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进水氨氮浓度对生物除磷颗粒系统的影响

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摘要:在 SBR 反应器中接种成熟的生物除磷颗粒,通过分阶段提高进水中氨氮浓度,研究了进水氨氮浓度对生物除磷颗粒系统的影响,确定系统对进水氨氮负荷的承受能力.结果表明,进水氨氮浓度低于 45 mg·L⁻¹时,生物除磷颗粒系统具有良好的性能,TP 去除率在 96%以上,COD 去除率在 89%以上,出水 TP 浓度和 COD 浓度分别在 0.4 mg·L⁻¹和 25 mg·L⁻¹以下,颗粒粒径在 950 μ m 以上,SVI 在 45 mL·g⁻¹以下;进水氨氮浓度为 60 mg·L⁻¹时,TP 去除率在 95%以上,出水 TP 浓度在 0.5 mg·L⁻¹以下,颗粒粒径为 760 μ m,SVI 为 56 mL·g⁻¹,系统中生物除磷颗粒出现部分解体,PAOs 代谢和生长开始受到抑制.进水氨氮浓度达到 70 mg·L⁻¹时,TP 去除率为 70%,出水 TP 浓度在 3 mg·L⁻¹左右,颗粒粒径为 570 μ m,SVI 为 75 mL·g⁻¹,PN/PS 值达到 7.50 左右,系统中生物除磷颗粒严重解体,PAOs 代谢和生长被严重抑制。随着进水氨氮浓度上升,导致生物除磷颗粒中微生物分泌蛋白质增加和多糖减少,PN/PS 值增大,出现生物除磷颗粒解体,颗粒粒径减小和 SVI 上升,生物除磷颗粒的结构和功能被破坏。

关键词:生物除磷颗粒; 氨氮浓度; 颗粒粒径; 胞外聚合物(EPS); PN/PS

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Effect of Influent Ammonia Concentration on a Biological Phosphorus Removal Granules System

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Abstract: Mature biological phosphorus removal granules were inoculated into a SBR. The effect of the ammonia concentration on biological phosphorus removal granules system was investigated by increasing the concentration of ammonia in the influent. The ability of the system to withstand ammonia loading was determined. The results showed that when the influent ammonia concentration was below 45 mg·L⁻¹, the biological phosphorus removal granule system showed good performance. The TP removal efficiency was above 96%, the COD removal efficiency was over 89%. The effluent TP concentration and COD concentration were 0.4 mg·L⁻¹ and 25 mg·L⁻¹ respectively. The particle size was above 950 μm and the SVI was below 45 mL·g⁻¹. When the influent ammonia concentration was 60 mg·L⁻¹, the removal efficiency of TP was more than 95%. The effluent TP concentration was below 0.5 mg·L⁻¹, the particle size was 760 μm, and the SVI was 56 mL·g⁻¹. Furthermore, the biological phosphorus removal granules partially disintegrated and the metabolism and growth of PAOs began to be inhibited in the system. When the influent ammonia concentration reached 70 mg·L⁻¹, the removal efficiency of TP was 70%, the effluent TP concentration was about 3 mg·L⁻¹, the particle size was 570 μm, the SVI was 75 mL·g⁻¹, and the value of PN/PS was about 7.50. The biological phosphorus granules severely disintegrated and the metabolism and growth of PAOs was severely inhibited in the system. Moreover, as the influent ammonia concentration increased, the protein increased and polysaccharide decreased from the microbial secretion of biological phosphorus removal granules disintegrated, the particle size decreased, the SVI increased, and the structure and function of the biological phosphorus removal granules were destroyed.

