

(HUANJING KEXUE)

ENVIRONMENTAL SCIENCE

第37卷 第3期

Vol.37 No.3

2016

中国科学院生态环境研究中心 主办

科学出版社出版



新始章 (HUANJING KEXUE)

ENVIRONMENTAL SCIENCE

第37卷 第3期 2016年3月15日

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. Noting # 1 Noting

复合催化膜生物反应器处理一氧化氮废气研究

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摘要:采用溶胶-凝胶法以聚砜(PSF)中空纤维膜为载体制备了 Fe-TiO₂/PSF 复合催化膜,以此构建新型复合催化膜生物反应器(HCMBR),实现膜催化与硝化反硝化耦合烟气脱硝,进一步提高 NO 去除能力. 采用 Fe-TiO₂/PSF 复合催化膜生物反应器(HCMBR)处理一氧化氮废气,实现了 180 d 长时间高效稳定运行, NO 去除效率可达 93.2%,去除能力可达 167.1 $g \cdot (m^3 \cdot h)^{-1}$. 适宜运行条件为:气体停留时间 $g \cdot (m^3 \cdot h)^{-1}$. 适宜运行条件为 $g \cdot (m^3 \cdot h)^{-1}$.

关键词:复合催化膜生物反应器;生物降解;光催化;一氧化氮;硝化反硝化

中图分类号: X701 文献标识码: A 文章编号: 0250-3301(2016)03-0847-07 **DOI**: 10.13227/j. hjkx. 2016. 03.008

Nitric Oxide Removal with a Fe-TiO₂/PSF Hybrid Catalytic Membrane Bioreactor

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Abstract: The Fe-doped titanium dioxide (Fe-TiO₂) was prepared by the sol-gel method and was loaded on polysulfone (PSF) hollow fiber membrane. A novel Fe-TiO₂/PSF hybrid catalytic membrane biofilm reactor (HCMBfR) was investigated for nitric oxide removal, to further improve the elimination capacity. HCMBfR exhibited a good stability in the 180-day operation period, the NO removal efficiency was up to 93.2% and the maximum elimination capacity reached 167.1 g·(m³·h)⁻¹. The additional use of the biofilm to wet Fe-TiO₂/PSF membrane catalysis reactor led to the enhancement of NO removal efficiency from 59.5% to 66%. The NO removal efficiency in the intimate coupling of Fe-TiO₂/PSF hybrid catalytic membrane and biofilm reactor (HCMBfR) increased from 1.4% to 13% as compared to that of the membrane biofilm reactor (MBfR) only. The optimal illumination intensity, gas residence time, pH and nC/nN were 670 lx, 9 s, 6.8-7.2 and 3.7, respectively.

Key words: hybrid catalytic membrane biofilm reactor; biodegradation; photocatalytic oxidation; NO; nitrification/denitrification

氮氧化物是形成酸雨、光化学烟雾污染和城市灰霾天气等环境问题的主要污染物. 2014 年我国氮氧化物排放总量已高达2 078万 t. 我国东部地区二氧化氮浓度增加量明显高于世界其他地区,已经成为全球对流层二氧化氮污染最严重的地区之一. 国家《"十二五"环保规划》和《重点区域大气污染防治"十二五"规划》提出氮氧化物排放总量削减 10%以上的约束性指标[1]. 现有的烟气脱硝技术中选择性催化还原(SCR)法所使用的复合催化膜价格昂贵、运行费用高,而生物法具有运行费用低、无二次污染及易于管理等优点已成为研究热点[2]. 因此,研究新型膜生物反应器烟气脱硝技术及机制有重要的科学意义和现实意义.

