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次 目

铁铜催化剂非均相 Fenton 降解苯酚及机制研究

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摘要:通过浸渍法制备了负载于活性炭(AC)上的金属催化剂 Fe/AC、Cu/AC 和 Fe-Cu/AC,并通过 X 射线衍射(XRD)、物理吸附仪及 X 射线光电子能谱(XPS)对其进行了表征. 研究了非均相 Fenton 反应催化 H_2O_2 降解苯酚废水的工艺参数,并通过中间产物分析和电子自旋共振谱(ESR)探讨了过程反应机制. 实验表明,Cu/AC 催化剂中铜主要以 CuO 形式存在,Fe/AC 中铁以多价态形式存在,以无定形形态分散于活性炭中. Fe/AC、Cu/AC 和 Fe-Cu/AC 催化过氧化氢降解苯酚 60 min 内降解率分别达到 96.7%、77.5%和 99%;Cu/AC 和 Fe-Cu/AC 催化剂中活性组分铜和铁有一定溶出,而 Fe/AC 中活性组分铁溶出很少,苯酚降解主要是以非均相催化为主,同时在三轮循环实验后的苯酚降解率仍然高达 93%以上,显示了良好的催化稳定性. 在优化条件 pH=3、T=303 K 及初始 H_2O_2 为 4.38 mmol·L⁻¹下,Fe/AC 催化过氧化氢对苯酚和 TOC 去除率分别达到 97%和 53%,没有催化剂时苯酚几乎不降解. ESR 结果表明 Fe/AC 催化过氧化氢产生了羟基自由基,证明苯酚降解是以羟基自由基氧化为主;通过高效液相色谱(HPLC)检测苯酚降解中间产物主要有邻苯二酚、对苯二酚和对苯醌,推测苯酚降解途径主要为邻位和对位的羟基取代反应.

关键词:活性炭; 酚类废水; 非均相 Fenton; 高级氧化; 催化剂

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Degradation of Phenol with a Fe/Cu-Catalytic Heterogeneous-Fenton Process

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(1. School of Chemical and Biological Engineering, Changsha University of Science and Technology, Changsha 410004, China; 2. Key Laboratory of Green Process and Engineering, Institute of Process Engineering, Chinese Academy of Sciences, Beijing 100190, China) Abstract: The catalysts of Fe/AC, Cu/AC and Fe-Cu/AC with active carbon as support were prepared by a wet impregnation method, and were characterized using X-ray diffraction (XRD), nitrogen adsorption and X-ray photoelectron spectroscopy (XPS) measurements; the catalytic heterogeneous-Fenton processes of phenol degradation with these catalysts were also investigated, and the degradation mechanism was discussed with analysis of intermediate products and electron spin resonance (ESR) measurement. The results showed that the active component states varied in different catalysts; CuO was the main state of Cu in Cu/AC and Fe exhibited various valence states in Fe/AC. The degradation rate of phenol with Fe/AC, Cu/AC and Fe-Cu/AC as catalyst in the initial 60 min reached 96.7%, 77.5% and 99%, respectively; the dissolution of a little active-component metal was found in Cu/AC and Fe-Cu/AC, but little Fe in Fe/AC was dissolved; the degradation of phenol was performed by heterogeneous Fe/AC instead of dissolved Fe, and the degradation rate was above 93% after Fe/AC was used for three cycle runs, showing a stable catalytic activity. Under the optimum conditions of pH = 3, T = 303 K, and 4.38 mmol·L⁻¹ H₂O₂, the removal of phenol and TOC in the Fe/AC-catalytic Fenton process could reach 97% and 53%, respectively, while little phenol was degraded without catalyst. The ESR results indicated that hydroxyl radical was produced in the catalytic decomposition of H2O2 with Fe/AC as catalyst, demonstrating that the degradation of phenol mainly followed an oxidation pathway of hydroxyl radical; intermediates such as hydroquinone, p-benzenequinone and catechol were obtained, and the results showed thatortho- and para-substitution reaction by hydroxyl might be the main mechanism of phenol oxidation.

