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目 次

深圳大气颗粒物中卤代多环芳烃污染研究 ····································	
	3)
北京市曲刑祭协众 JU VOC 批讲性红斑穴 出版 和蛙目 何下達 化块芒 耳石 公太鄉 迷溪(152	2)
北京中央望食队企业 VOUS 排放付证明九	(3)
2006~2010 年珠三角地区 SO ₂ 特征分析	80)
环境空气 PM、连续监测系统手工采样比对测试 ·························· 王强、钟琪、迟颖、张杨、杨凯(153	88)
燃煤由厂可凝结颗粒物的测试与排放 ***	۱ <u>۵</u>)
然外电产的观点软件的的现在分词从 主治无比学生的家庭化步入强压破损用地继续基础是自由了供使奶帕克	7
南海水坝不同深及非尤合似生物的固恢浴能及其对不同电士供体的响应····································	
	(0)
基于 GOCI 影像和水体光学分类的内陆湖泊叶绿素 a 浓度遥感估算 冯驰,金琦,王艳楠,赵丽娜,吕恒,李云梅(155贵州清水江流域丰水期水化学特征及离子来源分析 吕婕梅,安艳玲,吴起鑫,罗进,蒋浩(156东莞石马河流域水化学特征时空差异及来源辨析 高磊,陈建耀,王江,柯志庭,朱爱萍,许凯(157河东源)[河京水水北岩]	7)
告州清水汀流域主水期水化学转征及离子平源分析	55)
- 央川田小江加坡十小河小化寸竹皿及南 J 不極力切 - ロ灰梅, ×花々, 大尺鐘, 少址, 竹垣 (150 ナボアココドレルル・出げに) - マモ サ オ エマー レード よ	12)
乐完石马河流域水化字特征时仝差异及米源辨析 尚磊,陈廷雄,土江, 何态庭, 朱发泙, 计凯(15/	(3)
河南鸡冠洞洞穴水对极端气候的响应及其控制因素研究 ······	
	(2.)
石漠化治理对岩溶地下水水化学和溶解无机碳稳定同位素的影响 肖时珍,熊康宁,蓝家程,张晖,杨龙(159	(0)
旱季不同土地利用类型下岩溶碳汇效应差异 赵瑞一,梁作兵,王尊波,于正良,江泽利 (159	98)
有机氯农药在岩溶区上覆土壤中的垂直迁移特征及对地下水的影响 孙玉川,王永啟,梁作兵,袁道先(160)5)
山东南四湖沉积物中汞的污染现状及迁移研究 曹霏霏,杨丽原,庞绪贵,王炳华,王云倩(161	5)
摇蚊幼虫扰动下沉积物微环境和微界面对物理扰动强度的响应 史晓丹,李勇,李大鹏,王忍,邓猛,黄勇(162	2)
蓝玻矾式机矾于0.10个的成分另种成介田内的连轨到加度的响应	22)
南万红壤区氮湿沉降特征及具对流域氮输出的影响	80)
不同紫色母岩对景观水体氮磷及有机物去除的影响 黄雪娇,刘晓晨,李振轮,石纹豪,杨珊(163	39)
荔枝落叶对铜绿微囊藻牛长和光合作用的影响	18)
带连相节温相物对是菜的丰田作用	5)
與比似全位從例列球條的母连[F/用] 除亚洲,表对(103)
南方红壤区氮湿沉降特征及其对流域氮输出的影响	2)
水中利谷隆氯化降解动力学和消毒副产物生成特性 凌晓, 胡晨燕, 程明, 谷建(166	(8)
化学消毒的中和剂对水中内毒素活性检测的影响 ····································	/4)
11 11 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	10 \
十美生物灰外小中氨氮的吸附行性	0)
丁二酸改性茶油树木屑吸附铀的研究 张晓峰,陈迪云,彭燕,刘永胜,熊雪莹(168	36)
SPG 膜表面润湿性对膜污染和化学耐受性的影响 ·················· 张静,肖太民,张晶,曹丽亚,杜亚威,刘春,张磊 (169	94)
TiO. 诱导下左旋氧氟沙星的可见光降解及其机制	00.
TiO_2 诱导下左旋氧氟沙星的可见光降解及其机制 郭宏生,刘亚楠,乔琪,魏红,董呈幸,薛洁,李克斌(170新型高分子絮凝剂对废水中 $Cr(VI)$ 的捕集性能 王刚,杜凤龄,常青,徐敏(170	77)
利望前分丁系疑剂利及小中Cr(VI)的佣果性能	"
基于 OUR-HPR 测量在线估计活性污泥合成 PHA 量 曾善文,王泽宇,高敬,刘东,张代钧,卢培利(171	.3)
分离高浓度污泥产酸发酵液的自生动态膜形成机制 ····································	20)
通风强度对市政污泥生物干化中试效果的影响	
$\mathbb{Z}_{\mathcal{N}}$	7)
上版可收阅教人刘公复歌 N N 二乙酸四种对泛混由金人昆荽取盐或的研究	27)
生物可降解螯合剂谷氨酸 N,N-二乙酸四钠对污泥中重金属萃取效率的研究	
	(3)
	(3)
	(3)
	(3)
三年,崔延瑞,汤晓晓,杨慧娟,孙剑辉(173百乐克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析············· 田美,刘汉湖,申欣,赵方庆,陈帅,姚永佳(173异养硝化-好氧反硝化菌 YL 的脱氮特性····································	33) 39) 49)
三年,崔延瑞,汤晓晓,杨慧娟,孙剑辉(173百乐克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析············· 田美,刘汉湖,申欣,赵方庆,陈帅,姚永佳(173异养硝化-好氧反硝化菌 YL 的脱氮特性····································	33) 39) 49)
三年,崔延瑞,汤晓晓,杨慧娟,孙剑辉(173百乐克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析············· 田美,刘汉湖,申欣,赵方庆,陈帅,姚永佳(173异养硝化-好氧反硝化菌 YL 的脱氮特性····································	33) 39) 49)
三年,《中国 一年	33) 39) 49) 57) 53)
三年,《中国 一年	33) 39) 49) 57) 53)
三年克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析 田美,刘汉湖,申欣,赵方庆,陈帅,姚永佳(173) 异养硝化-好氧反硝化菌 YL 的脱氮特性 梁贤,任勇翔,杨全,赵思琪,夏志红(174) 菌株 Arthrobacter sp. CN2 降解对硝基苯酚的特性与动力学 任磊,史延华,贾阳,姚雪松,Ruth Nahurira,弥春霞,闫艳春(175) 短短芽胞杆菌及其芽胞对芘的降解 刘芷辰,叶锦韶,彭辉,刘则华,邓庭进,尹华,廖丽萍(176) 垃圾填埋场抗生素抗性基因初探 李蕾,徐晶,赵由才,宋立岩(176) 不同构型人工湿地基质中土著菌的耐药性及整合子丰度调查 麦晓蓓,陶然,杨扬,张敏,林剑华,满滢(177)	33) 39) 49) 57) 53) 59)