Key words: biological phosphorus removal granules; ammonia concentration; particle size; extracellular polymeric substance (EPS); PN/PS

近年来,过量的磷排放到天然水体中加速了水体富营养化,并导致水质恶化,磷的高效去除已经成为研究热点.目前,强化生物除磷以其高效除磷和节能环保的特点得到广泛应用,但在传统的强化生物除磷中,存在生物量低、易污泥膨胀以及二次释磷等缺点^[1~3].生物颗粒具有结构密实、沉降性能好、生物量高以及抗冲击能力强等优点^[4~6].因此,以聚磷菌(PAOs)为主体的生物除磷颗粒成为

了污水生物处理工艺的创新和最有发展前景的除磷技术,吸引了越来越多研究者的兴趣^[7-9].

目前,关于进水底物对生物除磷颗粒稳定性的影响研究有很多报道. 刘小英等[10]在 SBR 中探讨

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基金项目: 北京市优秀青年拔尖团队项目(2014000026833TD02) 作者简介: 李冬(1976~), 女,博士,教授,博士生导师,主要研究 方向为水环境恢复理论及关键技术, E-mail: lidong2006 进水 COD 浓度对系统稳定性的影响, 进水 COD 浓 度提高到550 mg·L-1时, 颗粒污泥周围丝状菌过度 生长, 颗粒污泥解体. Yu 等[11] 在 SBR 中研究了 COD 负荷对生物除磷颗粒系统的影响, 当 COD 浓 度大于500 mg·L-1时,聚磷菌(PAOs)的新陈代谢 能力受到抑制,系统的性能恶化,丝状菌过量繁殖 而导致污泥膨胀. Li 等[12]研究了 COD 负荷对生物 除磷颗粒连续流系统的影响, 当 COD 浓度达到 400 mg·L-1时, 由于丝状菌的增殖而导致系统厌氧 COD 和总磷(TP)去除率明显降低以及颗粒沉降能 力的恶化. Li 等[13]研究了不同 COD 负荷下污泥停 留时间(SRT)对生物除磷颗粒连续流的影响,较长 的 SRT 及较高的 COD 负荷(300 mg·L⁻¹)使颗粒沉 降能力和系统性能恶化. Zheng 等[14,15] 通过在 SBR 中研究了亚硝酸盐和游离氨对生物除磷颗粒系统的 影响, 由于亚硝酸盐和游离氨的影响, 生物除磷颗 粒系统中聚糖菌和丝状菌过量生长,污泥膨胀.生 物除磷颗粒工艺处理生活污水的过程中进水氨氮浓 度会对系统的性能和颗粒的特点产生不可忽视的影 响. 然而在同一生物除磷颗粒系统中探究进水氨氮 负荷的承受能力却鲜见报道.

本试验在 SBR 中接种成熟生物除磷颗粒,通过分阶段提高进水中氨氮浓度,测定系统中 TP 和 COD 的去除性能、颗粒的特性以及胞外聚合物 (EPS)等参数的变化,探究进水氨氮浓度对生物除磷颗粒系统的影响,确定系统对进水氨氮负荷的承受能力,以期为生物除磷颗粒实际应用提供基础依据和参考.

1 材料与方法

1.1 试验装置与运行方式

本试验采用由有机玻璃制成的 SBR 反应器,高50 cm,内径 14 cm,有效容积 6 L. 反应器垂直方向每隔 5 cm 设置取样口. 反应器内底部装有直径为 8 cm 的曝气盘,通过气体流量计控制曝气强度.

反应器每天运行 4 个周期,每周期运行 6 h,分为:6 min 进水,2 h 厌氧,3 h 好氧,3min 沉淀,5 min 排水,剩余时间闲置。整个试验过程温度和 pH 均不作控制,水温 $15 \sim 25^{\circ}\mathrm{C}$,pH 为 $7.0 \sim 8.0$.换水比为 2/3,曝气强度为 0.6 L·min $^{-1}$,污泥浓度控制在3 000 mg·L $^{-1}$ 左右.

1.2 接种污泥与试验用水

接种污泥取自本实验室培养成熟的生物除磷颗粒,浓度为3 000 $\text{mg} \cdot \text{L}^{-1}$ 左右,COD 去除率为 85% ~90%,TP 去除率为 96% ~99%.