Key words: activated carbon; phenolic wastewater; heterogeneous Fenton; advanced oxidation; catalyst

酚类废水产生于造纸、农药及煤化工等多种生产过程,这类废水不仅毒性大,而且具有致癌、致畸以及致突变的潜在毒性[1]. 采用驯化和构建的高效菌尽管能降解酚类有机物,但是容易受到高浓度酚类有机物抑制,以强氧化性自由基(主要是·OH)为氧化剂的高级氧化技术(AOPs)对于酚类废水处理效果显著而受到关注^[2~5]. ·OH作为强氧化剂,其氧化还原电势为 2.8 V/SHE,仅次于 F₂,可以无选择地与许多有机物发生去氢反应、亲电加成、取代

反应和电子转移反应,进而将有机物彻底矿化为 CO_2 和 H_2O 或者氧化分解为易生物降解产物 $^{[6]}$.传统 Fenton 技术 $^{[7]}$ 主要利用 Fe^{2+} 与 H_2O_2 反应生成 $\cdot OH$,因其操作条件温和,处理效果好以及环境友好等特点,已广泛应用于有机废水的处理 $^{[1.8,9]}$. 但传

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统 Fenton 技术通常限制在 pH 为 2~4 范围内,而且反应过程中产生铁泥,需要进一步地分离和处理,为此学者提出非均相 Fenton 以解决上述问题^[10~14]. 但是,非均相 Fenton 反应 H_2O_2 利用率较低,其 H_2O_2 /污染物(摩尔比)高达1000~6000^[15],反应一般需要在 40° C以上进行^[16],因此,研究在室温下进行高效反应的新型非均相催化剂,并提高 H_2O_2 利用率具有重要意义.

活性炭(AC)具有较高的比表面积,价格低廉,以及良好的吸附性能,是比较好的催化剂载体^[17~19].本研究选择活性炭作为载体,制备了铁铜/活性炭催化剂,在常温下实现了苯酚高效非均相类 Fenton 降解,考察了温度、pH及H₂O₂添加量等因素对苯酚的降解效果的影响,并证明反应主要以非均相催化为主,初步推测了苯酚的降解机制及途径.

1 材料与方法

1.1 实验试剂

苯酚、85%磷酸、30%过氧化氢、硝酸铁、硝酸铜均为分析纯,购于西陇化工股份有限公司.活性炭(AC)、邻苯二酚、对苯二酚和对苯醌购于Alfa-Aesar. AC 用稀盐酸浸泡 24 h 去除杂质,用去离子水洗涤至中性,烘干备用.

1.2 实验流程

催化剂的制备采用浸渍法. 分别称取一定量的 AC 浸渍于硝酸铁、硝酸铜或者硝酸铁和硝酸铜的 混合溶液, 充分搅拌均匀后, 室温静置 24 h, 在 100℃下干燥 12 h, 氮气气氛中 300℃煅烧 3 h, 洗涤干燥, 得到的催化剂分别标记为 Fe/AC、Cu/AC、Fe-Cu/AC.

将酚类模拟废水 (100 mg·L⁻¹) 倒入棕色广口试剂瓶 (避免光照),加入催化剂,恒温水浴搅拌过夜,达到吸附饱和后,用稀 HNO₃ 和 NaOH 调节溶液pH;加入一定量的 H_2O_2 作为反应起点,不同时间间隔取样.样品加入少量 MnO₂ 分解样品中 H_2O_2 终止反应,0. 22 μ m 滤膜过滤后 HPLC 测有机物浓度.

