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## 林 龙 科 享 (HUANJING KEXUE)

### ENVIRONMENTAL SCIENCE

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### 目 次

| 2008 ~ 2012 年上海里碳浓度亦化特征分析   |
|---|
|   |
| 2008~2012年上海黑碳浓度变化特征分析 ————————————————————————————————————   |
| 典型地区大气中多溴联苯醚和新型溴代阻燃剂的水平及组成分布 吴辉,金军,王英,李明圆,何松洁,徐萌,孙一鸣(1230)  |
| 某焦化厂周边大气 $PM_{10}$ 重金属来源及健康风险评价 董婷,李天昕,赵秀阁,曹素珍,王贝贝,马瑾,段小丽(1238)   |
| 本版化/ 四辺八、 $1 m_0$ 生産内本体及使体内燃料別  |
| 基于半流和人气污染物浓度问步增重的机动半半均排放凶于怕异方法。   |
| 要型地区大气中多展联本艇和新型溴代阻燃剂的水平及组成分布  |
| 珠江三角洲地区硫和氮沉降临界负荷研究  |
| 低温等离子体-生物法处理硫化氢气体研究 李华琴,何觉聪,陈洲洋,黎宝仁,黄倩茹,张再利,魏在山(1256)   |
| 太子河流域莠夫津的空间分布及风险评价  |
| 一种大批量测定沉积物微量间隙水样品中溶解态磷和铁含量的方法 干滤 朱春刚 许第 丁十明(1271)   |
| 外顶营姜扑给入巨水体由营姜扑浓度的时穴亦化   |
| イ   |
| 基于物理过程的例区地下水污染风险评价  |
| 重庆典型岩浴地下水系统水又地球化学特征研究   |
| 重庆老龙洞地卜河流域氮、磷及微生物污染调查研究 蓝家程,杨平恒,任坤,陈雪彬,徐昕,胡宁(1297)  |
| 苦草(Vallisneria natans)根系对沉积物中各形态磷的影响 李振国,王国祥,张佳,马久远,魏宏农,俞振飞(1304)   |
| 循环流廊道湿地中氯归趋过程模拟研究   |
| 不同环境因素下大湖中四环素的自然消减  |
| 再升水由5种拉升大型,150mm,150mm。   |
| TT工小丁了年7月工产,11日四日第77次入1日次久日刊上明几 吴昭明,初方,四功失,戊子从,明东台(1220)——如苏田山北村 III 平方 海夷 中国工作者和米国社会工作   |
| 一级处理山小的 UV-IIU (  |
| 水中 $C_{60}$ 别不规程的稳定性研究  |
| XDLVO 埋论解析不同离子条件下海澡酸钢微滤膜污染 赵应许,纵瑞强,高欣玉,谢慧君,殷永泉,梁爽(1343)   |
| 纳米零价铁催化过氧化氢强化修复 4-氯硝基苯污染地下水的研究 · · · · · · · · · · · · · · · · · · ·  |
| 共存氯苯类同系物对六氯苯厌氧降解活性的影响 王琪,刘辉,姜林,唐军(1358)   |
| 硫酸盐还原生物滤池对含镉废水去除效果试验研究  |
| 其于爱平衡原理对南方污水外理厂由讨脱复工艺调控等吸研究 美应和 刘佩炬 王吾 田由期 刘小茂(1372)  |
| 全上列于网络圣利田月月7万以至广于风加烈工石州江水响的几 文章中,为两角,正面,正面,可一见,为(不)(172)<br>措明由海岸湿阴南了湿山流进传,加市场上流光桥的影响 发展中,为两角,上面,面上面,为(不)(172)  |
| 医执电坡行化切离 了交山做外氧化业铁帆杆围泊住的影响  |
| 电活性生物膜介导 Cu <sup></sup> 生物还原的试验研究   |
| 模拟废旧线路板生物浸出液中铜的回收 程丹,朱能武,吴平霄,邹定辉,邢翊佳(1391)  |
| 填埋垃圾浸提液与地下水污染物组成差异及成因 何小松,余红,席北斗,崔东宇,潘红卫,李丹(1399)   |
| 化学合成施氏矿物与 H <sub>2</sub> O <sub>2</sub> 共存体系下光化学处理垃圾渗滤液的研究 王鹤茹,宋永伟,徐峙辉,崔春红,周立祥(1407)  |
| 外理 RPA 模拟废水的 SRR 工况参数对污泥有机毒性的影响研究 杨娜 陈秀莹 林逢凯 黄华 章辈 赵骏 工毅(1414)  |
| 利今远泥压每端40日8户中市执上产田岭苗群名样州的比较研究   |
| 化字音成爬民 物写 H.D.2 共仔体系下元化字处理垃圾修滤液的研究 生鹤如, 未水伟, 保崎辉, 崔春红, 周立梓(1407)处理 BPA 模拟废水的 SBR 工况参数对污泥有机毒性的影响研究 杨娜, 陈秀荣, 林逢凯, 黄华, 章斐, 赵骏, 丁毅(1414)剩余污泥厌氧消化甲烷生成势与产甲烷菌群多样性的比较研究                              董慧岭, 季民(1421)锰氧化菌 Aminobacter sp. H1 的分离鉴定及其锰氧化机制研究                                  基平, 善 建五, 何智敏, 肖少丹, 蒋轶锋(1428)1株铁基质自养反硝化菌的脱氮特性   |
| 恤氧化困 Aminoacter Sp. III 即为商金定及兵恤氧化机闸则允 "安上、安生央、陈廷血、門省墩、自夕方、荷状锌(1426)  |
| 上 张铁基灰目   |
| ლ普罗胺降解菌 Pseudomonas sp. 1-24 共代谢降解性能研究  |
| 利用流式细胞术研究鞘氨醇单胞菌 GY2B 降解菲过程中细菌表面特性的变化 ····································   |
|   |
| 毒性有机物 BPA 与普通小球藻的相互影响特性研究 ················· 陈善佳,陈秀荣,闫龙,赵建国,章斐,江子建(1457)   |
| 缺镁胁泊对普通小球藻光合生理及油脂积累的影响 王珊 赵树成 魏长龙 干水燕 史吉平 张保国(1462)   |
|   |
| 微囊藻毒素对水稻根系生长和拉氨化系统的影响   |
| 微囊藻毒素对水稻根系生长和抗氧化系统的影响   |
| 微囊藻毒素对水稻根系生长和抗氧化系统的影响   |
| 微囊藻毒素对水稻根系生长和抗氧化系统的影响   |
| 微囊藻毒素对水稻根系生长和抗氧化系统的影响   |
| 一个人们,我们就是一个人们,我们就要一个人们,我们就是一个人们的,我们就是一个人们的一个人们的,我们就是一个人们的一个人们的一个人们的一个人们的一个人们的一个人们的一个人们的一个人们的 |
| 微囊藻毒素对水稻根系生长和抗氧化系统的影响   |
| 選出。 一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學的學術,所以一個人工學學術,所以一個人工學學術,所以一個人工學學學術,所以一個人工學學學學學學學學學學學學學學學學學學學學學學學學學學學學學學學學學學學學  |
| 微囊藻毒素对水稻根系生长和抗氧化系统的影响   |

