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体积溶氧传递系数在好氧颗粒污泥系统中的变化特性 初步分析

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摘要:取成熟的好氧颗粒污泥,在同一测试装置中采用相同的曝气条件进行体积溶氧传递系数(k_La)的测试,当传统活性污泥和成熟好氧颗粒污泥浓度 MLSS 为2 000、4 000、6 000、8 000 mg·L⁻¹时,其 k_La (min⁻¹)值分别为0.586 1 ± 0.009 5、0.586 1 ± 0.027 2、0.555 6 ± 0.016 8、0.533 8 ± 0.026 8 和0.645 5 ± 0.027 6、0.632 0 ± 0.075 5、0.618 5 ± 0.062 5、0.640 6 ± 0.055 5,表明颗粒污泥 k_La 值高于同浓度条件下的絮体污泥,且随浓度增加,絮体污泥氧传递效率下降而颗粒污泥无明显变化.对好氧颗粒污泥进行筛分后,大颗粒和小颗粒在污泥浓度相同、体积相同、表面积相同以及个数相同的情况下二者的 k_La 值均无明显差别,由此可以推断,这些因素对好氧颗粒污泥 k_La 的影响可以忽略.研究结果对于污水处理厂节能运行具有一定的参考价值.

关键词:体积溶氧传递系数:好氧颗粒污泥:污水处理:絮体结构

中图分类号: X703.1 文献标识码: A 文章编号: 0250-3301(2013)06-2314-05

Preliminary Study on Characteristics of Volumetric Oxygen Transfer Coefficient in Granular Sludge Systems

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Abstract: The volumetric oxygen transfer coefficient (k_La) was tested with mature aerobic granules in the same aeration measurement device and under the same aeration conditions. The k_La (min⁻¹) was 0.586 1 ± 0.009 5, 0.586 1 ± 0.027 2, 0.555 6 ± 0.016 8, 0.533 8 ± 0.026 8 for floc sludge, and 0.645 5 ± 0.027 6, 0.632 0 ± 0.075 5, 0.618 5 ± 0.062 5, 0.640 6 ± 0.055 5 for aerobic granules, when the sludge concentration MLSS (mg·L⁻¹) was controlled at 2 000, 4 000, 6 000, 8 000, respectively. This indicated that granular sludge exhibited higher k_La values than the flocs, and the k_La value of floc sludge decreased with the increase of the sludge concentration; however, insignificant decease was found for granular sludge. After screening of granules with different diameter, the k_La values of the aerobic granular sludge with different sizes which had the same MLSS, volume, surface area and particle number were compared, and insignificant difference was found, suggesting that the effects of these factors on the k_La of granular sludge were negligible. The findings of this work may have significance for the energy-saving operation of wastewater treatment plants.

Key words: volumetric oxygen transfer coefficient; aerobic granular sludge; wastewater treatment; floc structure

曝气过程是污水生物处理过程的重要能耗控制单元[1],氧气传质速率是描述该过程效率的一个非常重要的指标,氧气传质速率的提高是降低好氧污水处理工艺能耗的最直接有效的手段[2~4]. 体积溶氧传递系数 $k_L a$ 是用来表征溶氧传递速率的重要参数,该参数为复合参数,是气液传质系数 $k_L a$ 的研究,主要集中在曝气设备、反应池尺寸形状和温度等物理因素方面,生物过程及工艺参数对溶氧传递过程的影响机制尚不清楚.

好氧颗粒污泥已经成为一个新的研究热点,因 其具有沉降性好、抗冲击负荷能力强、脱氮除磷效 果好等优点而受到国内外学者和工程技术人员的广 泛关注. 在当前对颗粒污泥的研究中,通常都是对 污泥的密度、沉速、形态、强度等常规性指标进行分析^[5~8],同时对于颗粒污泥稳定性的研究也是一个热点,而对于颗粒污泥系统在曝气过程的气液传质速率方面的研究却鲜见报道.

