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纳米零价铜活化分子氧降解水中恩诺沙星

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摘要:采用纳米零价铜(nanoscale zero-valent copper, nZVC)活化分子氧对水中恩诺沙星(enrofloxacin, ENR)的去除进行了系统研究. 通过表征可以发现,纳米铜粉比表面积高于微米级铜粉,无孔隙结构,表面粗糙且容易团聚. 纳米级 ZVC 活化分子氧的性能明显优于微米级 ZVC,这主要归因于其较大的比表面积,更容易被腐蚀. 通过探究活化机制可以发现,活化分子氧产生的 H_2O_2 和表面腐蚀产生的 Cu^+ 构成了新型类 Fenton 体系,持续释放的羟基自由基是造成水中 ENR 高效去除的主导活性物种;同时,反应过程中产生的超氧自由基能够促进 Cu^{2+} 还原成 Cu^+ ,从而加速 ENR 的去除过程. 反应条件对 nZVC 活化分子氧降解 ENR 有一定的影响,较高的 nZVC 投加量、较低 ENR 浓度、较高的反应温度以及强酸性条件均有利于 ENR 的去除.

关键词: 纳米零价铜(nZVC); 分子氧; 降解; 羟基自由基; 恩诺沙星(ENR)

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Nanoscale Zero-valent Copper-Activated Molecular Oxygen for the Degradation of Enrofloxacin in Water

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Abstract: Systematically studied the oxidation of enrolloxacin (ENR) in a nanoscale zero-valent copper (nZVC)-activated molecular oxygen system. The results show that nanoscale copper powder has a higher surface area than microscale copper powder, non-porous structure, and rough surface and exists in form of agglomerates. Nanoscale ZVC shows a superior activated performance toward molecular oxygen compared with microscale ZVC, which is due to its larger specific area and the fact that it corrodes easier. The H₂O₂ generated from the activation of molecular oxygen and the Cu⁺ released from surface corrosion form a novel Fenton-like system in which hydroxyl radicals are continuously produced, resulting in high-efficiency removal of ENR from water. The superoxide radicals produced during the reaction promote the reduction of Cu²⁺ to Cu⁺, thus speeding up the removal of ENR. The reaction conditions have a certain effect on the ENR degradation in nZVC-activated molecular oxygen systems. A higher nZVC dosage, lower ENR concentration, higher reaction temperature, and strong acidic conditions are favorable for the ENR removal.

Key words: nanoscale zero-valent copper(nZVC); molecular oxygen; degradation; hydroxyl radicals; enrofloxacin(ENR)

作为典型的氟喹诺酮类抗生素(FQs),恩诺沙星(enrofloxacin, ENR)是一种人工合成的广谱抗菌药,其广泛用于治疗动物的呼吸系统疾病和细菌感染^[1].由于 ENR 的广泛使用及其在动物体内的不完全代谢,大量残留的 ENR 通过动物排泄、畜牧业废水排放和垃圾渗滤等方式进入水环境^[2-4].水环境的自身规律决定了 ENR 将持续不断在水环境中进行迁移扩散,从而增加细菌的耐药性,对水生生态和人体健康构成潜在的危害^[5].目前在污水厂排水、地表水,甚至地下水中均检测到了 ENR 的存在,检出浓度从纳克级到微克级不等^[6-8].含 ENR的废水稳定性高、毒性大、可生化性差,很难通过传统的生物法去除,因此,寻求一种高效、安全、环保、节能的控制水中 ENR 的方法显得尤为重要.

