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目 次



3 种吸附剂对污水磷污染去除性能与机制比较

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摘要:为探索高效利用膨润土、红壤和炉渣去除 农业污水磷污染的可行性,对比分析了 3 种吸附剂对人工合成含磷污水的 吸附去除特性,结合 SEM、XDS 和 BET 等测试结果以及等温吸附、吸附动力学及 Ca^{2+} 释放量探讨了 3 种材料对磷的吸附机制.结果表明,炉渣对磷的吸附能力高于膨润土和红壤,吸附过程均适合 Langmuir 等温吸附方程($R^2 > 0.96$),对磷的理论饱和吸附量为:炉渣(16.87 $mg \cdot g^{-1}$) >红壤(1.21 $mg \cdot g^{-1}$) >膨润土(0.92 $mg \cdot g^{-1}$).炉渣对磷的吸附动力学特征符合 Elovich方程($R^2 = 0.966$),而膨润土和红壤对磷的吸附特征则更适合准二级动力学方程($R^2 = 0.966$),而膨润土和红壤对磷的吸附特征则更适合准二级动力学方程($R^2 = 0.966$),加速的 Ca^{2+} 释放量(10.46 $mg \cdot g^{-1}$) 显著大于膨润土(0.31 $mg \cdot g^{-1}$) 和红壤(0.03 $mg \cdot g^{-1}$)(P < 0.05).红壤对磷的吸附量随着 pH 的升高而降低;膨润土在初始 pH 为 7.0 时,吸附量最低;但初始 pH 值对炉渣去除磷的影响不大.相比红壤和炉渣,膨润土解吸较快,易于进行重复利用.综上所述,吸附材料的磷吸附能力主要与其结构、化学组成、 Ca^{2+} 释放能力及溶液初始 pH 值等有关,炉渣较膨润土和红壤对磷酸盐有着更强的去除能力,适合处理农村污水磷污染.

关键词:磷;膨润土;红壤;炉渣;吸附;废水

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Removal Performance and Mechanism for Treating Phosphorus in Agricultural Wastewater by Three Adsorbents

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Abstract: To screen the optimal absorbents for P removal from agricultural wastewater, the P adsorption capacity of bentonite, red soil, and slag was studied using synthetic wastewater. Combing the properties of three adsorbents measured by SEM, XDS, and BET methods, the isothermal adsorption, adsorption kineties, and Ca²⁺ release capacity were analyzed to elucidate the mechanisms of P adsorption. The results showed that the P adsorption capacity of slag was higher than that of bentonite and red soil, and the Langmuir isotherm model was able to better fit the adsorption data ($R^2 > 0.96$). The P theoretical saturation sorption capacity of slag was higher (16.87 $\mathrm{mg} \cdot \mathrm{g}^{-1}$) than that of bentonite (1.21 $\mathrm{mg} \cdot \mathrm{g}^{-1}$) and red soil (0.92 $\mathrm{mg} \cdot \mathrm{g}^{-1}$) (P < 0.05). The results for adsorption kinetics indicated that slag rapidly removed 95.6% of P from 10 mg·L⁻¹ solution, and the Elovich equation fit the data well ($R^2 = 0.812$). The adsorption kinetics of P on bentonite and red soil were better described by the pseudo-second-order kinetic equation ($R^2 = 0.982$ and 0.959, respectively). The Ca²⁺ release capacity of slag (10.46 mg·g⁻¹) was significantly higher compared to bentonite (0.31 $\text{mg}\cdot\text{g}^{-1}$) and red soil (0.03 $\text{mg}\cdot\text{g}^{-1}$) (P < 0.05). The P adsorption capacity of red soil was 0.26 $\text{mg}\cdot\text{g}^{-1}$ when the pH value was 3, and it decreased as the pH values increased. At the initial pH of 7.0, the P adsorption capacity of bentonite was about 0.01 mg·g lower than 0.04 mg·g⁻¹ at pH 3, and 0.05 mg·g⁻¹ at pH 11. The initial pH value had little effect on the P adsorption capacity of slag. The P-loaded bentonite, red soil, and slag were effectively regenerated by using CaCl, solution, and bentonite was easier to reuse compared to red soil and slag. The key factors affecting the P adsorption capacity of the three adsorbents were physical and chemical properties, such as crystal structure and the content of metal ions, Ca²⁺ release capacity, and initial pH. These findings demonstrated that slag was a better choice for P removal compared to bentonite and red soil and could be used as an effective P adsorbent for agricultural wastewater treatment.

Key words: phosphate; bentonite; red soil; slag; adsorption; wastewater

磷是重要的植物营养元素,也是造成地表水富营养化的一个重要因素[1].它主要来源于农业种植、城市雨水径流、市政和工业废水以及畜禽粪便排放等面源污染^[2-4].农业面源污染使我国太湖、巢湖、滇池等众多河流均受到不同程度的富营养化影响,且磷是水体富营养化的限制性因素^[5].目前国内外采用的除磷方法主要有化学沉淀法、生物去除法及吸附法^[6-8]等.其中,吸附法由于操作简单、

处理成本低、除磷效率高等优点得到广泛的应用. 寻找低价、高效的吸附剂是近年来除磷的研究 热点.

