庞凯莉、朱怡静、李臻、毛红梅、胡宝梅、杨锦锦、王斌(1670) 雾。罐天人体平均呼吸高度处不同粒径气溶胶的微生物特性 杨唐、韩云平、李珠、《敬(1688) 支持向量机回归在臭氧预报中的应用 苏筱倩、安俊琳、张玉欣、梁静舒、刘静达、王鑫(1697) 基于中国电网结构及一线典型城市车辆出行特征的 PHEV 二氧化碳排放分析 郝旭、王贺武、李伟峰、欧阳明高(1705) 岩溶槽谷区地下河硝酸盐来源及其环境效应:以重庆龙风槽谷地下河系统为例 标准,生工工建、吴韦、彭学义、刘九维(1715) 股州湾表层水体中邻苯二甲酸酯的污染特征和生态风险 刘成、孙翠竹、张哿、唐缭、邹亚丹、徐擎擎、李锋民(1726) 湛江湾沉积物中六六六(HCHs)、滴滴涕(DDTs)有机氯农药的分布特征与风险评估 张哿、唐缭、邹亚丹、徐擎擎、李锋民(1726) 湛江湾沉积物中六六六(HCHs)、滴滴涕(DDTs)有机氯农药的分布特征与风险评估 张哿、唐缭、邹亚丹、徐擎擎、李锋民(1726) 港位系化系统中,DOM 米偿特性及影响用表位任意、以为该准系表光,视镜明、陈法锦、于赤灵、李嘉诚、梁字钊、宋建中(1734)
内蒙古河套濯区不同盐碱程度土壤 CH。收収现律 物义柱,焦燕,物铭德,温息片(1950)水稻光合碳在植株-土壤系统中分配与稳定对施磷的响应 王莹莹,肖谋良,张昀,袁红朝,祝贞科,葛体达,吴金水,张广才,高晓丹(1957)土壤水分和温度对西南喀斯特棕色石灰土无机碳释放的影响 徐学池,黄媛,何寻阳,王桂红,苏以荣(1965)黄土丘陵区侵蚀坡面土壤微生物量碳时空动态及影响因素 覃乾,朱世硕,夏彬,赵允格,许明祥(1973)农用地土壤抗生素组成特征与积累规律 孔泉 是,张世文,爰起甲,胡青贵(1981)
  生物发酵制药 VOCs 与嗅味治理技术研究与发展 ··· 王东升,朱新梦,杨晓芳,焦茹媛,赵珊,宋荣娜,吕明晗,杨敏(1990)《环境科学》征订启事(1612) 《环境科学》征稿简则(1787) 信息(1663,1796,1833)
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赤铁矿抑制硫酸盐废水厌氧消化产甲烷过程中硫化氢 形成与机制

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摘要:为了实现高浓度硫酸盐废水厌氧消化过程中甲烷的高值化产出,本文探究了赤铁矿添加对硫酸盐废水厌氧消化系统中硫化氢形成的抑制效果与作用机制.以人工配制的硫酸盐废水为研究对象,考察不同赤铁矿投加量下高浓度硫酸盐废水的厌氧消化性能,并分析反应体系中硫元素的迁移转化途径.结果表明,未添加赤铁矿的反应器的厌氧消化启动时间及硫化氢浓度分别是 $0.5~{\rm g\cdot}(30~{\rm mL})^{-1}$ 赤铁矿添加组的 $1.64~{\rm fig}$ $1.64~{\rm$

关键词:硫酸盐废水; 厌氧消化; 赤铁矿; 硫化氢; 硫平衡

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Effect of Hematite on the Inhibition of Hydrogen Sulfide Formation and Its Mechanism During Anaerobic Digestion and Methanogenesis of Sulfate Wastewater

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Abstract: In order to achieve the high value production of methane, this paper investigated the effect and mechanism of hematite on the inhibitation of the formation of hydrogen sulfide during the anaerobic digestion of high-concentration sulfate wastewater. Different dosages of hematite were added to artificially prepared sulfate wastewater to analyze the migration and transformation pathways of sulfur in the reaction system. The results showed that the delay time of the anaerobic digestion process and the hydrogen sulfide concentration in the control reactor were 1.64 times and 180 times those in the reactor with the optimal hematite dosage of 0.5 g \cdot (30 mL)⁻¹, respectively. Thus, the addition of hematite effectively shortened the delay time and reduced the concentration of hydrogen sulfide. Dynamic equilibrium analysis of sulfur in different anaerobic digestion reactors showed that the solid sulfur content in the reactor accounted for 96.9% of the total sulfur. XPS results further demonstrated that hematite mainly enhanced the fixation of S²⁻ in the form of FeS₂. Therefore, the addition of hematite can effectively accelerate the anaerobic digestion of sulfate wastewater while reducing the concentration of hydrogen sulfide in the reactor.