1.3 分析方法

苯酚及降解中间产物的测定采用高效液相色谱 (HPLC),SB-C18 柱,流动相为 25% 甲醇和 75% 超 纯水(10 mmol·L⁻¹磷酸),流速为 0.25 mL·min⁻¹, 检测波长为 215 nm 和 254 nm,柱温 35℃. 有机物浓度通过标准曲线确定. 采用康塔物理吸附仪 (Quantachrome-IQ)测定样品在 77 K 下氮气吸附脱附等温线,通过 BET 方程计算样品的比表面积,总

孔容通过相对压力 $P/P_0 = 0.99$ 附近的 N_2 吸附量 计算,采用骤冷固体密度函数理论(OSDFT)分析孔 径分布,采用 t-plot 模型计算微孔体积和微孔表面 积. 通过 X 射线衍射仪(X'Pert PRO MPD)对样品进 行晶相分析(测试参数:管电压 40 kV,管电流 20 mA, CuKα, λ = 0.15406 nm, 扫描范围 10° ~90°). 样品中金属的价态通过 VG Scientific ESCALAB 250Xi 型光电子能谱仪(XPS)分析. 实验参数:激发 源为 Al KαX 射线,全谱和各元素的精细谱扫描步 长分别为 1 eV 和 0.05 eV,恒定分析能分别为 100 eV 和 20 eV, 电子结合能用污染碳的 C1. 峰(284.8 eV)校正. 总有机碳(TOC)采用岛津 TOC-V_{CPI}测定 仪测定. 催化剂金属含量以及反应溶解金属含量采 用电感耦合等离子体发射光谱仪(ICP-AES, Perkin Elmer Optima 5300DV) 测定; 溶出 Fe²⁺含量采用邻 菲罗啉分光光度法测定. 采用 DMPO 作为自由基自 旋捕获剂,自由基加合物采用 ESR 波谱测定. X-波 段 Bruker E-500 波谱仪的操作条件如下:磁场中心 3 480 × 10⁻⁴ T; 微波功率0.010 09 W; 时间常数 0.04096 s.

2 结果与讨论

2.1 AC 负载金属催化剂孔道结构及晶型特征

图 1 为 AC 及 AC 负载金属的催化剂氮气吸附脱附曲线及孔径分布图,介孔及微孔孔径分布采用 *t*-plot 模型计算. 所有等温线均为 I 型,并带有 H4型回滞环. 从孔径分布图可知,AC 主要为微孔结构(<2 nm),同时也含少量介孔(2~50 nm). 表 1 为样品孔道结构特征,AC 负载金属后,比表面积及孔容均有所下降,说明负载金属后,少量孔道堵塞.

图 2 为催化剂的 XRD 图,从中可知,催化剂在20°~30°间较宽的峰可归结为无定形碳,AC 各处衍射峰有可能是由微孔或大孔衍射形成;而 Cu/AC 在36.4°、42.1°、61.2°特征衍射峰明显,晶型良好,与 JCPDS 标准卡片 780428 相符,铜主要以 CuO 形式存在; Fe/Cu/AC 催化剂同样出现 CuO 特征峰,但是峰型较低而且不明显,可能是因为 Fe 的存在阻碍 Cu 团聚长成晶体;而 Fe/AC 催化剂未出现明显 Fe 氧化物特征峰,说明 Fe 主要以无定形形态存在.

图 3 为 Fe/AC 样品 Fe2p 的 XPS,经拟合分峰,该样品在 710.8 eV 和 712.7 eV 处的峰分别对应 Fe(\blacksquare)和 Fe(\blacksquare)2 $p_{3/2}$ 峰,724 eV 和 726 eV 处峰分别对应 Fe(\blacksquare)和 Fe(\blacksquare)2 $p_{1/2}$ 峰 $[^{20}]$,说明 Fe/AC 中铁以多价态形式存在.