# 处理 BPA 模拟废水的 SBR 工况参数对污泥有机毒性的影响研究

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摘要:在处理双酚 A(BPA)模拟废水的序批式活性污泥系统(SBR)反应器中,保持进水 COD 含量均为 300 mg·L<sup>-1</sup>左右,通过改变水力停留时间 HRT 从 12~8 h,污泥龄 SRT 从 20~10 d,考察污泥有机毒性和其他水质指标的变化. 试验分析了空白组和 40 mg·L<sup>-1</sup>初始浓度 BPA 对照组在不同工况条件下周期末出水 COD 值、污泥有机毒性分布规律以及稳定期单周期内 COD 值 和污泥有机毒性的变化趋势. 结果表明,缩短水力停留时间和污泥龄有利于活性污泥降解 BPA,并消减稳定期污泥的有机毒性;出水 COD 稳定在 50 mg·L<sup>-1</sup>左右,且水相和泥相均无 BPA 残留. 在应用 PCR-DGGE 技术分析 SBR 系统内微生物菌群多样性和不同样品间的相似性过程中,得出污泥总毒性抑制率与微生物多样性呈负相关性关系,进水成分的不同和运行参数改变是导致污泥总毒性差异的主要原因.

关键词:双酚 A; 污泥有机毒性; 序批式活性污泥系统(SBR); 水利停留时间(HRT); 污泥龄(SRT); PCR-DGGE 技术中图分类号: X131.1; X703.1 文献标识码: A 文章编号: 0250-3301(2014)04-1414-07 **DOI**: 10.13227/j. hjkx. 2014. 04. 030

# Effects of Operating Parameters on Organic Toxicity of Sludge Treating Synthetic Bisphenol A Wastewater

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**Abstract:** In order to investigate the influence of hydraulic retention time (HRT) and sludge retention time (SRT) on sludge organic toxicity in sequencing batch reactors (SBR<sub>S</sub>), the sludge toxicity was compared when HRT and SRT were controlled at various levels. The influents COD were controlled at around 300 mg·L<sup>-1</sup>, HRT and SRT were changed from 12 h to 8 h and from 20 d to 10 d, respectively. The effluents COD, BPA contents both in liquid and sludge were measured, and sludge toxicity was also analyzed and compared between the blank group (no BPA content) and BPA control groups (40 mg·L<sup>-1</sup>). The results showed that the effluents COD of two SBRs were both below 50 mg·L<sup>-1</sup>, and there were no BPA content in liquid and sludge. Furthermore, decrease HRT and SRT is helpful to remove BPA and reduce sludge toxicity. Additional investigation revealed a correlation between the properties of bacterial community and total sludge toxicity by the PCR-DGGE analysis, and different influent compositions and operation parameters were the main reasons for leading the difference of sludge toxicity.

**Key words:** bisphenol A (BPA); organic toxicity of sludge; sequencing batch reactor (SBR); hydraulic retention time (HRT); sludge retention time (SRT); PCR-DGGE

随着城市污水排放量的逐年增加,污泥产量也随之日渐增大[1].人们越来越重视剩余污泥的处理和处置,处理得当的污泥才会最大程度避免对环境的危害,目前已有学者研究剩余污泥中有机污染物对环境可能产生潜在危害[2~4].一些工业废水的生化处理装置中,活性污泥往往积累了较高浓度的有毒物质[5].废水中的有毒有机物进入生物处理装置后有不同归宿[6]:或被微生物代谢分解;或通过曝气挥发进入大气;或被活性污泥吸附;或随出水排放.故废水生物处理应以有毒有机物在水、泥两相间的最终去除作为目标,不单以处理后 COD、BOD、SS 等常规指标为标准[7].本研究以双酚 A(BPA)为目标污染物,重点考察双酚 A 在生物降解过程中有机毒性在水、泥相整体系统内的产生和消减,以期

为后续污泥处理与处置提供理论依据.

双酚 A 是一种环境激素,具有致畸、致突变性. 研究表明低浓度双酚 A 会使神经系统、免疫系统受损,引发肿瘤、肝功能衰竭等<sup>[8~12]</sup>. 但双酚 A 应用广泛<sup>[13]</sup>,生产量大,全球用量超 200 万 t<sup>[14]</sup>. 含 BPA 的工业废水和生活污水若处置不当, BPA 会以其他方式重新进入环境. 活性污泥法在处理含 BPA 废水中应用广泛. 王燕春等<sup>[15]</sup>利用 FBR 反应器研究活性污泥法处理 BPA 废水的降解动力特性以及活性

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污泥净化机制,指出 BPA 的去除主要通过生物降解过程而非吸附.有研究指出,消减活性污泥法的毒性,不仅可以采取污泥驯化方式,还可以利用加入新工艺或改变工况条件来消减毒性<sup>[16]</sup>.故本研究旨在以水、泥相为整体考虑,通过调整工况参数来考察污泥有机毒性源头消减和水相指标变化.

### 1 材料与方法

#### 1.1 试验装置及配水组成

试验采用序批式活性污泥废水处理反应器 SBR,共两组,有效容积 10 L,分别为空白组和  $40 mg \cdot L^{-1}$  BPA 对照组. 两组 SBR 除进水组成不同外,其它试验条件一致. 活性污泥取自上海长桥污水处理厂,污泥浓度保持在  $3\,000.0\,mg \cdot L^{-1}\,\pm\,100.0\,$ 

mg·L<sup>-1</sup>. 试验温度为 20℃ ±1℃,溶解氧维持在 2.0~3.0 mg·L<sup>-1</sup>. 模拟废水初始 COD 值为 300.0 mg·L<sup>-1</sup> ±21.5 mg·L<sup>-1</sup>,分别以尿素和磷酸二氢钾作为氮源和磷源;空白组由蛋白胨提供碳源,而含BPA 对照组则由 BPA 和蛋白胨共同提供碳源;SBR进水满足 C: N: P 为100: 5: 1的好氧污泥营养条件. 试验是在其它环境条件不变的情况下,改变水力停留时间 HRT 从 12~8 h,同时污泥龄 SRT 从 20~10 d,试验连续运行 33 d.

### 1.2 分析方法

试验中 COD(重铬酸钾法)、SVI(sludge volume index)、MLSS(mixed liquor suspended solids)等常规废水处理指标依照文献[17]测定;其它项目测定方法如表 1 所示.