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黏土矿物是我国重要的非金属矿产资源. 优越 的表面性能和特殊的电化学性质使其在环境保护领 域和污染物净化处理中得以广泛地应用[9,10]. 如 Yin 等[11] 通过天然海泡石处理初始浓度 5~1000 mg·L-1的人工模拟含磷废水,得到最大吸附量为 32.0 mg·g⁻¹, 显著高于其它天然黏土矿物, 并发现 溶液初始 pH 值对磷的吸附效果影响很大. Moharami 等[12]通过膨润土、方解石、高岭土和沸 石处理含磷废水,得到4种吸附剂磷的最大吸附量 分别为 0.28、1.82、0.32 和 0.37 mg·g⁻¹. 此外,一 些富含铁、铝、钙、镁等金属活性物质的工业副产 物也具有较强的吸附除磷能力. 如 Barca 等[13] 发现 电弧炉钢渣和碱性氧气炉钢渣具有较大的磷去除能 力,并且认为钢渣对磷酸盐的去除主要是通过钙元 素与磷酸盐产生的共沉淀复合物. Blanco 等[14]研 究了碱性氧气炉渣在批量实验中对磷的去除率达到 84%~99%, 去除能力在 0.12~8.78 mg·g⁻¹之间, 在连续运行的柱状实验中处理初始浓度为15 mg·L-1时,对磷酸盐的去除率高达99%以上,去除 能力为 3.1 mg·g⁻¹. 有研究表明, 黏土矿物与炉渣 等工业副产物对磷具有一定的吸附去除效应. 然而 同时对比分析不同类型吸附材料对农业废水中磷污 染的去除及其机制研究的相关报道却很少, 且鲜有 报道研究材料 Ca2+ 释放能力对磷吸附效果的影响 以及利用4种动力学模型分析吸附材料的动力学 过程.

鉴于此,本文对比研究黏土矿物膨润土、红壤与工业副产物炉渣对人工模拟含磷废水中磷酸盐的去除效率.利用扫描电镜(SEM)、能量色散 X 射线能谱仪(XDS)、BET 比表面积、孔径分析和阳离子交换量(CEC)对样品结构和性质进行表征分析.分析了溶液中磷酸盐初始浓度及 pH 值对吸附效果的影响,并通过等温吸附、吸附动力学实验及 Ca²+释放量,探讨3种材料对磷的吸附特征及其磷去除的主要机制,并探索3种材料的脱附再生能力,以期为选取适用于处理含磷废水的吸附材料提供理论依据.

1 材料与方法

1.1 实验材料

本实验所采用3种吸附材料分别为膨润土、红壤和炉渣. 红壤取自湖南省长沙县白沙镇旱地土,膨润土购自河南郑州海洲化工产品有限公司,炉渣取自长沙金薯食品有限公司. 所选吸附材料在实验之前用蒸馏水清洗3次,烘干至恒重,过20目标准筛(<1 mm),备用.

1.2 材料表征方法

膨润土、红壤和炉渣的表面形貌特征用扫描电子显微镜(SU8010,日立公司,日本)测定;化学成分采用能量色散 X 射线能谱仪(SU8010,日立公司,日本)测定;比表面积、孔体积和孔径特征采用BET 比表面仪(Quadrasorb SI,康塔仪器公司,美国)测定.阳离子交换量(CEC)采用乙酸铵交换法测定^[15,16].

1.3 吸附实验

1.3.1 吸附材料的磷吸附特征

称取 1.00 g 膨润土、红壤和炉渣样品置于 100 mL 离心管中,加入 50 mL 初始浓度为 10、50、100 mg·L⁻¹(以 P 计)的 KH₂PO₄ 标准溶液,恒温振荡 24 h(180 r·min⁻¹, 25°C),离心(4 000 r·min⁻¹, 5 min),取上清液采用钼锑抗分光光度法测定溶液中磷的质量浓度.实验设置 3 个重复.吸附材料的吸附量 Q_e [式(1)]和去除率 η [式(2)]计算如下:

$$Q_e = \frac{(c_0 - c_e) \times V}{m} \tag{1}$$

$$\eta = \frac{(c_0 - c_e)}{c_o} \times 100\%$$
 (2)

式中, Q_e 为吸附剂对磷的吸附量($mg \cdot g^{-1}$); η 为磷 去除 率(%); c_0 为溶液中磷的初始质量浓度($mg \cdot L^{-1}$); c_e 为 吸 附 平 衡 时 磷 质 量 浓 度($mg \cdot L^{-1}$); V 为溶液体积(L); m 为吸附剂质量(g).

1.3.2 等温吸附实验

P 溶液初始质量浓度分别设为 $1 \sim 300 \text{ mg} \cdot \text{L}^{-1}$, 吸附时间为 24 h. 等温线模型 Langmuir 方程[式(3)]和 Freundlich 方程[式(4)]用于拟合等温吸附实验数据:

$$\frac{1}{Q_e} = \frac{1}{aQ_m c_e} + \frac{1}{Q_m} \tag{3}$$

$$Q_e = \ln k + \frac{1}{n} \ln c_e \tag{4}$$

式中, Q_m 为理论最大吸附量 $(mg \cdot g^{-1})$; a 为吸附系数,与能量有关的常数; k 为 Freundlich 模型参数,是与最大吸附量有关的常数; n 是与温度有关的常数,可表征吸附剂与吸附质之间的亲和力.

1.3.3 吸附动力学实验

P 溶液初始质量浓度为 $10 \text{ mg} \cdot \text{L}^{-1}$,吸附时间设置为 0.1.2.5.10.20.30.60.120.180.240.480.720.1440和2160 min.4 个典型动力学方程[式(5)~(8)]用于拟合吸附动力学数据.

准一级动力学方程:

$$\ln(Q_e - Q_t) = \ln Q_e - k_1 t \tag{5}$$

准二级动力学方程:

$$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} + \frac{t}{Q_e} \tag{6}$$

Elovich 动力学方程:

$$Q_{t} = a + b \ln t \tag{7}$$

颗粒内扩散模型:

$$Q_t = k_i t^{0.5} + C (8)$$

式中, Q_t 为任意时刻 t 的吸附量($\operatorname{mg} \cdot \operatorname{g}^{-1}$); k_1 和 k_2 分别为准一级动力学和准二级动力学方程的速率常数; t 为吸附时间(min); a 和 b 为 Elovich 动力学参数; k_i 为颗粒内扩散速率常数($\operatorname{g} \cdot \operatorname{mg}^{-1} \cdot \operatorname{min}^{-0.5}$); C 为常数,表示吸附剂的边界层数,其值越大说明边界层对吸附的影响越大.