分子氧是一种绿色环保、容易获取的氧化剂, 通过分子氧来降解有机污染物引起了国内外学者的 广泛兴趣. 然而,分子氧结构稳定、氧化能力弱, 不足以直接氧化降解有机污染物. 因此,通过还原能力强的零价金属活化分子氧产生活性氧(ROS)降解有机污染物受到研究者的青睐. 目前,常用于活化分子氧的零价金属有零价铁(ZVI)^[9]、零价铝(ZVAI)^[10]和零价铜(ZVC)^[11]等. Cao等^[12]考察了不同pH值对nZVI/Air体系去除四环素的影响,结果表明,在酸性条件下四环素的去除效果较好,而在中性或碱性条件下,四环素的去除效果显著下降. 该体系中有机物的去除主要依赖于类 Fenton 反应生成的·OH,其次与 ZVI 的吸附作用、还原作用及 Fe(IV)的生成有一定的关系. 虽然酸性条件下

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的 nZVI/Air 体系能广泛去除各种污染物,但由于表面容易形成钝化层等原因,ZVI 的反应活性不高,nZVAl/Air 体系也开发出来用于有机物的降解,Liu 等[13] 发现在 pH < 3.5 的酸性溶液中,ZVAl 能快速去除双酚 A,其原因是由于体系中 O_2 被 ZVAl 还原生成 H_2O_2 ,然后进一步转化成 \cdot OH^[10]. 与 ZVAl 和 ZVI 的酸性体系类似,ZVC 表面氧化释放 Cu^+ 和 Cu^2+ 是 H_2O_2 生成的关键因素, Cu^+/Cu^2+ 循环则是活化 H_2O_2 产生 \cdot OH的有效方法 [14].

目前,nZVC 对分子氧的活化机制和以 Cu⁺为催化剂的类 Fenton 氧化体系对抗生素的降解过程尚不清楚.本实验首先采用一系列手段对 nZVC 进行了表征,以确保实验的准确性.以 ENR 为目标污染物,建立了 nZVC/Air 酸性体系降解 ENR 的动力学模型,并考察了 nZVC 投加量、ENR 初始浓度、初始 pH 值和反应温度对 ENR 降解效果的影响.最后,通过自由基和活性铜物种鉴定等提出了 nZVC 活化分子氧的机制,以期为研发基于活化分子氧的水处理技术提供理论基础和技术支持.

1 材料与方法

1.1 材料与仪器

微米铜粉和溴化亚铜购自上海阿拉丁生化科技股份有限公司,纳米铜粉(≥99.9%,10~30 nm)、恩诺沙星(ENR,≥98%)和二氧化硅(50 mmol·L¹NaOH)购自上海麦克林生化科技股份有限公司,浴铜灵二磺酸二钠盐水合物和乙腈(色谱纯)购自上海 Sigma-Aldrich 化学品有限公司;其他试剂包括硫酸、氢氧化钠、亚硫酸钠、双氧水、草酸钛钾、叔丁醇(TBA)和磷酸等购自上海国药集团化学试剂有限公司.

1.2 分析方法

ENR 浓度采用 Agilent1200 型高效液相色谱仪 (HPLC)测定. 测定条件为:① 色谱柱为 XDB-C18 柱(4.5 mm × 150 mm × 5 μ m);② 流动相为 pH = 2.5 的磷酸溶液:乙腈 = 82%:18% (体积比);③ 流速为 1.0 mL·min $^{-1}$,柱温 35°C;④ 检测波长为 278 nm,进样体积为 10 μ L.

1.3 纳米铜粉表征

采用 X 射线衍射仪分析纳米铜粉的材料成分, X 射线衍射仪(XRD)由荷兰 PNAlytical 公司生产, 型号为 X'Pert PRO. 采用 X 射线荧光谱仪确定纳米铜粉的元素组成, X 射线荧光谱仪(XRF)由美国Thermo 公司生产, 型号为 ARL ADVANT'X. 采用高分辨透射电子显微镜(TEM)观测纳米铜粉的微观形貌, TEM 由荷兰 FEI 公司生产, 型号为 Tecnai G²

F30. 采用比表面积分析仪测定纳米铜粉的比表面积、孔容及孔径分布,比表面积分析仪由美国Micromeritics 公司生产,型号为 ASAP 2010.