Key words: sulfate wastewater; anaerobic digestion; hematite; hydrogen sulfide; sulfur balance

化工、制药、造纸、食品加工和采矿等领域在生产过程中会排放出大量富含高浓度硫酸盐的有机废水.这种废水中含有多种有毒有害物质,如病原体,新兴污染物和重金属等^[1],给生态环境和人类的健康造成了严重的威胁.因此,寻找一种合适的方法用于处理含高浓度硫酸盐的有机废水成为了近年来研究的重点.

厌氧消化技术具有处理过程中能耗低、处理效率高、产生清洁能源(甲烷)等优点,被广泛运用于废水处理^[2]. 但是将常规的厌氧消化技术运用于高浓度硫酸盐废水的处理具有一定的局限性. 首先,相比于二氧化碳还原产甲烷过程,硫酸盐还原过程具有一定的热力学及动力学的优势,这将导致硫酸盐还原反应比产甲烷反应更容易进行,从而影响产甲烷过程的效率^[3];其次,硫酸盐还原过程会产生

大量硫化氢等有毒气体,不但会影响厌氧消化系统中微生物的活性^[4],而且还会造成管道和设备的严重腐蚀^[5].所以抑制硫化氢的产生对于强化厌氧消化技术在高浓度硫酸盐废水处理中的应用尤为重要.近年来,不同的物理、化学和生物学方法被广泛用于抑制厌氧消化过程中硫化氢的形成.这些方法主要包括高压、超声波处理、添加硝酸盐、引入空气调节微好氧消化条件改变微生物群落结构等来降低反应器中硫化氢浓度^[6-8].但是这些方法不仅能耗高、价格昂贵,而且还可能影响产甲烷性能,

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从而限制其在商业上的推广运用. 因此,有必要寻找一种新的方法用于抑制厌氧消化过程中硫化氢的生成,并对其调控机制进行深入探究.

铁、铁化合物及铁氧化物作为参与产甲烷代谢活动的重要金属,被广泛运用于抑制硫化氢的产生. Su 等^[9]的研究结果显示,纳米零价铁在 250℃的条件下可以较好地将硫以硫化物或二硫化物的形式固定. Lin 等^[10]的研究结果发现,原位电化学合成纳米磁铁矿可以有效地抑制溶液中硫化物浓度,从而抑制硫化氢的产生. 张玲等^[11]的研究显示,FeCl₃ 添加对厌氧消化系统中 H_2S 的产生具有较强的抑制作用. 但是这些研究所涉及的工艺及操作条件较为复杂,且溶液中大量存在 Fe^{3+} 或 Fe^{2+} 会对产甲烷微生物产生毒害作用,而且并未深入分析硫元素的动态变化过程,不利于大规模地推广应用.

针对这些问题,本研究选取高浓度硫酸盐废水为研究对象,进一步探究赤铁矿的添加对硫酸盐废水厌氧消化过程中产甲烷性能、有机物的去除和硫化氢生成的影响,通过分析厌氧消化体系中各形态硫的动态转化过程,来探明赤铁矿抑制硫化氢生成的作用机制,以期为高浓度硫酸盐废水生物处理提供一定的理论基础及工程指导.

1 材料与方法

1.1 材料

本实验采用人工配制的硫酸盐废水,通过添加硫酸钾(K_2SO_4)使反应系统中硫酸盐(SO_4^{2-})浓度为500 $mg \cdot L^{-1}$. 以葡萄糖为底物提供碳源,硫酸盐废水中化学需氧量(COD)浓度为5000 $mg \cdot L^{-1}$, 其它营养物质(国药集团化学试剂有限公司, $mg \cdot L^{-1}$)包括: NH_4Cl 955, KH_2PO_4 85, K_2HPO_4 170, $NaHCO_3$ 3 750, $MgCl_2 \cdot 6H_2O$ 300, $CaCl_2$ 100, $CoCl_2$ 55, $NiCl_2 \cdot 6H_2O$ 80 和 $C_6H_5Na_3O_7 \cdot 2H_2O$ 278^[12]. 实验中接种泥取自福州市某污水处理厂,使用前,在 37℃的恒温条件下培养 7 d,确保菌的活性.接种泥的基本理化性质包括: pH 为 7. 56,氧化还原电位为 – 17. 00 mV,电导率为 5. 88 $mS \cdot cm^{-1}$,总固体含量(TS)为 3. 2%,挥发性固体含量(VS)为 1. 7%.