1.3.4 初始 pH 值对磷吸附效果的影响

P 溶液初始质量浓度为 $10 \text{ mg} \cdot \text{L}^{-1}$,用 $1 \text{ mol} \cdot \text{L}^{-1}$ 的 HCl 和 NaOH 调节溶液 pH 值依次为 $3 \cdot \text{S} \cdot \text{T} \cdot \text{S} \cdot \text{P}$ 和 11,吸附时间为 24 h,并测定吸附后溶液 pH 值.

1.3.5 Ca²⁺释放特征

加入 50 mL 蒸馏水, 吸附时间设置为 0、1、2、5、10、20、30、60、120、180、240、480、720、1 440和2 160 min, 原子吸收法测定溶液中 Ca²⁺浓度.

1.3.6 磷的解吸

首先按照上述步骤进行吸附实验(吸附材料投加量为1g,磷溶液初始质量浓度为10 mg·L⁻¹,温度为25℃)通过离心获得含磷的膨润土、红壤和炉渣,并测定上清液中磷酸盐的剩余浓度,再用50 mL 0.02 mol·L⁻¹ CaCl₂ 溶液恒温振荡反应24 h后,离心,测定溶液中磷酸盐的剩余浓度,共循环4次.解吸率[式(9)]的计算如下:

解吸率 = $(解吸量 / 吸附量) \times 100\%$ (9)

2 结果与讨论

2.1 吸附材料的理化性质

X 射线荧光光谱分析结果表明, 3 种吸附材料

的主要化学成分差异明显(表 1). 其中, Mg 和 Al 元素含量差别较小, 而 Ca 和 Fe 含量差异较大, 可能是 3 种材料除磷差异的主要原因之一. 有研究表明, 材料的磷吸附能力与 Ca、Mg、Al 和 Fe 等金属氧化物成正相关^[17]. 水中的磷素可以与 Ca²⁺、Mg²⁺、Fe³⁺及 Al³⁺等离子及其水合物和氧化物反应形成难溶性化合物, 从而使磷得以去除^[18,19]. 吸附材料中主要金属离子的含量和化学形态是除磷的重要影响因素.

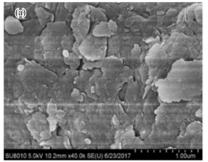
天然矿物材料特殊的表面化学特性使其具有阳离子交换能力,从而对磷酸盐等有机-无机化合物具有一定的吸附能力^[20]. 但有研究表明,填料的化学成分及其化学形态是影响其磷吸附能力的重要因素,填料的物理特性与其磷吸附能力相关关系相对较小^[21]. 物理结构显示,3 种材料的比表面积和孔径相差较小,但膨润土的阳离子交换量(CEC)(32.8 cmol·kg⁻¹)明显大于红壤(7.67 cmol·kg⁻¹)和炉渣(9.13 cmol·kg⁻¹).

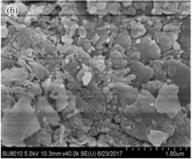
表 1 吸附材料部分物理化学特征

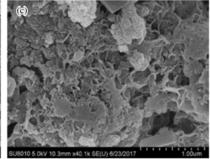
Table 1 Physical-chemical characteristics of the three adsorbents

7/ 理	化性质	膨润土	红壤	炉渣
10	Cá	0. 67	0. 005	3. 68
主要化学成分/%	Fe	4. 72	2. 17	1. 42
\ Mg /0	Al	15. 67	21. 29	29. 97
**	Mg	1.67	0.75	1. 93
	比表面积/m²·g-1	21. 85	24. 98	26. 44
	总孔容/cm³·g-1	0. 023	0.081	0.048
物理结构	孔径/nm	3. 97	4. 54	3. 79
	CEC/cmol·kg ⁻¹	32. 8	7. 67	9. 13
	pH(固:液=1:2.5)	8. 19	4. 90	8. 76

SEM 分析结果显示, 3 种材料的表面形貌差异明显(图 1). 炉渣的表面粗糙多孔, 形似蜂窝状, 孔径大小不一, 因而导致其比表面积相对较大 $(26.44 \text{ m}^2 \cdot \text{g}^{-1})$; 膨润土为层状结构, 表面构造紧致, 比表面积相对较小 $(21.85 \text{ m}^2 \cdot \text{g}^{-1})$. 由于比表







(a)膨润土; (b)红壤; (c)炉渣

图 1 吸附材料 SEM 图

Fig. 1 SEM images of the three adsorbents

面积较小,磷吸附位点相对较少,也可能是导致膨 润土对磷的吸附量低于红壤和炉渣的主要原因 $2^{-[22]}$.

2.2 3种材料的磷吸附能力比较

3种材料对磷的吸附能力差异明显(图2). 在 不同磷浓度条件下, 炉渣对磷的吸附量大于膨润土 和红壤. 如在磷初始浓度为 10 mg·L⁻¹时, 炉渣对 磷的吸附量为 $0.56 \text{ mg} \cdot \text{g}^{-1}$, 远大于膨润土(0.08 $mg \cdot g^{-1}$)及红壤(0.36 $mg \cdot g^{-1}$)(P < 0.05).3种材 料对磷的吸附量随初始浓度的增加有不同程度地变 化. 当初始浓度增加到 100 mg·L⁻¹时, 炉渣对磷的 吸附量为 4.69 mg·g⁻¹, 去除率达到 90% 以上. 而 随着磷初始浓度的升高,膨润土对磷的吸附量基本 保持不变, 红壤的吸附量却在逐渐下降, 但趋势不 明显(P > 0.05).