表 1 试验项目测定方法及其所需主要仪器

|                | Table 1 Analytical methods and main instru- | ments in the experiment  |
|----------------|---|--|
| 项目             | 测定方法  | 主要仪器   |
| 污泥絮体外层 EPS 提取  | 阳离子树脂低温搅拌交换法[18]                            | 多管架自动平衡离心机 TDZ5-WS,多头磁力搅拌器 JB-12,高速冷冻离心机 TGL-20bR  |
| 污泥破胞总物质提取      | 低温超声 + 高速离心法[19]                            | 超声波处理器 FS-300,高速冷冻离心机 TGL-20bR,多管架自动平衡离心机 TDZ5-WS,   |
| 污泥有机毒性测定       | 明亮发光杆菌 T3 菌种急性毒性测试国标法 <sup>[20]</sup>       | 生物毒性测试仪 DXY-2,全温振荡培养箱 HZP-250,立式<br>压力蒸气灭菌器筒 HC014-11-018-01(x)  |
| BPA 含量测定       | 高效液相色谱测定法[21]                               | 高效液相色谱仪 LC-20A   |
| DNA 提取和 PCR 扩增 | 琼脂糖凝胶电泳检测法                                  | 3S 离心柱环境样品 DNA 提取试剂盒; PCR 扩增仪  |
| DGGE 凝胶电泳      | /   | DCode Universal Mutation Detection System (Bio-Rad, USA) <sup>[22]</sup> ; 紫外凝胶成像系统(Gel Doc 2000)(Bio-Rad, |

### 2 结果与讨论

试验主要考察改变工况条件即缩短 HRT 和SRT后,SBR 系统在处理高浓度 BPA 废水时系统内污泥毒性变化趋势及新工况条件下的常规出水指标变化.

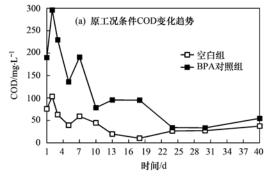
### 2.1 工况条件变化对 SBR 出水中 COD 和 BPA 浓

### 度变化的影响

USA)

### 2.1.1 改变工况条件后 SBR 出水 COD 随时间变 化趋势

由于 COD 是评判废水系统处理效果好坏的关键指标,因此试验对比改变工况条件前后同一 SBR 系统出水 COD 变化趋势来检验工况改变对系统的影响.



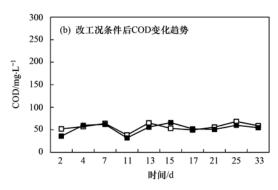


图 1 两工况条件周期末出水 COD 变化趋势

Fig. 1 Comparison of effluent COD variation with time between two operation conditions

由图 1 看出,当 SBR 系统 HRT 从 12 h 变为 8 h、SRT 从 20 d 变为 10 d 的初始 15 d,空白组与对照组周期末出水 COD 小幅波动,随后(第 15 d 至试验结束)维持在 50~70 mg·L<sup>-1</sup>,出水效果良好. 因此得出结论:改变工况条件(HRT 从 12~8 h、SRT 从 20~10 d)对 SBR 系统出水 COD 指标影响不大.

2. 1. 2 改变工况条件 SBR 运行周期末 BPA 浓度随时间变化趋势

为考察改变工况对 SBR 系统内 BPA 去除效果影响,试验随运行时间在周期末取样,测定出水、污泥相中 BPA 浓度,如图 2 和表 2 所示. 其中定义出水上清液中 BPA 含量为水相 BPA,泥水混合液经离心+超声破胞+高速离心处理后提取液中 BPA 含量为总泥相 BPA. 所得样品经过 0.22 μm 滤膜过滤后,应用 HPLC 高效液相色谱法测定 BPA 含量. 所得结果与改变工况前同区域 BPA 浓度对比.

由图 2 和表 2 可知,改变工况前 SBR 系统周期 末水相 BPA 含量和总泥相 BPA 含量总体上由高变 低,至试验结束时低于液相色谱检测限.说明试验初 期系统内微生物不能有效降解BPA,故出水和泥相

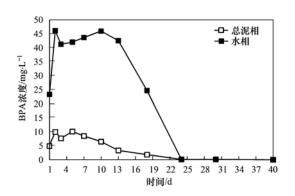


图 2 40 mg·L<sup>-1</sup> BPA 对照组污泥原工况条件周期末水相 和总泥相 BPA 浓度变化趋势

Fig. 2 Concentrations of BPA variation in effluent and sludge of 40 mg·L<sup>-1</sup> BPA control group at the end of a cycle during original operation condition

BPA 含量很高;随后经两个污泥龄驯化,系统内微生物可有效降解 BPA,水、泥相无残留. SBR 系统改变工况后,HRT 和 SRT 显著缩短,造成对 BPA 降解速率快、生长周期短的菌群逐步占据优势,虽然活性污泥内菌群结构可能有变化(论述详见 2.4 节),但未影响 BPA 在水、泥相的去除效果.

表 2 40 mg·L<sup>-1</sup> BPA 对照组污泥改变工况后周期末水相和泥相 BPA 浓度变化趋势<sup>1)</sup>

Table 2 Concentrations of BPA variation in effluent and sludge of 40 mg·L<sup>-1</sup>

BPA control group at the end of cycles during changed operation condition

| 项目         | 指标    |      |      |      |      | 运行   | 天数/d |      |      |      |      |
|------------|-------|------|------|------|------|------|------|------|------|------|------|
| 次日         | 1日 7小 | 2    | 4    | 7    | 11   | 13   | 15   | 17   | 21   | 25   | 33   |
| HRT = 8 h  | 水相    | < DL |
| SRT = 10 d | 总泥相   | < DL |

1) DL 为检测限,本试验 BPA 液相检测限 DL 为  $0.1~{\rm mg\cdot L^{-1}}$ 

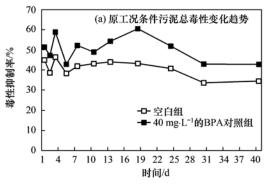
# 2.2 改变工况条件对 SBR 运行周期末污泥毒性的 影响

改变工况后, 为考察 HRT 和 SRT 缩短对污泥毒性的影响, 在33 d 的试验中通过发光细菌法测得污泥毒性抑制率并对照分析, 结果如图3 所示.