生物法脱硝可分为硝化烟气脱硝作用、反硝化烟气脱硝作用.采用生物过滤器和生物滴滤器硝化氧化一氧化氮^[3,4].利用脱氮菌在厌氧或缺氧的条件下,将 NO, 还原为无害的 N₂^[5],用反硝化去除烟

气中 NO^[6]. 在有氧条件下采用生物滤池、生物滴滤塔等好氧反硝化菌脱除 NO_x 气体^[7]. 在 50℃±1℃高温生物滴滤塔好氧反硝化处理氮氧化物^[8]. NO 去除过程属传质控制,限制了生物降解速率,为强化气液 NO 传质,采用化学络合吸收耦合生物还原法去除氮氧化物^[9],但络合物再生困难. 膜生物反应器是目前最具发展潜力的废气处理方法之一,膜材料能提高一氧化氮气体传质速率,提供较大的比表面积作为生物降解的传质界面. 采用中空纤维膜生物反应器处理一氧化氮,硝化/反硝化高效去除NO^[10,11]. 采用负载型 TiO₂光复合催化膜进行同时脱硫脱硝的实验研究^[12]. 虽然已有开展基于中空

收稿日期: 2015-07-25; 修订日期: 2015-10-14

基金项目: 国家自然科学基金项目(21377171);中央高校基本科研

业务费专项

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纤维膜的光催化降解废水中污染物^[13]和膜生物反应器处理 NO 废气的研究,但未见复合催化膜生物反应器处理氮氧化物废气报道.本研究的复合催化膜生物反应器 (hybrid catalytic membrane biofilm reactor, HCMBfR)烟气脱硝是利用复合膜催化和膜生物反应器厌氧好氧条件,实现膜催化与硝化反硝化耦合烟气脱硝,进一步提高 NO 去除能力.本研究构建 Fe-TiO₂/PSF 复合催化膜生物反应器,进行HCMBfR 处理一氧化氮废气,考察其长时间运行稳定性、研究影响因素,进一步提高 NO 去除能力,以期为复合催化膜生物反应器净化氮氧化物废气技术的应用奠定基础.

1 材料与方法

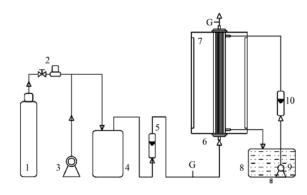
1.1 Fe-TiO₂/PSF 复合催化膜的制备

以聚砜中空纤维膜(PSF)为载体,溶胶-凝胶法 制备的 Fe-TiO, 溶胶,采用浸渍法制备 Fe-TiO,/PSF 复合催化膜. 采用溶胶-凝胶法制备 TiO,,即以钛酸 丁酯[Ti(OC,H,),]作为钛源,使用无水乙醇为溶 剂,冰醋酸为反应抑制剂,并以 Fe 过渡金属元素为 TiO₂ 表面改性的掺杂离子; 取 50 mL 钛酸丁酯溶于 350 mL 无水乙醇,加入 20 mL 冰乙酸,用磁力搅拌 器搅拌 45 min, 得溶液 A; 取 30 mL 浓度为 0.1% 的 Fe(NO₃),溶液溶于150 mL 无水乙醇,加入20 mL 冰乙酸,得溶液 B; 在 2 h 的时间内,一边用磁力搅 拌器搅拌,一边将 B 溶液逐滴加入 A 溶液中; 最后 在室温下用磁力搅拌器搅拌 24 h,使其形成 Fe-TiO。 溶胶. 采用浸渍法使 Fe-TiO, 溶胶与聚砜中空纤维 膜充分接触,使其匀称地负载在膜丝外表面,然后将 中空纤维膜置于60℃的恒温烘箱中干燥5h后,即 可得到 Fe-TiO,/PSF 复合催化膜.

1.2 实验装置与方法

Fe-TiO₂/PSF 复合催化膜生物反应器处理一氧化氮废气的流程如图 1 所示. 复合催化膜生物反应器为自制的 Fe-TiO₂/PSF 复合催化膜,外壁为透明有机玻璃管,聚砜 (PSF)中空纤维膜组件平均膜孔径 0.15 μm,膜纤维内/外径 0.38 mm/0.52 mm,纤维膜根数2 400根,膜孔隙率 60%,单根纤维膜有效长度 300 mm. NO 废气采用动态法配制,NO 气体与电磁式空气压缩机空气混合后从器底进入复合催化膜生物反应器,在上升的过程中 NO/空气混合气体由中空纤维膜内扩散传质至膜外的 Fe-TiO₂/PSF 复合催化膜、生物膜表面,与催化膜、湿润生物膜接触被微生物降解,净化后的气体从器顶排出. 实验

在常温(16~35℃)下进行,采用逆流操作,循环液体从复合催化膜生物反应器顶向下喷淋,在中空纤维膜外自上向下流动,由底排出至循环液储槽,再由循环潜水泵抽回复合催化膜生物反应器顶,定期向循环液贮存器投加氮磷营养液,维持微生物的生长繁殖活动.