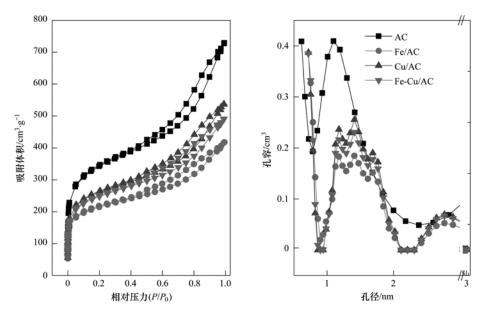


图 1 催化剂氮气吸附/脱附等温线及孔径分布

Fig. 1 Nitrogen adsorption-desorption isotherms and pore size distributions of catalysts

表 1 催化剂物理性能

Table 1 Physical properties of the catalysts

			- my order proportion of			
样品	ω(Fe) /%	ω(Cu) /%	比表面积 /m²·g ⁻¹	总孔容 /cm³·g ⁻¹	微孔孔容 /cm³·g ⁻¹	介孔孔容 /cm³·g ⁻¹
AC	_	_	1 232. 5	1. 13	0. 34	0.79
Cu/AC	_	10	941. 9	0. 83	0. 24	0. 59
Fe/AC	4. 1	_	779. 1	0.76	0.21	0. 55
Fe-Cu/AC	5	7.5	893. 1	0. 65	0. 23	0. 42

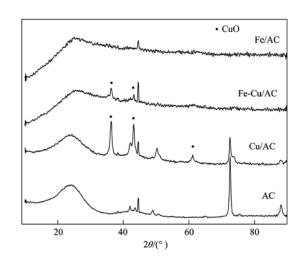


图 2 不同催化剂 XRD 图谱

Fig. 2 XRD images of catalysts

2.2 催化剂降解效果

图 4 为 H_2O_2 、AC 以及二者同时存在对苯酚的 去除效果. 从中可知,AC 较大的比表面积有利于苯酚的吸附,活性炭吸附苯酚在 10 min 左右即达到饱和,吸附容量达到 40 $\text{mg}\cdot\text{g}^{-1}$. AC 加入 H_2O_2 后,溶液中苯酚浓度随时间的变化曲线与 AC 吸附苯酚的

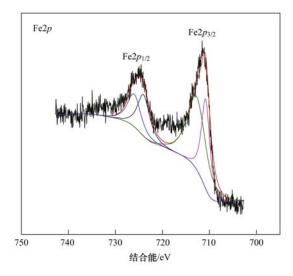
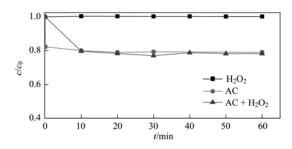


图 3 Fe/AC 催化剂 Fe2p XPS 图谱

Fig. 3 Fe2p XPS spectra of Fe/AC catalysts

曲线基本重合,表明苯酚浓度的降低主要是由于吸附作用,AC 直接催化 H_2O_2 生成·OH的效果不明显,可能是由于研究的时间较短(60 min). Ramirez 等^[10]的研究表明,活性炭能够催化 H_2O_2 降解有机污染物,但是降解速率非常缓慢. 单独投加 H_2O_2 由于

其氧化还原电位较低,基本不与苯酚反应. 图 5 为 不同催化剂降解苯酚效果,通过比较3种负载金属 AC 催化剂降解苯酚发现:Fe/AC 作为催化剂 60 min 降解苯酚效果达到96.7%,而Cu/AC作为催化剂降 解效果仅为77.5%,同时发现Fe/AC、Cu/AC作为 催化剂反应 60 min 后溶出 Fe3+、Cu2+量分别为 0.41 mg·L⁻¹和41.12 mg·L⁻¹,说明在酸性环境下 铁相对于铜不容易溶出,这与文献[11]研究结果一 致. 双金属 Fe-Cu/AC 催化剂表现出最佳的降解效 果,60 min 内苯酚完全去除,TOC 去除率达到 60%. 这可能是因为掺杂铜增加了活性位点数量,并改变 了铁系催化剂中颗粒的结构和价态[21],另外溶出的 金属也可能发生均相 Fenton 反应, 使降解效果增 加. 综合考虑降解效果及金属溶出情况,可以认为 Fe/AC 催化剂性能最好,后续实验以 Fe/AC 催化剂 进行实验.