如图 3 所示,改变工况参数后 2~17 d,空白组与 BPA 对照组污泥总毒性波动较大,但变化幅度与趋势类似;并在 1 个污泥龄后即第 13 d 达到峰值,空白组总毒性抑制率为 46.64%和 BPA 对照组为57.92%.说明污泥毒性的波动是由于工况条件改变而非原水中初始 BPA 含量引起的.随着试验的进行,两组污泥毒性均呈下降趋势,到 20 d 左右,污泥特性进入稳定阶段,空白组和 BPA 对照组污泥总毒性分别维持在 13.42%和 32.58%附近.对比工况条件改变前后,缩短 HRT和 SRT 且待系统稳定时,污泥总毒性抑制率空白组(13.42%)和 BPA 对照组(32.58%)低于原工况条件时的 33%和 43%.

BPA 对照组在工况条件改变后,试验初期污泥总毒性不稳定,照比原工况条件稳定期污泥总毒性有所下降,至第 4 d 总毒性抑制率降至最低(12.01%);随后迅速反升至43.51%;接着又持续下降至第 9 d(22.10%);之后再次回升至最高点(57.92%).对照组污泥总毒性抑制率经过了 20 d 近两个污泥龄的反复升降,系统趋于稳定,污泥总毒性抑制率最终稳定在 30% 左右.

分析认为,缩短 HRT 和 SRT 使系统受到冲击,在经过了 2 个污泥龄左右时间趋于稳定.试验初期,由于原工况条件下系统内已存在大量有效降解BPA 的优势菌群,缩短 HRT 和 SRT 促进了其中生长周期短的好氧降解菌大量繁殖生长[23-25],系统降解 BPA 能力有所增加,污泥总毒性持续下降;同时,生长周期较长的优势菌群受到抑制,逐渐消减过程中降低了系统总体降解 BPA 的效率,BPA 及其有毒副产物的累积并形成毒性,表现为在第 5 d 左右



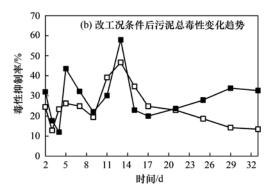


图 3 两工况条件周期末污泥总毒性抑制率变化趋势

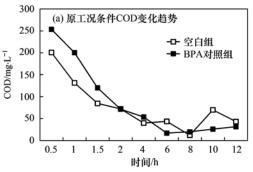
Fig. 3 Comparison of total sludge toxicity variation with time between two operation conditions

污泥总毒性的回升;在出现毒性抑制率较高值后系统继续运行,期间微生物菌群的不断变化来适应新工况条件,生长周期短的微生物增长加快,污泥总毒性下降;如此反复几个循环直至2个污泥龄后,系统达到均衡稳定状态,适应该工况条件的微生物菌群占明显优势且生长状况良好,因此 SBR 系统污泥总毒性抑制率(约33%)低于原工况条件系统稳定

时总毒性抑制率(43%).

- 2.3 对比不同工况条件系统稳定时期单周期内 COD、BPA 含量及污泥有机毒性变化趋势
- 2.3.1 单个 SBR 周期内不同工况水相 COD 变化

对比不同 HRT 和 SRT 的工况条件,两 SBR 系统稳定阶段周期内水相 COD 随时间的变化情况,结果如图 4 所示.



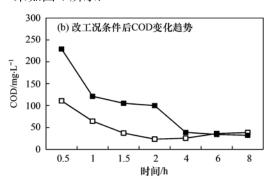


图 4 两工况条件稳定阶段单周期内水相 COD 值变化趋势

Fig. 4 Comparison of liquid COD variation with time during an operation cycle between two operation conditions

从图 4 看出,原工况稳定阶段,空白组与 BPA 对照组水相 COD 在单个 SBR 周期内随时间变化趋势相似,具体为:水相 COD 到第 4 h 已降至 50 mg·L<sup>-1</sup>以下;但第 8 h 开始,两组 SBR 水相 COD 略有回升,但仍维持在 50 mg·L<sup>-1</sup>左右. 缩减 HRT 和 SRT 到稳定阶段后,在 1 个 SBR 运行周期内,空白组与对照组SBR 水相 COD 下降趋势与改工况前类似,在第 4 h

降至最低并一直稳定在 35 mg·L<sup>-1</sup>左右;且空白组水相 COD 下降速率和幅度更显著,这说明改变工况更利于空白组 SBR 系统处理废水效能.

2. 3. 2 不同工况下 BPA 对照组单周期内 BPA 浓度 变化

对比两个工况条件稳定时 BPA 对照组水、泥相中BPA 含量在 1 个 SBR 周期内的变化趋势,如表 3 所示.

表 3 两工况条件稳定阶段 40  $\mathrm{mg}\cdot\mathrm{L}^{-1}\mathrm{BPA}$  组污泥单周期内水相和泥相  $\mathrm{BPA}$  浓度变化 $^{1)}$ 

Table 3 Concentrations of BPA variation in liquid and sludge of 40 mg  $\cdot$  L  $^{-1}$ 

BPA control group during an operation cycle between two operation conditions 运行时间/b

| 项目                        | 指标                       |      |        | 运行时间/h |       |      |      |      |      |      |      |
|---------------------------|--------------------------|------|--------|--------|-------|------|------|------|------|------|------|
| 次日                        | 1日7小                     | 0    | 0.5    | 1      | 1.5   | 2    | 3    | 6    | 8    | 10   | 12   |
| SRT = 20 d HRT = 12 h     | 水相 c/mg·L <sup>-1</sup>  | 40   | 17. 25 | 8. 36  | < DL  | < DL | < DL | < DL | < DL | < DL | < DL |
| Sitt = 20 ti fitt = 12 ii | 总泥相 c/mg·L <sup>-1</sup> | < DL | < DL   | < DL   | < DL  | < DL | < DL | < DL | < DL | < DL | < DL |
| SRT = 10 d HRT = 8 h      | 水相 c/mg·L-1              | 40   | 22. 1  | 19. 81 | 14.62 | 9.56 | < DL | < DL | < DL | _    | _    |
|                           | 总泥相 c/mg·L <sup>-1</sup> | < DL | < DL   | < DL   | < DL  | < DL | < DL | < DL | < DL | _    |      |

<sup>1)</sup> DL = 0.1 mg $\cdot$ L<sup>-1</sup>

从表 3 可知,两种工况稳定阶段,对照组泥相BPA 含量均低于检测限;水相BPA 在 3 h 内可被完全降解;改变工况后BPA 在水相中的降解速率低于原工况,但不影响出水效果.分析认为,原工况条件经高浓度BPA 驯化,对照组污泥相已存在大量可有效降解BPA 的优势菌群,因HRT和 SRT 较长,大量代谢速度慢,世代周期长的菌群可以存活,故污泥相菌群组成较为丰富、生物相较完善;而缩短HRT和 SRT后,污泥相中微生物菌群结构发生改变,主要以代谢速度快,世代周期短的微生物为主<sup>[23~26]</sup>,因缺乏不同菌群间"产物抑制"的消除效应,形成较多中间降解产物,一定程度上抑制了BPA 总体去除速率,故 BPA 在系统中降解去除速率较原工况条件稍慢.