三年克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析 田美,刘汉湖,申欣,赵方庆,陈帅,姚永佳(173) 异养硝化-好氧反硝化菌 YL 的脱氮特性 梁贤,任勇翔,杨全,赵思琪,夏志红(174) 菌株 Arthrobacter sp. CN2 降解对硝基苯酚的特性与动力学 任磊,史延华,贾阳,姚雪松,Ruth Nahurira,弥春霞,闫艳春(175) 短短芽胞杆菌及其芽胞对芘的降解 刘芷辰,叶锦韶,彭辉,刘则华,邓庭进,尹华,廖丽萍(176) 垃圾填埋场抗生素抗性基因初探 李蕾,徐晶,赵由才,宋立岩(176) 不同构型人工湿地基质中土著菌的耐药性及整合子丰度调查 麦晓蓓,陶然,杨扬,张敏,林剑华,满滢(177)	33) 39) 49) 57) 53) 59)
三年克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析 田美,刘汉湖,申欣,赵方庆,陈帅,姚永佳(173) 异养硝化-好氧反硝化菌 YL 的脱氮特性 梁贤,任勇翔,杨全,赵思琪,夏志红(174) 菌株 Arthrobacter sp. CN2 降解对硝基苯酚的特性与动力学 任磊,史延华,贾阳,姚雪松,Ruth Nahurira,弥春霞,闫艳春(175) 短短芽胞杆菌及其芽胞对芘的降解 刘芷辰,叶锦韶,彭辉,刘则华,邓庭进,尹华,廖丽萍(176) 垃圾填埋场抗生素抗性基因初探 李蕾,徐晶,赵由才,宋立岩(176) 不同构型人工湿地基质中土著菌的耐药性及整合子丰度调查 麦晓蓓,陶然,杨扬,张敏,林剑华,满滢(177)	33) 39) 49) 57) 53) 59)
三年克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析 田美,刘汉湖,申欣,赵方庆,陈帅,姚永佳(173) 异养硝化-好氧反硝化菌 YL 的脱氮特性 梁贤,任勇翔,杨全,赵思琪,夏志红(174) 菌株 Arthrobacter sp. CN2 降解对硝基苯酚的特性与动力学 任磊,史延华,贾阳,姚雪松,Ruth Nahurira,弥春霞,闫艳春(175) 短短芽胞杆菌及其芽胞对芘的降解 刘芷辰,叶锦韶,彭辉,刘则华,邓庭进,尹华,廖丽萍(176) 垃圾填埋场抗生素抗性基因初探 李蕾,徐晶,赵由才,宋立岩(176) 不同构型人工湿地基质中土著菌的耐药性及整合子丰度调查 麦晓蓓,陶然,杨扬,张敏,林剑华,满滢(177)	33) 39) 49) 57) 53) 59)
是青,崔延瑞,汤晓晓,杨慧娟,孙剑辉(173 百乐克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析	33) 39) 39) 37) 33) 36) 35)
早青,崔延瑞,汤晓晓,杨慧娟,孙剑辉(173 百乐克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析 田美,刘汉湖,申欣,赵方庆,陈帅,姚永佳(173 异养硝化-好氧反硝化菌 YL 的脱氮特性 梁贤,任勇翔,杨全,赵思琪,夏志红(174 菌株 Arthrobacter sp. CN2 降解对硝基苯酚的特性与动力学 任磊,史延华,贾阳,姚雪松,Ruth Nahurira,弥春霞,闫艳春(175 短短芽胞杆菌及其芽胞对芘的降解 刘芷辰,叶锦韶,彭辉,刘则华,邓庭进,尹华,廖丽萍(176 垃圾填埋场抗生素抗性基因初探 李蕾,徐晶,赵由才,宋立岩(176 不同构型人工湿地基质中土著菌的耐药性及整合子丰度调查 麦晓蓓,陶然,杨扬,张敏,林剑华,满滢(177 硝酸盐和甲烷对覆土中苯系物厌氧氧化的影响 柳蓉,龙焰,王立立,何婷,叶锦韶(178 山西高原落叶松人工林土壤呼吸的空间异质性 严俊霞,李洪建,李君剑,武江星(179 施氮对黄土旱塬区春玉米土壤呼吸和温度敏感性的影响 美继韶,郭胜利,王蕊,刘庆芳,王志齐,张彦军,李娜娜,李如剑,吴得峰,孙棋棋(180	33) 39) 39) 37) 33) 36) 35)
是青,崔延瑞,汤晓晓,杨慧娟,孙剑辉(173 百乐克(BIOLAK)活性污泥宏基因组的生物多样性及功能分析	33) 39) 49) 57) 53) 59) 76) 35)
「日のLAK 活性汚泥宏基因组的生物多样性及功能分析 日美、刘汉湖、申欣、赵方庆、陈帅、姚永佳 (173 早养硝化-好氧反硝化菌 YL 的脱氮特性 深景、任勇翔、杨全、赵思琪、夏志红 (174 菌株 Arthrobacter sp. CN2 降解对硝基苯酚的特性与动力学 任磊、史延华、贾阳、姚雪松、Ruth Nahurira、弥春霞、闫艳春 (175 短短芽胞杆菌及其芽胞对芘的降解 刘芷辰、叶锦韶、彭辉、刘则华、邓庭进、尹华、廖丽萍 (176 垃圾填埋场抗生素抗性基因初探 李曹、徐晶、赵由才、宋立岩 (176 不同构型人工湿地基质中土著菌的耐药性及整合子丰度调查 表晓蓓、陶然、杨杨、张敏、林剑华、满滢 (177 硝酸盐和甲烷对覆土中苯系物厌氧氧化的影响 柳蓉、龙焰、王立立、何婷、叶锦韶 (178 山西高原落叶松人工林土壤呼吸的空间异质性 严俊霞、李洪建、李君剑、武江星 (179 施氮对黄土旱塬区春玉米土壤呼吸和温度敏感性的影响 一一一一一一一一一一一一一一一一一一一一一一一一一一一一一一一一一一一	33) 39) 39) 37) 33) 36) 35) 33) 36) 37) 36)
三成街区AK)活性污泥宏基因组的生物多样性及功能分析	33) 39) 39) 37) 33) 35) 35) 33) 32) 36) 88) 87) 86)
三成街区AK)活性污泥宏基因组的生物多样性及功能分析	33) 39) 39) 37) 33) 35) 35) 33) 32) 36) 88) 87) 86)
「日の日の日の日の日の日の日の日の日の日の日の日の日の日の日の日の日の日の日の	33) 39) 39) 37) 33) 35) 35) 35) 32) 36) 36) 37) 36)
日	33) 39) 39) 37) 33) 35) 35) 33) 32) 36) 36) 36) 36) 36)
	33) 39) 39) 39) 37) 33) 35) 33) 32) 36) 36) 36) 36) 36) 36) 36) 36) 36) 36
	33) 39) 39) 39) 37) 33) 35) 33) 32) 36) 36) 36) 36) 36) 36) 36) 36) 36) 36
	33) 39) 39) 39) 37) 33) 35) 33) 32) 36) 36) 36) 36) 36) 36) 36) 36) 36) 36
	33) 39) 39) 39) 37) 33) 35) 33) 32) 36) 36) 36) 36) 36) 36) 36) 36) 36) 36
展青、崔延瑞、汤晓晓、杨慧娟、孙剑辉(173	33) 39) 39) 39) 37) 33) 35) 33) 32) 36) 36) 36) 36) 36) 36) 36) 36) 36) 36
	33) 39) 39) 39) 37) 33) 35) 33) 32) 36) 36) 36) 36) 36) 36) 36) 36) 36) 36