NO 气瓶; 2. 质量流量计; 3. 空气压缩机; 4. 气体混合瓶;
 转子流量计; 6. 中空纤维膜组件; 7. 光源; 8. 混合液循环池; 9. 潜水泵; 10. 玻璃转子液体流量计; G. 采样口

Fig. 1 Schematic diagram of Fe-TiO $_2$ /PSF HCMBfR for NO removal

1.3 分析方法

NO 气体浓度采用德国 TESTO Pro-350 烟气分析仪进行测定,测量范围为 0~1000×10⁻⁶;气体流量用 LZB 型玻璃转子流量计测定,测量范围为 0.1~2.0 L·min⁻¹. 紫外光的照射强度由香港希玛 AR823 型分体式照度计测量,测量范围为 1~10000 lx.

2 结果与分析

2.1 复合催化膜生物反应器运行稳定性

在NO进气负荷为23.3~200 g·(m³·h)⁻¹,自然光光照强度为620~700 lx,喷淋密度为42.4~84.7 mL·(m²·min)⁻¹,pH为6.8~7.2,C/N摩尔比为2.5~4.0 的条件下,Fe-TiO₂/PSF 复合催化膜生物反应器处理一氧化氮废气的长时间运行稳定性如图2所示.长时间运行主要分为Ⅰ、Ⅱ、Ⅲ这3个阶段. Ⅰ阶段为挂膜阶段(第1~20 d),NO进气负荷设置为较低的40 g·(m³·h)⁻¹,喷淋密度设置为42.4 mL·(m²·min)⁻¹,第1 d NO 去除效率为50%左右,这主要是中空纤维膜分离和Fe-TiO₂/PSF 复合催化膜去除NO的作用;随着时间的推移,中空纤维膜上附着硝化菌反硝化菌,生物降解NO作用稳步上升,第11 d NO 去除效率可达81.4%,第17

~20 d, 生物膜进入稳定期, NO 去除效率可达 84%. Ⅱ阶段为微生物驯化及生物膜强化阶段(第 21~112 d),第 21~39 d 进气负荷下调到了 25 g·(m³·h)⁻¹,使反应器平稳运行,NO 去除效率为 83.6%~90.2%; 第40~55 d 进气负荷提高到60 $g \cdot (m^3 \cdot h)^{-1}$, NO 去除效率上升至 85.7% ~93.2%, 最大可达93.2%; 第56~72 d 进气负荷提升至100 g·(m³·h)⁻¹,NO 去除效率略有下降,稳定在84.9% ~90.7%. 第73~92 d 进气负荷增加至125 g·(m³·h)⁻¹,NO 去除效率明显下降至 81.1%,第 75 d NO 去除率有所回升至 84.1%,最高可达 88.1%. 第 93~112 d 进气负荷继续增加至 150 g·(m³·h)⁻¹,NO 净化效率从 77.9% 逐渐提升至 85.7%, 去除负荷可达 130.8 g·(m³·h) -1. 通过进 气负荷的逐步提高,微生物成功驯化,在 Fe-TiO₃/ PSF 复合催化膜表面已形成具有一定抗冲击负荷的 生物膜,实现了生物降解与膜催化耦合去除 NO 废 气作用. Ⅲ阶段为高负荷运行阶段(第113~180 d),考察反应器在受到高进气负荷的冲击时长时间 运行稳定性. 第 113 d NO 进气负荷提升至 200 g·(m³·h)⁻¹, NO 去除效率由 83.9% 下降至 75.1%, 然后稳定在77%左右. 当进气负荷为

214.3 g·(m³·h) ⁻¹时,NO 去除效率为 78%,去除负荷可达 167.1 g·(m³·h) ⁻¹. 与一般的光催化、中空纤维膜生物反应器处理 NO 的方法 $^{[10,11,14]}$ 相比,使用 Fe-TiO₂/PSF 复合催化膜生物反应器能够提高 NO 去除能力,具有更好的工业应用前景.