实验中使用的赤铁矿(Strem Chemicals, Inc, 美国)铁纯度为 99. 8%, 主要为 α -Fe $_2$ O $_3$. 赤铁矿的比表面积为 7. 27 $\mathrm{m}^2 \cdot \mathrm{g}^{-1}$, 孔体积 0. 017 $\mathrm{cm}^3 \cdot \mathrm{g}^{-1}$, 吸附平均孔隙直径为 9. 55 nm.

1.2 厌氧消化实验

在厌氧消化实验中,使用 100 mL 厌氧血清瓶作为反应器,分别添加 5 mL 接种泥和 25 mL 人工配制的废水.实验设置4个处理,分别添加 0、0.1、

0.5 和1.0 g 赤铁矿,为保证实验数据的有效性,每个处理设置多组平行用于实验样品的保存和监测.同时为了保证严格的厌氧条件,在血清瓶溶液和顶空中各通15 min 氮气,以确保完全排空空气,然后用橡胶塞将厌氧血清瓶瓶口塞紧,置于37℃恒温培养箱中培养24 d.每间隔2 d 测定反应器中甲烷和硫化氢的浓度变化.每间隔4 d 测定 pH、SCOD、TCOD、亚铁离子浓度、硫酸盐浓度、硫化物浓度、固体中硫的含量变化.

1.3 分析方法

甲烷和硫化氢浓度采用日本岛津公司的 GC-2014 测定,检测器分别为火焰离子化检测器(FID)和火焰光度检测器(FPD).硫酸盐浓度采用美国赛默飞世尔公司的 IC900 离子色谱进行测定,色谱分析柱型号为 AS23.淋洗液为 4.50 mmol·L⁻¹的碳酸钠和 0.8 mmol·L⁻¹碳酸氢钠的混合溶液,淋洗液流速为 1 mL·min⁻¹.硫化物浓度采用美国哈希公司型号为 2244500/22445-00 的硫化物试剂盒测定^[13].固体底物中硫元素含量采用德国艾力蒙塔公司的元素分析仪测定.

pH 采用 pH 计测定(PHSJ-3F), COD 浓度采用 APHA 水与废水监测方法测定^[14]. 亚铁离子浓度采用比色法测定^[15]. 物质成分采用日本岛津公司 XRD-6000 的 X 射线衍射仪测定,在 40 kV 和 30 mA 条件下,电子束轰击金属"靶"产生的 X 射线穿透一定厚度的赤铁矿检测其 X 射线衍射图谱,靶源是采用铜靶,扫描的范围是 5°~80°,扫速1(°)·min^{-1[16]}. 比表面积(Brunauer-Emmett-Teller)采用美国 TriStar II 3020 型比表面积分析仪测定.元素化学态分析采用美国赛默飞世尔公司的ESCALAB 250 X 射线光电子能谱仪测定^[17].

1.4 数据分析

测得的甲烷数据用修正的 Gompertz 模型进行计算拟合^[18]:

$$M = P \cdot \exp \left\{ - \exp \left[\frac{R_{\text{max}} \cdot e}{P} (\delta - t) + 1 \right] \right\}$$

式中, M 是甲烷累积产量(mmol); P 是最大产甲烷 潜能(mmol); R_{max} 是最大产甲烷速率(mmol·d⁻¹); δ 是延迟时间(d); t 是运行时间(d).

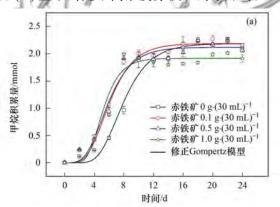
采用 Origin 9.0 软件进行数据处理,并利用 SPSS 20.0 软件进行统计学分析. 所有的实验均满足统计学分析要求,使用统计学中的 t 检验来分析数据,当 P < 0.05 认为具有显著相关性.