1.4 实验方法

ENR 降解实验均在恒温水浴反应装置中进行. 除了研究 ENR 初始浓度这一影响因素外, 其它实验均采用 5 mg·L $^{-1}$ 的 ENR 溶液作为初始浓度进行. 反应之前使用 100 mmol·L $^{-1}$ 的硫酸或者氢氧化钠将 ENR 溶液的初始 pH 值调节至 3,然后取 100 mL 加入一系列 250 mL 广口棕色瓶并置于恒温水浴振荡器中,水温设定为 25 °C. 在一定的时间间隔内,用移液枪从各棕色瓶内取出 1 mL 样品,立即用 100 µL 的 $Na_2S_2O_3$ 溶液 (100 mmol·L $^{-1}$) 淬灭反应,然后使用 0.22 µm 醋酸纤维膜过滤,滤液用于进一步分析.

2 结果与讨论

2.1 纳米铜粉表征

图 I 是纳米铜粉的 XRD 衍射图谱, 衍射峰出现的位置为 43.35°、50.51°、74.17°、89.97°和95.21°, 与标准 XRD 数据库中 Cu 的衍射图谱(JCPDS-PDF:04-0836)高度一致. XRD 衍射图谱中未检测到其它峰,可认为商用纳米铜粉主要成分是Cu°. 此外, 还利用 XRF 分析了纳米铜粉的表面元素组成, 结果见表 1. 纳米铜粉表面 Cu 元素最多,质量分数达 99.35%, 其他的元素还有 Na、Mg、Ba、Ca、Cl 和 Cs 等, 质量分数分别为 0.256%、0.134%、0.068%、0.613%、0.058% 和 0.036%.因此,商用纳米铜粉几乎不含杂质,能保证本实验的准确性.

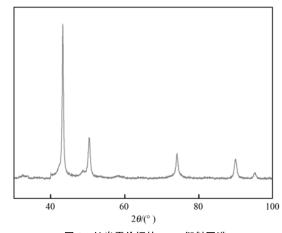


图 1 纳米零价铜的 XRD 衍射图谱 Fig. 1 XRD pattern of nZVC

采用 TEM 观测纳米铜粉的形貌,采用比表面积分析仪测定纳米铜粉的结构参数.由图 2和表 2可知,纳米铜粉的平均尺寸在 10~30 nm,表面粗

糙呈条纹状,比表面积为 9. 268 m²·g⁻¹,几乎无孔隙结构.铜粉大部分都团聚在一起,不易与反应底

物和活性点接触. 而微米级铜粉的比表面积为 $0.692 \text{ m}^2 \cdot \text{g}^{-1}$, 远低于纳米铜粉.

表 1 纳米零价铜的表面元素组成

| Table 1 | Surface | element | composition | of | nZVC |
|---------|---------|---------|-------------|----|------|
| | | | | | |

| 元素 | Cu | Na | Mg | Ba | Ca | Cl | Cs |
|--------|--------|--------|--------|-------|--------|----------|----------|
| 质量分数/% | 99. 35 | 0. 256 | 0. 134 | 0.068 | 0. 613 | 0. 057 9 | 0. 036 1 |

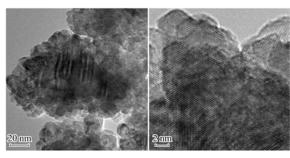


图 2 纳米铜粉的 TEM 图

Fig. 2 TEM images of nZVC

表 2 纳米零价铜的结构参数

Table 2 Structural parameters of ZVC and nZVC

| 样品 | 比表面积 /m²·g ⁻¹ | 孔容 /cm³·g ⁻¹ | 孔径/nm |
|------|-----------------------------|----------------------------|----------|
| 纳米铜粉 | 9. 268 | 0, 029 | 14. 255 |
| 微米铜粉 | 0. 692 | 0.003 | 117. 290 |