# 2.3.3 不同工况条件稳定期 BPA 对照组单周期内的污泥毒性变化

图 5 所示,原工况条件当活性污泥系统达到稳定阶段,由于系统内已大量存在有效降解 BPA 优势菌群,因此污泥总毒性抑制率在 2 h 处较低,为 36.97%;通过 BPA 优势降解菌作用,第 2 ~ 6 h 污泥总毒性抑制率持续下降至最低点不足 30%;随后污泥总毒性波动上升,在周期末第 12 h 达 42.75%,高于周期初始第 2 h 时的毒性值. 经分析,认为污泥总毒性在 6 h 后出现波动且重升至高点的原因是:一方面由于进水 BPA 含量较高,微生物降解过程中产生有毒副产物量多,毒性大,不能被微生物吸收和进一步降解为无毒物质,因此毒性有累积;另一方面由于系统在第 6 h 后停止曝气,系统溶解氧降低,微生物降解 BPA 及其有毒副产物速度减慢,效率降低,且产生大量 SMP 等难降解物质造成毒性升高.

调整工况条件缩短 HRT 和 SRT 后,系统内污

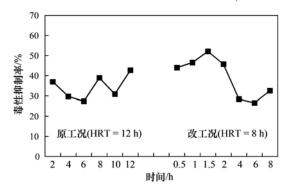


图 5 两工况条件稳定阶段单周期内污泥 总毒性抑制率变化趋势对比

Fig. 5 Comparison of total sludge toxicity variation with time during an operation cycle between two operation conditions

泥总毒性抑制率从第 0. 5 h 开始逐渐增加至第 1.5 h,随后又单调下降且在第 4 h 处达到稳定,直至周期结束维持在 30% 附近.同时对比第 2 h 时的污泥总毒性抑制率改工况后为 45.7%,高于原工况时的 36.97%;分析认为,由于 HRT 缩短,并保持进水 COD 和 BPA 含量不变,污泥负荷升高,因此相同 2 h 内降解 BPA 所产生的污泥毒性有所增加.改变工况后周末第 8 h 系统内污泥总毒性抑制率为 32.56%,明显低于原工况第 12 h 时的 42.75%.说明处理高浓度 BPA 模拟废水的 SBR 污泥系统,缩短 HRT 和 SRT 不仅筛选了代谢速率快,世代周期短的 BPA 降解菌,且微生物活性也显著增强,加快了系统中毒性残留物质的消耗,污泥总毒性削减明显,从而降低剩余污泥后续处理处置及资源化利用的成本和环境风险.

### 2.4 污泥总毒性与微生物群落之间的相关性分析

有机物对微生物菌群的生物多样性和变异特性的影响是复杂的<sup>[27]</sup>. 活性污泥降解 BPA 及其有毒副产物过程中产生了污泥毒性,势必导致污泥相微生物菌群发生变化. 通过 PCR-DGGE 分析技术,对两 SBR 污泥相微生物群落结构的多样性和相似性进行研究,得出菌群多样性与污泥总毒性间的相关性信息,分述如下.

**2.4.1** 香农-威尔指数 (Shannon-Weaver diversity index) 与污泥总毒性之间的相关性分析

Shannon-Weaver diversity index (H)是一种常用的评估微生物多样性的指标<sup>[28]</sup>,公式为:

$$H = - \sum (n_i/N) \ln(n_i/N)$$

式中, $n_i$  为 Band i 的峰值,i 为一条 DGGE 条带 Lane 上的 Band 的排序,N 为此条带 Lane 上所有 Band 的峰值总和. 应用香农-威尔指数的显著优势就是可以综合考虑菌种数量(number of species)和物种均匀度(evenness of given community); H 值越大,说明微生物群落多样性越高.

由表 4 可知,原工况条件稳定阶段 40 mg·L<sup>-1</sup> BPA 对照组(3 号)污泥系统微生物多样性(H=3.72)大于空白组(1 号)污泥系统(H=3.59);说明相对于空白组污泥,BPA 对照组由于进水中含有高浓度 BPA,污泥系统内微生物受到 BPA 驯化而产生降解 BPA 的优势菌群,同时对照组污泥中含有蛋白胨降解菌,故 BPA 对照组内的微生物多样性高于同时期的空白组污泥.而改变工况条件并重新到达稳定期后,空白组(2 号)污泥微生物菌群多样性明

显增加(H=3.88),而  $40 \text{ mg} \cdot \text{L}^{-1}$  BPA 对照组(4 号)则有所降低(H=3.67).结合 2.2 节中所得污泥毒性抑制率的变化趋势,即缩短 HRT 和 SRT 后,空白组和 BPA 对照组的污泥总毒性均明显降低.试验说明,新工况条件下空白组污泥微生物多样性增加,对降解有机物过程中产生的污泥毒性进行消耗,因此空白组污泥总毒性与微生物菌群多样性呈负相关关系,即污泥毒性抑制率随菌群多样性的增加而降低.

性和微生物菌群多样性都出现降低,即二者呈正相关性关系.分析原因为改变工况条件筛选了 40 mg·L<sup>-1</sup>BPA 对照组污泥中谢速率快、世代周期短的降解蛋白胨和 BPA 的优势菌,而部分代谢速率慢且世代周期长的 BPA 及其中间产物降解菌被淘汰,由此降低了系统内微生物的物种均匀度.且由于缩短了 HRT 和 SRT,污泥负荷增加、污泥活性也相应增强,筛选所得优势菌群对 BPA 及其降解过程中产生毒性物质的消耗速率较快,致使污泥毒性的消减.

表 4 两工况条件稳定阶段污泥样品总毒性抑制率和香浓-威尔指数分析

| ia         | ble 4 Analysis results of Shannon | i-weaver diversity index and to | otal sludge toxicity of four sludg        | e sampies                                |  |  |  |
|------------|-----------------------------------|---------------------------------|---|--|--|--|--|
| 项目         | 样品编号                              |                                 |   |  |  |  |  |
| 坝目         | 1 号                               | 2 号                             | 3 号                                       | 4 号                                      |  |  |  |
| 污泥样品信息     | 原工况条件稳定期空白组                       | 改工况后稳定期空白组                      | 原工况条件稳定期 40<br>mg·L <sup>-1</sup> BPA 对照组 | 改工况后稳定期 40<br>mg·L <sup>-1</sup> BPA 对照组 |  |  |  |
| 污泥总毒性抑制率   | 34. 43%                           | 13. 42%                         | 42.75%                                    | 32. 58%                                  |  |  |  |
| 香农-威尔指数(H) | 3. 59                             | 3. 88                           | 3.72                                      | 3. 67                                    |  |  |  |

Table 4 Analysis results of Shannon-Waavar diversity index and total sludge toxicity of four sludge camples

# **2.4.2** 改变工况条件对 SBR 系统内污泥相似性指数变化的影响

表 5 为用戴斯系数(Dice coefficient)<sup>[29]</sup>计算出的各污泥样品相似性矩阵,得出各样品的相似性.