通风强度对市政污泥生物干化中试效果的影响

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摘要:将污泥与树皮按照一定比例混合,利用自主研制的滚筒式污泥生物干化中试系统进行实验,通过对温度、含水率、 O_2 和 CO_2 浓度、挥发性固体(VS)、pH 等参数的检测,研究了通风强度对市政污泥生物干化效果的影响.结果表明,通风强度对污泥生物干化有较大影响,通风强度(以 VS 计)为 120 L·(h·kg) ⁻¹时,最高温度达到 66%,55%以上高温可以维持 40 h 以上,111 h 后污泥最终含水率可以降低至 56%;生物干化过程中 pH 始终保持在 6.5~8.5之间,不会影响微生物生命活动;滚筒式污泥生物干化反应器能够使反应器内基质均一性良好,对利用滚筒式反应器实现污泥连续流处理提供参考.

关键词:通风强度;污泥;滚筒;生物干化;中试

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Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test

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Abstract: A drum-type biodrying pilot scale test system was made to treat the municipal sludge. Sludge was mixed with barks according to certain proportion, and was used to study the influence of air flux on municipal sludge biodrying through parameter detection, such as temperature, moisture content, pH and volatile solid (VS). Results showed that air flux had a great influence on the effect of biodrying. When the air flux was 120 L·(h·kg)⁻¹, the best result was obtained, the highest sludge temperature was 66℃ and the temperature could remain upon 55℃ for more than 40 h. After 111 h, the moisture content reduced to 56%. The pH remained at 6.5-8.5 through the whole biodrying process. As a result, the microorganism activities would not be affected. The sludge inside the drum-type biodrying system was homogeneous. This research provides a reference about sludge treatment using a continues flow process by drum-type biodrying system.

Key words: air flux; sludge; drum-type biodrying system; biodrying; pilot scale test

市政污泥是污水处理的副产物. 随着我国经济的高速发展,污水排放量和处理率逐年提高,污泥产量急剧增加. 据统计^[1],2012 年我国污水排放总量684 亿 t,综合处理率按60% 计,污泥(含水率96%)产量达到20431万m³·a^{-1[2]}.

污泥成分复杂,有机质含量高,含有重金属、病原微生物,并带有强烈臭味,易造成二次污染. 高效的污泥处理处置措施,降低其含水率是关键,而目前,国内多数污水厂经过浓缩机械脱水后的污泥含水率为80%左右,不可能达到60%^[3],这对后续处理处置技术来说含水率过高^[4],干化成为污泥处理的瓶颈问题. 传统干化技术,如间接热干化和直接热干化,存在耗能高、热效率低、二次污染严重的问题^[5].

生物干化即利用微生物降解污泥中有机质产生的能量使堆体升温,实现水分快速蒸发,使其臭气减少,处理后污泥疏松、分散,成粒状,物理性状明显改善^[6],同时热值升高^[7],便于运输,有利于焚烧、填埋等各种后续技术,是一种经济节能的污泥干化

技术.