苯酚浓度为 100 mg·L $^{-1}$,AC 用量为 0.5 g·L $^{-1}$,pH = 3, T = 303 K,H $_2$ O $_2$ 初始浓度为 4.38 mmol·L $^{-1}$

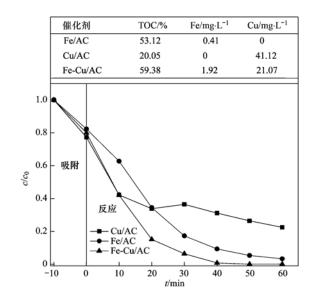
图 4 H₂O₂、AC 及H₂O₂ + AC 去除苯酚效果

Fig. 4 Phenol removal by $\mathrm{H_2O_2}$, AC and $\mathrm{H_2O_2} + \mathrm{AC}$

2.3 Fe/AC 降解苯酚影响因素研究

2.3.1 pH 的影响

在非均相 Fenton 反应中, pH 值影响催化剂中金属的溶出以及 H_2O_2 的分解. 图 6 为不同 pH 条件下苯酚及 TOC 的去除效果. 从中可知,随着 pH 的增加,苯酚及 TOC 去除率下降. 当 pH = 3 时,催化剂对苯酚的降解效果最好,60 min 内苯酚去除率接近 100%, TOC 去除率达到 53%; 当 pH = 4 时,TOC 去除率接近 40%; 而当 pH = 5 时,苯酚的去除主要依赖 AC 的吸附作用,基本上不发生 Fenton 反应. 这可能是因为 pH 增加, H_2O_2 容易无效分解成 H_2O_2 和 O_2 ,而不是形成·OH,从而使氧化能力下降. 另外,在 pH 分别为 3、4、5 条件下,ICP 测定溶出金属量分别为 0.41、0.30、0.15 mg·L⁻¹,邻菲罗啉显色法测定溶出金属中无 Fe²⁺,说明溶出金属为 Fe³⁺,为探讨均相 Fenton 反应对苯酚降解的影响,在相同

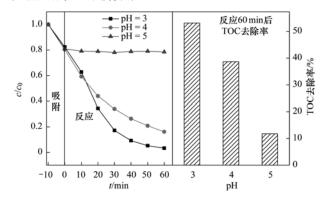


苯酚浓度为 $100~{\rm mg\cdot L^{-1}}$,催化剂用量为 $0.5~{\rm g\cdot L^{-1}}$, ${\rm pH=3}$, $T=303~{\rm K}$, ${\rm H_2O_2}$ 初始浓度为 $4.38~{\rm mmol\cdot L^{-1}}$, 插表为反应 $60~{\rm min}$ 后 ${\rm TOC}$ 去除率及金属溶出量

图 5 不同催化剂降解苯酚效果

Fig. 5 Phenol degradation by different catalysts

的条件下,加入与溶出金属等量的 Fe³⁺,苯酚几乎 无降解,说明 Fe/AC 降解苯酚主要是非均相 Fenton 反应生成·OH起作用.



苯酚浓度为 100 mg·L $^{-1}$,催化剂用量为 0.5 g·L $^{-1}$,T = 303 K, H, O, 初始浓度为 4.38 mmol·L $^{-1}$

图 6 Fe/AC 不同 pH 条件降解苯酚效果

Fig. 6 Effect of pH on the degradation of phenol

2.3.2 H,O,投加量的影响

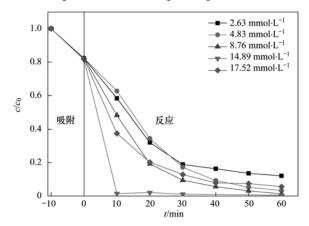
图 7 为 H_2O_2 添加量对苯酚降解的影响,从中可知,苯酚的降解速率随 H_2O_2 添加量的增加而增大,这是因为随着 H_2O_2 量的增加,Fenton 反应生成的 ·OH数量增多,从而加速苯酚的降解. 当 H_2O_2 投加量为将苯酚完全矿化的 14.89 mmol· L^{-1} 时[式(1)],苯酚降解速率达到最大,1 h 内苯酚降解率达到 100%, TOC 去除达到 60%. 但是,当 H_2O_2 添加量继续增加到 17.52 mmol· L^{-1} 时, 苯酚的降解速率反