2 结果与讨论

2.1 赤铁矿添加对产生物气性能的影响 图 1(a)显示了不同赤铁矿添加量对厌氧消化

产甲烷过程的影响. 厌氧消化反应器中, 添加赤铁 矿后甲烷累积量在0~8 d 显著高于无赤铁矿添加 组. 在第8 d, 添加 0.1、0.5 和 1 g 赤铁矿的反应器 中甲烷累计量达到(1.85±0.05)、(1.92±0.01)和 (1.99 ± 0.02) mmol, 显著高于无赤铁矿添加组的 (0.97 ± 0.07) mmol. 这与 Liu^[19]和 Park 等^[20]的研 究结果相类似. 可能的原因是导电物质添加可以促 进厌氧消化反应器中微生物之间的种间直接电子传 递(direct interspecies electron transfer, DIET),加速 电子传递效率,改善产甲烷性能.此外,修正的 Gompertz 模型拟合结果显示,添加 0、0.1、0.5 和 1 g赤铁矿的反应器中的最大产甲烷速率分别是 0.33、0.36、0.35 和 0.45 mmol·d⁻¹, 产甲烷过程 的延迟时间分别是 4.6、3.0、2.8 和 3.1 d. 可能的 原因是铁氧化物添加有助于促进水解酸化的过程, 从而影响有机物的消耗和厌氧消化速率[21]. 需要 强调的是, 虽然 1 g 赤铁矿添加组的最大产甲烷速 率高于0、0.1和0.5g赤铁矿添加组,但是,经过 24 d 的反应后, 0、0.1 和 0.5 g 赤铁矿添加组中甲 烷积累量没有显著差异;此外,1g赤铁矿添加组 的甲烷积累量较无赤铁矿添加组降低了11.3%.这 可能是由于溶液中游离的三价铁随着赤铁矿的增加 而增加, 从而造成更多的 Fe(Ⅲ) 异养铁还原, 消耗 更多的电子, 进而影响产甲烷性能[22]

图 1(b)显示的是不同浓度赤铁矿的添加对厌



氧消化过程中硫化氢浓度变化的影响. 本研究表 明,赤铁矿添加能有效降低厌氧消化体系中硫化氢 的浓度. 在前6d,添加0.1、0.5和1g赤铁矿的反 应器中硫化氢浓度达到最大值,分别是(0.69 ± (0.07), (0.37 ± 0.00) $\pi(0.14 \pm 0.04)$ mg·L⁻¹, χ 后硫化氢浓度开始迅速下降, 在第8d后逐渐趋于 稳定, 最终约为 0.018 mg·L-1. 而对于无赤铁矿添 加组而言, 硫化氢浓度在第 12d 达到最大值(7.10 ±0.26 mg·L⁻¹),随后反应器中硫化氢浓度逐渐开 始下降, 最终达到一个稳定的浓度范围「(3.24 ± 0.21)~(3.38±0.04) mg·L⁻¹]. 反应结束后,未 添加赤铁矿的反应器中硫化氢浓度约是添加组的 180 倍. 赤铁矿的添加可以加速反应器中硫化氢生 成的同时抑制硫化氢的浓度, 这和 Zhou 等[23]的研 究结果相似. 添加赤铁矿的反应器在第6 d 后硫化 氢浓度开始逐渐下降,这可能原因是硫化氢和硫化 物之间存在动态平衡($S^{2-} + 2H^{+} \rightleftharpoons H, S$). 当赤铁 矿释放的三价铁被还原成二价铁离子时, 亚铁离子 能够与S2-形成沉淀物,从而抑制硫化氢的产生. 亚铁离子浓度变化也显示,在0~8 d,反应器中亚 铁离子浓度是先增加再降低的过程, 随着赤铁矿添 加量的增加, 在第4 d 时亚铁离子浓度达到最大 值,添加0.1、0.5和1g赤铁矿的反应器中亚铁离 子浓度比无赤铁矿添加组高 0.07、0.12 和 0.37 mg·L⁻¹, 随后亚铁离子浓度会快速下降.