目前国内外学者在污泥生物干化领域已经开展了一些研究,内容包括辅料种类^[8,9]及其与污泥的混合比例^[10,11],以及温度^[12,13]、含水率^[14,15]、通风强度、通风方式^[16-18]等因素对生物干化的影响.

目前关于生物干化研究主要集中在实验室规模,利用滚筒式装置进行污泥生物干化的中试规模研究鲜有报道.通风强度是影响污泥生物干化过程的重要参数,通风强度过小,则污泥中微生物得不到充足氧气影响好氧降解过程,温度难以维持高温,水分蒸发量减少,水分排出困难,最终影响含水率去除效果;通风强度过大,反应器中热量随通风流失严重,温度降低,污泥水分蒸发困难,同样影响含水率去除效果.本实验利用自主研制的滚筒式反应器,在中试规模条件下,研究通风强度对污泥生物干化

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的影响,同时结合实验效果,对利用滚筒式反应器实 现污泥连续流处理的可行性提供参考.

1 材料与方法

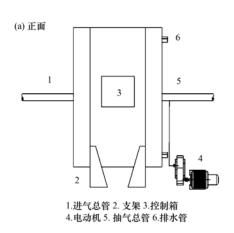
1.1 实验材料

污泥样品为北京清河污水处理厂脱水污泥,并 保证当天取泥当天实验,由于污泥没有经过消化,有 机质含量较高,更利于生物干化. 所用辅料为樟松 和落叶松树皮,由上海丘山环保科技有限公司提供. 本实验树皮为已经接种驯化过的回流树皮. 实验材 料基本性质见表 1.

表 1 实验材料基本性质

Table 1 Basic property of experimental materials

原料	含水率/%	VS/%	pН
污泥	81. 61 ~ 82. 69	68. 22 ~71. 53	7. 0 ~ 7. 4
回流树皮	12. 89 ~ 13. 41	83. 48 ~ 84. 90	_



生物干化系统

Fig. 1 Biodrying system

1.3 实验方法

进行批式实验,将污泥与树皮按照质量比(湿 基比)5:3进行混合,每批进料量在1130 kg 左右,同 时保证反应器容积率达到75%. 小试试验结果表 明,转速对于化效果影响较小,同时确定了合理的通 风强度区间. 基于此,调节滚筒转动周期为 18 h·r-1,调节空压机,使得不同批次进气强度(以 VS 计,下同)依次为60、120、180 L·(h·kg)⁻¹. 每日早 晚各取一次样,每个样做2个平行样. 反应器温度 降至50℃以下时,单批实验结束,出料放置在通风 处晾晒,直至含水率下降至15%以下,经过筛分,得 到回流树皮作为辅料进行下一批实验,筛分得到的 干化污泥含水率低,方便用于后续处理.

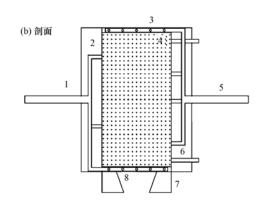
1.4 测试项目

温度、O₂、CO₂浓度监测:滚筒内均布深入基

1.2 实验装置

实验装置采用滚筒式生物干化系统,由清华大 学环境学院自主研发,其正面及剖面见图 1.

滚筒有效直径设计为2 m,配置合适长度,便可 保证小型污水厂污泥日处理要求. 本实验取反应器 断面进行研究,长度设计为1 m,滚筒外壁及气孔盖 均以聚氨酯材料保温. 采用调频电机带动滚筒转 动,实现转速调节. 滚筒内沿圆周均匀布设 6 根温 度探头,气体出口处设置 O,、CO, 检验装置,减少随 意取点造成的误差. 滚筒内均匀布设 6 块布气板, 每块布气板表面布满直径3 mm,间距5 cm 的布气 孔. 滚筒转动过程中,时刻保持最下面两块布气板 向反应器内充空气,最上面一块布气板与大气联通, 其余布气板关闭. 每块布气板与一排水管相连,当 布气板与大气相通时,排水管打开,排出布气板与反 应器内壁间隙的冷凝水.



1.进气总管 2. 进气支管 3.抽气孔 4.布气板(孔) 5. 抽气总管 6.排水管 7.支架 8.进气孔

质 15 cm 的 6 个温度传感器,出气口内侧装有 0,、 CO₂ 传感器,实现监测. 样品检测项目包括:含水 率、VS、pH.

含水率:采用公式(1)计算.

含水率 =
$$\frac{m_1 - m_2}{m_1}$$
 (1)

式中,*m*, 为样品新鲜质量,kg; *m*, 为样品 105℃条 件下烘干至恒重时的质量,kg.

VS: 采用公式(2)计算.

$$VS = \frac{m_2 - m_3}{m_2}$$
 (2)

式中, m, 为样品 105℃条件下烘干至恒重时的质 量,kg; m, 为样品烘干后,550℃灼烧2h后的质量.

pH 值:污泥样品与去离子水按质量比1:10 混 合,用玻璃棒剧烈搅动 1~2 min,静置 30 min,而后 用 pH 计测定.