有研究表明, 炉渣能有效降低水体中磷含量, 其主要原因是炉渣中含有大量能吸附可溶性无机磷 酸盐的钙, 通过钙磷沉淀实现废水中磷的去 除 $^{[23,24]}$. 红壤中 Ca^{2+} 含量较低, 而 Fe^{2+} 、 Al^{3+} 含量 较高(表1), 易与磷酸盐反应生成溶解性低的铁磷 和铝磷, 甚至进一步生成有效性更低的闭蓄态磷, 使磷在红壤中固定起来[25],对磷的有效性影响很 大,造成红壤的吸附量较低. 膨润土对磷的吸附能 力小于红壤和炉渣,主要可能原因是膨润土表面硅 氧结构极强的亲水性, 以及在层间大量可交换性阳 离子水解的共同作用下, 其表面通常被一层薄水膜 所包裹, 阻碍了对磷酸根等阴离子的吸附作 用[26,27]. 因此, 为了提高膨润土处理污水的能力, 需对其进行改性处理, 以增强其对污染物(如 P)的 吸附能力及去除效果[16].

2.3 3种吸附材料对磷的吸附特征

2.3.1 等温吸附过程

3种吸附材料对磷的等温吸附特征如图 3 所 示. 随着溶液中 P 初始浓度的增加, 炉渣对磷的吸

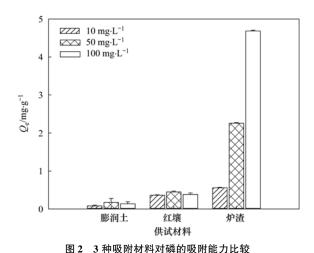
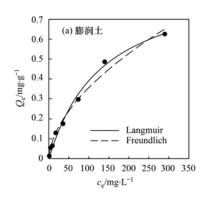
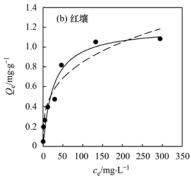


Fig. 2 Comparison of the phosphorus adsorption capacity of the three adsorbents

附量呈快速增加趋势,去除率达到91.3%.膨润土 和红壤随着溶液中 P 浓度的增大, 吸附量也随之增 加. 在低初始浓度时(<50 mg·L⁻¹), 红壤和膨润 土的吸附量均快速增长, 但达到吸附平衡时, 红壤 的吸附量高于膨润土;在高初始浓度时(>100 mg·L-1),红壤的吸附量基本趋于平稳,呈现出吸 附饱和状态,而膨润土经过缓慢增长而后达到吸附 饱和状态.

等温吸附拟合结果表明(表2), Langmuir 模型 能更好地描述3种吸附材料对磷的等温吸附过程 $(R^2 为 0.995, 0.969, 0.963)$, 表明 3 种吸附材料 对磷的吸附以同质单层吸附为主[28,29],理论最大吸 附量分别为炉渣(16.870 mg·g⁻¹) > 红壤(1.203 mg·g⁻¹) > 膨润土(0.921 mg·g⁻¹). 研究表明, 材 料的磷吸附能力与所含 Ca、Mg、Al 和 Fe 等金属氧 化物成正相关,同时,pH值、CEC、比表面积和孔 容对吸附容量也起重要作用[17]. 炉渣的 Ca、Fe 含 量明显大于膨润土和红壤, Al 含量也较高, 且具有 较大的比表面积和孔容积, 因此对磷的理论饱和吸 附量也较高.





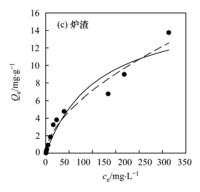


图 3 3 种吸附材料对磷等温吸附曲线

Fig. 3 Isothermal adsorption of the three adsorbents

主っ	3 种吸附材料对磷等温吸附模型拟合参	*h
表 2	3.种吸附材料划罐弄温吸附模型拟合家	÷ 42√V

Table 2	Isothermal	adsorption	parameters	of	the	three	adsorbents

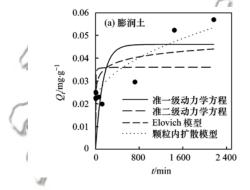
吸附材料		Langmuir 方程			Freundlich 方程	
100 PM 171 144	$Q_{\rm m}/{\rm mg}\cdot{\rm g}^{-1}$	a	R^2	$K_{ m F}$	n	R^2
膨润土	0. 921	0. 007	0. 995	0. 023	0. 564	0. 983
红壤	1. 203	0. 038	0. 969	0. 206	0.308	0. 940
炉渣	16. 870	0.088	0. 963	1. 885	0. 581	0. 957

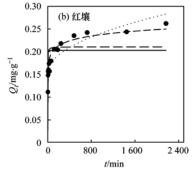
2.3.2 吸附动力学

3 种吸附材料的磷吸附动力学特征如图 4 所示,随吸附时间的增加,炉渣和红壤对磷的吸附量逐渐增大,12 h 后基本达到吸附平衡.膨润土对磷吸附特征随时间的变化有所改变.加入初始浓度的30 min 时,其对磷的吸附量达到饱和吸附量的22%,随着吸附时间的增长,吸附量持续增加;但在30 min 到1 h 之间,对磷的吸附量有所下降;在1 h 之后,对磷的吸附量持续增加直至到吸附平衡.主要原因可能是由于膨润土表面比较光滑,构造紧致(图1),致使在吸附初期的30 min 内,绝大部分磷占据了其表面活性位点.而在30 min 后,由于表

面活性位点的减少而对磷的吸附量逐渐降低. 但在 1 h 后, 磷进入膨润土内部, 吸附量也随之增加, 直至达到吸附平衡.