本试验采用自来水配制的人工合成废水,采用

丙酸钠为碳源,磷酸二氢钾为磷源,硫酸铵为氮源,进水 NH_4^+ -N浓度由试验阶段决定,其余主要水质指标如表 1 所示.

表 1 讲水水质指标

Table 1 Characteristics of the influent

成分	数值	成分	数值
COD/mg·L ⁻¹	200	MgSO ₄ /mg·L ⁻¹	40
TP/mg·L ⁻¹	10	pН	7. 0 ~ 8. 0
$CaCl_2/mg \cdot L^{-1}$	30	温度/℃	15 ~ 25

1.3 试验参数

本试验分阶段逐步提高进水中氨氮浓度,探究 生物除磷颗粒系统对进水氨氮负荷的承受能力. 具 体试验参数如表 2 所示.

表 2 试验参数

Table 2 Operation parameters

Table 2 Operation	parameters
运行阶段	NH ₄ -N浓度/mg·L ⁻¹
I (1 ~ 14 d)	15
II (15 ~42 d)	30
Ⅲ (43 ~70 d)	45
IV (71 ~ 105 d)	60 (//
V (106 ~147 d)	70
VI (148 ~ 197 d)	60
1110 41	(0)

1.4 分析方法

COD 和 TP 的测定采用 5B-3B 型 COD 多参数 快速测定仪, NH_4^+-N 、 NO_2^--N 、 NO_3^--N 、MLSS、MLVSS、SV30、SVI 等指标均采用国家规定的标准方法^[16]. 本试验中 pH、DO 和温度的测定均采用WTW-pH/Oxi 340i 便携式多参数测定仪.

颗粒粒径采用 Mastersize 2000 激光粒度仪测定. EPS 的提取步骤^[17]:取 25 mL 泥水混合物,8 000 r·min⁻¹离心 15 min;去掉上清液后加入 PBS 溶液(50 mmol·L⁻¹磷酸钠、150 mmol·L⁻¹NaCl 及pH = 7)稀释至原体积;超声破碎 3 min;然后 80℃水浴加热 30 min,冷却后,8 000 r·min⁻¹离心 15 min,取上清液测定蛋白质(PN)和多糖(PS),剩余污泥测定 MLSS. PN 采用考马斯亮蓝法; PS 采用苯酚硫酸法.

2 结果与讨论

2.1 不同氨氮浓度下生物除磷颗粒系统的处理性能

本试验研究分为 6 个阶段,进水氨氮浓度分别为 15、30、45、60、70 和 60 $mg \cdot L^{-1}$,其中阶段 VI 为主要恢复系统活性阶段。图 1 为不同阶段系统中 TP 浓度及去除率的变化情况。阶段 I 为生物除磷颗粒系统的适应阶段,进水 氨氮浓度为 15 $mg \cdot L^{-1}$,反应器运行 14 d,主要是恢复系统中聚磷菌 (PAOs) 的活性,以 TP 去除率达到 95% 以上

为 PAOs 活性恢复成功的标志;该阶段 TP 去除率达到 97%,出水 TP 浓度在 0.3 mg·L⁻¹以下,低于我国城镇污水处理厂污染物排放标准一级 A 标准(0.5 mg·L⁻¹)[¹8²],说明系统中 PAOs 活性得到了良好的恢复. 在阶段 II、III,进水氨氮浓度分别为 30 mg·L⁻¹、45 mg·L⁻¹,TP 去除率均在 96%以上,出水 TP 浓度在 0.4 mg·L⁻¹以下,系统中聚磷菌活性较高. 在阶段 IV,进水 氨氮浓度为 60 mg·L⁻¹,系统运行到第 7 d 时,TP 去除率下降到82%,出水 TP 浓度达到 1.8 mg·L⁻¹左右,但系统经过 13 d 的适应,TP 去除率恢复到 95%以上,出