### 表 5 戴斯系数分析 PCR-DGGE 图谱的相似性矩阵

Table 5 Dice coefficients comparing the similarities

|     | 01 F C I | t-DGGE imger | orints |       |
|-----|----------|--------------|--------|-------|
|     | 1号       | 2 号          | 3 号    | 4 号   |
| 1号  | 100.0    | 63. 0        | 55.0   | 58. 7 |
| 2号  | 63.0     | 100.0        | 57.0   | 55. 2 |
| 3 号 | 55. 0    | 57. 5        | 100.0  | 71.0  |
| 4 号 | 58. 7    | 55. 2        | 71.0   | 100.0 |
|     |          |              |        |       |

如表 5 所示,样品 1~4 号分别代表的样品信息同表 4. 相似性分析结果可看出,样品 3 与 4 相似性最高,为 71.0%,样品 1 与 2 相似性其次,为 63.0%,而样品 1与 3及 2与 4 的相似性最低,分别为 55.0%和 55.2%.这说明改变工况条件前后,BPA 对照组污泥内菌群结构相似度极高.另一方面,对比空白组和 40 mg·L<sup>-1</sup>BPA 对照组,由于进水成分的巨大差异,使得两系统分别在两工况条件下的微生物菌群相似性均很低,分别为原工况的55.0%和变工况的55.2%.充分说明进水成分对于SBR 系统污泥中微生物菌群结构的影响远大于工况条件改变的影响.由于 40 mg·L<sup>-1</sup>BPA 对照组的污泥总毒性始终大于空白组,同样也说明有毒物质的加入才是引起污泥毒性增加的关键因素.

另外, 通过 UPGMA (unweighted pair group

method with arithmetic averages) 算法对样品进行聚类分析<sup>[30]</sup>,如图 6 所示. 更显著地表明 4 个样品共分为两大族群,族群间的相似性仅为 57%,族群内的样品 1 与 2(空白组污泥系统)相似性为 63%,样品 3 与 4(40 mg·L<sup>-1</sup>BPA 对照组)相似性为 71%. 试验运用 UPGMA 算法与用 WPGMA (weighted pair group method with arithmetic averages) 算法所做的系统树状图(图略) 基本相同. 因此断定,应用系统树状图来表示不同污泥样品之间微生物群落的同源性,虽然所用计算方法不同但所得结论基本一致.

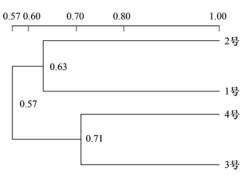


图 6 UPGMA 算法所得污泥样品的系统树状图

Fig. 6 Dendrogram of DGGE patterns of 4 types of sludge samples by UPGMA

### 3 结论

(1)改变工况条件对于空白组和 BPA 对照组周期末出水 COD 影响不大,虽有小幅波动但基本维持在 50 mg·L<sup>-1</sup>左右;新工况条件下 BPA 对照组内微生物可有效降解进水中 BPA,使得整个试验过程周期末出水 BPA 含量低于检测限.

- (2)改变工况条件加速了稳定阶段单个 SBR 运行周期内 COD 的去除速率,减慢了水相 BPA 的去除速率.
- (3)缩短 HRT 和 SRT 有利于降低污泥有机毒性,降低剩余污泥处理处置的成本和资源化利用的环境风险.
- (4)空白组与 40 mg·L<sup>-1</sup>BPA 对照组内微生物 属两大族群;工况参数变化会改变污泥内菌群结构,进而造成污泥毒性变化;而原水中毒性有机物 的存在与否则是引起污泥毒性显著差异的主要 因素.