2.2 活化性能

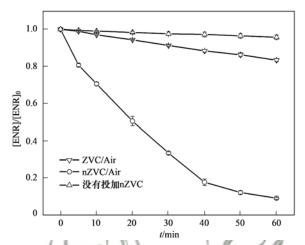
图 3 呈现了在不同反应体系下,作为目标污染物的 ENR 随反应时间的浓度变化规律. 其中, [ENR]。为 ENR 的初始浓度 (mg·L⁻¹), [ENR]为 ENR 在 t 时刻的浓度 (mg·L⁻¹), [nZVC]和 [ZVC]为催化剂的投加量 (g·L⁻¹).将没有投加 nZVC 的酸性 ENR 溶液 (pH = 3) 振荡 60 min,几乎没有 ENR 被去除,说明 ENR 结构稳定,不易被空气氧化. 在 ZVC/Air 和 nZVC/Air 酸性体系中,60 min内 ENR 的去除率分别为 16.6% 和 90.8%,其主要原因是 ZVC 和 nZVC 与 O_2 反应产生一系列的ROS,如 H_2O_2 、·OH等,这些 ROS 能够氧化水中有机污染物 [15].

ENR 在零价铜活化分子氧体系中的降解符合 拟一级反应动力学, 可表示为:

 $\ln([ENR]/[ENR]_0) = -k_{app}t$ (1) 式中, $k_{app}(\min^{-1})$ 为拟一级动力学常数; $t(\min)$ 为反应时间.nZVC/Air 体系的 k_{app} 值为 0. 040 \min^{-1} ,是 ZVC/Air 体系 k_{app} 值的 13. 4 倍,其催化性能的大幅提高可归因于 nZVC 较大的比表面积,可以提供更多的活性位点,更容易活化分子氧,促进 H_2O_2 的生成及 Cu^+ 、 Cu^2^+ 的释放[16].

2.3 活化机制

为了探究 nZVC 对分子氧的活化机制, 首先需

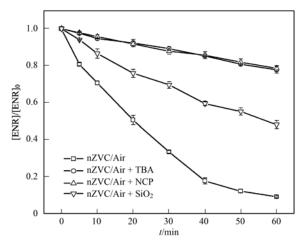


反应条件: [ENR] = 5 mg·L⁻¹, [nZVC] = [ZVC] = 0.5 mg·L⁻¹, pH = 3, T = 25°C

图 3 不同体系中 ENR 浓度随反应时间的变化 Fig. 3 Changes of the ENR concentrations with the reaction time in different systems

要鉴别该体系中的活性铜物种. 如图 4 所示, 将溶 解状态的 SiO, 和新亚铜试剂(NCP)分别用来确定 nZVC和 Cu⁺在体系中的作用,其主要原因是 SiO, 能吸附在 nZVC 表面,占据 nZVC 的活性位点,抑 制 nZVC 的活化性能, 而 NCP 能够选择性地螯合 Cu⁺, 抑制 Cu⁺的活化性能^[17]. 结果发现, ENR 的 去除率由 90.8% 分别下降到 51.8% 和 21.4%, 这 说明 nZVC 和 Cu⁺都参与到了 nZVC/Air 体系的反 应过程中, 但分工有所不同, Cu⁺直接参与 ENR 降 解,而 nZVC 可能对某些重要活性物质的生成起一 定作用但并未直接参与 ENR 降解. 此外, 还需要进 一步确定的是对降解反应起主导作用的 ROS^[17]. 实验通过分光光度法测定了 nZVC/Air 体系中不同 反应时间产生的 Cu^+ 和 H_2O_2 浓度^[18,19]. 如图 5 所 示, 反应体系中确实产生了 H,O,, 其浓度在 0.1~ 0.7 mmol·L⁻¹之间变化. 通过向反应体系中加入 100 mmol·L⁻¹叔丁醇(TBA)可以发现, ENR 的降解 受到了显著抑制,其去除率仅为22.2%(图4),这 说明·OH 是 nZVC/Air 体系的主导 ROS. Zhang 等^[20]还发现, nZVC/Air 体系中还存在大量的超氧 自由基 $(\cdot O_2^-)$, 它能够间接参与反应过程.