水 TP 浓度在 0.5 mg·L^{-1} 以下,在此阶段,PAOs 活性开始受到抑制. 在阶段 V,进水氨氮浓度为 70 mg·L^{-1} ,经过 10 d 运行,TP 去除率由 98% 下降到 30%,出水 TP 浓度仅为 7.3 mg·L^{-1} ;随后 TP 去除率提高至 70%,出水 TP 浓度稳定在 3 mg·L^{-1} 左右,系统中 PAOs 活性被严重抑制. 在阶段 VI,进水氨氮浓度调回 60 mg·L^{-1} ,此阶段主要恢复系统的处理性能. 系统经过 14 d 的运行,TP 去除率达到了 95% 以上,出水 TP 浓度在 0.4 mg·L^{-1} 以下,系统的处理性能得到了良好的恢复.

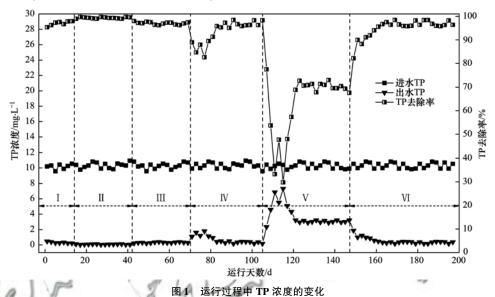


Fig. 1 Variation of TP concentration during the operation process

图 2 为不同阶段系统中 COD 浓度及去除率的变化情况. 从中可以看出,在阶段 I、Ⅱ、Ⅲ,进水氨氮浓度低于 45 mg·L⁻¹, 厌氧 COD 去除率与总COD 去除率相近,均在 89% 以上, 厌氧末期 COD

浓度与出水 COD 浓度相近,都在 25 mg·L⁻¹以下,远低于我国城镇污水处理厂污染物排放标准一级 A标准(50 mg·L⁻¹)^[18].在阶段IV,进水氨氮浓度为60 mg·L⁻¹,系统运行第 5 d, 厌氧 COD 去除率和总

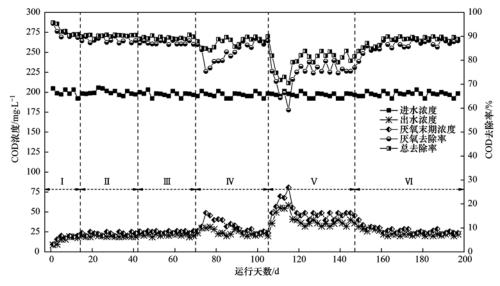


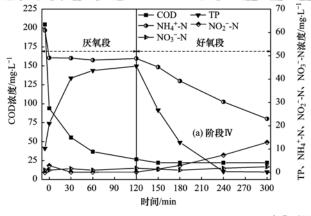
图 2 运行过程中 COD 浓度的变化

Fig. 2 Variation of COD concentration during the operation process

COD 去除率分别降低至 75% 和 85%,厌氧末期 COD 浓度和出水 COD 浓度分别达到 49 mg·L⁻¹和 30 mg·L⁻¹;系统经过 19 d 的运行,厌氧 COD 去除率和总 COD 去除率相近,都在 85% 以上,厌氧末期 COD 浓度和出水 COD 浓度均在 30 mg·L⁻¹以下.在阶段 V,进水氨氮浓度为 70 mg·L⁻¹,厌氧 COD 去除率和总 COD 去除率呈现先降低后增大的趋势,最后分别稳定在 75% 和 80%,厌氧末期 COD 浓度和出水 COD 浓度分别为 48 mg·L⁻¹和 36 mg·L⁻¹.在阶段 VI,系统经过 12 d 的运行恢复,厌氧 COD 去除率和总 COD 去除率均达到 85% 以上,厌氧末期 COD 浓度和出水 COD 浓度和出水 COD 浓度都在 26 mg·L⁻¹以下.整个运行过程中,COD 去除率都维持比较高的状态.