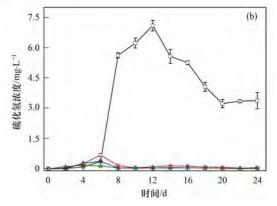


图 1 添加不同量赤铁矿对厌氧消化体系中产甲烷量和硫化氢浓度变化的影响

Fig. 1 Effects of hematite on the methane and hydrogen sulfide production in the anaerobic digestion system

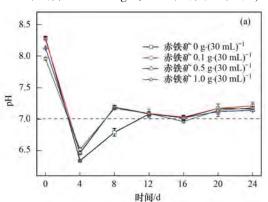
2.2 赤铁矿对厌氧消化系统 pH 和 SCOD 去除的 影响

pH 和 SCOD 是反映厌氧消化稳定运行的重要参数,也是影响厌氧消化过程的关键因素^[24]. 研究表明厌氧消化过程需要一个相对稳定的 pH 范围,产甲烷古菌最适合的 pH 范围是在 6.8 ~ 7.2^[25], 硫酸盐还原菌的最适合的 pH 是在 6.5 ~ 7.4^[26]. 图 2(a)显示厌氧消化过程中反应器中 pH 的变化过程,随着培养时间的变化,在第 4 d,所有处理的 pH 快速地

下降至 6.5 左右,这个结果和前人的研究结果相类似^[27],可能的原因是前期厌氧消化过程中水解的速度大于产氨的速度.也有研究表明^[28],厌氧消化前期有机酸的产量大于消耗量,所以会使 pH 下降.在第 4d 之后,反应器中 pH 开始逐渐上升,最终赤铁矿添加组 pH 保持在 6.96~7.21,而无赤铁矿添加组的 pH 则是在第 12 d 后才达到稳定状态.这可能是因为赤铁矿的添加使微生物、底物和赤铁矿三者的接触几率变大,加快反应器中微生物对有机物消耗,

进而加速反应器达到稳定的状态[29].

图 2(b)显示厌氧消化系统中 SCOD 的变化过程,反应器中 SCOD 先下降而后趋于稳定. 在第 8 d时,添加 0.1、0.5 和 1 g 赤铁矿的实验组 SCOD 的去除率分别是 89%、94%和 95%,显著高于对照的 48%. 有研究表明,铁氧化物作为导电物质的添加有助于促进厌氧消化系统中蛋白酶和葡萄苷酶的活性,因此加速了蛋白质和碳水化合物的分解,从而加快 SCOD 的去除^[30]. Meng 等^[31]的研究还发现,



亚铁离子存在会提高水解酸化酶的活性.根据实验结果显示,随着赤铁矿用量的增加,反应前期亚铁离子浓度在增加,所以可能会提高水解酸化酶活性促进 SCOD 的去除.但是需要强调的是,不同条件下 SCOD 的总去除效率并没有显著的差异.这和 Li 等^[32]的研究结果类似.他们发现导电碳纳米管 (carbon nanotube)的添加不影响厌氧消化过程 SCOD 的总去除率.可能的原因是反应后期大部分 SCOD 作为碳源已被消耗完(<0.2 g·L⁻¹).

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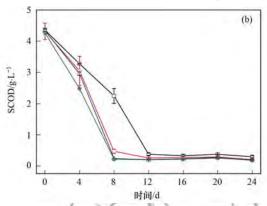


图 2 添加不同量赤铁矿对厌氧消化体系中 pH 和 SCOD 浓度变化的影响

Fig. 2 Effects of different amounts of hematite on the pH and SCOD concentration in the anaerobic digestion system

2.3 赤铁矿对硫迁移转化的影响

为了探究赤铁矿对高浓度硫酸盐废水厌氧消化 过程硫化氢产生的影响机制,对不同厌氧消化反应 器中硫的动态平衡进行了分析讨论. 厌氧消化过程 中硫元素主要是以固体、液体及气体这3种主要形 态存在. 固体中的硫元素主要是指"有机硫","单 质硫"及"难溶性固体硫化物/硫酸盐",统一用"固 体总硫"来表征:液体中的硫元素主要是指"可溶性 硫酸盐"及"可溶性硫化物";气体中的硫元素主要 是指"硫化氢". 厌氧消化过程中硫元素 3 种主要形 态之间的转化如图 3 所示. 此外, 由于仪器精度及 操作误差等因素的影响,反应过程中固液气三相还 存在一些无法准确测定的反应中间产物,如亚硫酸 盐等,用"其它"表示[33].通过分析图 4 不同赤铁矿 添加量下厌氧消化体系中各形态硫含量的变化发现, 随着反应的进行,在液相中,反应器中的硫酸盐被大 量消耗, 无赤铁矿添加组的硫酸盐在第8 d 有 67.6% 被消耗,添加0.1、0.5和1g赤铁矿反应器在第8d 时硫酸盐的消耗量比无赤铁矿添加组高23.9%、 31.3% 和 22.9%. 这和 Zhang 等^[34]的研究结果相似. 但是添加0.5g赤铁矿反应器硫酸盐还原率比添加1 g 赤铁矿反应器高 8.5%,可能的原因是过多的赤铁 矿添加到体系中会有更多的三价铁释放到溶液当中, 三价铁离子可作为电子受体与硫酸盐竞争电子,从 而影响厌氧体系中电子的再分配过程. 还有研究表