而下降,这是因为过量的H,O,作为·OH的捕获剂, 导致溶液中 \cdot OH的数量减少[式(2)和式(3)][22].

$$C_6H_6O + 14 H_2O_2 \longrightarrow 6CO_2 + 17H_2O$$
 (1)

$$H_2O_2 + \cdot OH \longrightarrow H_2O + HO_2 \cdot$$
 (2)

$$HO_2 \cdot + \cdot OH \longrightarrow H_2O + O_2$$
 (3)



苯酚浓度为 100 mg·L⁻¹,催化剂用量为 0.5 g·L⁻¹,pH = 3,T = 303 K 图 7 不同H₂O₂投加量对 Fe/AC 降解苯酚影响

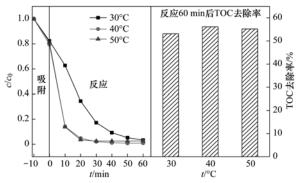
Fig. 7 Effect of H₂O₂ concentration on the degradation of phenol

2.3.3 温度的影响

如图 8 所示, 当温度从 30℃升高至 40℃时, 苯 酚的降解速率迅速增加;但继续升高温度至50℃ 时,降解速度几乎不再变化. 同时发现 TOC 去除率 并没有随着温度的升高而增加. 这可能是由于升高 温度既有利于 Fenton 反应的快速进行,也加快了 H,O,的无效分解. 温度的升高也使得铁溶出量大大 增加, 当温度为 30、40 和 50℃, Fe3+溶出量分别为 0.40、4.76 和 10.31 mg·L⁻¹, Fe³⁺ 容易与羧酸络 合,不能被·OH降解,从而难以达到完全矿化^[6]. 可 以看出,30℃时反应 60 min 时苯酚降解率达到 95% 以上,TOC 去除率大于50%,说明Fe/AC 实现了苯 酚的常温高效催化降解. 考虑到升温能耗的经济性 和活性组分铁的溶出效应,所以30℃为较合适的反 应温度.

2.3.4 Fe/AC 催化剂稳定性

图 9 为 Fe/AC 降解苯酚循环实验,在最优条件 下: pH = 3, 温度为 30℃, H₂O₂ 用量为 4.38 mmol·L⁻¹以及0.5 g·L⁻¹ Fe/AC. 每次反应结束,催 化剂通过过滤分离,超纯水洗涤3次,60℃烘干.从 图 9 可知,随着循环次数增加,Fe/AC 吸附能力明显 下降, 其吸附容量从 36.54 mg·g⁻¹ 下降至 21.5 mg·g⁻¹和17.98 mg·g⁻¹,这是因为残余的中间产物 吸附于 Fe/AC 表面,降低了碳材料的有效吸附面

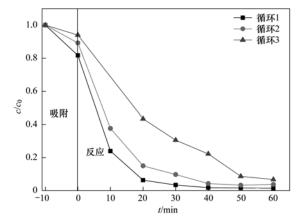


苯酚浓度为 $100 \text{ mg} \cdot \text{L}^{-1}$,催化剂用量为 $0.5 \text{ g} \cdot \text{L}^{-1}$, pH = 3, H, O, 初始浓度为 4.38 mmol·L⁻¹

图 8 不同温度下苯酚降解效果

Fig. 8 Effect of temperature on the degradation of phenol

积,从而使吸附容量下降[23].同时,发现苯酚的降 解速度也大幅下降,可能是由于有机物吸附于活性 位点上或者铁的溶出导致催化剂失活[24]. 在 3 次 循环实验后,1 h 内苯酚的降解率仍达到93%,说明 该催化剂可循环使用,具有一定的稳定性.