2 结果与讨论

2.1 通风强度对污泥生物干化温度影响

不同通风强度条件下,温度随时间变化情况如 图 2 所示. 可以看出,反应过程大致分为升温期(0 ~40 h)、高温期(40~80 h)和降温期(80~111 h),随着通风强度的不同,3个时期的长短不尽相 同. 不同通风强度对基质温度有较大影响. 通风 后,微生物开始进行好氧呼吸,放出大量热量,随着 反应进行可供利用的有机物逐渐减少,微生物产生 热量随之减少,故温度均呈现先升高后降低的趋势. 当通风强度为 60 L·(h·kg) ⁻¹时,基质升温速率介于 120 L·(h·kg) ⁻¹和 180 L·(h·kg) ⁻¹之间. 这是由于 过大的通风强度导致热量随着气体快速流失,升温速 率最慢;通风强度过低,污泥升温所需氧气量得不到 满足,升温速率较慢. 通风强度为 60 L·(h·kg) -1 时 最高温度可以达到 66℃,且在 60℃以上可维持 40 h 以上,但降温速率较慢,111 h 后温度仍达到 51℃,这 会导致干化周期变长, VS 消耗大, 干化污泥热值降 低. 通风强度为 180 L·(h·kg) -1 时,升温速率最慢, 最高温度只能达到56℃,之后迅速降温,并没有起到 高温强蒸发效果. 通风强度为 120 L·(h·kg)⁻¹时,升 温速率最快,因为此时通风强度适中,微生物不会因 氧气过少而生命活动减缓,也不会因为通风强度过大 而带出过多热量;最高温度达到66℃,可以达到高温 调质及水分强蒸发的效果;之后温度迅速下降,111 h 后降至36℃.

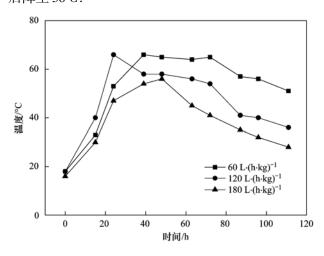


图 2 不同通风强度条件下温度随时间变化

Fig. 2 Changes of temperature with time under different air fluxes

2.2 通风强度对污泥含水率的影响 通风强度对污泥含水率影响见图 3. 高温使得

污泥中的束缚水活化[19],同时极大地促进水分蒸 发,而进气造成污泥表面空气流动速率加快,气体将 自身所含水分带出,故反应过程中污泥含水率逐渐 降低. 通风强度为60 L·(h·kg)⁻¹时,含水率在反应 初期下降幅度相对较小,24 h 仅下降 5.66%,进入 高温期后,虽然基质可以在高温下持续较长时间,但 较小的通风强度限制了水分带出速率,导致基质周 围空气含水率较高,基质水分蒸发强度下降,由于没 有及时排出水分,部分水分也会冷凝,回流入基质, 最终污泥含水率下降了23.84%,达到59.07%.通 风强度为 180 L·(h·kg) ⁻¹时,虽然升温速率较慢, 温度较低造成水分蒸发速率下降,但强劲的通风对 流作用依然使污泥快速达到较好的脱水效果,污泥 含水率下降 26. 26%, 含水率降至 56. 79%, 然而高 通风强度对设备要求更高,污泥处理成本提升. 通 风强度为 120 L·(h·kg) ⁻¹时,通入空气即保证了微 生物活动放热所需,也可及时带出水分,基质含水率 最低降到 55.66%, 污泥含水率降低 26.41%, 污泥 含水率下降至最低同时能耗相对较低.

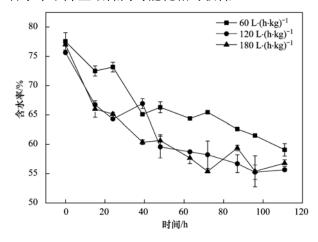


图 3 不同通风强度条件下含水率随时间变化

Fig. 3 Changes of water content with time under different air fluxes

2.3 通风强度对污泥降解情况的影响

污泥降解情况用出气口 O₂ 和 CO₂ 浓度表征, 他们在不同通风强度条件下随时间变化趋势见图 4 和 5.

污泥中微生物降解有机物同时消耗 O_2 , 放出 CO_2 . 实验初期随着微生物对环境的适应,且温度适中,降解速率逐渐增加;随着实验进行,温度升高及有机质的消耗,微生物的活动受到抑制,降解速率逐渐下降. 故总的来看出气口 O_2 浓度先降后升, CO_2 浓度先升后降. 通气强度为 O_2 浓度在 O_3 次度在 O_3 次度在 O_3 次度在 O_4 的时达到最低,但仍有 O_3 35%,说明较

低通气强度对微生物活动抑制作用较弱,微生物依然可以在较为充足的氧气环境中进行好氧呼吸; CO_2 浓度在 24 h 时达到最大的 8.83%,说明反应器中产生的 CO_2 没有被及时排出,继而可推断出空气中水分没有被及时排出,这也正是反应器内温度较高但含水率下降速率有限的原因. 通风强度为 180 $L\cdot(h\cdot kg)^{-1}$ 时,过大的通风使得 O_2 利用效率下降,同时稀释了 CO_2 ,24 h O_2 浓度最低时依然达到 15.19%, CO_2 浓度最高时仅为 3.18%. 通风强度为 120 $L\cdot(h\cdot kg)^{-1}$ 时,出气口 O_2 和 CO_2 浓度介于另外两种通风强度之间,分别达到 12.97%、5.07%,此时反应器内 O_2 浓度充足,通风量适中,保证了有充足的通风带出水分而不使温度下降过快.

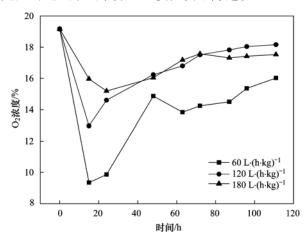


图 4 不同通风强度条件下氧气浓度随时间变化

Fig. 4 Changes of oxygen percent with time under different air fluxes

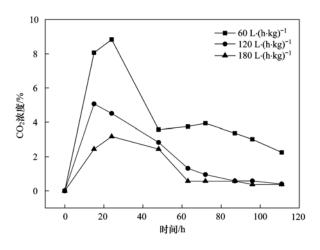


图 5 不同通风强度条件下二氧化碳浓度随时间变化

Fig. 5 Changes of carbon Dioxide percent with time under different air fluxes

2.4 通风强度对污泥 pH 的影响

污泥的 pH 对污泥中微生物生命活动有重要影响,它可引起细胞膜及细胞内的蛋白质、核酸等物

质所带电荷发生变化,改变环境中营养物质的可给性及有害物质的毒性^[20]. 微生物适宜生长的 pH 值范围大约为 6.5~8.5. 生物干化过程中会产生大量的氨气,随着温度的升高挥发出来并溶解于污泥中,这是导致污泥 pH 值升高的主要原因.