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## **HUANJING KEXUE**

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### **CONTENTS**

| Analysis of Characteristics of Black Carbon Concentration in Shanghai from 2008 to 2012 · · · · · · · · · · · · · · · · · · ·  |   |
|--|---|
| Chemical Characteristics and Insoluble Particulates' Surface Morphology of a Snowfall Process in the Southeastern Suburb of Urumqi   | LU Hui, WEI Wen-shou, CUI Cai-xia, et al. (1223)  |
| Comparative Study of the Level and Distribution of Polybrominated Diphenyl Ethers and New Brominated Flame Retardants in the A   | tmosphere of Typical Urban  |
|  |   |
| Source and Health Risk Assessment of Heavy Metals in Ambient Air PM <sub>10</sub> from One Coking Plant  |   |
| Estimation of Average Traffic Emission Factor Based on Synchronized Incremental Traffic Flow and Air Pollutant Concentration   |   |
| Study on Critical Loads of Sulfur and Nitrogen in the Pearl River Delta  |   |
| Hydrogen Sulfide Removal by the Combination of Non-Thermal Plasma and Biological Process   |   |
| Spatial Distribution and Risk Assessment of Atrazine in Taizi River Basin, China   |   |
| Development of a Method for Measuring Dissolved Reactive Phosphorus (DRP) and Dissolved Ferrous Iron in Large Batch in Pore  | Water Samples of Sediments with Micro-volumes   |
|  | WANG Yan, ZHU Chun-gang, XU Di, et al. (1271)   |
| Temporal and Spatial Variation of Water Nutrient Level After Exogenous Nutrient Input  |   |
| Physical Process Based Risk Assessment of Groundwater Pollution in the Mining Area   |   |
| Hydrogeochemical Characteristics of a Typical Karst Groundwater System in Chongqing  |   |
| Investigation of Nitrogen, Phosphorus and Microbial Contamination in Laolongdong Underground River System of Chongqing   |   |
| Effects on Phosphorus Fraction Distribution in Sediment by Roots of Vallisneria natans   |   |
| Modeling Nitrogen Transformation in a Novel Circular-Flow Corridor Wetland   |   |
| Natural Attenuation of Tetracycline in the Water of Taihu Lake Under Different Environmental Conditions  | ···· DUAN Lun-chao, WANG Feng-he, JI Ying-xue, et al. (1318)  |
| Inactivation and Reactivation of Antibiotic-Resistant Bacteria During and After UV Disinfection in Reclaimed Water   |   |
| Photoreactivation of Escherichia coli and Enterococcus faecalis in the Secondary Effluent Disinfected by UV-TiO <sub>2</sub>   |   |
| Stability of C <sub>60</sub> Nanoparticles in Aquatic Systems ····   |   |
| Fouling Behavior of Sodium Alginate During Microfiltration at Various Ionic Compositions: XDLVO Approach   | ···· ZHAO Ying-xu, ZONG Rui-qiang, GAO Xin-yu, et al. (1343)  |
| Enhanced Remediation of 4-Chloronitrobenzene Contaminated Groundwater with Nanoscale Zero-valence Iron (nZVI) Catalyzed Hydrogenetics (nZVI) Catalyzed (nZVII) Catalyzed (nZVIII) Catalyzed (nZVIIII) Catalyzed (nZVIII) Catalyzed (nZVIIII) (nZVIIII) (nZVIIII) (nZVIIII) (nZVIIII) (nZVIIII) (nZVIIIII) (nZVIIIII) (nZVIIIII) (nZVIIIIIIIII) (nZVIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIII |   |
| Effect of the Coexistence of Chlorobenzene Homologue on Anaerobic Degradation of Hexachlorobenzene   |   |
| Research on Removal Efficiency of Cd( II )-bearing Wastewater by Sulfate-reducing Biological Filter  |   |
| Control Strategies of Nitrogen Removal Process in a Pilot Test of the Southern WWTP Based on the Nitrogen Balance  | JIANG Ying-he, LIU Pei-ju, WANG Lei, et al. (1372)  |
| Effect of Simulated Inorganic Anion Leaching Solution of Electroplating Sludge on the Bioactivity of Acidithiobacillus ferrooxidans  |   |
| Microbial Reduction of Cu <sup>2+</sup> Mediated by Electroactive Biofilms ·····   |   |
| Copper Recovery from Artificial Bioleaching Lixivium of Waste Printed Circuit Boards   |   |
| Difference of Contaminant Composition Between Landfill Leachates and Groundwater and Its Reasons   | ······ HE Xiao-song, YU Hong, XI Bei-dou, et al. (1399)   |
| Photochemical Degradation of Landfill Leachate Facilitated by Combined Schwertmannite and H <sub>2</sub> O <sub>2</sub> ······   |   |
| Effects of Operating Parameters on Organic Toxicity of Sludge Treating Synthetic Bisphenol A Wastewater  |   |
| Comparative Study on Biological Methane Potential and Methanogen Biodiversity in the Anaerobic Digestion of Excess Sludge · · · · · ·  |   |
| Isolation and Identification of Mn Oxidizing Bacterium Aminobacter sp. H1 and Its Oxidation Mechanism  | ······ YAN Ping, JIANG Li-ying, CHEN Jian-meng, et al. (1428)   |
| Nitrate Removal by a Strain of Nitrate-Dependent Fe( II )-Oxidizing Bacteria   |   |
| Study on the Iopromide-Degrading Characteristics of Strain Pseudomonas sp. I-24 via Co-Metabolism  |   |
| Using Flow Cytometry to Explore the Changes of Sphingomonas sp. GY2B Bacterial Surface Characteristics in the Process of Degrad  | ling Dhananthrona   |
|  | ing i nenantirene   |
|  | ZHANG Meng-lu, DANG Zhi, WU Feng-ji, et al. (1449)  |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  | ZHANG Meng-lu, DANG Zhi, WU Feng-ji, et al. (1449)  |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris   |   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  |   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris   |   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots   |   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots  Responses of Soybean Cultivar Dongsheng-1 to Different O <sub>3</sub> Concentrations in Northeast China  Z   |   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots  Responses of Soybean Cultivar Dongsheng-1 to Different O <sub>3</sub> Concentrations in Northeast China  Z Development and Succession of Biological Soil Crusts and the Changes of Microbial Biomasses   |   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots  Responses of Soybean Cultivar Dongsheng-1 to Different O <sub>3</sub> Concentrations in Northeast China  Z Development and Succession of Biological Soil Crusts and the Changes of Microbial Biomasses  Effects of Lead on the Growth and Reproduction of Eisenia fetida with Aged Soils   |   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots  Responses of Soybean Cultivar Dongsheng-1 to Different O <sub>3</sub> Concentrations in Northeast China  Z Development and Succession of Biological Soil Crusts and the Changes of Microbial Biomasses  Effects of Lead on the Growth and Reproduction of Eisenia fetida with Aged Soils  Soil Heavy Metal Cadmium Standard Limit and Range of Background Value Research  Study on Soil Element Background Values of the Hoh Xil Area in North Tibet  Transfer Characteristic and Source Identification of Soil Heavy Metals from Water-Level-Fluctuating Zone Along Xiangxi River, Thr  | ZHANG Meng-lu, DANG Zhi, WU Feng-ji, et al. (1449) CHEN Shan-jia, CHEN Xiu-rong, YAN