复合催化膜生物反应器的烟气脱硝是利用膜传 质、复合膜催化和膜生物反应器,实现膜催化与硝 化反硝化耦合烟气脱硝. 首先是 NO 和氧气与 Fe-TiO₂/PSF 复合催化膜接触,气体产生的浓度梯度使 气体在中空纤维膜中向前扩散,NO 和氧气由膜的 另一侧脱附出去至 Fe-TiO₂/PSF 复合催化膜,光催 化产生羟基自由基和超氧负离子,NO 气体被羟基 自由基和超氧负离子氧化成易生物降解的 NO₂ 和 HNO; 然后光催化产生的物质与未反应的 NO 进入 生物膜; 氧气进入复合膜生物反应器中的生物膜中 依次形成好氧区、缺氧区或厌氧区发生同时硝化反 硝化; 在好氧区 NO 被亚硝化细菌氧化成 NO2,进 而被硝化细菌氧化 NO;;在缺氧区或厌氧区,反硝 化细菌的同化反硝化还原成有机氮化物,成为菌体 的一部分,异化反硝化转化为 No; 硝化产物可作为 反硝化的底物,硝化与反硝化在生物膜相完成,实现 膜催化与同时硝化反硝化耦合烟气脱硝.

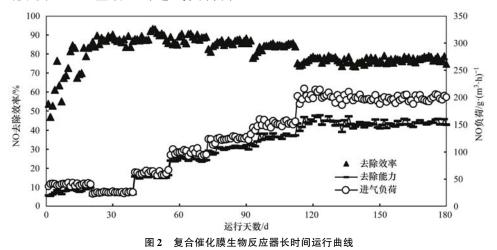


Fig. 2 Long-term operation curves of the HCMBR

2.2 进气负荷对 NO 去除效率的影响

在气体停留时间为 9.0 s, 自然光光照强度为 620 ~ 700 lx, 喷淋密度为 84.7 mL·(m²·min) $^{-1}$, pH 为 6.8 ~ 7.2 的条件下,进气负荷对 NO 去除效率的影响如图 3 所示. 在复合催化膜生物反应器内,较低的进气负荷为 27.5 ~ 95.7 g·(m³·h) $^{-1}$ 时, NO 去除效率变化小,为 89.3% ~ 88.8%,去除负荷从 24.6 g·(m³·h) $^{-1}$ 提升到 85.2 g·(m³·h) $^{-1}$; 但当进气负荷从 128.2 g·(m³·h) $^{-1}$ 到 193.3 g·(m³·h) $^{-1}$

时,NO 去除效率逐渐降低,去除负荷从 111.4 g·(m³·h) ⁻¹ 提升到 160.8 g·(m³·h) ⁻¹,提高了 49.4 g·(m³·h) ⁻¹. 当进气负荷为 193.3 g·(m³·h) ⁻¹时,NO 去除效率为 78%. 随着 NO 进口负荷的增加,HCMBfR、聚砜中空纤维膜生物反应器 (MBfR)、湿式 Fe-TiO₂/PSF 复合催化膜(WMCR)对 NO 去除效率都逐渐下降. 当 NO 的进气负荷 27.5 g·(m³·h) ⁻¹, WMCR 对 NO 去除效率 只有 25.7%, MBfR 对 NO 去除效率为 87.9%,

HCMBfR 对 NO 去除效率为 89.3%. 当 NO 的进气负荷增加至 193.3 g·(m³·h) -1, WMCR 对 NO 去除效率只有 18.5%, MBfR 对 NO 去除效率为 65%, HCMBfR 对 NO 去除效率为 78%. Fe-TiO₂/PSF 复合催化膜加入,复合催化膜生物反应器去除 NO 的效率比膜生物反应器提高了 1.4% ~13%. 在 Fe-TiO₂/PSF 复合催化膜附着稳定的生物膜后,复合催化膜生物反应器去除 NO 的效率比湿式膜催化反应器提高了 59.5% ~66%,催化降解脱硝量高13.6%. 复合催化膜生物反应器的湿式膜催化和生物的耦合作用能提高对 NO 去除能力.