为分析磷素在 3 种材料上的吸附过程,本文采用准一级动力学、准二级动力学、Elovich 方程及颗粒内扩散模型拟合吸附动力学参数(表 3). 结果表明,在初始浓度为 $10~\text{mg}\cdot\text{L}^{-1}$ 的含磷水体中,准二级动力学方程更适合描述膨润土($R^2=0.982$)与红壤($R^2=0.959$)的磷吸附动力学特征,表明吸附过程是化学反应^[29];但 Elovich 型方程对炉渣的拟合效果最好($R^2=0.812$),说明炉渣在整个吸附过程中具有均匀分布的表面吸附能^[30].





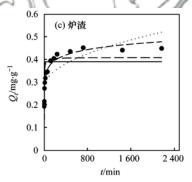


图 4 3 种吸附材料的磷吸附动力学曲线

Fig. 4 Adsorption kinetics of the three adsorbents

表 3 3 种吸附材料对磷吸附动力学模型拟合参数

Table 3 Adsorption kinetics parameters of the three adsorbents

吸附材料	准一组	吸动力学		准二组	级动力学		E	lovich 模	型	颗	粒内扩散	模型
"汉阳 77 平	$Q_{\rm e}/{ m mg}\cdot{ m g}^{-1}$	k_1	R^2	$Q_{\rm e}/{ m mg}\cdot{ m g}^{-1}$	k_2	R^2	a	b	R^2	k_i	C	R^2
膨润土	0. 10	0. 25	0. 689	0. 11	7. 92	0. 982	0. 02	0.01	0.457	0.01	0.07	0. 359
红壤	0. 20	1.03	0.823	0. 21	6. 29	0. 959	0. 13	0.02	0.677	0.01	0. 15	0.912
炉渣	0.39	0.38	0. 594	0. 41	1. 23	0. 721	0. 21	0.04	0.812	0. 01	0. 28	0.810

2.4 初始 pH 值对磷吸附效果的影响

初始 pH 对磷的吸附影响在 3 种材料之间差异较大(图 5). 其中,红壤对磷的吸附量随溶液初始pH 值增大而降低. 当 pH 为 3.0 时,吸附量为 0.26 mg·g⁻¹,去除率为 56.01%,除磷效果最好;而随着溶液 pH 值升高到 11.0 时,吸附量下降至 0.05 mg·g⁻¹,去除率为 10.65%.溶液 pH 值不仅影响磷在水体中的存在形态,还直接影响材料表面孔隙的结构和化学特性,及材料表面碱性氧化物的带电情况^[31]. 在初始 pH 值较高时,大量 OH⁻与 PO₄³⁻的

同时存在会产生竞争吸附,或使红壤表面负电荷增多而导致吸附剂与磷的排斥力增加^[32],从而使红壤对磷的吸附能力下降.而炉渣对磷的吸附量随溶液初始 pH 变化基本保持不变,平均为 0.46 mg·g⁻¹.在本研究的 pH 范围内(3.0~11.0),吸附饱和后的 pH 值接近于炉渣本身(8.76),说明 pH值的变化对炉渣去除磷的影响不大,这与吴丽萍等^[33]的研究结果一致.初始 pH 在小于 7.0 或大于7.0 的两个范围内,膨润土对水体中磷去除效果较好,可能是在 pH 小于 7.0 时,膨润土 Fe³⁺和 Al³⁺

的活性较高,从而引起对 $H_2PO_4^-$ 的沉淀和固定作用加强;而在 pH 大于 7.0 时,膨润土对磷的去除能力主要与矿物中的钙等离子形成的共沉淀为 $\dot{\mathbf{1}}^{[34]}$.

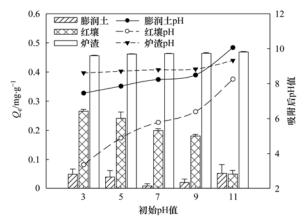


图 5 初始 pH 值对磷吸附效果的影响

Fig. 5 Effect of initial pH on phosphate adsorption of the three adsorbents

2.5 3 种材料的 Ca²⁺释放能力

3 种材料的 Ca²⁺释放能力如图 6 所示. 炉渣的 Ca²⁺释放量达到 11. 24 mg·g⁻¹, 显著大于膨润土 (0. 31 mg·g⁻¹) 和红壤(0. 02 mg·g⁻¹) (*P* < 0. 05). 有研究表明,炉渣溶出的 Ca²⁺能与磷酸盐反应生成 Ca₁₀(PO₄)₆(OH)₂ 沉淀,其溶解度随 pH 的增加而减小,因而碱性环境下可达到良好的磷酸盐去除效果^[13]. 膨润土的 Ca²⁺释放量较高(0. 31 mg·g⁻¹),在其溶液 pH 为碱性的环境条件下,会产生更多的 OH⁻与 HPO₄²⁻ 在膨润土表面与 Ca²⁺竞争结合,从而导致膨润土表面的 Ca-P 结合能力较弱,对磷的去除能力较差. 红壤为弱酸性黏土矿物,其 Ca²⁺含量较低,因此红壤通过 Ca-P 形式对磷酸盐的去除作用较低. 在红壤溶液中,由于 Fe、Al 含量较高,更容易发生 Fe³⁺和 Al³⁺与 PO₃⁴⁻反应形成稳定的 AlPO₄和 FePO₄^[35].

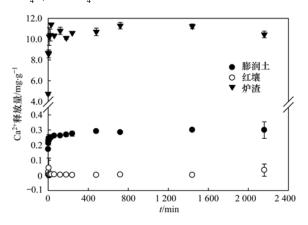


图 6 3 种吸附材料的 Ca2+ 释放量特征

Fig. 6 Ca²⁺ release characteristics of the three adsorbents

2.6 磷的解吸

为了有效评估已使用过的膨润土、红壤和炉渣的重复利用性能,需对其进行磷的解吸^[36,37].本实验结果表明,红壤和炉渣的解吸率随着解吸次数的增加而增加,解吸率分别为 59.6% 和31.6%;膨润土的解吸率在前3次随着解吸次数的增加而增加,当进行第4次解吸时,解吸率由60.5%下降至38.5%(图7).红壤和炉渣对磷的去除率随着解吸次数的增加而下降,分别由初始的去除率 83.4% 和53.9% 下降到 22.6% 和31.1%,膨润土在第4次循环时的去除率最大(10.1%).上述结果说明红壤和炉渣需要通过多次解吸才能将所吸附的磷完全释放出来,膨润土所需要的解吸次数较少,相比较红壤与炉渣,膨润土更容易进行重复利用.