Long, et al. (1457) WANG Shan, ZHAO Shu-xin, WEI Chang-long, et al. (1462) WANG Wei-min, DENG Yu, ZOU Hua, et al. (1468) HANG Wei-wei, WANG Guang-hua, WANG Mei-yu, et al. (1473) WU Li, ZHANG Gao-ke, CHEN Xiao-guo, et al. (1479) CHEN Li-hong, LIU Zheng-tao, FANG Zheng, et al. (1486) ZHAO Xiao-jun, LU Si-jin, XU Ren-ji, et al. (1491) BAI Jian-kun, WANG Jian-li, LI Chao-liu, et al. (1498)   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots  Responses of Soybean Cultivar Dongsheng-1 to Different O <sub>3</sub> Concentrations in Northeast China  Z Development and Succession of Biological Soil Crusts and the Changes of Microbial Biomasses  Effects of Lead on the Growth and Reproduction of Eisenia fetida with Aged Soils  Soil Heavy Metal Cadmium Standard Limit and Range of Background Value Research   | ZHANG Meng-lu, DANG Zhi, WU Feng-ji, et al. (1449) CHEN Shan-jia, CHEN Xiu-rong, YAN Long, et al. (1457) WANG Shan, ZHAO Shu-xin, WEI Chang-long, et al. (1462) WANG Wei-min, DENG Yu, ZOU Hua, et al. (1468) HANG Wei-wei, WANG Guang-hua, WANG Mei-yu, et al. (1473) WU Li, ZHANG Gao-ke, CHEN Xiao-guo, et al. (1479) CHEN Li-hong, LIU Zheng-tao, FANG Zheng, et al. (1486) ZHAO Xiao-jun, LU Si-jin, XU Ren-ji, et al. (1491) BAI Jian-kun, WANG Jian-li, LI Chao-liu, et al. (1498)   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots  Responses of Soybean Cultivar Dongsheng-1 to Different O <sub>3</sub> Concentrations in Northeast China  Z Development and Succession of Biological Soil Crusts and the Changes of Microbial Biomasses  Effects of Lead on the Growth and Reproduction of Eisenia fetida with Aged Soils  Soil Heavy Metal Cadmium Standard Limit and Range of Background Value Research  Study on Soil Element Background Values of the Hoh Xil Area in North Tibet  Transfer Characteristic and Source Identification of Soil Heavy Metals from Water-Level-Fluctuating Zone Along Xiangxi River, Thr  | ZHANG Meng-lu, DANG Zhi, WU Feng-ji, et al. (1449) CHEN Shan-jia, CHEN Xiu-rong, YAN Long, et al. (1457) WANG Shan, ZHAO Shu-xin, WEI Chang-long, et al. (1462) WANG Wei-min, DENG Yu, ZOU Hua, et al. (1468) HANG Wei-wei, WANG Guang-hua, WANG Mei-yu, et al. (1473) WU Li, ZHANG Gao-ke, CHEN Xiao-guo, et al. (1479) CHEN Li-hong, LIU Zheng-tao, FANG Zheng, et al. (1486) ZHAO Xiao-jun, LU Si-jin, XU Ren-ji, et al. (1491) BAI Jian-kun, WANG Jian-li, LI Chao-liu, et al. (1498) ee-Gorges Reservoir Area XU Tao, WANG Fei, GUO Qiang, et al. (1502)   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots  Responses of Soybean Cultivar Dongsheng-1 to Different O <sub>3</sub> Concentrations in Northeast China  Z Development and Succession of Biological Soil Crusts and the Changes of Microbial Biomasses  Effects of Lead on the Growth and Reproduction of Eisenia fetida with Aged Soils  Soil Heavy Metal Cadmium Standard Limit and Range of Background Value Research  Study on Soil Element Background Values of the Hoh Xil Area in North Tibet  Transfer Characteristic and Source Identification of Soil Heavy Metals from Water-Level-Fluctuating Zone Along Xiangxi River, The  | ZHANG Meng-lu, DANG Zhi, WU Feng-ji, et al. (1449) CHEN Shan-jia, CHEN Xiu-rong, YAN Long, et al. (1457) WANG Shan, ZHAO Shu-xin, WEI Chang-long, et al. (1462) WANG Wei-min, DENG Yu, ZOU Hua, et al. (1468) HANG Wei-wei, WANG Guang-hua, WANG Mei-yu, et al. (1473) WU Li, ZHANG Gao-ke, CHEN Xiao-guo, et al. (1479) CHEN Li-hong, LIU Zheng-tao, FANG Zheng, et al. (1486) ZHAO Xiao-jun, LU Si-jin, XU Ren-ji, et al. (1491) BAI Jian-kun, WANG Jian-li, LI Chao-liu, et al. (1498) ee-Gorges Reservoir Area XU Tao, WANG Fei, GUO Qiang, et al. (1502) LI Jiong-hui, WENG Shan, FANG Jing, et al. (1509)   |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots  Responses of Soybean Cultivar Dongsheng-1 to Different O <sub>3</sub> Concentrations in Northeast China  Z Development and Succession of Biological Soil Crusts and the Changes of Microbial Biomasses  Effects of Lead on the Growth and Reproduction of Eisenia fetida with Aged Soils  Soil Heavy Metal Cadmium Standard Limit and Range of Background Value Research  Study on Soil Element Background Values of the Hoh Xil Area in North Tibet  Transfer Characteristic and Source Identification of Soil Heavy Metals from Water-Level-Fluctuating Zone Along Xiangxi River, Thr  | ZHANG Meng-lu, DANG Zhi, WU Feng-ji, et al. (1449) CHEN Shan-jia, CHEN Xiu-rong, YAN Long, et al. (1457) WANG Shan, ZHAO Shu-xin, WEI Chang-long, et al. (1462) WANG Shan, ZHAO Shu-xin, WEI Chang-long, et al. (1468) WANG Wei-min, DENG Yu, ZOU Hua, et al. (1468) WANG Wei-wei, WANG Guang-hua, WANG Mei-yu, et al. (1473) WU Li, ZHANG Gao-ke, CHEN Xiao-guo, et al. (1479) CHEN Li-hong, LIU Zheng-tao, FANG Zheng, et al. (1486) ZHAO Xiao-jun, LU Si-jin, XU Ren-ji, et al. (1491) BAI Jian-kun, WANG Jian-li, LI Chao-liu, et al. (1498) ee-Gorges Reservoir Area XU Tao, WANG Fei, GUO Qiang, et al. (1502) LI Jiong-hui, WENG Shan, FANG Jing, et al. (1509) ZHANG Hai-zhen, TANG Yu-li, LU Jun, et al. (1516)  |
| Research on Characteristic of Interrelationship Between Toxic Organic Compound BPA and Chlorella vulgaris  Effect of Magnesium Deficiency on Photosynthetic Physiology and Triacylglyceride (TAG) Accumulation of Chlorella vulgaris  Effects of Microcystins on Growth and Antioxidant System of Rice Roots  Responses of Soybean Cultivar Dongsheng-1 to Different O <sub>3</sub> Concentrations in Northeast China  Z Development and Succession of Biological Soil Crusts and the Changes of Microbial Biomasses  Effects of Lead on the Growth and Reproduction of Eisenia fetida with Aged Soils  Soil Heavy Metal Cadmium Standard Limit and Range of Background Value Research  Study on Soil Element Background Values of the Hoh Xil Area in North Tibet  Transfer Characteristic and Source Identification of Soil Heavy Metals from Water-Level-Fluctuating Zone Along Xiangxi River, The  Heavy Metal Pollution Characteristics and Ecological Risk Analysis for Soil Around Haining Electroplating Industrial Park  Sources and Spatial Distribution of Typical Heavy Metal Pollutants in Soils in Xihu Scenic Area  | ZHANG Meng-lu, DANG Zhi, WU Feng-ji, et al. (1449) CHEN Shan-jia, CHEN Xiu-rong, YAN Long, et al. (1457) WANG Shan, ZHAO Shu-xin, WEI Chang-long, et al. (1462) WANG Shan, ZHAO Shu-xin, WEI Chang-long, et al. (1468) WANG Wei-min, DENG Yu, ZOU Hua, et al. (1468) WANG Wei-wei, WANG Guang-hua, WANG Mei-yu, et al. (1473) WU Li, ZHANG Gao-ke, CHEN Xiao-guo, et al. (1479) CHEN Li-hong, LIU Zheng-tao, FANG Zheng, et al. (1486) ZHAO Xiao-jun, LU Si-jin, XU Ren-ji, et al. (1491) WEO-Gorges Reservoir Area XU Tao, WANG Fei, GUO Qiang, et al. (1502) LI Jiong-hui, WENG Shan, FANG Jing, et al. (1509) ZHANG Hai-zhen, TANG Yu-li, LU Jun, et al. (1516)  |
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