在阶段IV和阶段 V,进水氨氮浓度分别为 60 mg·L⁻¹和 70 mg·L⁻¹,氨氮浓度对 TP和 COD 去除效果的影响程度不同.原因可以归结于:①较高的氨氮浓度会抑制生物除磷颗粒中 PAOs 的代谢和生长,同时使其他异养菌增殖;②可能是氨氮转化成亚硝酸盐和硝酸盐,造成亚硝酸盐和硝酸盐的积累,抑制了生物除磷颗粒中 PAOs 的代谢和生长;③可能发生了反硝化异养菌反硝化作用与 PAOs 竞争碳源.为了进一步确定出水 TP 浓度上升和出水 COD 浓度变化不大的原因,在反应器运行 100 d(阶

段IV)和142 d(阶段V)的第二个周期进行周期试验. 由图 3 可以看出, 前 60 min 的 COD 去除速率较快, 在阶段Ⅳ中, COD 浓度由 200 mg·L-1 快速降至 35 mg·L⁻¹左右; 阶段V中, COD 浓度由 200 mg·L⁻¹快 速降至50 mg·L-1左右. 在两个阶段的厌氧段, NH₄⁺-N、NO₂⁻-N、NO₃⁻-N浓度的变化不大,初始 NO_2^- -N浓度都在3 $mg \cdot L^{-1}$ 左右, NO_3^- -N浓度在2 mg·L-1以下, 反硝化消耗的有机物相差不大. 两个 阶段厌氧段的释磷量相差很大, 在阶段IV中, 厌氧末 期的 TP 浓度达到 45 mg·L⁻¹左右, 而在阶段 V中, 厌 氧末期的 TP 浓度只有 20 mg·L⁻¹左右. 较高的氨氮 浓度抑制了生物除磷颗粒中 PAOs 的厌氧代谢. 在两 个阶段中,系统在好氧进行2h左右基本完成了磷的 吸收, 在好氧末期, 系统中积累了较高的NO; -N浓 度, 分别达到 13 mg·L⁻¹和 15 mg·L⁻¹, 可能会抑制 生物除磷颗粒中 PAOs 的好氧代谢. 但 Zeng 等[19]的 研究表明, 20 mg·L⁻¹的NO₂-N浓度对 PAOs 的好氧 磷吸收没有明显的影响. 徐少娟等[20]的研究表明较 高的进水氨氮浓度会抑制 PAOs 的代谢和生长. 从以 上分析结果可知,在阶段IV和阶段V,氨氮浓度对TP 和 COD 去除效果的影响程度不同的主要原因是较高 的氨氮浓度会抑制生物除磷颗粒中 PAOs 的代谢和 生长,同时使其他异养菌增殖,故而 TP 去除效果变 化大, COD 去除效果变化相对小.



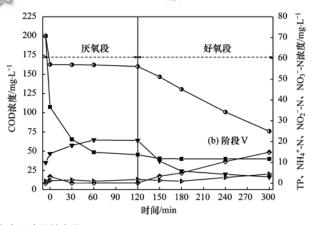


图 3 一个典型周期内污染物的变化

Fig. 3 Variation of pollutants in one typical cycle

2.2 不同氨氮浓度下生物除磷颗粒的特性

沉降能力和颗粒粒径是颗粒污泥在生物反应器中持留能力的重要特征.通常,颗粒粒径越大意味着颗粒沉降速率越大[12]; SVI 通常被用作污泥沉降能力的指标,较低的 SVI 意味着污泥具有良好的沉降能力[11,14].因此,本试验通过测定平均粒径、SVI 和 MLVSS/MLSS,评估不同氨氮浓度下系统中颗粒特性的变化.