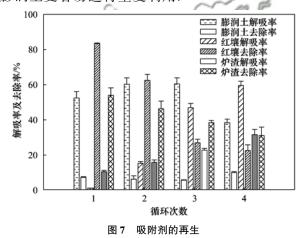


Fig. 7 Regeneration of the three adsorbents

3 结论

- (1) 炉渣对废水中磷的吸附能力强于膨润土和红壤, Langmuir 方程更适合描述 3 种材料的等温吸附过程, 最大理论饱和吸附量分别为炉渣 (16.87 $\text{mg}\cdot\text{g}^{-1}$) > 红壤 (1.21 $\text{mg}\cdot\text{g}^{-1}$) > 膨润土 (0.92 $\text{mg}\cdot\text{g}^{-1}$).
- (2)在不同的 pH 范围内(3.0~11.0),炉渣对磷都具有较高的去除率,而红壤在酸性条件下对磷的吸附效果较好;在 pH 为 7.0 时,膨润土对磷的吸附量最低.
- (3) 炉渣的 Ca^{2+} 的释放能力(11. 24 $mg \cdot g^{-1}$) 远大于膨润土(0. 31 $mg \cdot g^{-1}$) 和红壤(0. 02 $mg \cdot g^{-1}$).
- (4)较高的 Ca²⁺含量及稳定的 pH 范围是炉渣 对磷高效去除的主要机制,而含有较大阳离子交换 量的膨润土则需要改性才能提高其对磷的吸附 能力.
- (5)膨润土吸附饱和后磷的解吸效果优于红壤和炉渣,更容易重复利用.

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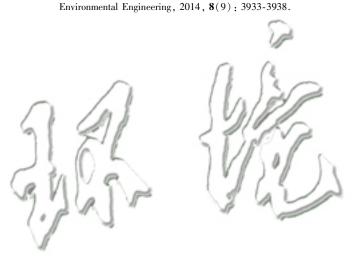
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CONTENTS