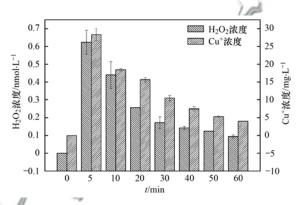
由以上结论并结合相关研究可分析出 nZVC 对分子氧的活化机制,其主要过程如图 6 所示. 在有



反应条件: $[ENR] = 5 \text{ mg} \cdot L^{-1}$, $[nZVC] = 0.5 \text{ g} \cdot L^{-1}$, $[TBA] = 0.5 \text{ mmol} \cdot L^{-1}$, $[NCP] = [SiO_2] = 1 \text{ mmol} \cdot L^{-1}$, pH = 3, T = 25 °C

图 4 不同自由基或铜离子抑制剂对 ENR 降解的影响

Fig. 4 Effect of different radical or copper scavengers on the ENR degradation



反应条件: [ENR] = 5 mg·L⁻¹, [nZVC] = 0.5 g·L⁻¹, pH = 3, T = 25 °C

图 5 nZVC/Air 体系中 H₂O₂ 和 Cu⁺浓度随时间的变化

Fig. 5 Variation of ${\rm H_2O_2}$ and ${\rm Cu^+}$ with the reaction time in an nZVC/air system

但促进了 Cu^{2+} 还原成 Cu^{+} 这一过程[式(7)]. 反应 系统中 Cu^{2+} 和 Cu^{+} 的循环确保了·OH的持续产生. ·OH直接攻击 ENR 分子,产生一系列的中间体和 降解产物[式(8)].

$$4Cu^{0} + O_{2} + 2H_{2}O \longrightarrow 4Cu^{+} + H_{2}O_{2} + 2OH^{-}$$
(2)

$$2Cu^0 + O_2 + 2H_2O \longrightarrow$$

$$2Cu^{2+} + H_2O_2 + 2OH^-$$
 (3)

$$Cu^{+} + H^{+} + H_{2}O_{2} \longrightarrow Cu^{2+} + \cdot OH + H_{2}O$$
 (4)

$$Cu^{2+} + H_2O_2 \longrightarrow Cu^+ + \cdot O_2^- + 2H^+ \qquad (5)$$

$$\cdot OH + H_2O_2 \longrightarrow \cdot O_2^- + H^+ + H_2O \qquad (6)$$

$$Cu^{2+} + \cdot O_2^- \longrightarrow Cu^+ + O_2 \tag{7}$$

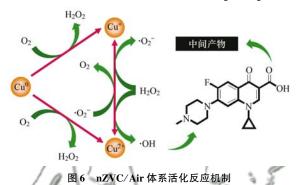


Fig. 6 Proposed activation mechanism in an nZVC/air system

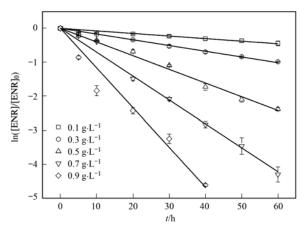
2.4 影响因素

2.4.1 nZVC 投加量

通过设定 nZVC 投加量分别为 0.1、0.3、0.5、0.7 和 0.9 g·L⁻¹,在其他基准条件相同的情况下考察 nZVC 投加量对 nZVC/Air 体系降解 ENR 的影响. 如图 7 所示,ENR 的去除率随 nZVC 投加量的增加而提高. 当 nZVC 投加量为 0.1 g·L⁻¹时,反应 60 min 后 ENR 的去除率仅为 35.7%;但当 nZVC 投加量增加到 0.9 g·L⁻¹时,反应 40 min 后 ENR 就能够完全去除. 从动力学角度看,随着 nZVC 投加量从 0.1 增加到 0.9 g·L⁻¹,相应地 $k_{\rm app}$ 值也从 0.008 提高至 0.117 min⁻¹. 当更多的 nZVC 加入到反应体系中,会有更多的分子氧被活化,产生的更 8 H₂O₂ 并释放大量 8 Cu⁺,因此,生成的大量 8 ROS 能够显著提高 8 ENR 的降解速率 8 [20].