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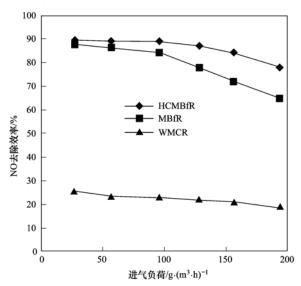


图 3 进气负荷对 NO 去除效率的影响

Fig. 3 Influence of the inlet load on NO removal

2.3 气体停留时间对 NO 去除效率的影响

复合催化膜生物反应器的停留时间以膜的容积 即参与反应的膜的容积计算[15],以膜的容积计算 NO 气体停留时间, 进气速率为 0.32 ~ 0.8 L·min⁻¹,相应的气体停留时间为 6.7~16.8 s. 在 NO 进气负荷为 83. 8 g·(m³·h) -1, 自然光光照强度 为620~700 lx, 喷淋密度为84.7 mL·(m²·min)⁻¹, pH 为 6.8~7.2, C/N 摩尔比为 2.5~4.0 的条件 下,气体停留时间对 NO 去除效率影响如图 4 所示. 当气体停留时间为 6.5~10.7 s 时, NO 去除效率随 气体停留时间的增加而升高,在6.5 s 时为76.6%, 在 10.7 s 时为 87.7%; 当气体停留时间从 10.7 s 增加到 16.8 s, NO 去除效率仅提高了约 2%. 中空 纤维膜虽能提高 NO 的传质速率,但气体停留时间 较短会影响在纤维膜层、催化层和生物膜层之间的 NO 传质、催化转化和生物降解效果; 气体停留时 间越长就越有利于 HCMBfR 对 NO 催化和生物降 解. Devahasdin 等^[16]和 Wang 等^[17]研究表明,光催化处理 NO 时转化速率随气体停留时间增加而增加的变化规律会在气体停留时间为 12~15 s 的时候停止,这是因为催化反应达到了动态平衡^[18,19]. 而这个动态平衡在 HCMBfR 中更短的停留时间内(9~12 s),催化反应和生物降解达到了动态平衡,湿式催化与生物降解耦合作用实现 NO 的高效转化.

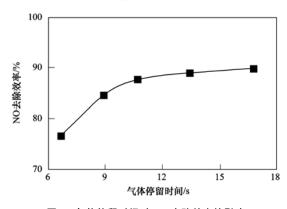


图 4 气体停留时间对 NO 去除效率的影响

Fig. 4 Influence of gas residence time on NO removal

2.4 光源对 NO 去除效率的影响

在气体停留时间为9.0 s,光照强度为620~700 lx,喷淋密度为84.7 mL·(m²·min)⁻¹,pH 为 6.8 ~ 7.2,C/N 摩尔比为 2.5~4.0 的条件下,进行了自然 光(VL)、紫外光(UV)照射下以及黑暗(Dark)运行 情况下 Fe-TiO₂/PSF 复合催化膜生物反应器处理一 氧化氮废气的实验,考察光源对 NO 去除效率的影 响如图 5 所示. 在进气负荷为 26.1~193.3 g·(m³·h) -1范围内,紫外光照射下复合催化膜生物 反应器 NO 去除效率略高于自然光光照下复合催化 膜生物反应器 NO 去除效率,约为 2.6% ~ 6.1%. 当 NO 进气负荷为 95.7 g·(m³·h) -1 时,自然光湿式 膜催化 NO 的效率为 23%,非光条件下湿式膜催化 NO 的效率为 16%; 膜生物反应器非光照、自然光 光照下 NO 去除效率分别为 78%、84.1%;复合催 化膜生物反应器非光照、自然光和紫外光光照下 NO 去除效率分别为 81.4%、89%、91.1%; 因此 在非光照条件下,复合催化膜生物反应器去除 NO 的效率比膜生物反应器提高了 3.4%, 这说明 Fe-TiO₂/PSF 复合催化膜加入,非光照光催化 NO 效率 为零,但 Fe-TiO,仍有一定的催化作用. 自然光波长 在 400~780 nm 之间,紫外光波长在 10~400 nm 之 间,物体吸收入射光的效率与光波波长呈反相关关 系^[20]. 短波照射在复合催化膜吸附 NO 后能激发更 高能量的电子-空穴对,增强电子的还原性和空穴的

氧化性,更易于在 Fe-TiO₂ 复合催化膜表面产生活性基团,使 HCMBfR 的催化步骤更快达到动态平衡的状态. 紫外线虽对微生物有一定的杀菌作用,但若控制好其光照强度(620~700 lx),再加上HCMBfR 的循环液回流系统,生物膜更新速度快,并不会对生物相造成太大的冲击.