1 材料与方法

1.1 实验装置

本研究 $k_{L}a$ 数据测量采用图 1 所示装置,实验过程中通过水浴将实验温度控制在 (20 ± 0.5) $^{\circ}$,

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搅拌桨保证泥水混合均匀且转速恒定,底部设有曝气砂芯曝气,曝气量用流量计维持恒定.实验数据通过溶氧仪测量,溶氧仪连接电脑采集数据.数据测量过程如图 2 所示,首先曝气使装置内污泥溶解氧达到饱和并平稳 5 min 左右,停止曝气开启搅拌,此时需要将通气孔关闭来保证装置内的密闭性,当溶解氧下降到 1 mg·L⁻¹左右,开始曝气,这时需要打开曝气孔来维持装置内外气压平衡,曝气直到溶解氧达到饱和并平稳 15~20 min 后完成测试,将收集数据拟合得到 $k_{\rm L}a$ 值.在一开始停止曝气后溶解氧曲线的下降斜率可以得到污泥耗氧速率 OUR,打开曝气后溶解氧变化速率为:

$$\frac{\mathrm{d}C}{\mathrm{d}t} = k_{\mathrm{L}}a \cdot [C^{\infty} - C(t)] - \mathrm{OUR}$$

式中, $\frac{dC}{dt}$ 为溶解氧浓度变化速率, $mg \cdot (L \cdot min)^{-1}$; $k_L a$ 为氧传质系数, min^{-1} ; C^{∞} 为饱和溶解氧浓度, $mg \cdot L^{-1}$; C 为溶解氧浓度, $mg \cdot L^{-1}$; OUR 为污泥耗氧速率, $mg \cdot (L \cdot min)^{-1}$.

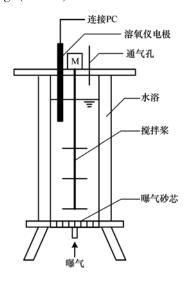


图 1 测量装置示意

Fig. 1 Schematic diagram of measuring device

1.2 实验方法

1.2.1 污泥浓度对好氧颗粒污泥和传统活性污泥 $k_1 a$ 的影响对比

取西安市第四污水处理厂 A^2/O 工艺二沉池回流污泥代表传统絮状活性污泥,实验室气提式反应器内培养的成熟颗粒污泥代表好氧颗粒污泥,反应器运行条件如表 1、2 所示. 分别取指定浓度的两种形态的污泥 $300\,$ mL 放入图 1 所示装置内进行 $k_{\rm L}a$ 测量,控制 MLSS 分别为2 000、4 000、6 000、8 $000\,$ mg·L $^{-1}$.

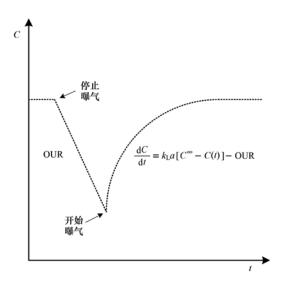


图 2 $k_L a$ 测量过程示意

Fig. 2 Measurement process of $k_{\rm L}a$

表1 反应器运行周期/min

Table 1 Periods of sequencing operation/min

进水	曝气	沉淀	出水	周期时间
2	234	2	2	240

表 2 模拟废水组成/mg·L-1

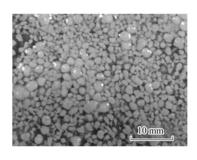
Table 2 Components of the synthetic wastewater/mg·L⁻¹

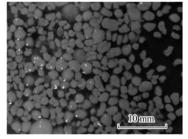
基质名称		基质名称	浓度
COD	1 200	MgSO ₄ ·7H ₂ O	180
NH ₄ -N	1 200 120	CaCl₂ •2H₂ O	28
TP	80	MgSO ₄ ·7H ₂ O CaCl ₂ ·2H ₂ O 微量元素使用液 ¹⁾ /mL·L ⁻¹	0.3

1) 微量元素使用液配方(g·L⁻¹); EDTA 10.00, FeCl₃·6H₂O 1.50, H₃BO₃ 0.15, CuSO₄·5H₂O 0.03, KI 0.18, MnCl₂·H₂O 0.12, NaMoO₄·2H₂O 0.06, ZnSO₄·7H₂O 0.12, CoCl₂·6H₂O 0.15

1.2.2 不同粒径下好氧颗粒污泥表观特性对于 $k_1 a$ 的影响分析

取实验室气提式反应器内培养的成熟颗粒污泥筛分粒径大于1 mm 的大颗粒和0.2~1 mm 的小颗粒,分别测量大颗粒和小颗粒在表观特性 MLSS、体积、表面积、个数相同情况下的 k_La . 具体步骤为,取大颗粒污泥浓度为4 000 mg·L⁻¹时的 k_La 作为参照项,此时 SV30 为 27 mL. ①测量小颗粒在污泥浓度相同时 (4 000 mg·L⁻¹) 的 k_La 与参照项进行对比;②取小颗粒在 SV30 为 27 mL 时的 k_La 与参照项进行对比;②取小颗粒在 SV30 为 27 mL 时的 k_La 与参照项进行对比;③对比大、小颗粒表面积相同时的 k_La ,即将大、小颗粒污泥拍摄如图 3 所示的培养皿照片,利用本课题组编写的 Size-Analysis 软件对照片进行分析,每组测量 600 个粒径,然后利用高斯拟合计算出平均粒径 $R_{\Lambda m m n}$, $R_{\Lambda m n n}$,表面积相同即大