苯酚浓度为 100 mg·L⁻¹,催化剂用量为 0.5 g·L⁻¹, pH = 3, T = 303 K, H₂O₂ 初始浓度为 4.38 mmol·L⁻¹

图 9 Fe/AC 催化剂重复实验

Fig. 9 Reuse of catalyst Fe/AC

3 Fe/AC 降解苯酚机制及途径

图 10 为 Fe/AC 催化剂分解H,O,的过程中进行 DMPO·HO 加合物的 ESR 波谱图. 催化剂催化过程 中,检测到一个明显的四重峰,峰强度比为1:2: 2:1,超精细分裂常数: AN = 14.9 G 和 AH = 14.9 G, 是典型的羟基自由基 ESR 信号[25],从而可以确定 体系中生产了·OH. Fe/AC 催化剂分解H,O,发生类 Fenton 反应^[26]:

$$=$$
 Fe(\mathbb{I}) + H₂O₂ \longrightarrow = Fe(\mathbb{I}) + OH⁻ + HO •

图 11 为 Fe/AC 对苯酚降解中间产物变化曲 线,在1h内,苯酚去除率达到98%. 根据文献

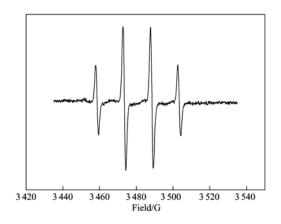


图 10 非均相催化剂 Fe/AC 生成自旋加合物 DMPO·HO 的 ESR 波谱

Fig. 10 ESR spectrum of spin adduct of DMPO·HO' produced by the Fe/AC heterogeneous catalyst

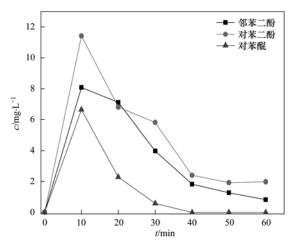


图11 苯酚降解中间产物的浓度变化

Fig. 11 Concentration curves of the phenol degradation intermediates

[27],可初步推测苯酚可能的降解途径为:苯酚在 ·OH攻击下,在邻位或者对位发生去氢反应,生成邻 苯二酚和对苯二酚;同时对苯二酚经过电子转移或 者氧化作用得到对苯醌(图 12). 从图 11 可知,在 前 10 min 内是一个快速降解过程,同时各中间产物 的量均达到峰值;随着时间延长,苯酚降解速度明显下降,这是因为中间产物吸附于 Fe/AC 上,减少了可与H₂O₂反应的活性中心数量,同时中间产物和 苯酚之间竞争作用也降低了苯酚的分解速度. 另外,对苯二酚和对苯醌二者含量之和是邻苯二酚的 2 倍,说明主要发生的是苯酚的对位羟基取代反应.

4 结论

通过浸渍法得到 Fe/AC、Cu/AC、Fe-Cu/AC 这 3 种催化剂,实现苯酚的常温非均相催化氧化. Cu/

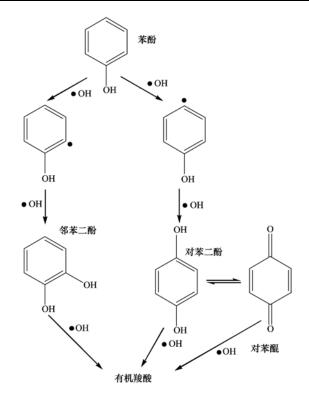


图 12 苯酚可能降解途径

Fig. 12 Possible degradation pathways of phenol

AC、Fe-Cu/AC 一定活性组分溶出, Fe/AC 金属溶出很少,且苯酚降解效率高,同时重复使用催化效率稳定性较好.对比平行实验和 ESR 结果表明,过程主要以非均相催化产生的羟基自由基氧化为主,中间产物分析可推测苯酚主要降解途径为邻位和对位的羟基取代反应.

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