A Method of Aerosol Particle Number Size Distribution Inversed by PM _{2,5} Mass Concentration in PRD	on LI Qing-chun, LI Ju, ZHENG Zuo-iang, et al	. (515)
Light Absorption and Fluorescence Characteristics of Atmospheric Water-soluble Organic Compounds and Humic-like Substances Du		
Light Absolption and Photescence Characteristics of Atmospheric water-soluble Organic Compounds and Humic-like Substances Du	FAN Ying-ium VII Yu-fang CAO Tao et al	(532)
Source Apportionment and Heath Risk Quantification of Heavy Metals in PM _{2, 5} in Yangzhou, China	DONC Shi-hoo VIE Vong HUANCEU Von-gi et al	(540)
Pollution Characteristics and Source Analysis of <i>n</i> -alkanes and Saccharides in PM _{2.5} During the Winter in Liaocheng City	IIII Xiao di MENG ling iing HOII Zhan-fang et al	(548)
Pollution Characteristics Dry Denosition Fluxes and Sources for Atmospheric Polycyclic Aromatic Hydrocarbons in the Rosten Lake	e Watershed	
Tollution Characteristics, Dry Deposition Plaxes, and Sources for Athospheric Polycyclic Afonaute Trydiocarbons in the Dosten Law	SONC Shi iio HIJANC Too 7HAO Liu yuun et el	(558)
Distribution Characteristics of Antibiotic Resistance Genes in PM _{2, 5} of a Concentrated Broiler Feeding Operation	SONG SIII-JIE, HUANG 180, ZHAO LIU-yuan, et al	. (330) ! (567)
Effects of Water Vapor Source and Local Evaporation on the Stable Hydrogen and Oxygen Isotopic Compositions of Precipitation	LIU Fei, AU Ala, IU Bo-weii, et al	. (507)
Characteristics of Nitrogen and Phosphorus Formation in Atmospheric Deposition in Dianchi Lake and Their Contributions to Lake La		
Temporal-spatial Distribution of Nitrogen and Phosphorus Nutrients in Lake Taihu Based on Geostatistical Analysis	LU Wei-wei, YAU Ain, ZHANG Bao-hua, et al	. (390)
Effects of Cyanobacterial Blooms in Eutrophic Lakes on Water Quality of Connected Rivers		
Contamination and Potential Ecological Risk Assessment of Heavy Metals in the Sediments of Yilong Lake, Southwest China	LI Xiao-lin, LIU En-teng, YU Zhen-zhen, et al	. (614)
Temporal and Spatial Characteristics of Heavy Metals in Suspended Particulate Matter in Pearl River Estuary and Its Influencing Fac	ctors	. ((25)
	DU Jia, WANG Yong-hong, HUANG Qing-hui, et al	. (625)
Pollution Characteristics and Health Risk Assessment of Microorganism Pollutions in the Beiyun River	····· CHEN Lei, LI Lei-tang, ZHI Xiao-sha, et al	. (633)
Speciation and Transformation of Phosphorus in Sediments During the Redox Cycle		
Effect of Magnetic Zirconium/Iron-Modified Bentonite Addition on Phosphorus Mobilization and Species Transformation in River Sed	liments	•
	······ WANG Yan, LIN Jian-wei, ZHAN Yan-hui, et al	. (649)
Influence of Calcium Ion Pre-treatment on Phosphate Adsorption onto Magnetic Zirconium/Iron-modified Bentonite		
Effect of Nitrogen on Magnesium Modified Biochar Adsorption to Phosphorus	··· ZHI Meng-meng, WANG Peng-fei, HOU Ze-ying, et al	. (669)
Removal Performance and Mechanism for Treating Phosphorus in Agricultural Wastewater by Three Adsorbents Photolysis Mechanism of p-Nitrophenol by Nitrocellulose Membrane in Aqueous Solution	WU Lu, LIU Feng, LONG Rui, et al	. (677)
Photolysis Mechanism of p-Nitrophenol by Nitrocellulose Membrane in Aqueous Solution	· DAI Zhi-feng, ZHAO Tong-qian, YIN Yong-guang, et al	. (685)
Preparation of ZnTiO ₃ /TiO ₂ Photocatalyst and Its Mechanism on Photocatalytic Degradation of Organic Pollutants	···· ZHANG Wen-hai, JI Qing-hua, LAN Hua-chun, et al	. (693)
Adsorption and Photocatalytic Removal of Chromium on High-index TiO ₂ Facet	······ ZHONG De-jian, ZHANG Jian-feng, LI Yao, et al	. (701)
Reduction Cooperated Fenton Oxidation of Zero-valent Iron (ZVI) Immobilized in Alginate Microsphere for Degradation of Acid Red	d B	
	···· ZHANG Huan, LI Shuang-shuang, WEI Jun-fu, et al	. (708)
Mechanism of Removing Iron and Manganese from Drinking Water Using Manganese Ore Sand and Quartz Sand as Filtering Material	l ····· CAI Yan-an, BI Xue-jun, ZHANG Jia-ning, et al	. (717)
Preparation of Sulfonated Graphene Oxide Modified Composite Nanofiltration Membrane and Application in Salts Separation		
ZHA	ANG Yan-jun, ZHANG Shao-feng, ZHAO Chang-wei, et al	. (724)
Purification Efficiency and Mechanism of Integrated Al Salt Floc-ultrafiltration Membrane Process	XUE Wen-jing, LI Wen-jiang, LIU Juan, et al	. (730)
Threshold Flux and Membrane Fouling Analysis of the Hybrid Pre-ozonation and CNTs Membrane Modification Process		
Distribution and Removal of Polycyclic Aromatic Hydrocarbons and Their Derivatives in SBR/MBBR Process		
Biological Nitrogen Removal Process in a Microbubble-aerated Biotilm Reactor Treating Low C/N Wastewater	··· LIU Chun. WANG Cong-cong. CHEN Xiao-xiian. et al	. (/.)4)
Biological Nitrogen Removal Process in a Microbubble-aerated Biofilm Reactor Treating Low C/N Wastewater Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Reds Enhanced with Arbuscula	ar Mycorrhiza ·····	
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscula	ar Mycorrhiza ·····	
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscula	ar Mycorrhiza	· . (761)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer	ar Mycorrhiza	. (761) . (768)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer	ar Mycorrhiza	. (761) . (768) . (774)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer	ar Mycorrhiza	. (761) J. (768) J. (774) J. (783)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration	ar Mycorrhiza	. (761) L (768) L (774) L (783) L (791) L (799)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process Adjusting Temperature and Settling Time to Achieve ANAMMOX Particles Rapid Start-up and Stable Operation	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823) . (829) . (837)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process Adjusting Temperature and Settling Time to Achieve ANAMMOX Particles Rapid Start-up and Stable Operation Effect of C/N and Sludge Concentration on the pH-Regulated Nitrosation System	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823) . (829) . (837) . (845)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process Adjusting Temperature and Settling Time to Achieve ANAMMOX Particles Rapid Start-up and Stable Operation Effect of C/N and Sludge Concentration on the pH-Regulated Nitrosation System Growth Features of Water Supply Pipeline Biofilms Based on Active Microorganisms	ar Mycorrhiza The Mycorrhiza Song Tian-wei, SHENG Xiao-lin, WANG Jia-de, et al Song Tian-wei, SHENG Xiao-lin, WANG Jia-de, et al YU De-shuang, LÜ Ting-ting, CHEN Guang-hui, et al DU Shi-ming, YU De-shuang, DU Shi-ming, et al THAO Zhi-chao, HUANG Jian-ming, LI Jian, et al WEI Jia-min, JIANG Zhi-yun, CHENG Cheng, et al LI Tian, YIN Wen, WANG Xin-zhu, et al LI Dong, GAO Xue-jian, ZHANG Jie, et al LI Hai-ling, LI Dong, ZHANG Jie, et al ZHANG Min, WEI Jia-min, HUANG Hui-min, et al WANG Yang, ZHU Bin, TONG Jun, et al	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823) . (829) . (837) . (845) . (853)