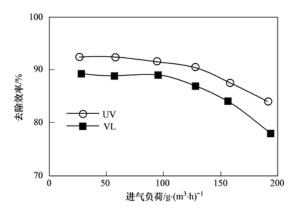


图 5 不同光源对 NO 去除效率的影响

Fig. 5 Influence of different light sources on NO removal

2.5 光照强度对 NO 去除效率的影响

光照强度改变时,单位时间和单位面积内中空纤维膜复合催化膜表面接受的光能量不同,因此会影响 Fe-TiO₂/PSF 膜催化速率,进而影响到复合催化膜生物反应器处理 NO 的效果. 在气体停留时间为 9. 0s,喷淋密度为 84. 7 mL·(m²·min) -1, pH 为 6. 8 ~ 7. 2, C/N 摩尔比为 2. 5 ~ 4. 0 的条件下,自然光光照强度对 NO 去除效率影响如图 6 所示. 随着进气负荷增加,NO 去除效率逐渐下降;在进气负荷为 25. 1 ~ 189. 7 g·(m³·h) -1 范围内,自然光光照强度由 320 lx 增大到5 430 lx,NO 去除效率提高了 1. 9% ~ 5. 7%;自然光光照强度由 320 lx 增大到5 430 lx (即增大 17 倍),NO 去除效率提高了 4. 4% ~

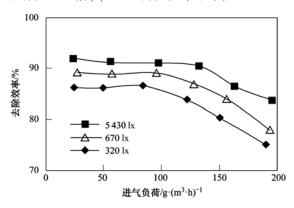


图 6 光照强度对 NO 去除效率的影响

Fig. 6 Influence of illumination intensity on NO removal

8.5%,提高的幅度较小. 光照强度对 HCMBfR 的影响主要体现在对 Fe-TiO₂/PSF 复合催化膜相的影响,光照强度越高能够提供更多数量的电子-空穴对,强化 NO 的催化氧化步骤^[21],与生物降解协同作用,提高 NO 转化率.

2.6 pH 值对 NO 去除效率的影响

循环液 pH 值对复合催化膜生物反应器 NO 去 除效率有重要影响,会对硝化反硝化菌的生物活性 产生影响,从而对 NO-生物膜和 NO-液相两者的传 质过程都会产生影响. 在 NO 进气负荷为 83.8 g·(m³·h)⁻¹,气体停留时间为9.0 s,自然光光照强 度为 620 ~ 700 lx, 喷淋密度为 84.7 mL·(m²·min)⁻¹,C/N 摩尔比为 2.5~4.0 的条件 下,pH 值对 NO 去除效率的影响如图 7 所示. 随着 循环液的 pH 值升高, NO 去除效率先升高后下降; 当循环液中性偏酸 pH 值为 6.86 时,NO 去除效率 最高,可达到84.1%. 循环液pH偏低和偏高均会 对系统产生影响,如 pH 较低(2.95)时,NO 去除效 率为 68.7%, pH 较高(9.06)时, NO 去除效率为 80.1%. pH 对 Fe-TiO₂/PSF 复合催化膜生物反应器 的生物相产生影响,有研究表明[22,23],反硝化菌活 性最高,生长适宜 pH 范围为偏碱 7~9,而生物相降 解 NO 主要依靠生物膜中的硝化菌和反硝化菌的共 同作用,硝化菌生长适宜 pH 范围为 5~8. 为使生 物膜能充分实现同时硝化反硝化的作用,必须同时 满足硝化菌与反硝化菌对 pH 的要求,则满足系统 运行的 pH 值应控制为 6.8~7.2, 若循环液 pH 超过 这个范围,将抑制硝化菌和反硝化菌的活性和新陈 代谢,不利于同时硝化反硝化过程,进而影响到复合 催化膜生物反应器对 NO 的处理效果.