通风强度对污泥 pH 影响见图 6. 不同通风强度条件下,污泥 pH 随时间变化不大,维持在 6.5~8.5之间,不会影响微生物活性,整个生物干化过程中无需对 pH 进行调节. 当通风强度为 60 L·(h·kg)⁻¹时,污泥温度维持高温时间长,大量可溶性蛋白转化成氨气挥发,同时碳水化合物转化成CO₂进行碱中和,系统的 pH 处于动态平衡,固相中的 pH 升高幅度较小,最高 pH 为 7.6. 随着通风强度的增大,系统维持高温时间变短,生物转化速率降低,挥发性的 NH₃则随过量气体(空气)持续逸散,使得污泥固相的 pH 值升高幅度变大.

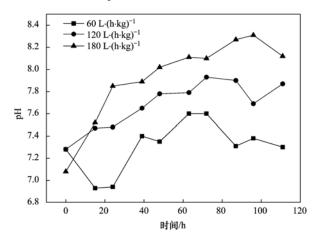


图 6 不同通风强度条件下 pH 随时间变化

Fig. 6 Changes of pH with time under different air fluxes

2.5 通风强度对污泥 VS 的影响

所有的有机质都是 VS,通过测定污泥中的 VS 可大致得知其中有机质含量的变化情况. 生物干化过程中微生物通过降解污泥中的 VS 释放出热量,达到升温调质降低污泥含水率的目的,故在生物干化过程中 VS 均有逐渐降低的趋势,且升温阶段有机质含量高,微生物活性高,VS 迅速降低,高温期和降温期 VS 下降缓慢.

图 7 可以看出,通风强度为 180 $L\cdot(h\cdot kg)^{-1}$ 时, VS 下降幅度最小, 111 h 内从 66. 70% 下降至 60. 76%, 下降了 8. 91%. 通风强度变为 60 $L\cdot(h\cdot kg)^{-1}$ 、120 $L\cdot(h\cdot kg)^{-1}$ 时, 基质 VS 分别下降了 10. 21% 和 13. 50%. 总体看来, VS 下降幅度都比较小, 说明生物干化过程可以较大程度地保留污泥

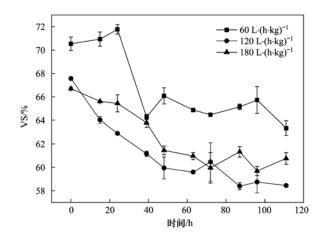


图 7 不同通风强度条件下 VS 随时间变化

Fig. 7 Changes of VS with time under different air fluxes

中的有机物,方便污泥后续处理.

综合上述讨论,将各主要监测参数与通风强度 的关系进行总结,如图 8.

可以看出,随着通风量的增加,反应器出口 O_2 浓度的上升趋势和 CO_2 浓度的下降趋势均较为明显,经过生物干化过程,污泥中的 VS 下降比例均较小. 当 通 风 强 度 为 60 L·(h·kg) $^{-1}$ 、 120 L·(h·kg) $^{-1}$ 时,污泥可以上升至高温 66 $^{\circ}$ 、通风强度升至 180 L·(h·kg) $^{-1}$ 时,最高温度大幅下降至 56 $^{\circ}$ 。通风强度为 60 L·(h·kg) $^{-1}$ 时,虽然可达高温,但通风量过小,水分不能及时带出导致含水率下降比例有限,通风强度为 180 L·(h·kg) $^{-1}$ 时通风量过大,热量散失过快,高温难以达到,虽可较快去除水分,但耗能过大。可见,120 L·(h·kg) $^{-1}$ 是本实验条件下最优通风强度。

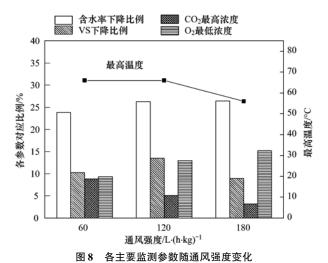


Fig. 8 Changes of main parameters during biodrying process under different air fluxes

3 结论

- (1)通风强度对污泥生物干化有较大影响,适宜通风强度可以保证充足的氧气供应前提下及时把水分从反应器带出,同时可以维持一段时间高温.通风强度为 120 L·(h·kg)⁻¹时,最高温度达到66℃,55℃以上高温可以维持40h以上,水分蒸发迅速,111h后污泥最终含水率可以降低至最好效果55.66%,耗能相对较小.
- (2)通风强度对 pH 影响较小,pH 始终保持在 6.5~8.5之间,不会影响微生物生命活动,实验过程无需对 pH 进行调节. 控制污泥生物干化条件,可以达到较短周期内污泥含水率迅速降低至 60%以下,同时较大程度保持污泥中有机质的效果,方便后续处理.
- (3)滚筒式污泥生物干化反应器能够使反应过程中反应器内基质保持良好的均一性,利用滚筒式反应器实现污泥连续流生物干化过程可行性较大.