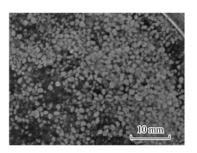


图 3 好氧颗粒污泥形态

Fig. 3 Morphology of aerobic granules

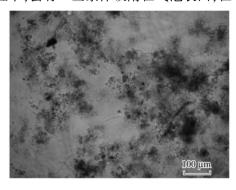
颗粒和小颗粒两者 SV30 比为 $R_{\text{top}}: R_{\text{top}}: 4$ 对比大、小颗粒个数相同时的 $k_{\text{L}}a$,即在个数相同的条件下大颗粒和小颗粒两者 SV30 比为 $R_{\text{top}}^3: R_{\text{top}}^3: R_{\text{top}}^3$.

2 结果与讨论

2.1 污泥浓度对好氧颗粒污泥和传统活性污泥 k_1a 影响对比

好氧颗粒污泥和传统活性污泥在不同污泥浓度下的 $k_{\rm L}a$ 如图 4 所示,当传统活性污泥和成熟好氧颗粒污泥浓度为2 000、4 000、6 000、8 000 mg·L⁻¹时,其 $k_{\rm L}a$ (min⁻¹)值分别为 0. 586 1 ± 0. 009 5、0. 586 1 ± 0. 027 2、0. 555 6 ± 0. 016 8、0. 533 8 ± 0. 026 8 和 0. 645 5 ± 0. 027 6、0. 632 0 ± 0. 075 5、0. 618 5 ± 0. 062 5、0. 640 6 ± 0. 055 5. 可以看出在每一个相同污泥浓度下,好氧颗粒污泥的 $k_{\rm L}a$ 均大于传统活性污泥.

对比分析造成这一差异的根本原因是二者污泥 形态的不同(图 5),颗粒污泥和传统活性污泥在结 构上有着明显的差异,颗粒污泥比较密实且表面较 光滑,而传统活性污泥为絮状污泥,其大小较颗粒污 泥小很多.这种形态上的差异导致了在曝气过程中 污泥和气泡位置关系有着较大的区别(图 6).传统 活性污泥絮体由于体积相对于气泡要小得多,在气 泡上升的过程中,会有一些絮体吸附在气泡表面,在



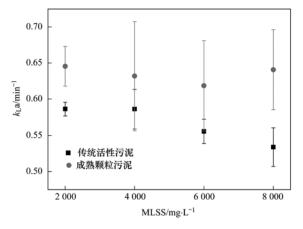


图 4 不同形态污泥在不同 MLSS 下的 $k_L a$ (清水 $k_L a$ 为0.908 9 min $^{-1}$)

Fig. 4 $k_{\rm L}a$ of different sludge type with different MLSS($k_{\rm L}a$ in clean water was 0. 908 9 min $^{-1}$)

曝气过程中和气泡是一种附着关系; 好氧颗粒污泥 由于密度和颗粒尺寸相对于传统活性污泥要大得 8,其体积和气泡体积相差不大,颗粒表面光滑,存在明显边界,在曝气过程中和气泡是一种碰撞关系. 体积溶氧传递系数 $k_L a$ 是用来表征溶氧传递速率的 重要参数,该参数为复合参数,是气液传质系数 k_L 和气液接触面积 a 的乘积. 在曝气的过程中,由于 絮状污泥会附着在气泡的表面,这种吸附关系会导致气液接触面积 a 下降; 而相对应的好氧颗粒污泥



图 5 不同的污泥形态对比

Fig. 5 Morphology of sludge formed in different reactors

在曝气的过程中和气泡是一种碰撞关系,并不会影响气液接触面积 a,而且气液传质系数 k_L 只和气体和液体本身性质以及外界温度等有关. 因此,二者对于气液接触面积 a 的影响不同就导致了好氧颗粒污泥的 $k_L a$ 大于传统活性污泥.