Treatment of Simulated Saline Wastewater from the Coal Chemical Industry Using Ecological Floating Beds Enhanced with Arbuscular Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process Adjusting Temperature and Settling Time to Achieve ANAMMOX Particles Rapid Start-up and Stable Operation Effect of C/N and Sludge Concentration on the pH-Regulated Nitrosation System Growth Features of Water Supply Pipeline Biofilms Based on Active Microorganisms Elevational Distribution Characteristics of Soil Bacterial Community and Enzyme Activities in Mount Huangshan	ar Mycorrhiza Wen-qing, HE Hao, SONG Wen-ping, et al SONG Tian-wei, SHENG Xiao-lin, WANG Jia-de, et al WYU De-shuang, LÜ Ting-ting, CHEN Guang-hui, et al WEI Jia-ming, YU De-shuang, DU Shi-ming, et al WEI Jia-min, JIANG Zhi-yun, CHENG Cheng, et al UYe-qi, YU De-shuang, ZHEN Jian-yuan, et al LI Tian, YIN Wen, WANG Xin-zhu, et al LI Dong, GAO Xue-jian, ZHANG Jie, et al LI Hai-ling, LI Dong, ZHANG Jie, et al WANG Yang, ZHU Bin, TONG Jun, et al	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823) . (829) . (837) . (845) . (853)
Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process Adjusting Temperature and Settling Time to Achieve ANAMMOX Particles Rapid Start-up and Stable Operation Effect of C/N and Sludge Concentration on the pH-Regulated Nitrosation System Growth Features of Water Supply Pipeline Biofilms Based on Active Microorganisms Elevational Distribution Characteristics of Soil Bacterial Community and Enzyme Activities in Mount Huangshan Microbial Community Structure Shift during Bioremediation of Petroleum Contaminated Soil Using High Throughput Sequencing	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823) . (829) . (837) . (845) . (859)
Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process Adjusting Temperature and Settling Time to Achieve ANAMMOX Particles Rapid Start-up and Stable Operation Effect of C/N and Sludge Concentration on the pH-Regulated Nitrosation System Growth Features of Water Supply Pipeline Biofilms Based on Active Microorganisms Elevational Distribution Characteristics of Soil Bacterial Community and Enzyme Activities in Mount Huangshan Microbial Community Structure Shift during Bioremediation of Petroleum Contaminated Soil Using High Throughput Sequencing Effect of Nitrification on N ₂ O Emissions and Their Environmental Factors in Saline-alkali Wetlands	ar Mycorrhiza To DOU Wen-qing, HE Hao, SONG Wen-ping, et al. SONG Tian-wei, SHENG Xiao-lin, WANG Jia-de, et al. YU De-shuang, LÜ Ting-ting, CHEN Guang-hui, et al. BI Chun-xue, YU De-shuang, DU Shi-ming, et al. DU Shi-ming, YU De-shuang, BI Chun-xue, et al. KHAO Zhi-chao, HUANG Jian-ming, LI Jian, et al. WEI Jia-min, JIANG Zhi-yun, CHENG Cheng, et al. LI Tian, YIN Wen, WANG Xin-zhu, et al. LI Dong, GAO Xue-jian, ZHANG Jie, et al. ZHANG Min, WEI Jia-min, HUANG Hui-min, et al. WANG Yang, ZHU Bin, TONG Jun, et al. WANG Yang, ZHU Ghang-cheng, et al. QI Yan-yun, WU Man-li, ZHANG Huan-chao, et al. YANG Qu, GAO Wei-feng, LIU Feng-qin, et al.	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823) . (829) . (839) . (835) . (859) . (859) . (859) . (859)
Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process Adjusting Temperature and Settling Time to Achieve ANAMMOX Particles Rapid Start-up and Stable Operation Effect of C/N and Sludge Concentration on the pH-Regulated Nitrosation System Growth Features of Water Supply Pipeline Biofilms Based on Active Microorganisms Elevational Distribution Characteristics of Soil Bacterial Community and Enzyme Activities in Mount Huangshan Microbial Community Structure Shift during Bioremediation of Petroleum Contaminated Soil Using High Throughput Sequencing Effect of Long-term Dairy Manure Amendment on N ₂ O and NO Emissions from Summer Maize-Winter Wheat Cropping Systems	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823) . (829) . (837) . (845) . (853) . (859) . (859) . (869) . (876)
Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process Adjusting Temperature and Settling Time to Achieve ANAMMOX Particles Rapid Start-up and Stable Operation Effect of C/N and Sludge Concentration on the pH-Regulated Nitrosation System Growth Features of Water Supply Pipeline Biofilms Based on Active Microorganisms Elevational Distribution Characteristics of Soil Bacterial Community and Enzyme Activities in Mount Huangshan Microbial Community Structure Shift during Bioremediation of Petroleum Contaminated Soil Using High Throughput Sequencing Effect of Long-term Dairy Manure Amendment on N2O and NO Emissions from Summer Maize-Winter Wheat Cropping Systems	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823) . (829) . (845) . (853) . (859) . (859) . (859)
Nitrification and Bioaugmentation of Biological Treatment System of Sewage Treatment Plant at High Temperature in Summer Characteristics of Ammonia Adsorption and Kinetics by Nitrifying Sludge Immobilized Pellets Nitrite Accumulation Characteristics of Partial Denitrification in Different Sludge Sources Using Sodium Acetate as Carbon Source Operating Characteristics of a DPR-SNED System Treating Low C/N Municipal Wastewater and Nitrate-containing Sewage Simultaneous Nitrification and Denitrifying Phosphorus Removal in Continuous Flow Reactor with Intermittent Aeration Start-up and Stable Operation of ABR-MBR Denitrifying Phosphorus Removal Process Effect of Influent C/N Ratio on the Nutrient Removal Characteristics of SNEDPR Systems Carbon and Nitrogen Removal Characteristics of ABR Decarbonization-CANON Coupling Process Effect of Aeration Density on Start-up of CANON Process Adjusting Temperature and Settling Time to Achieve ANAMMOX Particles Rapid Start-up and Stable Operation Effect of C/N and Sludge Concentration on the pH-Regulated Nitrosation System Growth Features of Water Supply Pipeline Biofilms Based on Active Microorganisms Elevational Distribution Characteristics of Soil Bacterial Community and Enzyme Activities in Mount Huangshan Microbial Community Structure Shift during Bioremediation of Petroleum Contaminated Soil Using High Throughput Sequencing Effect of Long-term Dairy Manure Amendment on N ₂ O and NO Emissions from Summer Maize-Winter Wheat Cropping Systems Effects of Plastic Film Mulching and Nitrogen Fertilizer Application on N ₂ O Emissions from a Vegetable Field	ar Mycorrhiza	. (761) . (768) . (774) . (783) . (791) . (799) . (808) . (816) . (823) . (829) . (839) . (853) . (859) . (859) . (859) . (859) . (876)
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