图 4 为运行过程中颗粒粒径、SVI 和 MLVSS/

MLSS 的变化. 在阶段 I ,颗粒平均粒径、SVI 和 MLVSS/MLSS 分别为1 120 μ m、30 μ m、30 μ m、85,说明生物除磷颗粒具有良好的沉降能力和较高的微生物含量. 在阶段 II ,颗粒平均粒径减小至1 090 μ m,SVI 升高到 35 μ mL·g⁻¹,MLVSS/MLSS 为 0. 84;在阶段 III,颗粒平均粒径减小至 950 μ m,SVI 和 MLVSS/MLSS 分别升高到 45 μ m、87;在阶段 IV,颗粒平均粒径大幅度减小,最终为 760 μ m,生物除磷颗粒出现部分解体现象,SVI 和 MLVSS/

MLSS 升高到 56 mL·g⁻¹和 0.87; 在阶段 V, 颗粒平均粒径减小到 570 μm, 生物除磷颗粒解体严重, SVI 逐渐升高 75 mL·g⁻¹, MLVSS/MLSS 升高到 0.89. 随着进水氨氮浓度的升高, SVI 和 MLVSS/MLSS 呈现上升趋势, 颗粒平均粒径呈下降趋势; 进水氨氮浓度为 60 mg·L⁻¹和 70 mg·L⁻¹时, 颗粒平均粒径和 SVI 变化显著, 生物除磷颗粒沉降性能严重恶化. Zou 等^[21]的研究表明较高的氨氮浓度会导致大的生物除磷颗粒解体成小颗粒, 颗粒粒径下

降. Zheng 等^[14]的研究也表明较高的氨氮浓度会导致大颗粒不稳定并破碎成较小的颗粒,同时 SVI 会升高;同时也暗示 MLVSS/MLSS 升高可能是由于颗粒崩解导致比表面积增大,促进更多有机物质的吸附. 在阶段 VI,系统经过 21 d 的运行,颗粒平均粒径、SVI 和 MLVSS/MLSS 分别恢复到 780 μ m、56 mL·g⁻¹和 0.86,系统中生物除磷颗粒的沉降性能得到一定的恢复. 以上结果表明进水氨氮浓度对生物除磷颗粒系统中颗粒的沉降性能有重要的影响.

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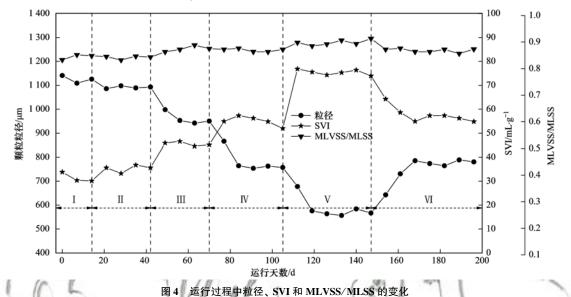


Fig. 4 Variation of particle size, SVI, and MLVSS/MLSS during the operation process

2.3 不同氨氮浓度下 EPS 中 PN 和 PS 的变化 胞外聚合物(EPS)是由微生物分泌的胞外聚合 物黏度物质,在细胞自凝聚中起着重要的作 用[22,23],主要成分为蛋白质(PN)和多糖(PS),它 们有助于细菌聚集在一起并黏附每个细胞^[14],且颗粒的特性与 PN/PS 值有关^[21,24,25].