2.4.2 ENR 浓度

通过设定目标污染物 ENR 的浓度为初定浓度 $(5 \text{ mg} \cdot \text{L}^{-1})$ 的 0.2、0.4、1、2 和 4 倍,在其他条件相同的情况下考察不同 ENR 浓度对 nZVC/Air 体系降解 ENR 的影响,实验结果见图 $8. \text{ 显然,随着ENR 浓度的增加,ENR 降解受到的抑制作用增强.} <math>1 \text{ mg} \cdot \text{L}^{-1}$ 的 ENR 只需 $40 \text{ min 就能被完全去除,相$

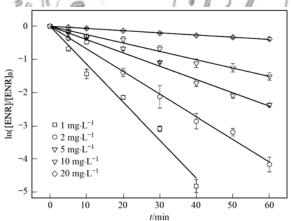


反应条件: $[ENR] = 5 \text{ mg} \cdot L^{-1}$, $[nZVC] = 0.1 - 0.9 \text{ g} \cdot L^{-1}$, pH = 3, $T = 25 \text{ }^{\circ}\text{C}$

图 7 nZVC 投加量对 ENR 降解的影响

Fig. 7 Effect of the nZVC dosage on the ENR degradation

应地 $k_{\rm app}$ 值为 0. 115 min ⁻¹. 而当 ENR 浓度升至 20 mg·L⁻¹, 30 min 内 ENR 的去除率仅为 31. 8%,同时 $k_{\rm app}$ 值降至 0. 007 min ⁻¹. 在 nZVC 投加量和反应环境相同的情况下,nZVC/Air 体系中产生的 ROS数量是相同且有限的,当 ENR 浓度增加到超过体系降解能力时就会限制部分 ENR 的去除,从而使去除率和 $k_{\rm app}$ 值降低. 此外,ENR 降解产生的有机中间体会与 ENR 分子竞争有限的 ROS,因此,降低了高浓度 ENR 的反应速率^[23].



反应条件: [ENR] = 1-20 mg·L⁻¹, [nZVC] = 0.5 g·L⁻¹, pH = 3, T = 25 °C

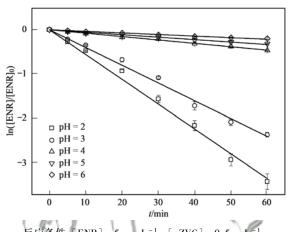
图 8 ENR 浓度对 ENR 降解的影响

Fig. 8 Effect of the ENR concentration on the ENR degradation

2.4.3 初始 pH 值

调节溶液初始 pH 值分别为 2、3、4、5 和 6,在 其他条件相同情况下进行实验研究,考察不同初始 pH 值对 nZVC/Air 体系降解 ENR 的影响(图 9). 随着初始 pH 值的增加,ENR 去除率和 k_{app} 值均出现了不同程度地下降,这种趋势与 Wen 等[11]的研究结果相似. 当初始 pH 值在 2~3 之间时,ENR 能够被迅速去除,相应地去除率分别为 96.8% 和

90.8%. 当初始 pH 值在 $4 \sim 6$ 之间时,ENR 的降解受到的抑制作用急剧增强,相应地去除率仅有 37.3%、27.3% 和 18.1%. 反应溶液的酸性越强,nZVC/Air 体系的氧化能力越强,其原因可以归因于以下 3 个方面:① 反应过程会不断消耗 H^+ ,用于 H_2O_2 的形成和氧化反应的进行 [24];② 高浓度的 H^+ 可以促进 nZVC 表面氧化层的腐蚀,从而促进铜离子的释放 [11];③ 体系中·OH/ H_2O 氧化还原电子对的氧化电动势随 pH 值的提升而减弱,这意味着在酸性条件下会生成更多的·OH [25]. 因此,nZVC/Air 体系在应用于有机污染物的去除时需要严格的酸性条件以保证反应的高效性.