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HUANJING KEXUE

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Vol. 36 No. 5 May 15, 2015

CONTENTS

Pollution of Halogenated Polycyclic Aromatic Hydrocarbons in Atmospheric Particulate Matters of Shenzhen	
Emission Characteristics of VOCs from Typical Restaurants in Beijing	
Characteristics Analysis of Sulfur Dioxide in Pearl River Delta from 2006 to 2010	
Comparison Test Between PM _{2.5} Continuous Monitoring System and Manual Sampling Analysis for PM _{2.5} in Ambient Air Determination and Emission of Condensable Particulate Matter from Coal-fired Power Plants	WANG Qiang, ZHONG Qi, CHI Ying, et al. (1538)
Potential Carbon Fixation Capability of Non-photosynthetic Microbial Community at Different Depth of the South China Sea and Its	
rotential Carbon Fixation Capability of Non-photosynthetic successful Community at Different Depth of the South China Sea and its	Response to Different Electron Donois
Remote Sensing Estimation of Chlorophyll-a Concentration in Inland Lakes Based on GOCI Image and Optical Classification of Wat	
Hydrochemical Characteristics and Sources of Qingshuijiang River Basin at Wet Season in Guizhou Province	
Temporal-spatial Variation and Source Identification of Hydro-chemical Characteristics in Shima River Catchment, Dongguan City	
Response and Control Factors of Groundwater to Extreme Weather, Jiguan Cave, Henan Province, China	
Impact of Rocky Desertification Treatment on Underground Water Chemistry and Dissolved Inorganic Carbon Isotope in Karst Areas	······
Difference of Karst Carbon Sink Under Different Land Use and Land Cover Areas in Dry Season Vertical Migration Characteristics of Organochlorine Pesticides in Overlying Soil in Karst Terranes and Its Impact on Groundwater	
	·· SUN Yu-chuan, WANG Yong-qi, LIANG Zuo-bing, et al. (1605)
Pollution Status and Migration of Mercury in the Sediments of Nansi Lake in Shandong Province	
Response of Sediment Micro Environment and Micro Interface to Physical Disturbance Intensity Under the Disturbance of Chironom	nus plumosus ·····
Characteristics of Atmospheric Nitrogram Was Describing and Associated Laurest on N. Tayarons in the Wastenhald of Ded Scil Associated	
Characteristics of Atmospheric Nitrogen Wet Deposition and Associated Impact on N Transport in the Watershed of Red Soil Area i	
Effect of Different Purple Parent Rock on Removal Rates of Nitrogen, Phosphorus and Organics in Landscape Water	
Effects of Litchi chinensis Defoliation on Growth and Photosynthesis of Microcystis aeruginosa	
Effects of Literal crunensis Detoliation on Growth and Photosynthesis of Microcystis aeruginosa Toxicity of Coptis chinensis Rhizome Extracts to Green Algae	··· WAING Alao-xiong, JIAING Chen-chun, Li Jin-wei, et al. (1048)
Formation Mechanism of the Disinfection By-product 1,1-Dichloroacetone in Drinking Water	
Degradation Kinetics and Formation of Disinfection By-products During Linuron Chlorination in Drinking Water	
Interference for Various Quench Agents of Chemical Disinfectants on Detection of Endotoxin Activities in Water	
Ammonium Adsorption Characteristics in Aqueous Solution by Dairy Manure Biochar	
Absorption of Uranium with Tea Oil Tree Sawdust Modified by Succinic Acid	
Effect of Membrane Wettability on Membrane Fouling and Chemical Durability of SPG Membranes	
TiO ₂ -Induced Photodegradation of Levofloxacin by Visible Light and Its Mechanism	
Performance of Novel Macromolecule Flocculant in the Treatment of Wastewater Containing Cr(VI) Ions	
On-line Estimation for the Amount of Stored PHA in Activated Sludge Based on OUR-HPR Measurements	
Formation Mechanism of Self-forming Dynamic Membrane During Separation of High-concentration Sewage Sludge Fermented for Ac	CIG Production
	HITANC Shari THI Hong by VIN Do at al. (1720)
Influence of Air Flor on Municipal Studeo Biodesine in a Pilat Scale Test	HUANG Shuai, LIU Hong-bo, YIN Bo, et al. (1720)
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test	HUANG Shuai, LIU Hong-bo, YIN Bo, et al. (1720) ZHANG Yu, HAN Rong, LU Wen-jing, et al. (1727)
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis(carboxymethyl) Glutamic Acid Tetrasodium	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Bretibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis (carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Breeibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau Effects of Nitrogen Fertilization on Soil Respiration and Temperature Sensitivity in Spring Maize Field in Semi-Arid Regions on Loe	HUANG Shuai, LIU Hong-bo, YIN Bo, et al. (1720) ZHANG Yu, HAN Rong, LU Wen-jing, et al. (1727) WU Qing, CUI Yan-rui, TANG Xiao-xiao, et al. (1733) TIAN Mei, LIU Han-hu, SHEN Xin, et al. (1739) LIANG Xian, REN Yong-xiang, YANG Lei, et al. (1749) REN Lei, SHI Yan-hua, JIA Yang, et al. (1757) LIU Zhi-chen, YE Jin-shao, PENG Hui, et al. (1763) LI Lei, XU Jing, ZHAO You-cai, et al. (1769) of Different Configurations MAI Xiao-bei, TAO Ran, YANG Yang, et al. (1776) LIU Rong, LONG Yan, WANG Li-li, et al. (1785) YAN Jun-xia, LI Hong-jian, LI Jun-jian, et al. (1793)
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N,N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau	HUANG Shuai, LIU Hong-bo, YIN Bo, et al. (1720) ZHANG Yu, HAN Rong, LU Wen-jing, et al. (1727) WU Qing, CUI Yan-rui, TANG Xiao-xiao, et al. (1733) TIAN Mei, LIU Han-hu, SHEN Xin, et al. (1739) LIANG Xian, REN Yong-xiang, YANG Lei, et al. (1749) REN Lei, SHI Yan-hua, JIA Yang, et al. (1757) LIU Zhi-chen, YE Jin-shao, PENG Hui, et al. (1763) LI Lei, XU Jing, ZHAO You-cai, et al. (1769) of Different Configurations MAI Xiao-bei, TAO Ran, YANG Yang, et al. (1776) LIU Rong, LONG Yan, WANG Li-li, et al. (1785) YAN Jun-xia, LI Hong-jian, LI Jun-jian, et al. (1793)