图 5 为整个运行过程中 PN、PS 含量及 PN/PS 的变化情况. 在阶段 I, EPS 中 PN 和 PS 含量(以

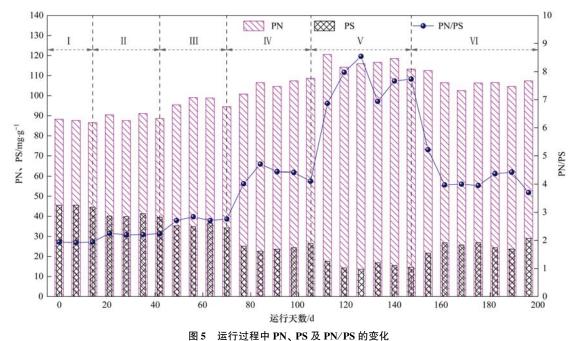


Fig. 5 Variation of PN, PS, and PN/PS during the operation process

MLSS 计) 比较稳定, 分别为 87 mg·g⁻¹ 和 45 mg·g⁻¹, PN/PS 值为 1.94. 在阶段 II, PN 含量为 88 mg·g⁻¹, PS 含量下降至 39 mg·g⁻¹, PN/PS 值增 大到 2. 20; 在阶段 Ⅲ, PN 含量上升到 98 mg·g⁻¹, PS含量略微降低至35 mg·g⁻¹, PN/PS值增大到 2.70; 在阶段 IV, PN 含量上升至 106 mg·g⁻¹, PS 含量下降明显,达到 23 mg·g⁻¹, PN/PS 值增大到 4.42; 在阶段 V, PN 含量上升到 115 mg·g⁻¹, PS 含量降低至 15 mg·g-1, PN/PS 值明显增大, 达到 7.50 左右. 当进水氨氮浓度高于 45 mg·L⁻¹时, PN 含量略微上升, 而 PS 含量急剧减少, PN/PS 值急 剧增大, 即较高的进水氨氮浓度会抑制 PS 的分泌. Zou 等[21]的研究表明在较高的进水氨氮浓度下, 大 部分有机物用于生物合成而不是分泌 PS, 而反应 器中的氮(N)用于合成 PN. Yang 等[26]也暗示较高 的氨氮浓度会导致 PS 产量的显著下降, 不利于颗 粒的稳定. Tay 等[27] 已经表明 PS 可以作为细胞凝 聚和黏附的介质, 有助于颗粒的形成和维持颗粒中 细胞群的结构完整性. 因此, 上述研究中随着进水 氨氮浓度上升,导致微生物分泌蛋白质增加和多糖 减少, PN/PS 值增大, 出现生物除磷颗粒解体, 颗 粒粒径减小和 SVI 上升(图 4), 生物除磷颗粒的结 构和功能被破坏,这些结果表明 PN/PS 较低的颗粒 具有更好的结构和功能. 在阶段 VI, 进水氨氮浓度 恢复到 60 mg·L-1, PN 含量逐渐降低至 106 mg·g⁻¹, PS 含量升高至 26 mg·g⁻¹, 说明系统中生 物除磷颗粒的结构和功能得到一定的恢复.

3 结论

- (1) 进水氨氮浓度低于 45 mg·L⁻¹, 生物除磷颗粒系统具有良好的处理性能, TP 去除率在 96%以上, COD 去除率在 89%以上, 出水 TP 浓度和COD 浓度分别在 0.4 mg·L⁻¹和 25 mg·L⁻¹以下; 进水氨氮浓度为 60 mg·L⁻¹时, 系统中 PAOs 的代谢和生长开始受到抑制, 经过 13 d 的适应, TP 去除率恢复到 95%以上, 出水 TP 浓度在 0.5 mg·L⁻¹以下. 进水氨氮浓度达到 70 mg·L⁻¹时, 系统中 PAOs 的代谢和生长被严重抑制, TP 去除率为 70%, 出水 TP 浓度稳定在 3 mg·L⁻¹左右.
- (2) 进水氨氮浓度高于 60 mg·L⁻¹时, 生物除磷颗粒系统中颗粒粒径和 SVI 变化显著, 生物除磷颗粒沉降性能严重恶化.
- (3)进水氨氮浓度对生物除磷颗粒系统中颗粒的结构和性能有重要的影响. 随着进水氨氮浓度上升,导致生物除磷颗粒中微生物分泌蛋白质增加和多糖减少, PN/PS 值增大, 出现生物除磷颗粒解

体,颗粒粒径减小和 SVI 上升, 生物除磷颗粒的结构和功能被破坏.

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