反应条件:[ENR] = 5 mg·L⁻¹, [nZVC] = 0.5 g·L⁻¹, pH = 2 ~ 6, T = 25℃

图9 初始 pH 值对 ENR 降解的影响

Fig. 9 Effect of the initial pH on the ENR degradation

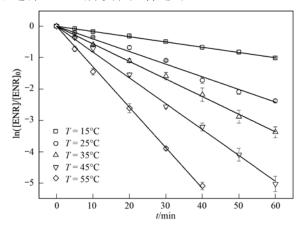
2.4.4 反应温度

在其他反应条件相同的情况下,调节 nZVC/Air 体系的反应温度分别为 15、25、35、45 和 55℃,考察不同反应温度对 ENR 降解速率的影响,结果如图 10 所示. 随着反应温度的升高,nZVC 的催化活性迅速增强. 当反应温度从 15℃增加到 55℃时,ENR 的去除率从 60 min 内的 63.9%增加到 40 min 内几乎完全去除,相应的 $k_{\rm app}$ 值也从 0.017 min ⁻¹提高到 0.129 min ⁻¹. 此外, $\ln k_{\rm app}$ 和 1/T 存在着线性关系,且这种线性关系可以用阿仑尼乌斯方程描述(图 11) ^[26]:

$$\ln k_{\rm app} = -\frac{1}{RT}E_{\rm a} + \ln A \tag{8}$$

式中, k_{app} 为降解速率常数(\min^{-1}),R 为理想气体常数[$8.314 \text{ J·}(\text{mol·K})^{-1}$],T 为温度(\mathbb{C}), E_a 为活化能(J·mol^{-1}). 从拟合方程的斜率可以计算出 $E_a = 37.95 \text{ kJ·mol}^{-1}$. 高温条件可以为反应物分子提供大量能量,使分子的动能增加,溶液中的 H_2O_2 与 Cu^+ 、 Cu^2+ 的碰撞更剧烈,从而产生更多的·OH,

对 ENR 的去除有利^[27]. 综上所述, 高温条件能促进反应, 但综合 ENR 降解速率和成本来看, 在常温下进行 ENR 去除实验是合适的.



反应条件: [ENR] = $5 \text{ mg} \cdot \text{L}^{-1}$, [nZVC] = $0.5 \text{ g} \cdot \text{L}^{-1}$, pH = 3, $T 为 15 \sim 55 ^{\circ}\text{C}$

图 10 反应温度对 ENR 降解的影响

Fig. 10 Effect of the reaction temperature on the ENR degradation

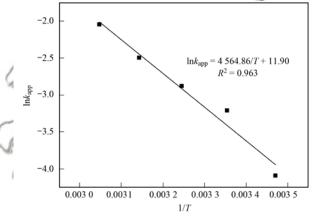


图 11 lnk_{app} 和 1/T 的拟合曲线

Fig. 11 $\,$ Fitting curve for ${\rm ln}k_{\rm app}$ and 1/T

3 结论

- (1)采用 XRD、XRF、TEM 和 BET 等方法对纳 米铜粉进行表征. 测试结果表明, 纳米铜粉比表面 积高于微米级铜粉, 无孔隙结构, 表面粗糙且容易 团聚.
- (2) nZVC 活化分子氧的效果优于 ZVC, 其原因是 nZVC 具有较大的比表面积, 更容易被腐蚀, 释放出大量的 Cu⁺和 Cu²⁺, 促进 H₂O₂ 的生成, 增加·OH的产量.
- (3)较高的 nZVC 投加量、较低 ENR 浓度、较高的反应温度以及酸性条件有利于 ENR 的降解.
- (4) nZVC 能与 O_2 反应生成 H_2O_2 , 并释放大量 Cu^+ 和 Cu^{2+} , Cu^+ 与 H_2O_2 构成类 Fenton 体系, 生产出大量·OH直接参与 ENR 降解; 而体系中产生的· O_7 不直接参与反应, 但促进了 Cu^{2+} 还原成

Cu⁺这一过程.

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