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N,N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau Effects of Nitrogen Fertilization on Soil Respiration and Temperature Sensitivity in Spring Maize Field in Semi-Arid Regions on Loe	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N,N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau Effects of Nitrogen Fertilization on Soil Respiration and Temperature Sensitivity in Spring Maize Field in Semi-Arid Regions on Loe Distribution Characteristics of Heavy Metals in the Street Dusts in Xuanwei and Their Health Risk Assessment	HUANG Shuai, LIU Hong-bo, YIN Bo, et al. (1720) ZHANG Yu, HAN Rong, LU Wen-jing, et al. (1727) WU Qing, CUI Yan-rui, TANG Xiao-xiao, et al. (1733) TIAN Mei, LIU Han-hu, SHEN Xin, et al. (1739) LIANG Xian, REN Yong-xiang, YANG Lei, et al. (1749) REN Lei, SHI Yan-hua, JIA Yang, et al. (1757) LIU Zhi-chen, YE Jin-shao, PENG Hui, et al. (1763) LI Lei, XU Jing, ZHAO You-cai, et al. (1769) of Different Configurations MAI Xiao-bei, TAO Ran, YANG Yang, et al. (1776) LIU Rong, LONG Yan, WANG Li-li, et al. (1785) YAN Jun-xia, LI Hong-jian, LI Jun-jian, et al. (1793) Ses Plateau JIANG Ji-shao, GUO Sheng-li, WANG Rui, et al. (1802) ZHANG Wen-chao, LÜ Sen-lin, LIU Ding-yu, et al. (1810)
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N, N-bis (carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau Effects of Nitrogen Fertilization on Soil Respiration and Temperature Sensitivity in Spring Maize Field in Semi-Arid Regions on Loe Distribution Characteristics of Heavy Metals in the Street Dust in Baoji City and Its Implications of Environment Effect of Long-term Fertilizer Application on the Stability of Organic Carbon in Particle Size Fractions of a Paddy Soil in Zhejiang I	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N,N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau Effects of Nitrogen Fertilization on Soil Respiration and Temperature Sensitivity in Spring Maize Field in Semi-Arid Regions on Loe Distribution Characteristics of Heavy Metals in the Street Dusts in Xuanwei and Their Health Risk Assessment Spatial Distribution of Magnetic Properties of Street Dust in Baoji City and Its Implications of Environment Effect of Long-term Fertilizer Application on the Stability of Organic Carbon in Particle Size Fractions of a Paddy Soil in Zhejiang I	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N,N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau Effects of Nitrogen Fertilization on Soil Respiration and Temperature Sensitivity in Spring Maize Field in Semi-Arid Regions on Loe Distribution Characteristics of Heavy Metals in the Street Dusts in Xuanwei and Their Health Risk Assessment Spatial Distribution of Magnetic Properties of Street Dust in Baoji City and Its Implications of Environment Effect of Long-term Fertilizer Application on the Stability of Organic Carbon in Particle Size Fractions of a Paddy Soil in Zhejiang I	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N,N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau Effects of Nitrogen Fertilization on Soil Respiration and Temperature Sensitivity in Spring Maize Field in Semi-Arid Regions on Loe Distribution Characteristics of Heavy Metals in the Street Dusts in Xuanwei and Their Health Risk Assessment Spatial Distribution of Magnetic Properties of Street Dust in Baoji City and Its Implications of Environment Effect of Long-term Fertilizer Application on the Stability of Organic Carbon in Particle Size Fractions of a Paddy Soil in Zhejiang I Effects of Different Reclaimed Scenarios on Soil Microbe and Enzyme Activities in Mining Areas	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N,N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau Effects of Nitrogen Fertilization on Soil Respiration and Temperature Sensitivity in Spring Maize Field in Semi-Arid Regions on Loe Distribution Characteristics of Heavy Metals in the Street Dusts in Xuanwei and Their Health Risk Assessment Spatial Distribution of Magnetic Properties of Street Dust in Baoji City and Its Implications of Environment Effect of Long-term Fertilizer Application on the Stability of Organic Carbon in Particle Size Fractions of a Paddy Soil in Zhejiang I Effects of Different Reclaimed Scenarios on Soil Microbe and Enzyme Activities in Mining Areas Soil Microorganism Characteristics and Soil Nutrients of Different Wetlands in Sanjinag Plain, Northeast China	
Influence of Air Flux on Municipal Sludge Biodrying in a Pilot Scale Test Extraction of Heavy Metals from Sludge Using Biodegradable Chelating Agent N,N-bis(carboxymethyl) Glutamic Acid Tetrasodium Biodiversity and Function Analyses of BIOLAK Activated Sludge Metagenome Characteristics of Nitrogen Removal by a Heterotrophic Nitrification-Aerobic Denitrification Bacterium YL Biodegradation Characteristics and Kinetics of p-nitrophenol by Strain Arthrobacter sp. CN2 Biodegradation of Pyrene by Intact Cells and Spores of Brevibacillus brevis Investigation of Antibiotic Resistance Genes (ARGs) in Landfill Investigation of Antibiotic Resistance of Indigenous Bacteria and Abundance of Class I Integron in Matrix of Constructed Wetlands Effects of Nitrate and CH ₄ on Anaerobic Oxidation of BETX in Landfill Cover Soils Spatial Heterogeneity of Soil Respiration in a Planted Larch Forest in Shanxi Plateau Effects of Nitrogen Fertilization on Soil Respiration and Temperature Sensitivity in Spring Maize Field in Semi-Arid Regions on Loe Distribution Characteristics of Heavy Metals in the Street Dust in Baoji City and Its Implications of Environment Effect of Long-term Fertilizer Application on the Stability of Organic Carbon in Particle Size Fractions of a Paddy Soil in Zhejiang I Effects of Different Reclaimed Scenarios on Soil Microbe and Enzyme Activities in Mining Areas Soil Microorganism Characteristics and Soil Nutrients of Different Wetlands in Sanjinag Plain, Northeast China Strengthening Effects of Sodium Salts on Washing Kerosene Contaminated Soil with Surfactants	
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