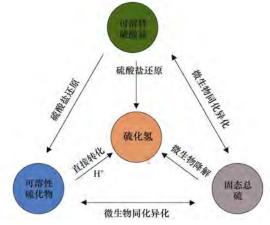


图 3 厌氧消化过程中硫的迁移转化途径

Fig. 3 Sulfur migration and transformation pathways during anaerobic digestion

明溶液中游离的三价铁含量过多会对硫酸盐还原过程中的关键酶——亚硫酸盐还原酶活性产生明显抑制,从而导致硫酸盐还原过程受影响^[35].此外,不同赤铁矿投加量对硫酸盐最终的还原量并没有显著影响. 厌氧消化体系中硫化物的变化趋势分析表明,在第 24 d 时无赤铁矿添加组的硫化物中的硫占总硫的 1.5%,而赤铁矿添加组中硫化物的浓度约等于 0,远远低于无赤铁矿添加组,也证明了赤铁矿添加有助于降低溶液中硫化物含量.

固相中,各反应器中固体硫含量在厌氧消化前4d降低了0.43~9.14 mg,这可能是由于接种泥中

的非可溶性的含硫蛋白质水解形成甲硫醇或者硫化氢,导致固体中的硫含量降低^[36]. 在反应结束后,未添加赤铁矿的对照组中固体硫含量占总硫的71.5%,而在添加0.1、0.5和1g赤铁矿的实验组分别占79.7%、96.9%和98.6%,赤铁矿添加组中的固体硫含量高于无赤铁矿添加组,这表明赤铁矿

添加有助于将硫元素固定.

气相中,在反应结束后,没有添加赤铁矿的气态硫占总硫的4.3%,而添加0.1、0.5和1g赤铁矿的实验组气相中硫占总硫的比例约等于0,这表明了赤铁矿的添加对抑制反应器中硫化氢浓度具有明显效果.

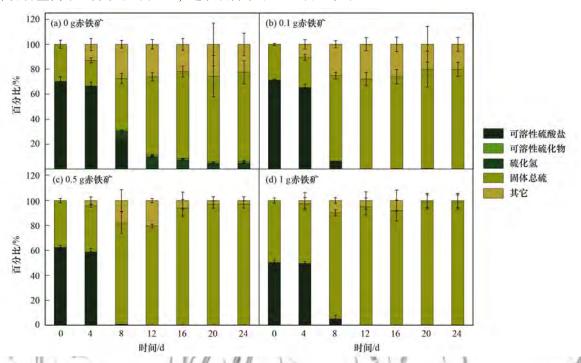


图 4 不同赤铁矿添加量下厌氧消化体系中各形态硫含量的变化

Fig. 4 Changes in the sulfur contents in the anaerobic digestion system with the addition of different amounts of hematite

2.4 赤铁矿抑制硫化氢产生的机制

赤铁矿添加有助于将硫化物固定,抑制硫化氢 的生成, 但是反应体系中沉淀物的化学形态尚不清 楚. 因为添加 0.5 g 赤铁矿对厌氧消化产甲烷性能 和硫化氢的抑制效果最佳, 所以本研究通过进一步 分析该实验组中固体底物的化学形态来分析硫化氢 的抑制机制. 通过图 5(a)和(b)添加赤铁矿的反应 器底物的 Fe 2p 和 S 2p 的 XPS 谱图分析发现, 原始 的 Fe 2p 谱图是由 6 条曲线拟合而成. 结合能 710.89 eV 和 725.77 eV 为 Fe₂O₃ 的特征峰^[37,38], 结合能为709.70、712.40和723.90 eV分别表示的 是 FeS₂、FeOOH 和 Fe₃O₄^[39,40,17]; 而 S 2p 谱图中在 163. 28 eV 是 S₂^{2-[37]} 特征峰, Fe 2p 中存在 FeS, 的 峰, 由此分析 S_{2p} 中硫化物的峰可能是与 Fe^{2+} 相 结合. 通过对比分析图 5(a) 和 5(b) 中两种元素的 谱图表明,添加赤铁矿的反应器硫化物可能主要以 黄铁矿(FeS,)的形式固定硫. 未添加赤铁矿的反应 器中 Fe 2p 和 S 2p 的 XPS 谱图如图 5(c) 和 5(d) 显 示. Fe 2p 的谱图中并未发现与 Fe^{2+} 形成化合物的 峰, 而 S_{2p} 谱图中 163. 59 eV 的峰被证实为 S_{n} (硫 单质)[35]. 综上分析表明, 添加赤铁矿的反应器中 亚铁离子可以有效地固定反应器中的硫化物,而未添加赤铁矿的反应器中亚铁离子的浓度较低,从而导致硫化物不能以黄铁矿的形式固定.