2.7 C/N 摩尔比(nC/nN)对 NO 去除效率的影响

在 NO 进气负荷为 83. 8 g·(m^3 ·h) $^{-1}$, 气体停留时间为 9. 0 s, 自然光光照强度为 620 ~ 700 lx, pH 为 6. 8 ~ 7. 2, 喷淋密度为 84. 7 mL·(m^2 ·min) $^{-1}$ 的条件

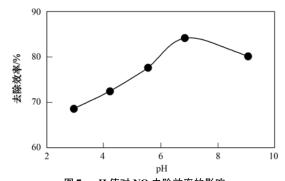


图 7 pH 值对 NO 去除效率的影响

Fig. 7 Influence of pH on NO removal

下,nC/nN 对 NO 去除效率的影响如图 8 所示. nC/nnN为COD/TN摩尔比. 随着 nC/nN的增加,NO去 除效率先升高后下降, 当 nC/nN 为 3.7 时, NO 去除 效率最高为85.3%,过高和过低的nC/nN比均不利 于复合催化膜生物反应器生物降解 NO. 在复合催 化膜生物反应器烟气脱硝系统内,反硝化菌为异养 菌,碳源不足会造成反硝化菌脱氮性能下降,因此循 环液必须保持—定的有机碳源. 在有机碳源保持— 定量(nC/nN) 为 $0.8 \sim 2.3$ 的条件下, 硝化菌的硝化 能力不会受到异养菌的影响,硝化速率随着碳源的 增加而增加,NO 去除效率升高,这是由于一定的碳 源保证了硝化细菌繁殖所需的营养物质; 但有机碳 源含量过高(nC/nN 为 5.2 以上)时,NO 去除效率 开始下降,这是由于碳源的过量造成异养菌的大量 繁殖,从而抑制了硝化细菌的正常代谢,导致硝化细 菌的硝化速率下降. 因此 HCMBfR 系统循环液应保 持合适的 nC/nN 比(2.5~4.0).

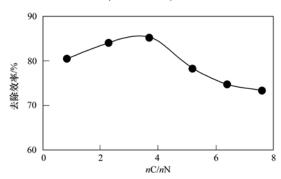


图 8 nC/nN 对 NO 去除效率的影响

Fig. 8 Influence of nC/nN on NO removal

3 结论

- (1)采用溶胶-凝胶法以聚砜(PSF)中空纤维膜为载体制备了 Fe-TiO₂/PSF 复合催化膜,以此构建新型复合催化膜生物反应器(HCMBfR),实现膜催化与硝化反硝化耦合烟气脱硝.
- (2)采用 Fe-TiO₂/PSF 复合催化膜生物反应器处理—氧化氮废气,实现了 180 d 长时间高效稳定运行,NO 去除效率可达 93.2%,去除能力可达 167.1 g·(\mathbf{m}^3 · \mathbf{h}) $^{-1}$. 适宜运行条件为:气体停留时间 9 s、自然光光照强度 670 lx,pH 为 6.8 ~ 7.2, nC/nN 为 3.7.
- (3) Fe-TiO₂/PSF 复合催化膜加入,复合催化膜生物反应器去除 NO 的效率比膜生物反应器提高了1.4%~13%,在 Fe-TiO₂/PSF 复合催化膜附着稳定的生物膜后,复合催化膜生物反应器去除 NO 的效率比湿式膜催化反应器提高了59.5%~66%.

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《环境科学》再获"百种中国杰出学术期刊"称号

2015年10月21日,中国科技论文统计结果发布会在北京举行,会议公布了"百种中国杰出学术期刊" 获奖名单.《环境科学》连续14次荣获"百种中国杰出学术期刊"称号."百种中国杰出学术期刊"是根据中国科技学术期刊综合评价指标体系进行评定.该体系利用总被引频次、影响因子、基金论文比、他引总引比等多个文献计量学指标进行统计分析,对期刊分学科进行评比,其评价结果客观公正,为我国科技界公认,并具有广泛影响.

HUANJING KEXUE

Environmental Science (monthly)

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(HUANJING KEXUE)

(月刊 1976年8月创刊) 2016年3月15日 第37卷 第3期

ENVIRONMENTAL SCIENCE

(Monthly Started in 1976)

Vol. 37 No. 3 Mar. 15, 2016

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中国标准刊号: ISSN 0250-3301 CN 11-1895/X

国内邮发代号: 2-821

国内定价:120.00元

国外发行代号: M 205

国内外公开发行