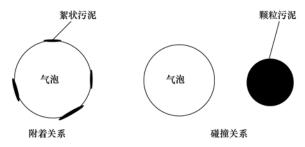


图 6 不同形态污泥和气泡位置关系

Fig. 6 Relationship of bubbles and different types of sludge

在污水处理工艺中污泥浓度是一个重要的控制 参数^[9],并且随着污泥浓度的提高,污泥之间的空隙发生变化也会影响氧气在水中的传递^[10]. 对比 好氧颗粒污泥和传统活性污泥的 $k_L a$ (图 4)发现:传统活性污泥的 $k_L a$ 随着浓度的增加呈现出逐渐减小的趋势;好氧颗粒污泥的 $k_L a$ 基本维持恒定,并且在高浓度的时候还略有上升.

由于传统活性污泥随着污泥浓度的增加,附着在气泡表面的絮体会越来越多(图7),气液接触面积 a 会随着污泥浓度的增加进一步减小,因此传统活性污泥随着污泥浓度的增加其 k_a 会减小. 而对于好氧颗粒污泥而言,颗粒和气泡之间的碰撞关系(图6)并不会随着污泥浓度的增大而改变,所以气液接触面积 a 并不会随着污泥浓度的增大减少,相反的是颗粒和气泡的这种碰撞作用起到了一种搅拌的作用,反而会使得好氧颗粒污泥的 k_a 在浓度升高时会有一些轻微的增大,因此污泥浓度对好氧颗粒污泥的 k_a 影响很小.

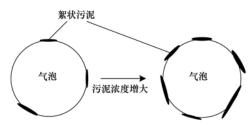


图 7 不同条件下絮体覆盖气泡表面情形

Fig. 7 Coverage of flocs on the surface of bubbles with different sludge concentrations

2.2 不同粒径下的好氧颗粒污泥表观特性对 $k_{\rm L}a$ 的影响

通过对比好氧颗粒污泥和传统活性污泥的

 $k_{L}a$,发现好氧颗粒污泥相对于传统活性污泥在混合液气液传质方面有着明显的优势,而且根据好氧颗粒污泥在不同浓度下的 $k_{L}a$ 可以看出污泥浓度并不是影响好氧颗粒污泥 $k_{L}a$ 的因素.

在污泥颗粒化的过程中粒径是最显著的变化特征,因此从粒径入手,通过颗粒污泥的表观特性来探索影响好氧颗粒污泥 $k_{\rm L}a$ 的因素. 取实验室气提式反应器内颗粒,筛分为粒径大于 1 mm 的大颗粒和粒径为 $0.2 \sim 1$ mm 的小颗粒,如图 6 所示,分别测量大、小颗粒在 MLSS、体积、表面积、个数 4 项表观特性相同下的 $k_{\rm L}a$.

所得结果如表 3 所示,可以看出筛分粒径后大、小颗粒在每一种表观特性相同的情况下, k_La 相差均不大. 说明无论大颗粒和小颗粒都存在如图 6 所示的颗粒污泥和气泡的碰撞关系,这种碰撞关系在颗粒形成后并不会随着颗粒粒径的改变而产生较大的变化,相对于絮状污泥而言,成熟的好氧颗粒污泥粒径变化前后颗粒污泥的体积都和气泡体积在一个数量级上,这样才能够使得这种碰撞关系得以延续,粒径的差异对 k_La 是没有明显影响的. 因此通过表 3 中所列出的 4 种表观特性对好氧颗粒污泥 k_La 的影响,可以推断颗粒污泥的浓度、体积、表面积、个数对好氧颗粒污泥系统 k_La 的影响并不明显.

表 3 好氧颗粒污泥在不同表观特性下的 $k_{\rm L}a/{ m min}^{-1}$

Table 3 The $k_{\rm L}a$ of aerobic granular sludge with different

apparent characteristics/ min					
清水	大颗粒	小颗粒与大颗粒对应项 MLSS 相同 体积相同 表面积相同 个数相同			
		MLSS 相同	体积相同	表面积相同	个数相同
		0. 547 3	0. 556 2	0. 555 5	0. 580 7

3 结论

- (1)相同污泥浓度下,好氧颗粒污泥的体积溶氧传递系数 $k_{L}a$ 高于传统活性污泥,并且随着污泥浓度的升高,这种差别更明显. 说明好氧颗粒污泥的气液传质优于传统活性污泥. 推断原因主要是由于好氧颗粒与传统活性污泥絮体在大小尺寸上的差异,使得它们与气泡的位置关系不同.
- (2) 对于颗粒污泥系统而言,污泥浓度的变化对 $k_L a$ 的影响甚微,而传统活性污泥系统的 $k_L a$ 则会随着污泥浓度的增大而减小. 且污泥浓度、体积、表面积、数量对好氧颗粒污泥系统 $k_L a$ 的影响都不显著. 表明好氧颗粒污泥系统在曝气过程中具有节能的潜力.

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