赤铁矿添加对厌氧消化硫化氢产生的抑制作用 的可能机制如图 6 所示. 反应器中有机物被微生物 分解产生的电子被溶液中的硫酸盐还原菌和产甲烷 古菌用于硫酸盐和二氧化碳的还原, 生成硫化物和 甲烷, 硫化物与溶液氢离子结合产生硫化氢等有毒 气体,溢出水面. 当反应器中添加赤铁矿,可以加 速电子的传递效率,促进硫酸盐的还原过程,同 时,在微生物的作用下,溶液中会发生Fe(Ⅲ)异养 铁还原过程,产生 Fe2+与溶液中的硫化物结合,产 生硫化亚铁沉淀,抑制硫化氢的产生. 但是硫化亚 铁并不是最稳定的矿物形态, 研究表明初始 FeS 是 一种亚稳定矿物, 当环境中存在多硫化物、硫元素 等氧化剂时, FeS 会逐步转化成较稳定的黄铁 矿[41]. 与添加赤铁矿的硫酸盐去除机制不同, 厌氧 消化体系中存在丰度较高的硫酸盐还原菌, 这些硫 酸盐还原菌会将 SO_4^{2-} 还原成 $S^{2-[11]}$, 在未添加赤 铁矿的反应器中,这些 S^{2-} 不能被亚铁离子固定, 从而导致其与溶液中的 H+结合生成 H₂S 气体溢出

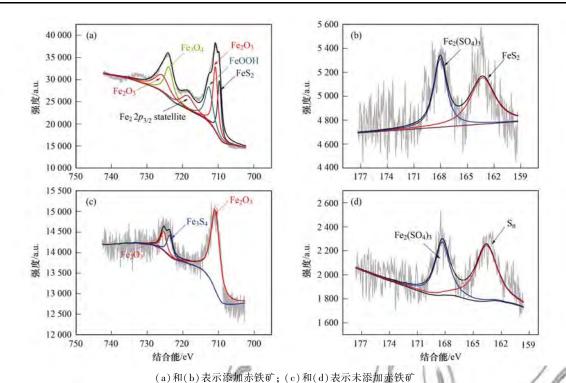


图 5 厌氧消化反应器中底物中 Fe 2p 和 S 2p 的 XPS 谱图 Fig. 5 XPS spectra of Fe 2p and S 2p in residues in the anaerobic digestion system

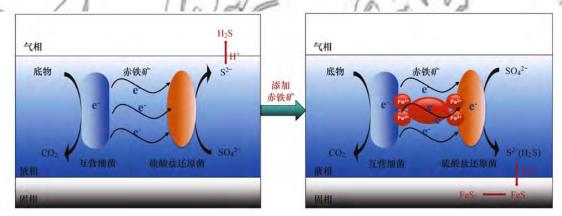


图 6 厌氧消化体系中抑制硫化氢产生的机制

Fig. 6 Mechanism of the inhibition of hydrogen sulfide generation in anaerobic digestion

水面, 进而导致大量 H₂S 的生成.

3 结论

本研究结果表明,未添加赤铁矿的反应器的厌氧消化启动时间及硫化氢浓度分别是 0.5 g·(30 mL)⁻¹赤铁矿添加组的 1.64 倍及 180 倍. 这说明赤铁矿的添加不仅缩短了高浓度硫酸盐废水厌氧消化过程延迟时间,提高有机物的消耗速率,而且能够有效地抑制硫化氢的生成. 硫元素的动态平衡及 XPS 谱图分析进一步表明,赤铁矿的作用机制主要是使 S²⁻以 FeS₂ 的固体形式固定,从而有效降低反应器中硫化氢的浓度.

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